PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

CAPTIVE USAGE T/D	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
LIQUID PHASE EDC														
To														
TCE Mfg. & MC Mixes	188.5	190.5	199.1	203.7	202.2	205.6	209.7	129.5	187.0	232.4	216.6	255.6	261.9	207.8
Perchlor	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Trichlor Mfg. & Mixes	1.9	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Vinyl Chloride	682.9	429.9	237.6	539.0	611.6	811.8	928.0	718.2	731.3	720.0	668.9	564.7	679.8	636.7
P/T-TETRA UNIT	59.1	125.8	108.6	29.6	69.0	11.3	2.0	38.1	60.3	45.7	16.2	94.2	46.8	54.0
OHC EDC														
To														
Perchlor					6.1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.5
Trichlor					10.5	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.9
No. 2 EDC Plant	3.3	0.0	0.0	19.0	74.4	79.5	135.5	57.7	129.9	163.0	112.9	180.1	144.5	91.4
P/T-TETRA UNIT	258.4	285.9	189.6	268.6	192.9	343.0	326.1	293.6	265.9	272.7	251.2	177.6	298.5	263.8

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

LABORATORY PRODUCT REPORT

EDC SHIPMENTS	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TRANS 1.2. DICHLOROETHYLENE PPM	1	0	0	(1	0	0	0	0	0	0	0	0	0	0
1.1 DICHLOROETHANE PPM	16	22	27	26	14	17	16	11	18	13	16	11	17	17
CIS 1.2 DICHLOROETHYLENE PPM	5	4	3	5	6	5	4	5	4	4	4	3	32	7
CHLOROFORM PPM	24	66	43	26	21	19	27	32	13	23	23	53	55	33
ETHYLENE DICHLORIDE %	99.987	99.983	99.981	99.983	99.989	99.988	99.987	99.986	99.988	99.983	99.983	99.979	99.976	99.984
TRICHLOROETHYLENE PPM	8	(1	0	0	0	0	0	2	0	0	1	52	37	7
PERCHLOROETHYLENE PPM	(1	0	9	0	(1	14	0	0	5	9	37	41	13	10
1.1.2 TRICHLOROETHANE PPM	7	(1	36	30	11	14	15	17	31	46	42	33	48	27
ETHYLENE CHLOROBROMIDE PPM	11	14	0	14	0	2	3	3	11	7	10	4	12	7
ETHYL CHLORIDE PPM	40	23	44	44	31	26	39	52	29	27	22	8	13	30
COLOR (APHA)	7	8	8	7	7	5	6	7	6	5	6	6	8	7
APPEARANCE	Clear	Clear	Clear	Clear	Clear	Clear	Clear	CLEAR	CLEAR	Clear	CLEAR	CLEAR	CLEAR	CLEAR
ACIDITY PPM	(1	(1	2	(1	(1	(1	(1	(1	1	1	(1	(1	(1	(1
WATER PPM	45	49	64	38	39	51	89	50	27	50	41	38	38	48
NON-VOLATILES PPM	3	(1	(1	6	(1	(1	(1	(1	(1	5	5	(1	(1	1
TOTAL IRON PPM	0.17	0.24	0.49	0.23	0.10	0.20	0.28	0.14	0.21	0.28	0.25	0.27	0.24	0.24
SPECIFIC GRAVITY 60°/60°F	1.262	1.263	1.262	1.262	1.262	1.261	1.262	1.261	1.262	1.261	1.260	1.263	1.263	1.262

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CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY PRODUCT REPORT

METHYLCHLOROFORM SHIPMENTS		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG;
Type 314															
Color	APHA	6	6	-	-	-	-	-	-	-	-	-	(5	-	(5
Specific Gravity	25/25 °C	1.330	1.335	-	-	-	-	-	-	-	-	-	-	-	1.335
Distillation Range	°C								-	-	-	-			
Low		73.9	73.9	-	-	-	-	-	-	-	-	-	-	-	73.9
High		74.7	75.2	-	-	-	-	-	-	-	-	-	-	-	75.2
Moisture	PPM	42	40	-	-	-	-	-	-	-	-	-	23	-	32
Acidity	PPM asHCl	(1	(1	-	-	-	-	-	-	-	-	-	1	-	(1
Non-Volatile Residue	%	.0005	(.0001	-	-	-	-	-	-	-	-	-	-	-	(.0001
Soluble Chlorides	PPM	(0.5	(0.5	-	-	-	-	-	-	-	-	-	-	-	(0.5
Type 321															
Assay	%														
Moisture	PPM														
Distillation Range	°C														
Low															
High															
Specific Gravity	25/25 °C														
Color	APHA														
Acidity	PPM as HCl														
N n-Volatile Residue	%														
Soluble Chlorides	PPM														

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LABORATORY PRODUCT REPORT

TRI-ETHANE ® SHIPMENTS		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
Type 324															
Color	APHA	6	6	8	6	6	6	7	6	5	(5	(5	(5	6	5
Specific Gravity	25/25 °C	1.305	1.315	1.305	1.303	1.305	1.305	1.304	1.306	1.305	1.307	1.304	1.304	1.305	1.306
Distillation Range	°C														
Low		73.2	73.2	72.8	72.8	72.8	72.8	72.8	72.8	72.8	73.1	73.0	73.5	73.5	73.0
High		82.9	84.6	82.8	83.4	82.3	82.1	82.5	82.8	82.8	83.6	83.3	83.4	83.6	83.1
Moisture	PPM	50	51	67	60	58	68	63	64	88	54	46	56	43	60
Acidity	PPM as HCl	(1	(1	(1	2	1	2	2	1	1	1	2	1	2	1
Soluble Chlorides	PPM	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5
Aluminum Scratch	APHA	38	53	21	-	28	26	34	31	14	16	12	9	20	24
Non-Volatile Residue		.0001	.0003	.0002	.0002	(.0001	(.0001	.0003	(.0001	.0006	(.0001	.0002	.0002	.0002	.0002
Type 339															
Color	APHA	6	8	7	7	6	6	-	-	-	-	-	-	-	7
Specific Gravity	25/25 °C	1.322	1.324	-	1.332	1.323	1.323	-	-	-	-	-	-	-	1.326
Distillation Range	°C														
Low		74.0	73.8	-	73.8	72.5	72.5	-	-	-	-	-	-	-	73.2
High		83.0	83.5	-	83.2	81.5	81.5	-	-	-	-	-	-	-	82.4
Moisture	PPM	55	52	97	68	49	44	-	-	-	-	-	-	-	62
Acidity	PPM as HCl	(1	1	(1	(1	(1	1	-	-	-	-	-	-	-	(1
Non-Volatile Residue	%	.0001	(.0001	-	.0004	.0006	.0006	-	-	-	-	-	-	-	.0004
Soluble Chlorides	PPM	(1.0	(0.5	-	(0.5	(0.1	-	-	-	-	-	-	-	-	(0.5

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CHEMICAL DIVISION

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LABORATORY PRODUCT REPORT

TRICHLOR SHIPMENTS	1973 AVG.	JAN	FEB	MAR *	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 122 (Degreasing & Solvent Grade)														
COLOR APHA	8	7	9	8	8	7	10	9	7	5	7	(5	6	7
SPECIFIC GRAVITY 20/20 °C	1.461	1.460	1.460	1.460	1.460	1.460	1.462	1.462	1.462	1.460	1.462	-	1.461	1.461
DISTILLATION RANGE °C														
LOW	86.1	86.1	86.1	86.1	86.0	86.1	86.1	86.0	86.0	86.1	86.2	-	86.1	86.1
HIGH	87.6	87.7	87.8	87.9	87.7	87.7	87.9	87.8	87.5	87.5	87.4	-	88.0	87.7
WATER CONTENT CLOUD POINT °C	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10
NON-VOLATILE %	.0013	.0014	.0016	.0012	.0006	.0002	.0006	.0012	-	.0003	.0005	-	.0005	.0008
ACID ACCEPTANCE % AS NAOH	0.14	.14	.14	.15	.15	.16	.16	.19	-	.19	.19	-	.20	0.17
pH	7.7	7.4	7.7	9.0	9.0	9.0	9.0	8.9	9.1	9.1	9.1	9.2	9.3	8.8
Acidity/Alkalinity	.0003	.0002	.0003	.0017	.0019	.0020	.0019	.0017	.0026	.0026	.0024	.0030	.0028	.0019
TYPE E-110														
COLOR APHA	8													
SPECIFIC GRAVITY 20/20 °C														
DISTILLATION RANGE °C														
LOW														
HIGH														
WATER CONTENT CLOUD POINT °C	(-10													
NON-VOLATILE %														
ACID ACCEPTANCE % AS NAOH														
TYPE 113 (High Purity Grade)														
COLOR APHA	7	7	7	7	7	7	8	7	6	6	(5	(5	6	6
SPECIFIC GRAVITY 20/20 °C														
DISTILLATION RANGE °C														
LOW														
HIGH														
WATER CONTENT CLOUD POINT °C	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10	(-10
NON-VOLATILE %	.0002	.0002	.0005	.0004	.0003	.0002	.0004	.0005	.0004	.0006	.0005	.0003	.0003	.0004

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*Type 122 is Type 132 subsequest to Feb.

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY PRODUCT REPORT

TRICHLOR SHIPMENTS	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 115 (Dual Purpose Grade)														
COLOR APHA	8													
SPECIFIC GRAVITY 20/20 °C														
DISTILLATION RANGE °C														
LOW														
HIGH														
WATER CONTENT CLOUD POINT °C	(-10													
NON-VOLATILE %	.0004													
ACID ACCEPTANCE % AS NAOH														

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LABORATORY PRODUCT REPORT

PERCHLOR SHIPMENTS	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 207														
COLOR APHA	10	11	10	9	11	9	11	14	10	15	15	10	12	11
SPECIFIC GRAVITY 20/20 °C														
DISTILLATION RANGE °C														
LOW														
HIGH														
WATER CONTENT CLOUD POINT °C	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0
NON-VOLATILE wt.%														
PH	8.2	8.3	8.1	8.3	8.3	8.3	8.3	8.3	8.4	8.2	8.4	8.5	8.5	8.3
ACID ACCEPTANCE % AS NAOH														
COPPER CORROSION														
ACIDITY ML OF 0.01 N NAOH														
FLASK MG/30 CM^2														
SOXHLET MG/30 CM^2														
CONDENSER MG/30 CM^2														
CHLORIDES PPM														
TYPE 208														
COLOR APHA	9	10	10	8	10	8	10	12	9	11	10	7	10	10
SPECIFIC GRAVITY 20/20 °C	1.625	1.624	1.624	1.624	1.624	1.625	1.626	1.627	-	1.626	1.625	-	1.624	1.625
DISTILLATION RANGE °C														
LOW	120.8	120.8	120.9	120.7	120.8	120.9	120.8	120.8	-	120.9	120.9	-	120.8	120.8
HIGH	121.6	121.7	121.6	121.6	121.6	121.8	121.7	121.7	-	121.7	121.7	-	121.7	121.7
WATER CONTENT CLOUD POINT °C	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0	(0
NON-VOLATILE wt.%	.0003	.0003	.0002	.0006	(.0001	.0006	(.0001	.0006	-	.0005	.0002	-	.0005	.0003
PH	6.6	6.5	6.8	6.7	6.5	6.5	6.5	6.4	6.8	6.8	6.5	6.6	6.6	6.6
COPPER CORROSION														
ACIDITY ML OF 0.01 N NAOH	1	2	1	1	2	2	1	1	-	2	2	-	2	2
FLASK MG/30 CM^2	2	1	2	1	(1	2	1	(1	-	2	1	-	1	1
SOXHLET MG/30 CM^2	6	7	8	9	5	5	6	6	-	7	7	-	7	7
CONDENSER MG/30 CM^2	7	8	10	10	5	6	6	9	-	7	8	-	7	8
CHLORIDES PPM	0.13	0.11	0.11	(.06	.18	.10	(0.06	0.06	-	0.10	0.16	-	0.08	0.09

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PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY PRODUCT REPORT

PERCHLOR SHIPMENTS	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 203														
COLOR APHA														
SPECIFIC GRAVITY 20/20 °C														
DISTILLATION RANGE °C														
LOW														
HIGH														
WATER CONTENT CLOUD POINT °C														
NON-VOLATILE wt.%														
PH														
ACID ACCEPTANCE % AS NAOH														
COPPER CORROSION														
ACIDITY ML OF 0.01 N NAOH														
FLASK MG/30 CM^2														
SOXHLET MG/30 CM^2														
CONDENSER MG/30 CM^2														
CHLORIDES PPM														
TYPE 209														
COLOR APHA														
SPECIFIC GRAVITY 20/20 °C														
DISTILLATION RANGE °C														
LOW														
HIGH														
WATER CONTENT CLOUD POINT °C														
NON-VOLATILE wt.%														
PH														
ACID ACCEPTANCR % AS NAOH														
COPPER CORROSION														
ACIDITY ML OF 0.01 N NAOH														
FLASK MG/30 CM^2														
SOXHLET MG/30 CM^2														
CONDENSER MG/30 CM^2														
CHLORIDES PPM														

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PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY PRODUCT REPORT

ETHYL CHLORIDE SHIPMENTS	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
COLOR APHA	6	6	(5	(1	(5	(5	(5	(5	(5	4	(5	(5	(5	(5
MOISTURE PPM	24	14	29	57	9	4	45	75	30	37	30	30	14	31
SPECIFIC GRAVITY 0/4 °C	0.924	0.923	0.924	0.924	0.924	0.923	0.923	0.923	0.924	0.924	0.924	0.924	0.923	0.924
ACIDITY AS HCL WT. %	(.0001	(.0001	(.0001	(.0001	.0008	.0004	(.0010	(.0010	(.0001	(.0001	(.0001	(.0001	(.0001	(.0001
NON-VOLATILE RESIDUE WT. %	.0002	(.0001	.0013	.0002	(.0001	.0008	.0010	.0005	.0005	.0010	(.0003	(.0001	(.0001	.0004
ETHYL CHLORIDE WT. %	99.96	99.97	99.95	99.96	99.98	99.97	99.97	99.97	99.97	99.96	99.95	99.98	99.97	99.97
Distillation Range °C														
Low	12.3	-	-	-	-	-	-	-	-	-	-	-	-	-
High	12.6	-	-	-	-	-	-	-	-	-	-	-	-	-

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CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY PRODUCT REPORT

VINYL CHLORIDE SHIPMENTS		1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
H_2	PPM	38	48	41	40	19	36	19	38	43	59	41	37	28	37
HCl	PPM	(1	(1	(1	(1	(1	(1	(1	1	(1	(1	(1	(1	(1	(1
Fe	PPM	0.06	0.07	0.09	(0.1	(0.1	0.1	0.24	0.13	0.10	(0.1	(0.1	(0.1	(0.1	(0.1
SULFUR	PPM	(1	(1	(1	(1	(1	(1	(1	(1	-	(1	(1	(1	(1	(1
ACETYLENE	PPM	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1
ALDEHYDES, AS ACETALDEHYDE	PPM	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1
PEROXIDES, AS H_2 2	PPM	0.02	(0.01	0.03	(0.01	0.04	(1.00	0.05	0.01	0.01	0.02	0.02	0.01	(1.00	(1.00
N N-VOLATILE RESIDUE	PPM	3	(1	4	6	(1	10	(1	10	4	4	14	14	(1	5

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FORM NO. AA 202-4

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

EDC	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
PRODUCT #1 PPM*														
TRANS 1.2 DICHLOROETHYLENE	(1	(1	1	-	-	-	-	-	-	-	-	-	1	1
1.1 DICHLOROETHANE	15	18	22	-	-	12	12	15	14	11	12	15	19	15
CIS 1.2 DICHLOROETHYLENE	2	3	5	-	-	8	3	4	7	13	11	9	4	7
CHLOROFORM	29	56	35	-	-	21	23	20	61	179	59	37	40	53
ETHYLENE DICHLORIDE (WT. %)	99.989	99.989	99.979	-	-	99.989	99.979	99.983	99.981	99.963	99.968	99.976	99.987	99.979
1.1.2 TRICHLOROETHANE	6	2	15	-	-	17	19	27	28	28	21	29	-	21
ETHYLENE CHLOROBROMIDE	13	2	0	-	-	5	8	9	5	5	2	5	6	5
ETHYL CHLORIDE	27	7	43	-	-	28	29	37	30	5	(1	14	6	19
UNIDENTIFIED	(1	0	6	-	-	-	-	-	4	6	1	0	5	3
H_2O	22	24	25	-	-	30	30	42	44	42	46	26	34	34
FE	0.04	0.04	0.03	-	-	0.07	0.04	0.02	0.06	0.05	0.06	0.24	0.10	0.07
HCL	0.45	0.76	1.61	-	-	0.45	0.67	0.61	0.70	1.77	1.12	1.56	0.89	1.01

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*UNLESS OTHERWISE SPECIFIED

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PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS' REPORT

EDC	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
PRODUCT #2 PPM*														
TRANS 1.2 DICHLOROETHYLENE	2	4	4	1	13	-	-	5	1	-	-	-	(1	4
1.1 DICHLOROETHANE	19	51	21	14	15	12	12	12	8	13	11	13	11	16
CIS 1.2 DICHLOROETHYLENE	8	8	4	7	17	3	4	3	6	6	9	12	10	7
CHLOROFORM	42	18	33	21	416	39	32	14	8	31	36	127	90	72
ETHYLENE DICHLORIDE (WT. %)	99.984	99.981	99.985	99.985	99.906	99.988	99.985	99.992	99.994	99.987	99.988	99.971	99.979	99.978
1.1.2 TRICHLOROETHANE	2	0	24	12	15	8	28	15	9	39	3	11	13	15
ETHYLENE CHLOROBROMIDE	5	19	(1	4	1	13	8	7	3	4	1	0	6	5
ETHYL CHLORIDE	50	67	40	72	58	23	51	20	18	3	(1	5	2	29
UNIDENTIFIED	7	8	3	(1	12	-	-	-	-	10	0	0	6	4
H_2O	23	35	23	49	35	30	36	48	42	33	36	28	27	35
FE	0.04	0.06	0.01	0.08	0.03	0.06	0.04	0.03	0.01	0.04	0.02	0.03	0.03	0.04
HCL	0.45	1.71	2.42	0.33	0.94	0.52	0.58	0.58	0.94	1.09	.80	1.98	0.66	1.05

SL 013372

CONFIDENTIAL
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

*UNLESS OTHERWISE SPECIFIED

Form No. 202-0

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

EDC	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
REACTOR #1 WT. %														
Ethylene Dichloride	98.71	97.98	98.18	98.99	99.22	99.27	99.34	98.90	98.94	98.45	98.96	98.78	99.36	98.86
Trichloroethylene	0.02	0.02	0.12	0.02	0.01	0.04	0	0.08	(0.01	0.03	0.02	0	0	0.02
Perchloroethylene	0.01	0	0	0	0	0	0	0	0	0	0.01	(0.01	0	0
1,1,2 Trichloroethane	0.34	0.69	0.31	0.30	0.26	0.38	0.24	0.30	0.44	0.67	0.39	0.68	0.24	0.41
U-Tetrachloroethane	0.02	0	0	0	0	0	0	0	0	0	0	0	0	0
S-Tetrachloroethane	0.30	0.62	0.19	0.21	0.16	0.13	0.09	0.18	0.18	0.25	0.26	0.32	0.10	0.22
Pentachloroethane	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethylene Chlorobromide	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethyl Chloride	0.05	0.34	0.12	0.14	0.11	0.03	0.11	0.08	0.06	0.03	0.05	0.02	(0.01	0.09
Unidentified	0.56	0.35	1.07	0.34	0.23	0.18	0.24	0.46	0.38	0.55	0.28	0.20	0.29	0.38
H_2O ppm	(166	(126	(252	(126	(191	(124	(164	(165	(119	(165	(141	(182	(196	(163
Total Fe as $FeCl_3$ %	0.41	0.58	0.48	0.29	0.48	0.31	0.42	0.47	0.27	0.39	0.36	0.41	0.45	0.41
Tars %	4.63	4.71	6.37	2.83	7.63	2.95	5.50	6.23	2.68	4.67	4.19	5.51	6.79	5.00
Specific Gravity 60^0-60^0F	1.303	1.287	1.298	1.280	1.297	1.273	1.284	1.289	1.269	1.299	1.287	1.291	1.323	1.290

SL 013373

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

FORM NO. CA 202- 7

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

EDC	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
REACTOR #2 WT. %														
Ethylene Dichloride	98.61	97.48	98.86	98.82	99.04	99.24	99.44	98.71	98.96	98.60	98.70	99.14	99.27	98.86
Trichloroethylene	0.02	0	0.05	0.04	0.03	0.02	0	0.14	0.02	0.01	0.01	0	0	0.02
Perchloroethylene	0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
1.1.2 Trichloroethane	0.35	0.71	0.32	0.27	0.32	0.39	0.27	0.33	0.42	0.59	0.35	0.32	0.19	0.37
U-Tetrachloroethane	0.02	0	0	0.02	0	0	0	0	0	0	0	0	0	0
S-Tetrachloroethane	0.31	0.67	0.21	0.19	0.12	0.13	0.15	0.26	0.20	0.97	0.39	0.23	0.15	0.26
Pentachloroethane	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethylene Chlorobromide	0	0	0	0	0	0	0	0	0	0	(0.01	0	0	0
Ethyl Chloride	0.03	0.13	0.11	0.14	0.05	0.03	0.08	0.09	0.08	0.04	0.05	0.04	0.02	0.07
Unidentified	0.65	1.01	0.42	0.51	0.41	0.19	0.29	0.48	0.32	0.38	0.48	0.28	0.37	0.43
H_2O PPM	(207	(217	(236	(157	(214	(100	(148	(115	(127	(137	(150	(108	(130	(153
Total Fe as $FeCl_3$ %	0.51	0.59	0.46	0.44	0.45	0.24	0.38	0.29	0.28	0.32	0.34	0.28	0.30	0.36
Tars %	5.83	3.62	4.43	5.08	8.58	2.56	3.98	3.77	4.54	4.99	4.23	3.49	4.34	4.47
Specific Gravity 60^0-60^0F	1.299	1.301	1.288	1.290	1.306	1.271	1.280	1.282	1.283	1.296	1.279	1.278	1.294	1.287

SL 013374

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

FORM NO. A 202- 8

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

EDC	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
REACTOR #3 WT. %														
Ethylene Dichloride	98.45	97.28	96.96	97.82	97.99	99.06	98.99	98.73	98.49	97.16	98.26	97.88	96.71	97.94
Trichloroethylene	0.03	0.06	0.16	0.11	0.03	(0.01	0.02	0.06	0.02	0.04	0.04	0	0	0.05
Perchloroethylene	0.01	0	0	0.01	0	0	0	0	0	0	0	0.02	(0.01	(0.01
1.1.2 Trichloroethane	0.58	1.72	1.72	0.88	0.84	0.54	0.52	0.64	0.76	1.47	1.03	1.34	1.80	1.11
U-Tetrachloroethane	0.06	0	0	0	0	0	0	0	0	0	0	(0.01	(0.01	(0.01
S-Tetrachloroethane	0.35	0.16	0.18	0.43	0.60	0.16	0.18	0.18	0.26	0.78	0.50	0.47	1.35	0.44
Pentachloroethane	(0.01	0	0	0	0	0	0	0	0	0	0	0.06	0.01	(0.01
Ethylene Chlorobromide	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethyl Chloride	0.03	0.04	0.02	0.22	0.04	0.03	0.10	0.04	0.03	(0.01	(0.01	0.05	(0.01	0.05
Unidentified	0.53	0.73	1.01	0.53	0.34	0.16	0.20	0.35	0.43	0.54	0.24	0.14	0.12	0.40
H_2O ppm	(226	(324	(272	(157	(248	(192	(210	(205	(248	(235	(223	(159	(233	(226
Total Fe as $FeCl_3$ %	0.59	0.82	0.60	0.44	0.56	0.46	0.48	0.52	0.52	0.60	0.51	0.37	0.54	0.54
Tars %	5.37	4.63	3.50	5.08	4.58	3.19	4.98	5.28	4.82	5.31	3.94	1.59	2.81	4.14
Specific Gravity 60^0-60^0F	1.310	1.295	1.296	1.290	1.292	1.283	1.292	1.294	1.286	1.295	1.286	1.271	1.282	1.289

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

SL 013375

FORM N A 202- 9

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

EDC	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
STILL BOTTOMS #1 WT%														
Ethylene Dichloride	35.29	53.25	-	-	-	-						89.17	71.64	71.35
Trichloroethylene	0.14	0	-	-	-	-						-	(0.01	(0.01
Perchloroethylene	0	0	-	-	-	-						0.23	0.08	0.10
1.1.2 Trichloroethane	44.45	32.36	-	-	-	-						9.11	22.53	21.33
U-Tetrachlorethane	0.28	0	-	-	-	-						-	0.05	0.03
S-Tetrachloroethane	11.97	10.54	-	-	-	-						1.14	3.84	5.17
Pentachloroethane	0.01	0	-	-	-	-						0.05	0.01	0.02
				-										
Ethylene Chlorobromide	0	0	-	-	-	-						0.24	0.42	0.22
Ethyl Chloride	0	0	-	-	-	-						-	-	0
Unidentified	7.23	3.84	-	-	-	-						0.06	1.32	1.74
H_2O PPM	16	24	-	-	-	-						67	10	34
Fe PPM	50.67	35.04	-	-	-	-						40.85	89.59	55.16
HCL PPM	697	1308	-	-	-	-						550	433	764
Specific Gravity 60^0-60^0F	1.386	1.355	-	-	-	-						1.319	1.320	1.331

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

SL 013376

Form NC-JA 202-10

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

EDC	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
STILL BOTTOMS #2 WT%														
Ethylene Dichloride	15.88	25.67	50.67	65.99	66.64	33.25	35.70	26.71	17.25	17.98	12.31	18.99	17.00	32.35
Trichloroethylene	0.03	0	0	0.13	0.40	0.44	1.14	0.53	0.15	0.12	0.12	0.08	0.14	0.27
Perchloroethylene	0	0	0	0	0	0	0	0	0.04	0	2.38	1.86	0.85	0.43
1.1.2 Trichloroethane	62.79	69.37	45.16	21.43	25.63	56.18	53.20	58.33	64.45	64.94	67.02	64.13	66.60	54.70
U-Tetrachlorethane	0.20	0	0	0	0.28	0	0	0	1.06	0	0.04	0.06	0.62	0.17
S-Tetrachloroethane	14.67	2.55	2.61	9.90	5.82	8.82	8.43	10.34	12.94	13.90	14.40	11.54	13.43	9.56
Pentachloroethane	0.01	0	0	0	0.42	0	0	0	0	0	0.10	0.03	0.06	0.05
Ethyl Chloride	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Unidentified	6.42	3.40	2.21	1.89	0.81	1.30	1.52	2.35	4.12	3.09	3.52	0.64	1.19	2.17
H_2O PPM	9	189	22	60	28	32	30	60	127	25	26	42	65	59
Fe PPM	74.82	54.17	40.15	58.84	54.88	42.48	50.71	46.66	40.71	24.96	41.14	34.61	10.35	41.64
HCL PPM	932	2702	1168	874	812	1066	800	1427	1495	951	862	989	192	1112
Specific Gravity 60^0-60^0F	1.429	1.388	1.345	1.353	1.330	1.394	1.266	1.407	1.421	1.419	1.430	1.422	1.421	1.383

CONFIDENTIAL:
Subject to Protective Order
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No. 91-1145

SL 013377

FORM I 5A 202 - 11

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

"TRI-ETHANE"@	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TCE REACTOR WT.%														
ETHYL CHLORIDE	(0.01	0	0	(0.01	(0.01	0	0	0	0	0	0	0	0	(0.01
CIS 1.2 DICHLOROETHYLENE	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0	0	0	0	0	0	(0.01
1.2 DICHLOROETHANE	65.28	63.40	64.42	62.69	62.43	62.63	60.63	63.63	63.82	61.16	61.63	57.24	59.16	61.90
TRICHLOROETHYLENE	(0.01	(0.01	0.01	0.01	(0.01	(0.01	0.02	0.03	0.03	(0.01	(0.01	0.01	(0.01	0.02
1.1.2 TRICHLOROETHANE	31.06	32.60	31.54	32.88	32.77	32.71	33.86	31.33	30.35	33.48	33.67	36.64	35.40	33.11
U-TETRACHLOROETHANE	1.59	1.74	1.74	1.96	1.95	1.95	2.04	1.73	1.59	2.00	2.02	2.72	2.47	1.99
S-TETRACHLOROETHANE	1.90	2.04	2.04	2.29	2.30	2.29	2.40	2.02	1.89	2.36	2.39	3.07	2.65	2.31
PENTACHLOROETHANE	0.06	0.06	0.07	0.08	0.09	0.10	0.11	0.13	0.20	0.09	0.08	0.13	0.08	0.10
Fe PPM	3	2	3	3	5	13	20	13	12	14	22	27	56	16
HEAVIES STILL REFLUX WT.%	*													
CIS 1.2 DICHLOROETHYLENE	(0.01	0	0	0	0	0	0	0	0	(0.01	(0.01	36	61	48**
1.2 DICHLOROETHANE	(0.01	0	0	(0.01	(0.01	0	0	(0.01	0	0	(0.01	0	6	3**
TRICHLOROETHYLENE	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0	0.01	(0.01	(0.01	(0.01	58	139	98**
1.1.2 TRICHLOROETHANE	99.97	99.99	99.98	99.97	99.96	99.98	99.98	99.78	99.91	99.95	99.74	99.95	99.89	99.92
U-TETRACHLOROETHANE	0.01	(0.01	(0.01	0.02	(0.01	(0.01	(0.01	0.80	(0.01	(0.01	0.01	493	420	456**
H_2O PPM	-		-	-	-	-	-	-	-	-	-	-	-	-
Fe PPM	(1	0.4	(0.1	0.08	(1	(1	(1	2	-	-	(1	(1	(1	(1
LIGHT STILL REFLUX PPM														
H_2O	-													
Fe	2	2	2	3	3	6	4	5	6	4	5	2	2	4

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 71-1145

SL 013378

*Subesquent to Nov. values will be reported in PPM

** Average in PPM

FORM NO. A 202 - 12

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

"TRI-ETHANE"®	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
HEAVIES STILL FEED WT%														
1,1,2 TRICHLOROETHANE	89.56	88.58	88.58	87.42	87.20	87.10	87.13	86.98	87.10	87.09	86.89	86.62	87.25	87.33
U-TETRACHLOROETHANE	4.98	5.09	5.15	5.51	5.64	5.68	5.67	5.53	5.62	5.79	5.84	6.12	5.98	5.64
S-TETRACHLOROETHANE	5.59	6.13	6.08	6.65	6.85	6.94	6.86	7.10	6.65	6.87	6.95	6.97	6.59	6.72
PENTACHLOROETHANE	0.19	0.20	0.18	0.37	0.29	0.24	0.34	0.39	0.62	0.25	0.29	0.26	0.18	0.30
VDC REFLUX WT. %														
VINYLIDENE CHLORIDE	99.70	99.57	99.53	99.55	99.35	99.57	99.38	99.34	99.38	99.42	99.18	99.16	99.37	99.40
TRANS. 1,2 DICHLOROETHYLENE	0.13	0.28	0.33	0.32	0.24	0.28	0.39	0.40	0.36	0.43	0.30	0.25	0.35	0.33
CIS 1,2-DICHLOROETHYLENE	(0.01	(0.01	0	0	0	0	0.02	0.03	0.11	(0.01	0.02	0.01	0.05	0.02
HOMME PPM	198	213	174	177	188	230	234	198	204	168	148	205	361	208
VDC PRODUCT PPM														
H_2O	20	26	35	51	28	28	28	46	59	34	46	35	34	38
HOMME	257	289	224	190	265	294	318	220	243	194	178	214	297	244

SL 013379

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

FORM N[redacted]5A 202 - 13

PPG IN[redacted]STRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

"TRI-ETHANE"®	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
MC REACTOR WT. %														
ETHYL CHLORIDE	(0.01	(0.01	(0.01	0.01	0.01	(0.01	(0.01	0.02	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01
VINYLIDENE CHLORIDE	3.68	5.17	4.64	4.58	4.02	3.55	3.94	4.78	3.56	3.61	4.36	3.92	4.20	4.19
TRANS 1,2-DICHLOROETHYLENE	0.28	1.36	1.18	1.16	0.66	0.73	0.80	0.83	0.93	1.27	0.68	0.53	0.67	0.90
CIS 1,2-DICHLOROETHYLENE	(0.01	0	0	0	0	0	0	0.03	0.06	(0.01	(0.01	0	(0.01	(0.01
METHYL CHLOROFORM	95.95	93.35	92.29	94.16	95.40	95.45	94.97	94.19	95.33	95.06	94.89	95.35	94.95	94.62
TRICHLOROETHYLENE	(0.01	0	0.01	(0.01	(0.01	(0.01	(0.01	0	(0.01	0	0	0	0	(0.01
1,1,2-TRICHLOROETHANE	0.06	0.11	0.12	0.07	0.04	0.08	0.14	0.13	0.11	0.05	0.04	0.04	0.03	0.08
U-TETRACHLOROETHANE	(0.01	(0.01	(0.01	(0.01	0	0	0	(0.01	(0.01	0	0	0	0	(0.01
PENTACHLOROETHANE	0	0	0	0	0	0	0	0	0	0	0	0	0	0
UNKNOWN	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0.02	(0.01	(0.01	(0.01	0	0	(0.01
FE PPM	848	514	436	788	876	719	807	1380	1481	588	587	566	710	788
TOPPING STILL PRODUCT WT.%														
VINYLIDENE CHLORIDE *	0.02	0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0.02	0.02	0.01	0.01	100	97	98 **
TRANS 1,2-DICHLOROETHYLENE	0.07	0.22	0.16	0.21	0.20	0.15	0.21	0.23	0.17	0.23	0.22	0.18	0.21	0.20
1,1-DICHLOROETHANE	0.01	0.01	0.01	(0.01	0.02	(0.01	0.04	0.06	0.04	0.08	0.13	0.05	0.11	0.05
CIS 1,2-DICHLOROETHYLENE	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0.01	0.05	0.09	(0.01	0.01	(0.01	0.03	0.02
METHYL CHLOROFORM	99.80	99.66	99.64	99.67	99.66	99.75	99.55	99.42	99.56	99.55	99.51	99.64	99.50	99.59
1,2-DICHLOROETHANE	0.03	0.03	0.06	0.05	0.06	0.04	0.07	0.07	0.03	0.03	0.03	0.02	0.03	0.04
TRICHLOROETHYLENE	(0.01	(0.01	(0.01	0	0	0	(0.01	0	0	0	0	0	0	(0.01
1,1,2-TRICHLORCETHANE	0.06	0.06	0.11	0.04	0.04	0.05	0.09	0.12	0.08	0.08	0.07	0.07	0.07	0.07

SL 013380

CONFIDENTIAL
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

* Subsequent to Nov. values will be reported in PPM
** Average in PPM

FORM 45A 202- 14

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

'TRI-ETHANE'®	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 324 STABILIZATION WT. %														
VINLYIDENE CHLORIDE	0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0.02	0.01	0.02	0.01	0.02	0.01
BLM	0.39	0.55	0.46	0.52	0.51	0.40	0.43	0.49	0.46	0.48	0.49	0.46	0.50	0.48
BTE	0.76	1.04	0.82	0.76	0.79	0.76	0.79	0.81	0.78	0.77	0.73	0.81	0.87	0.81
METHYL CHLOROFORM	94.02	93.52	93.78	93.86	93.68	94.07	93.89	94.11	93.87	94.03	93.85	93.77	93.48	93.83
DOL	1.00	1.06	1.06	1.07	1.05	1.00	0.98	0.88	0.97	0.93	1.01	1.03	1.04	1.01
CIS 1.2-DICHLOROETHYLENE	0	(0.01	0	0	0	0	(0.01	0.03	0.04	0	0.01	0.01	0.04	0.01
TRICHLOROETHYLENE	(0.01	(0.01	(0.01	0	0	0	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01
1.2-DICHLOROETHANE	0.03	0.02	0.02	0.04	0.03	0.03	0.04	0.07	0.02	(0.01	0.0	0.0	0.0	0.02
IBL	0.37	0.36	0.06	0.02	(0.01	0	0	0	0.11	0.73	0.84	0.83	0.87	0.32
NRE	2.19	2.12	2.05	2.05	2.25	2.06	2.10	1.92	2.10	2.07	2.08	2.04	2.22	2.09
NITROETHANE	0.06	0.06	0.10	0.11	0.08	0.10	0.11	0.09	0.03	0	0	0	0	0.06
NPL	0.65	0.42	0.75	0.79	0.79	0.78	0.78	0.50	0.72	0.08	(0.01	(0.01	0.01	0.47
TLE	0.80	0.82	0.75	0.76	0.78	0.72	0.77	0.70	0.80	0.80	0.89	0.85	0.89	0.79
1,1,2-TRICHLOROETHANE	0.04	0.05	0.10	0.07	0.06	0.06	0.11	0.11	0.08	0.07	0.06	0.08	0.08	0.08
STABILIZING TANKS														
MOISTURE PPM	46	54	63	57	52	62	50	44	66	61	29	47	44	52
PH	7.0	7.0	7.0	6.9	6.9	6.9	6.8	6.8	6.9	6.8	6.8	6.8	6.7	6.9
HCL ACIDITY PPM	(1	(1	(1	2	1	1	1	2	1	2	2	2	2	1
NON-VOLATILE RESIDUE %	.0002	.0002	.0002	.0002	.0003	.0002	.0002	.0002	.0004	.0002	.0003	.0002	.0002	.0002
COLOR APHA	6	5	6	6	6	6	7	9	5	(5	(5	(5	6	5
SPECIFIC GRAVITY	1.305	1.306	1.305	1.305	1.304	1.305	1.305	1.305	1.304	1.304	1.304	1.304	1.304	1.305
AVG. DISTILLATION RANGE °C														
LOW	73.2	73.0	72.8	72.8	72.8	72.8	72.8	72.8	72.8	73.2	73.4	73.4	73.4	73.0
HIGH	82.7	82.7	82.8	82.2	82.2	82.3	82.5	82.8	83.1	82.8	82.8	83.3	83.3	82.9
SOLUBLE CHLORIDES PPM	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5	(0.5

SL 013381

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

FORM 95A202- 15

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

PER - TRI HEAVIES STILL BOTTOMS		1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TRICHLOROETHYLENE	%	(0.01	0	0.06	0	0.03	0	0	0	0	(0.01	0	0	(0.01	(0.01
1.1,2TRICHLOROETHANE	%	(0.01	0	0.25	0.03	(0.01	0	0	0	0	(0.01	0	0	(0.01	0.03
PERCHLOROETHYLENE	%	13.84	7.50	13.83	17.51	30.85	23.50	17.18	18.30	24.49	26.92	28.63	17.98	20.81	20.63
U-TETRACHLOROETHANE	%	2.16	3.88	6.54	4.09	3.56	4.43	5.25	4.34	4.12	3.94	3.82	4.62	4.19	4.40
S-TETRACHLOROETHANE	%	34.38	42.96	28.83	26.20	27.90	28.69	39.66	26.49	26.90	25.77	27.34	31.03	22.48	29.52
PENTACHLOROETHANE	%	22.33	28.30	30.00	26.85	20.84	22.72	22.80	24.49	24.16	21.34	21.79	27.45	29.88	25.05
HEXACHLOROETHANE	%	1.67	1.83	2.30	3.23	2.81	3.71	2.57	4.42	4.12	5.61	4.18	2.94	4.94	3.56
HEAVY UNKNOWNS	%	5.27	5.13	7.55	9.81	4.52	4.24	3.99	6.51	4.81	5.37	4.81	5.50	6.27	5.71
$FeCl_3$	PPM	22	14	22	31	54	10	46	34	52	69	84	41	47	42
NON-VOLATILE	%	2.64	2.33	3.87	6.10	4.07	2.40	3.68	-	-	-	-	-	-	3.74

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of 14th Judicial District Court
No. 91 1145

FORM [redacted]5A 202-16

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

PERCHLOR STABILIZATION	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 208 WT. %														
PERCHLOROETHYLENE	99.89	99.77	99.85	99.88	99.86	99.87	99.87	99.87	99.89	99.86	99.85	99.87	99.86	99.86
1,1-DICHLOROBROMOETHYLENE	(0.01	(0.01	(0.01	0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01
1,2-DICHLOROBROMOETHYLENE	0.01	(0.01	0.01	0.02	0.01	0.01	0.01	0.01	(0.01	0.01	0.02	0.02	0.01	0.01
1,1,2-TRICHLOROETHANE	0.01	0.02	0.02	0.01	0.02	0.02	0.04	0.03	0.01	0.03	0.04	0.03	0.03	0.03
U-TETRACHLOROETHANE	0.04	0.05	0.05	0.04	0.05	0.04	0.03	0.03	0.04	0.05	0.05	0.04	0.06	0.04
EPE	0.04	0.05	0.05	0.05	0.05	0.05	0.04	0.05	0.05	0.04	0.04	0.04	0.04	0.05
TYPE 207 WT %														
PERCHLOROETHYLENE	99.80	99.81	99.80	99.81	99.80	99.76	99.80	99.79	99.80	99.79	99.79	99.81	99.82	99.80
1,1-DICHLOROBROMOETHYLENE	(0.01	0	(0.01	0.01	0	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01
1,2-DICHLOROBROMOETHYLENE	(0.01	0	0	0.02	0	0	0	0	0	0	0	0	(0.01	(0.01
1,1,2-TRICHLOROETHANE	0.01	0.01	0.02	0.02	0.02	0.02	0.02	0.04	0.02	0.04	0.03	0.02	0.02	0.02
U-TETRACHLOROETHANE	0.04	0.05	0.04	0.03	0.03	0.05	0.04	0.03	0.03	0.05	0.05	0.04	0.05	0.04
EPE	0.05	0.05	0.05	0.05	0.05	0.05	0.04	0.04	0.05	0.05	0.04	0.04	0.05	0.05

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FORM [redacted]5A 202-17

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

TRICHLOR STABILIZATION	1973 AVG.	JAN	FEB	MAR *	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 115 WT.%														
CARBON TETRACHLORIDE	(0.01													
ADH	0.03													
NPL	(0.01													
TRICHLOROETHYLENE	99.46													
PERCHLOROETHYLENE	(0.01													
1,1,2-TRICHLOROETHANE	0.02													
UNIDENTIFIED, TOTAL	(0.01													
TYPE 122 WT. %														
CARBON TETRACHLORIDE	(0.01	0.02	0.01	(0.01	0	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01
ADH	0.03	0.03	0.04	-	-	-	-	-	-	-	-	-	-	0.04
NPL	0.16	0.16	0.16	0.13	0.16	0.14	0.14	0.14	0.14	0.13	0.13	0.14	0.14	0.14
TRICHLOROETHYLENE	99.52	99.46	99.48	99.59	99.47	99.40	99.38	99.39	99.46	99.39	99.37	99.35	99.38	99.43
PERCHLOROETHYLENE	(0.01	0	(0.01	-	(0.01	0	0	0	0	0	0	0	0	(0.01
1,1,2-TRICHLOROETHANE	0.02	0.01	0.02	0.01	0.02	0.01	0.01	0.01	0.02	0.02	0.03	0.02	0.02	0.02
GDL	0.06	0.06	0.06	0	-	-	-	-	-	-	-	-	-	0.06
UNIDENTIFIED, TOTAL	(0.01	(0.01	(0.01	(0.01	(0.01	0.01	0.01	0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01
NMP				0.027	0.03	0.03	0.03	0.03	0.026	0.028	0.028	0.031	0.030	0.029
NRE				0.05	0.06	0.06	0.06	0.06	0.06	0.06	0.05	0.05	0.05	0.06
DPE				.0093	.0150	.0110	.0110	0.014	0.010	0.013	0.009	0.010	0.009	0.011

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CONFIDENTIAL
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

* Type 122 is Type 132 Subsequent to Feb.

FORM NO. 15A 202- 18

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

TRICHLOR STABILIZATION	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
TYPE 110E WT. %														
CARBON TETRACHLORIDE	0.01													
ADH	0.08													
NPL	0.32													
TRICHLOROETHYLENE	98.88													
PERCHLOROETHYLENE	0													
1.1.2-TRICHLOROETHANE	0.03													
GDL	0.12													
UNIDENTIFIED, TOTAL	(0.01													
TYPE 113 WT. %														
CARBON TETRACHLORIDE	(0.01	(0.01	0.01	(0.01	0	(0.01	(0.01	(0.01	0	(0.01	(0.01	(0.01	0	(0.01
NPL	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
TRICHLOROETHYLENE	99.97	99.98	99.97	99.98	99.99	99.99	99.98	99.98	99.98	99.96	99.98	99.98	99.98	99.98
PERCHLOROETHYLENE	(0.01	0	0		0	0	0	0	(0.01	(0.01	0	0	(0.01	(0.01
1.1.2-TRICHLOROETHANE	0.02	0.01	0.01	(0.01	(0.01	(0.01	0.01	(0.01	(0.01	0.01	0.02	0.01	0.02	0.01
UNIDENTIFIED, TOTAL	(0.01	(0.01	(0.01	0	0	0	0	0.01	(0.01	(0.01	(0.01	(0.01	0	(0.01

SL 013385

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

FORM [illegible] 45A 202 - 19

PPG USTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

ETHYL CHLORIDE	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
C_2H_4 Feed %	99.92	99.87	99.92	99.91	99.94	99.97	99.95	99.93	99.95	99.91	99.86	99.94	99.88	99.92
PRIMARY STRIPPER														
Bottoms PPM														
HCl	242.9	43.7	-	117.5	99.8	-	-	99.7	-	-	-	-	-	90.2
$FeCl_3$	10.3	2.1	-	60.9	4.3	6.2	3.4	11.4	6.93	0.81	4.40	1.68	1.37	2.18
H_2O	122	117	-	64	89	68	56	56	66	112	126	66	36	78
Still Overhead														
C_2H_5Cl Wt. %	99.96	99.95	-	99.97	-	-	-	-	-	-	-	-	-	99.96
HCl PPM	294	-	-	55	-	-	-	-	-	-	-	-	-	55
H_2O PPM	161	256	-	46	-	-	-	-	-	-	-	-	-	151

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Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

FOI NO. 202).

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

VINYL CHLORIDE		1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
FEED TO UNIT	% EDC	99.98	99.97	99.98	99.98	99.98	99.99	99.99	99.99	99.99	99.99	99.97	99.96	99.99	99.98
VAPORIZING FURNACE															
FEED															
VINYLIDENE CHL RIDE	WT. %	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01
1.1-DICHLOROETHANE	WT. %	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.05	0.05	0.04	0.05	0.04
CHLOROF RM	WT.%	0.05	0.02	0.04	0.03	0.39	0.14	0.03	0.02	0.03	0.23	0.14	0.20	0.27	0.13
1.2-DICHLOROETHANE	WT.%	99.78	99.88	99.86	99.87	99.13	99.62	99.82	99.85	99.84	99.53	99.72	99.68	99.31	99.68
OTHERS	WT.%	0.01	0.01	(0.01	(0.01	0.01	(0.01	(0.01	(0.01	(0.01	0.03	0.01	0.01	0.01	0.01
H_2O	PPM	41	56	29	76	65	76	89	87	96	67	76	33	51	67
HCl	Wt.%	0.03	0.03	0.04	0.02	0.02	0.04	0.08	0.02	0.03	0.04	0.02	0.01	0.01	0.03
Fe	PPM	0.20	0.24	0.89	0.24	0.35	0.35	0.48	0.33	0.18	0.23	0.22	0.51	0.46	0.37
Cl_2	PPM	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1	(1
ABSORBER-STRIPPER COLUMNS															
QUENCH LIQUOR															
VINYL CHLORIDE	WT.%	9.86	10.68	3.39	-	-	-	-	-	-	-	-	-	-	7.04
VINYLIDENE CHL RIDE	WT.%	(0.01	0.02	0.01	-	-	-	-	-	-	-	-	-	-	0.02
t-1.2 DICHLOROETHYLENE	WT.%										-				
1 1-DICHL R ETHANE	WT.%	0.07	0.04	0.06	-	-	-	-	-	-	-	-	-	-	0.05
CHLOR PRENE	WT.%	0.02	0.02	0.01	-	-	-	-	-	-	-	-	-	-	0.02
CHL R FORM	WT.%	0.06	0.03	0.05	-	-	-	-	-	-	-	-	-	-	0.04
1.2-DICHLOROETHANE	WT.%	89.41	89.16	96.44	-	-	-	-	-	-	-	-	-	-	92.80
THERS	WT.%	0.08	0.04	0.03	-	-	-	-	-	-	-	-	-	-	0.04
H_2O	PPM	191	213	150	-	-	134	101	79	146	179	219	44	194	146
HCl	WT.%	0.85	0.93	0.98	-	-	-	-	-	-	-	-	-	-	0.96
Fe	PPM	12.05	17.46	61.28	-	13.70	14.99	3.45	10.31	2.60	12.27	19.33	4.40	23.23	16.64
FURNACE FEED	% CCl_4	0.04	(0.01	(0.01	(0.01	0.34	0.09	(0.01	(0.01	0.01	0.08	0.02	0.01	0.04	0.05

SL 013387

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Subject to Protective Order
of 14th Judicial District Court
No. [illegible]

FORM NO. 202-21

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

VINYL CHLORIDE		1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
ABSORBER-STRIPPER COLUMNS															
LEAN IL															
VINYL CHLORIDE	WT.%														
VINYLIDENE CHLORIDE	WT.%	(0.01	0.03	0.02	0.01	-	-	-	-	-	-	-	-	-	0.02
1.1- DICHL ROETHANE	WT.%	0.06	0.05	0.07	0.07	-	-	-	-	-	-	-	-	-	0.06
CHLOROPRENE	WT.%	0.04	0.04	0.06	0.03	-	-	-	-	-	-	-	-	-	0.04
CHLOROFORM	WT.%	0.06	0.03	0.06	0.04	-	-	-	-	-	-	-	-	-	0.04
1.2- DICHL ROETHANE	WT.%	99.47	99.82	99.59	99.83	-	-	-	-	-	-	-	-	-	99.75
OTHERS	WT.%	0.05	0.02	0.04	0.02	-	-	-	-	-	-	-	-	-	0.03
H_2O	PPM	51	51	25	82	-	-	-	-	-	-	-	-	-	53
HCl	PPM	1.57	5.68	15.57	6.18	-	-	-	-	-	-	-	-	-	9.14
Fe	PPM	0.43	0.47	0.80	0.42	-	-	-	-	-	-	-	-	-	0.56
UPPER INTERC LER															
VINYL CHL RIDE	WT.%	1.93	2.64	0.76	-	-	-	-	-	-	-	-	-	-	1.70
H_2	PPM	396	275	180	-	233	287	226	215	221	107	105	-	116	197
HCl	WT.%	1.57	1.68	1.30	-	-	-	-	-	-	-	-	-	-	1.49
Fe	PPM	31.01	11.70	22.49	-	15.81	31.00	29.63	29.65	8.27	3.56	4.86	-	11.00	16.80
LOWER INTERC OLER															
VINYL CHLORIDE	WT.%	6.11	3.20	1.23	-	-	-	-	-	-	-	-	-	-	2.22
H_2	PPM	215	163	65	-	364	283	198	212	306	322	187	-	108	221
HCl	WT.%	1.54	2.02	5.50	-	-	-	-	-	-	-	-	-	-	3.76
Fe	PPM	18.37	4.44	2.75	-	27.28	23.51	26.50	30.87	19.04	11.48	8.70	-	8.56	16.31

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

SL 013388

FORM [illegible]SA 202-22

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

VINYL CHLORIDE		1973 AVG	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG
VC PRODUCT STILL															
FEED															
VINYL CHL RIDE	WT.%	15.98	12.58	-	-	-	-	-	-	-	-	-	-	-	12.58
VINYLIDENE CHLORIDE	WT.%	0.01	0.02	-	-	0.07	-	-	-	-	-	-	-	-	0.05
1.1- DICHLOR ETHANE	WT.%	0.06	0.05	-	-	0.07	-	-	-	-	-	-	-	-	0.06
CHL ROPRENE	WT.%	0.04	0.04	-	-	-	-	-	-	-	-	-	-	-	0.04
CHLOROF RM	WT.%	0.07	0.03	-	-	0.10	-	-	-	-	-	-	-	-	0.07
1.2- DICHL ROETHANE	WT.%	83.89	87.23	-	-	99.34	-	-	-	-	-	-	-	-	93.29
OTHERS	WT.%	0.03	0.02	-	-	-	-	-	-	-	-	-	-	-	0.02
H_2	PPM	48	67	20	-	45	75	69	53	60	87	95	66	32	61
HCl	PPM	3.83	7.38	6.08	-	-	-	-	-	-	-	-	-	-	6.73
Fe	PPM	0.83	0.99	0.63	-	1.63	1.85	1.45	0.39	1.90	2.08	0.86	0.32	0.28	1.13
PRODUCT MONOMER (DAY TANKS)															
VINYL CHL RIDE	WT.%	99.990	99.995	99.990	99.976	99.986	99.977	99.988	99.984	99.991	99.995	99.994	99.995	99.994	99.989
BUTADIENE	PPM	5	6	9	8	7	8	10	6	5	3	4	2	2	6
METHYL CHLORIDE	PPM	12	21	23	31	33	32	33	26	22	25	29	26	30	28
ETHYL CHLORIDE	PPM	37	21	64	124	90	72	56	52	34	17	16	17	21	23
OTHERS	PPM	0.2	(0.1	(0.1	0.1	0.1	(1	(0.1	0.5	0.3	0.3	0.2	0.2	0.3	0.2
H_2O	PPM	41	45	40	49	37	39	30	37	45	57	46	34	45	42
Fe	PPM	0.20	0.12	0.20	0.16	0.13	0.11	0.08	0.04	0.06	0.12	0.04	0.09	0.04	0.10
pH		7.4	7.0	7.2	7.1	7.2	7.2	7.3	7.3	7.5	7.6	7.5	7.5	7.3	7.3
HCl		(1	0.2	(1	(1	(0.1	(1	(0.1	(0.1	0.2	0.2	(0.1	(0.1	(0.1	0.2
Vinyl Acetylene	PPM	4	5	5	4	5	8	9	5	5	4	4	2	5	5
1,1 - Dichloroethane	PPM	(1	(1	0	-	3	-	-	-	-	-	-	-	-	1.2
1,2 - Dichloroethane	PPM	0	(1	0	-	-	-	-	-	-	-	-	-	-	(1

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FORM 15A 202 / 23

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

LABORATORY OPERATIONS REPORT

VINYL CHLORIDE		1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
HEAVIES STILL															
FEED															
VINYLIDENE CHLORIDE	WT.%	(0.01	0.02	0.02	(0.01	0.02	(0.01	(0.01	(0.01	(0.01	0.02	(0.01	0.02	0.02	0.01
1.1- DICHLOROETHANE	WT.%	0.06	0.05	(0.01	0.06	0.07	0.07	0.08	0.08	0.07	0.08	0.08	0.08	0.10	0.07
C- 1.2- DICHLOROETHYLENE	WT.%					(0.01	0	0	0	0	0	0	0	0	(0.01
CHLOROFORM	WT.%	0.07	0.03	0.06	0.05	0.84	0.20	0.05	0.03	0.04	0.44	0.20	0.21	0.50	0.22
1.2- DICHL ROETHANE	WT.%	99.31	99.68	99.58	99.82	98.07	99.69	99.48	99.65	99.63	98.65	98.90	99.32	98.03	99.21
1.1.2- TRICHLOROETHANE	WT.%	0.19	0.15	0.18	0.02	0.12	0.10	0.18	0.11	0.15	0.18	0.27	0.05	0.05	0.13
OTHERS	WT.%	0.06	0.03	0.02	0.04	0.02	0.04	0.06	0.04	0.02	0.02	0.08	0.03	0.13	0.05
H_2O	PPM	38	73	30	101	71	55	102	77	70	55	96	51	44	69
HCl	WT.%	0.13	0.03	0.04	0.01	0.03	0.06	1.44	0.03	0.03	0.02	0.02	0.02	0.01	0.15
Fe	PPM	1.30	2.49	1.51	3.49	8.63	6.17	9.36	3.12	2.29	2.89	3.25	2.18	2.68	4.01
Cl_2	PPM	2	(1	(1	1	(1	(1	1	(1	1	(1	(1	1	(1	1
BOTTOMS															
CHLOROF RM	WT.%	(0.01	(0.01	0	0	0	0	0	0	0	0	0	0	0	(0.01
1.2- DICHL R ETHANE	WT.%	73.47	61.92	66.22	86.11	86.88	85.18	82.07	86.74	82.85	82.15	69.36	91.87	87.34	80.72
Trichloroethylene	Wt.%	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
1.1.2- TRICHLOROETHANE	WT.%	18.61	25.95	22.90	8.04	7.45	7.93	7.95	8.14	11.32	11.62	20.32	2.44	4.17	11.52
OTHERS	WT.%	7.83	11.79	10.88	5.47	5.67	6.89	8.56	5.12	5.83	6.22	10.32	5.70	8.49	7.58
HCl	WT.%	0.08	0.02	0.03	0.02	0.05	0.03	0.03	0.02	0.01	0.02	0.02	0.02	0.04	0.03
Fe	PPM	39.76	97.38	109.28	87.55	99.02	136.82	73.43	71.55	58.74	77.89	49.41	51.20	51.85	80.34
WASTE-DOPP KETTLE BOTTOMS															
1.2- DICHLOROETHANE	WT.%														
PERCHLOROETHYLENE	WT.%														
1.1.2- TRICHLOROETHANE	WT.%														
U-TETRACHLOROETHANE	WT.%														
S-TETRACHLOR ETHANE	WT.%														
PENTACHLOROETHANE	WT.%														
THERS	WT.%														
Fe	PPM														
TARS	WT.%														
RESIDUE	WT.%														

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

OHC-EDC CONDENSED ORGANIC	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
REACTOR NO. 1														
Methyl Chloride %*	0.04	0.05	0.03	0.04	0.04	0.05	0.05	0.06	0.03	0.04	0.04	0.06	0.05	0.05
Vinyl Chloride	0.08	0.10	0.07	0.08	0.08	0.08	0.07	0.04	0.05	0.05	0.05	0.06	0.06	0.07
Ethyl Chloride	0.74	0.62	0.24	0.49	0.58	0.79	0.48	0.29	0.32	0.38	0.52	0.32	0.31	0.45
Vinylidine Chloride	0.05	0.05	0.05	0.06	0.04	0.06	0.05	0.06	0.03	0.04	0.04	0.06	0.06	0.05
1, 1-Dichloroethylene	0.18	0.19	0.12	0.16	0.18	0.26	0.26	0.20	0.23	0.22	0.15	0.18	0.13	0.19
cis-1, 2-Dichloroethylene	0.21	0.26	0.17	0.20	0.17	0.23	0.29	0.23	0.27	0.28	0.17	0.36	0.16	0.23
Chloroform	0.64	0.62	0.46	0.80	0.37	0.60	0.39	0.59	0.36	0.85	0.71	0.73	1.08	0.63
EDC	94.61	94.43	96.09	94.93	96.16	95.09	95.54	94.31	96.11	93.88	94.89	94.26	93.42	94.93
Carbontetrachloride	0.79	0.88	0.64	0.77	0.41	0.46	0.39	0.56	0.29	0.93	0.83	1.01	1.65	0.74
Trichloroethylene	0.13	0.09	0.08	0.10	0.08	0.19	0.13	0.13	0.13	0.12	0.10	0.12	0.11	0.12
Chloral	0.56	0.63	0.37	0.58	0.41	0.33	0.31	0.21	0.16	0.43	0.34	0.27	0.24	0.36
1, 1, 2- Trichloroethane	1.74	1.92	1.54	1.64	1.30	1.70	1.69	2.48	1.64	2.24	1.74	2.09	2.24	1.85
Perchloroethylene	0.02	0.02	(0.01	0.02	0.02	0.03	0.05	0.03	0.03	0.02	0.03	0.03	0.03	0.03
U-Tetrachloroethane	0.01	(0.01	(0.01	0.01	(0.01	(0.01	(0.01	0.01	(0.01	0.01	0.01	0.02	0.02	(0.01
S-Tetrachloroethane	0.18	0.16	0.15	0.13	0.16	0.25	0.30	0.82	0.39	0.49	0.37	0.51	0.39	0.34
Pentachloroethane	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
Unknowns	(0.01	(0.01	0	0	0	0	0	0.01	(0.01	(0.01	(0.01	0.01	0	(0.01

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

OHC-EDC CONDENSED ORGANIC REACTOR NO. 2	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
Methyl Chloride %*	0.03	0.03	0.04	0.04	0.04	-	0.03	0.04	0.03	0.03	0.04	0.05	0.07	0.04
Vinyl Chloride	0.06	0.08	0.09	0.06	0.07	-	0.06	0.05	0.04	0.05	0.06	0.06	0.05	0.06
Ethyl Chloride	0.57	0.51	0.36	0.37	0.84	-	0.53	0.43	0.21	0.39	0.42	0.34	0.32	0.43
Vinylidine Chloride	0.05	0.05	0.05	0.06	0.04	-	0.03	0.05	0.03	0.04	0.06	0.05	0.07	0.05
1, 1-Dichloroethylene	0.15	0.15	0.18	0.13	0.18	-	0.22	0.17	0.16	0.13	0.16	0.15	0.14	0.16
cis-1, 2-Dichloroethylene	0.14	0.18	0.20	0.16	0.21	-	0.11	0.14	0.14	0.10	0.16	0.16	0.18	0.16
Chloroform	0.69	0.66	0.50	0.82	0.50	-	0.35	0.63	0.49	0.97	0.98	0.98	0.97	0.71
EDC	94.89	94.81	95.15	95.23	95.46	-	96.23	95.33	96.44	94.72	94.79	94.21	93.46	95.08
Carbontetrachloride	1.02	1.15	0.79	0.87	0.37	-	0.58	0.97	0.49	1.60	1.18	1.43	1.69	1.01
Trichloroethylene	0.12	0.09	0.11	0.09	0.10	-	0.08	0.11	0.09	0.12	0.12	0.11	0.13	0.10
Chloral	0.41	0.38	0.53	0.37	0.44	-	0.36	0.30	0.25	0.26	0.23	0.28	0.32	0.34
1, 1, 2 Trichloroethane	1.55	1.77	1.80	1.63	1.56	-	1.25	1.55	1.40	1.39	1.58	1.87	2.11	1.63
Perchloroethylene	0.02	0.02	0.02	0.01	0.03	-	0.02	0.04	0.03	0.03	0.03	0.02	0.02	0.02
U-Tetrachlorcethane	0.02	0.01	(0.01	0.01	(0.01	-	0.01	0.01	(0.01	0.02	0.02	0.02	0.02	0.01
S-Tetrachloroothane	0.14	0.11	0.17	0.15	0.16	-	0.14	0.19	0.21	0.15	0.20	0.25	0.46	0.20
Pentachloroethane	(0.01	0	0	0	0	-	0	0	0	0	0	0	0	0
Unknowns	(0.01	0	0	0	0	-	0	(0.01	(0.01	(0.01	0.01	0.01	(0.01	(0.01

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PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

OHC-EDC CONDENSED ORGANIC	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
REACTOR NO. 3														
Methyl Chloride %	-	-	-	0.02	0.03	0.07	0.06	0.06	0.05	0.04	0.05	0.05	0.06	0.05
Vinyl Chloride	-	-	-	0.08	0.07	0.08	0.08	0.06	0.09	0.08	0.07	0.06	0.05	0.07
Ethyl Chloride	-	-	-	0.28	0.59	0.64	0.35	0.31	0.29	0.31	0.59	0.36	0.28	0.40
Vinylidine Chloride	-	-	-	0.03	0.03	0.09	0.06	0.07	0.04	0.06	0.05	0.05	0.07	0.06
1, 1-Dichloroethylene	-	-	-	0.12	0.18	0.25	0.34	0	0.29	0.29	0.23	0.16	0.16	0.22
cis-1, 2-Dichloroethylene	-	-	-	0.14	0.15	0.34	0.48	0.26	0.46	0.44	0.30	0.21	0.23	0.30
Chloroform	-	-	-	0.44	0.35	0.67	0.46	0.63	0.54	1.04	0.64	0.81	0.99	0.66
EDC	-	-	-	96.38	96.25	94.09	94.02	94.04	94.60	93.49	94.55	94.80	93.61	94.58
Carbontetrachloride	-	-	-	0.44	0.45	0.49	0.47	0.72	0.43	1.23	0.52	0.92	1.51	0.72
Trichloroethylene	-	-	-	0.06	0.09	0.25	0.17	0.14	0.13	0.16	0.09	0.07	0.13	0.13
Chloral	-	-	-	0.27	0.39	0.43	0.52	0.25	0.48	0.21	0.54	0.28	0.28	0.37
1, 1, 2-Trichloroethane	-	-	-	1.64	1.30	2.26	2.37	2.48	2.11	2.11	1.96	1.90	2.10	2.02
Perchloroethylene	-	-	-	0.01	0.03	0.03	0.06	0.05	0.06	0.07	0.04	0.04	0.03	0.04
U-Tetrachloroethene	-	-	-	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0.01	(0.01
S-Tetrachloroethane	-	-	-	0.08	0.10	0.37	0.59	0.56	0.42	0.46	0.38	0.30	0.40	0.37
Pentachloroethane	-	-	-	0	0	0	0	0	0	0	0	0	0	0
Unknowns	-	-	-	0	-	-	-	-	0.02	0	(0.01	0	0	(0.01

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

OHC-EDC	1973 avg.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 avg.
DH STILL BOTTOM														
Methyl Chloride %*	(0.01	(0.01	0	0	0	0	0	(0.01	(0.01	0	0	0	(0.01	(0.01
Vinyl Chloride	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0	(0.01	(0.01	(0.01	0	0	(0.01	(0.01
Ethyl Chloride	0.16	0.14	0.06	0.10	0.06	0.09	0.03	0.09	0.11	0.07	0.10	0.18	0.14	0.10
Vinylidine Chloride	0.04	0.04	0.03	0.04	0.03	0.05	0.04	0.04	0.04	0.04	0.04	0.06	0.07	0.04
1, 1-Dichloroethylene	0.15	0.19	0.12	0.14	0.15	0.22	0.23	0.18	0.27	0.20	0.18	0.15	0.16	0.18
cis-1, 2-Dichloroethylene	0.18	0.20	0.17	0.17	0.16	0.28	0.33	0.27	0.36	0.31	0.23	0.17	0.24	0.24
Chloroform	1.23	1.03	0.84	1.09	0.91	0.98	0.81	1.17	1.33	1.72	1.56	1.94	1.86	1.27
EDC	95.29	95.05	95.59	95.70	96.46	95.26	95.37	94.44	94.92	93.62	94.52	93.65	93.05	94.80
Carbontetrachloride	0.92	1.05	0.78	0.66	0.39	0.42	0.52	0.79	0.36	1.43	0.78	1.22	1.65	0.84
Trichloroethylene	0.13	0.10	0.12	0.10	0.10	0.14	0.14	0.14	0.12	0.17	0.15	0.12	0.16	0.13
Chloral	0.06	0.18	0.15	0.12	0.10	0.12	0.16	0.12	0.16	0.06	0.36	0.02	0.05	0.13
1, 1, 2- Trichloroethane	1.68	1.90	1.84	1.72	1.50	2.01	1.92	2.23	2.41	1.95	1.96	2.06	2.17	1.97
Perchloroethylene	0.02	0.02	0.02	0.01	0.02	0.03	0.04	0.04	0.05	0.04	0.04	0.03	0.03	0.03
U-Tetrachloroethane	0.01	0.01	0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	(0.01	0.01	0.01	0.02	(0.01
S-Tetrachloroethane	0.17	0.11	0.21	0.13	0.12	0.32	0.39	0.48	0.37	0.39	0.38	0.38	0.44	0.31
Pentachloroethane	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
Unknowns	(0.01	(0.01	0	0.14	0	0	(0.01	(0.01	0	0	(0.01	0.02	(0.01	0.03
Water PPM	36	67	37	73	64	62	93	85	70	59	71	28	34	62
Fe PPM	0	0	0	0	0	0	0	0	0	0	0	0	0	0

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

OHC-EDC	1973 avg.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 avg.
DH STILL BOTTOM #2														
Methyl Chloride %*									0	(0.01	0	0	(0.01	(0.01
Vinyl Chloride									0	(0.01	(0.01	0	0	(0.01
Ethyl Chloride									(0.01	0.08	0.06	0.06	0.05	0.05
Vinylidine Chloride									0.01	0.04	0.03	0.04	0.05	0.03
1, 1-Dichloroethylene									0.10	0.21	0.15	0.16	0.12	0.15
cis-1, 2-Dichloroethylene									0.29	0.32	0.23	0.22	0.21	0.25
Chloroform									1.07	2.05	1.71	1.81	1.74	1.68
EDC									95.50	93.26	94.39	93.62	93.44	94.04
Carbontetrachloride									0.41	1.62	0.78	1.29	1.43	1.11
Trichloroethylene									0.13	0.19	0.17	0.18	0.15	0.16
Chloral									0.09	0.05	0.19	0.02	0.05	0.08
1, 1, 2-Trichloroethane									2.04	1.88	1.97	2.13	2.32	2.07
Perchloroethylene									0.05	0.05	0.05	0.08	0.04	0.05
U-Tetrachloroethane									(0.01	0.01	0.01	0.02	0.02	0.01
S-Tetrachloroethane									0.35	0.36	0.40	0.39	0.42	0.38
Pentachloroethane									0	0	0	0	0	0
Unknowns									(0.01	(0.01	(0.01	0.01	0	(0.01
Water PPM									79	72	67	29	36	57
Fe PPM									0	0	0	0	0	0

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

OHC-EDC	1973 avg.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 avg.
LIGHTS STILL BOTTOMS (Product)														
Methyl Chloride %*	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
Vinyl Chloride	(0.01	0	0	0	0	0	0	0	0	0	0	0	0	0
Ethyl Chloride	0.06	0	0	0	0	0	0	(0.01	0	0	0	0	0	(0.01
Vinylidine Chloride	0.03	(0.01	0.02	0	0	(0.01	(0.01	0.02	(0.01	0	0.01	0	0	(0.01
trans-1, 2 Dichloroethylene	0	0	0	0	0	0	0	0	0	0	0	0	0	0
1, 1-Dichloroethylene	0.04	0.02	0.09	0	0	0.01	0.02	0.08	(0.01	(0.01	0	0.03	0.02	0.03
cis-1, 2-Dichloroethylene	0.07	0.02	0.15	(0.01	0.03	0.01	0.01	0.03	0.07	(0.01	0.01	0.03	(0.01	0.03
Chloroform	0.06	(0.01	0.05	(0.01	0.14	0.01	0.04	0.02	0.12	0.04	0.03	0.07	0.07	0.05
EDC	98.75	99.02	99.24	99.58	99.04	99.72	99.12	99.55	98.20	96.84	97.24	96.46	92.60	98.05
Carbontetrachloride	0.56	0.90	0.57	0.08	0.84	0.02	0.20	0.08	0.23	0.04	0.03	0.11	0.06	0.26
Trichloroethylene	0.20	0.12	0.20	0.32	0.30	0.21	0.16	0.27	0.89	0.12	0.18	0.10	0.09	0.25
Chloral	0.03	0.01	(0.01	0.01	0.01	0.01	0.12	(0.01	0.06	0.06	0.06	0.03	0.08	0.04
1, 1, 2- Trichloroethane	0.51	(0.01	0	0.03	0.03	0.04	1.94	0.34	1.72	2.43	2.18	2.73	5.51	1.54
Perchloroethylene	0.04	0.02	0.03	0.03	0.17	0.04	0.04	0.02	0.05	0.07	0.15	0.08	0.15	0.07
U-Tetrachloroethane	(0.01	0	0	0	(0.01	(0.01	0.04	0.07	(0.01	0.01	0.02	0.03	0.04	0.03
S-Tetrachloroethane	0.04	0	0	0	(0.01	0.10	0.42	0.24	0.62	0.43	0.50	0.51	1.54	0.37
Pentachloroethane	0.01	0.02	0	0	0	0	0	0	0	0	0.57	0	0	0.05
Unknowns	(0.01	0	0	(0.01	0	0.02	0	0.01	(0.01	(0.01	0.01	0.01	0.01	(0.01
Water PPM	4	0	0	0	0	0	(0.01	0	0	119	0	0	0	10

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*Unless Otherwise Indicated

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

VINYLIDENE CHLORIDE MONOMER		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
VDCM REACTOR CRUDE															
Acetylene	PPM														
Monochloroacetylene	PPM														
Dichloroacetylene	PPM														
Vinylidene Chloride	Wt. %														
trans-1,2 Dichloroethylene	PPM														
cis-1,2 Dichloroethylene	PPM														
Trichloroethylene	PPM														
1,2-Dichloroethane	PPM														
Unknowns (Total)	PPM														
Toluene	PPM														
DAY TANK *															
Monochloroacetylene	PPM	5	1	1	11	28	50	16	27	40	43	75	27	25	29
Dichloroacetylene	PPM	52	64	56	138	73	63	60	84	98	100	80	68	92	81
Vinylidene Chloride	Wt. %	99.97	99.85	99.81	99.77	99.70	99.83	99.78	99.76	99.80	99.77	99.80	99.77	99.89	99.79
trans-1,2 Dichloroethylene	PPM	211	1458	1216	2145	2736	1672	1968	2249	1779	2191	1827	2192	1035	1872
cis-1,2 Dichloroethylene	PPM	(1	1	6	4	8	3	2	(1	5	2	2	5	7	4
Trichloroethylene	PPM	(1	0	(1	0	1	1	0	0	1	0	0	0	0	(1
1,2-Dichloroethane	PPM	(1	(1	16	3	5	1	0	0	0	0	1	(1	(1	2
Unknowns (Total)	PPM	3	2	1	2	3	1	2	1	2	1	2	1	2	2
Toluene	PPM	(1	(1	(1	0	(1	-	(1	0	(1	(1	2	(1	1	(1
H_2O	PPM	21	20	16	38	24	18	19	24	38	24	26	16	23	24
Acidity, As HCl	PPM	(1	(1	(1	(1	(1	(1	0.05	(1	0.31	(1	(1	(1	2	3
Color	APHA	5	5	(5	(5	(5	(5	(5	(5	(5	(5	(5	(5	(5	(5
Peroxide, As H_2O_2	PPM	(1	(1	(1	(1	(1	(1	(1	(1	(0.01	(1	(1	(1	(1	(1
HQMME	PPM	191	204	205	204	210	189	187	194	189	193	200	185	215	198
Phenol	Wt. %	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Appearance		CLEAR	-	CLEAR	CLEAR	CLEAR	CLEAR	Clear	CLEAR	CLEAR	-	CLEAR	-	CLEAR	CLEAR

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** Storage Tank Subsequent to Jan.

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

WASTE RECOVERY UNIT	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
Ethyl Chloride Wt. %	-	-	0.16	0.38	0.40	-	0.26	0.11	0.14	0.19	0.47	0.22	0.27	0.26
Vinylidene Chloride	-	-	0.02	0.03	0.01	-	(0.01	0.01	0.01	(0.01	0.11	0.01	0.01	0.02
t-1,2-Dichloroethylene	-	-	0	0	(0.01	-	0	0	0	0	0	0	0	0
1,1-Dichloroethane	-	-	0.10	0.31	0.08	-	0.08	0.06	0.17	0.12	0.24	0.14	0.10	0.14
c-1,2-Dichloroethylene	-	-	0.16	0.33	0.18	-	0.22	0.11	0.34	0.29	0.40	0.22	0.32	0.26
Chloroform	-	-	0.42	1.30	0.34	-	0.13	0.22	0.69	0.49	0.47	0.64	0.66	0.54
1,2-Dichloroethane	-	-	13.22	23.90	13.26	-	11.88	7.67	18.13	17.05	14.49	15.19	17.14	15.19
Carbon Tetrachloride	-	-	0.26	0.50	0.18	-	0.14	0.14	0.20	0.11	0.04	0.12	0.11	0.18
Trichloroethylene	-	-	0.08	0.22	0.07	-	0.11	0.11	0.17	0.11	0.10	0.17	0.15	0.13
1,1,2-Trichloroethane	-	-	28.41	27.84	28.35	-	27.69	43.20	33.67	30.23	28.52	27.74	28.36	30.40
Perchloroethylene	-	-	6.09	8.11	12.28	-	14.84	6.39	9.54	17.43	23.62	10.21	10.81	11.93
U-Tetrachloroethane	-	-	6.93	3.42	5.74	-	5.39	7.94	5.38	4.44	4.56	6.42	7.13	5.74
S-Tetrachloroethane	-	-	24.52	17.26	23.52	-	23.90	21.04	18.30	16.84	14.57	23.08	21.18	20.42
Pentachloroethane	-	-	12.56	9.56	10.49	-	10.33	8.57	9.66	8.77	8.37	11.39	11.19	10.09
Hexachloroethane	-	-	0.71	0.48	0.43	-	0.58	0.49	0.41	0.44	0.57	0.60	0.34	0.51
Pentachloro Butadiene	-	-	~~12.56~~	-	0.86	-	0.64	0.91	0.55	0.59	0.39	0.75	0.48	~~1.97~~ 0.45
Hexachloro Butadiene	-	-	0.71	-	1.27	-	1.08	1.29	0.59	0.66	0.33	0.77	0.48	0.80
Unknowns	-	-	4.62	6.33	2.52	-	2.52	1.40	2.34	2.24	2.26	2.30	1.25	2.78
						-								
Specific Gravity	-		1.509	1.458	1.488	-	1.481	1.482	1.452	1.480	1.466	1.475	1.461	1.475
	-													

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PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
LABORATORY OPERATIONS REPORT

CONFIDENTIAL:
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INCINERATOR	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
WASTE GAS FEED Wt. %														
C_2H_4			-	5.33	-	-	9.94	5.80	13.56	16.18	11.68	4.51	6.17	9.15
HCl			-	36.42	-	-	18.06	21.21	16.00	8.11	23.03	18.23	18.48	19.94
EC			-	0.71	-	-	0.81	0.33	1.45	1.66	0.51	0	0.33	0.83
VDC			-	2.12	-	-	2.11	1.46	1.13	1.82	1.92	2.71	1.23	1.81
EDC			-	2.01	-	-	2.01	1.14	2.65	2.88	2.28	0.46	2.32	1.97
Perchlor			-	0.13	-	-	0.12	0.06	0.07	0.10	0.17	0.18	0.43	0.16
Trichlor			-	1.04	-	-	1.03	2.24	1.36	1.14	1.28	2.28	0.71	1.26
Trans			-	1.88	-	-	1.86	1.97	1.42	1.92	2.04	3.07	1.26	1.93
Cis			-	1.14	-	-	1.34	1.57	1.08	1.24	1.39	2.08	0.58	1.30
Other			-	0.08	-	-	0.20	0.09	0.27	-	0.05	0.10	0.00	0.13
No. 1 INCINERATOR														
HCl in Stack PPM			320	-	116	121	144	195	164	159	151	183	101	165
Cl_2 in Stack PPM			440	-	164	95	122	111	197	220	269	191	99	191
HCl in Effluent GPL			21.1	18.8	8.6	14.2	9.5	13.9	16.9	19.5	17.5	16.8	11.8	15.3
Stack HCB PPM			-		-	-	-	-	-	-	-	-	-	-
Aqueous HCB PPM			-		-	-	-	-	-	-	-	-	-	-
No. 2 INCINERATOR														
HCl in Stack PPM			147	168	164	109	155	220	161	167	166	154	94	155
Cl_2 in Stack PPM			355	242	300	95	137	152	150	203	237	181	54	191
HCl in Effluent GPL			19.4	18.4	23.0	23.1	20.3	18.0	17.4	18.5	17.6	15.7	10.1	18.3
Stack HCB PPM			-	-	-	-	-	-	-	-	-	-	-	-
Aqueous HCB PPM			-	-	-	-	-	-	-	-	-	-	-	-
STACK GAS ANALYSES PPM														
CO			-	-	-	-	-	-	-	-	-	-	-	-
NOX			-	-	-	-	-	-	-	-	-	-	-	-
Organics			-	-	-	-	-	-	-	-	-	-	-	-
CH_4			-	-	-	-	-	-	-	-	-	-	-	-
HCl			-	-	-	-	-	-	-	-	-	-	-	-
Cl			-	-	-	-	-	-	-	-	-	-	-	-
								-	-	-	-	-	-	-

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PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

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LIQUID PHASE ETHYLENE DICHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
EDC Production	T/D	1082.3	628.1	941.6	964.4	896.4	978.9	996.7	880.2	882.8	811.2	765.5	860.7	875.7	873.5
EDC Area Production	T/D	1081.3	648.4	967.4	956.0	903.4	987.1	987.7	895.2	889.2	811.0	758.1	862.9	878.0	878.7
EDC Shipments	T/D	145.0	53.3	110.9	64.0	11.3	14.5	421.1	14.2	20.2	14.9	9.4	16.4	53.1	66.9
Purchased Ethylene to EDC	T/D	312.6	185.5	279.3	279.3	260.7	288.4	287.4	255.5	260.5	234.6	221.4	253.8	252.5	254.9
% C_2H_4 in Purchased Ethylene		99.92	99.87	99.92	99.91	99.94	99.97	99.95	99.93	99.95	99.91	99.86	99.94	99.88	99.92
Cl_2 to EDC	T/D	785.4	469.4	704.1	693.8	657.0	726.1	726.8	657.1	661.6	592.6	560.4	626.5	639.6	642.9
YIELDS															
Area Prod. + Trans. Credits															
Basis	Cl_2	99.0	99.9	99.0	99.8	99.2	98.0	97.8	98.0	96.7	99.0	97.7	99.3	99.2	98.6
	C	98.3	99.8	98.6	97.9	98.8	97.5	97.7	99.6	97.0	98.7	97.6	96.8	99.2	98.3
Records Prod. + Trans.															
Credits Basis	Cl_2	99.1	96.8	96.4	100.6	98.4	97.2	98.6	96.4	96.0	99.0	98.6	99.0	99.0	98.0
	C	98.4	96.7	96.0	98.8	98.0	96.7	98.6	98.0	96.3	98.7	98.5	96.6	99.0	97.7
Excess C_2H_4	%	2.0	0.9	1.8	3.0	1.8	3.0	2.6	0.6	3.3	2.0	3.0	3.7	1.4	2.3
Excess C_2H_4	T/Mo.	187.5	51.8	143.8	258.6	139.2	267.4	222.9	53.9	262.4	141.7	201.6	276.7	110.8	177.6
Stillbottoms To W.Rec.	T/D	3.4	5.5	5.1	9.5	5.8	5.6	3.4	3.3	3.0	7.2	5.3	4.7	7.0	5.4
Total Losses	T/D	-1.0	20.4	25.9	-8.4	7.0	8.2	-9.0	15.0	6.5	-0.1	-7.4	2.2	2.3	5.2
Loading Losses	T/D	-1.0	20.4	25.9	-8.4	7.0	8.2	-9.0	15.0	6.5	-0.1	-7.4	2.2	2.3	5.2
EDC Inventory	Tons	6927.8	2709.6	11704.7	16261.4	18558.1	19030.7	6173.8	7346.5	7774.1	6610.1	5593.1	12963.8	13632.1	10696.5
EDC REACTOR NO. 1															
Pressure Bott m	PSIG	18.6	16.7	18.5	18.0	17.8	18.1	18.9	19.0	19.2	19.4	20.8	20.3	21.0	19.0
Temp. °F Bottom		227	224	227	224	224	225	227	229	227	228	230	230	231	227
Top		216	214	215	214	214	214	216	219	219	218	221	220	220	217
EDC REACTOR NO. 2															
Pressure Bottom	PSIG	17.5	17.0	18.5	17.9	17.9	18.0	18.6	19.1	19.6	19.3	19.9	20.0	20.0	18.8
Temp. °F Bottom		222	221	223	223	222	221	224	226	226	226	229	227	228	225
Top		213	212	215	213	213	213	215	219	219	218	220	220	220	217
EDC REACTOR NO. 3															
Pressure Bottom		21.5	21.6	22.3	22.6	22.3	24.2	23.4	23.9	23.5	23.2	22.7	23.5	23.8	23.1
Temp. °F Bottom		224	224	225	228	227	227	226	228	220	218	217	217	218	223
Top		213	216	223	218	218	219	216	218	211	209	208	209	209	214

SL 013400

FORM [illegible]5A 208-2

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

CONFIDENTIAL
Subject to Protect[illegible]er
of 14th Judicial District Court
No. 91-1145

ETHYLENE DICHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
EDC STRIPPER NO. 1														
PRESSURE TOP PSIG	9.3	8.9	9.3	9.1	9.0	9.2	10.0	10.8	11.1	10.5	11.2	11.2	11.2	10.1
TEMP. °F BOTTOM	214	213	215	214	213	214	216	219	219	218	221	220	220	217
T P	209	199	201	206	206	209	210	211	213	213	214	214	216	209
FEED RATE GPM	67.2	42.9	64.9	57.6	54.8	71.6	77.3	47.7	46.3	44.8	55.4	50.0	58.9	56.0
EDC STRIPPER NO. 2														
PRESSURE TOP PSIG	11.4	11.8	11.2	13.0	11.8	13.7	3.9	16.2	16.4	15.3	11.8	11.7	11.3	13.2
TEMP. °F BOTTOM	217	220	218	222	221	224	222	227	226	224	217	216	216	221
T P	213	217	213	217	217	220	220	224	223	222	214	214	214	218
FEED RATE GPM	82.5	67.0	73.8	77.2	81.3	72.3	66.4	81.5	82.9	89.1	72.3	96.8	93.3	79.5
EDC STILL NO. 1														
FEED RATE GPM	44.7	32.5	52.0	-	-	-	-	-	-	-	-	27.0	40.4	38.0
REFLUX RATE GPM	24.3	25.0	25.2	-	-	-	-	-	-	-	-	21.8	24.7	24.2
PRODUCTION GPM	45.9	33.7	53.0	-	-	-	-	-	-	-	-	27.7	40.4	38.7
EDC STILL NO. 2														
TEMP. °F BOTTOM	255	248	242	245	243	247	253	250	256	257	259	261	263	252
TOP	195	194	201	202	204	203	210	204	194	196	194	199	195	200
FEED RATE GPM	101.6	65.2	129.4	130.2	130.4	132.2	131.6	132.5	130.9	134.5	122.7	133.7	107.7	123.4
REFLUX RATE GPM	77.3	79.6	100.4	105.4	111.1	114.3	114.6	105.5	109.5	116.9	100.7	122.8	124.1	108.7
PRODUCTION GPM	96.9	61.4	123.0	124.0	124.6	128.0	123.4	123.0	123.4	126.4	115.5	126.2	134.1	119.4
STEAM (140# BASIS) LBS./T EDC	772	831	-	310	194	583	658	636	839	974	887	935	914	706
KWH/T EDC	13.4	23.2	15.5	15.8	15.3	14.7	14.8	15.2	16.2	17.1	18.1	14.0	16.3	16.4
WELL WATER M GALS./T EDC	0.57	0.98	0.75	0.74	0.78	0.72	0.70	0.78	0.82	0.89	0.94	0.74	0.69	0.79
GAS MCF/T EDC	0.06	0.06	0.05	0.05	0.05	0.07	0.06	0.06	0.07	0.14	0.12	0.11	0.09	0.08
NITROGEN TONS/T EDC	0.005	0.008	0.006	0.005	0.005	0.005	0.006	0.005	0.005	0.006	0.006	0.005	0.006	0.006
OPERATING TIME (ANY RX) %	99.5	83.2	100.0	100.0	100.0	100.0	100.0	91.3	100.0	100.0	100.0	100.0	100.0	97.9

SL 013401

FORM N[illegible]A .208-3

PPG IN[illegible]STRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

ETHYLENE DICHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
EQUIPMENT HOURS *														
AIR COMPRESSORS #1	6001	621	544	480	720	690	126	4	0	0	0	642	744	4571
#2	6108	744	672	664	272	246	714	696	712	720	744	77	220	6481
#3	5080	123	128	344	448	700	654	696	712	720	744	720	520	6509
#4														
#5														
MAN HOURS PER TON EDC														
PRODUCTION	0.035	0.056	0.041	0.048	0.040	0.042	0.040	0.040	0.043	0.045	0.047	0.040	0.042	0.044
MAINTENANCE	0.023	0.080	0.024	0.018	0.023	0.023	0.022	0.026	0.053	0.031	0.028	0.017	0.019	0.030
SALARIED	0.012	0.020	0.013	0.013	0.015	0.013	0.012	0.014	0.014	0.015	0.018	0.013	0.014	0.014
TOTAL	0.070	0.156	0.078	0.079	0.078	0.078	0.074	0.080	0.110	0.091	0.093	0.070	0.075	0.088
CONTRACT MAINT. INCLUDED IN ABOVE	0.001	0.000	0.004	0.000	0.000	0.000	0.006	0.002	0.035	0.011	0.000	0.000	0.001	0.005
MAN HOURS/TON SHIPPED**														
BULK	0.024	0.073	0.038	0.063	0.328	0.399	0.015	0.143	0.127	0.161	0.220	0.284	0.083	0.161
SALARIED	0.002	0.008	0.004	0.005	0.028	0.032	0.001	0.014	0.013	0.015	0.020	0.023	0.008	0.014

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No 91-1145

SL 013402

* TOTALS

** OPERATIONS + MAINTENANCE

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
"TRI-ETHANE" ® DEPARTMENT OPERATIONS REPORT

CONFIDENTIAL
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

GENERAL DEPARTMENT		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
MC Production	T/D	153.4	137.7	149.0	149.7	159.0	137.3	130.2	75.4	149.6	163.6	172.3	173.6	211.0	150.7
MC Area Production	T/D	158.0	146.5	152.0	154.7	163.9	138.0	136.9	87.9	146.6	164.0	180.1	178.0	219.4	155.7
"Tri-Ethane" ® Production	T/D	162.4	144.9	157.8	160.6	165.1	147.3	138.0	76.5	164.1	160.5	195.5	183.9	226.8	160.1
"Tri-Ethane" ® Shipments	T/D	162.8	126.5	182.2	157.6	211.5	122.6	131.0	112.3	152.1	168.0	149.9	211.8	135.1	155.1
Chlorine Consumed	T/D	146.6	146.2	153.6	152.7	156.9	154.4	165.1	103.5	142.7	182.3	173.9	191.8	195.6	159.9
EDC Consumed	T/D	186.6	190.5	199.1	203.7	202.2	205.6	209.7	129.5	187.0	232.4	216.6	255.6	261.9	207.8
C_2H_4 Consumed	T/D														
YIELDS															
Area Prod. + Trans. Credits															
Basis	Cl_2	93.2	94.6	91.9	97.6	97.5	90.7	94.6	90.5	93.8	93.1	93.0	91.1	93.6	93.5
	C	91.8	89.8	89.0	92.1	92.2	85.5	90.7	89.2	91.4	89.0	90.2	89.0	91.4	90.0
Records Prod. + Trans.															
Credits Basis	Cl_2	91.5	91.3	90.8	95.8	95.8	90.4	92.3	83.8	95.0	93.0	90.5	89.8	91.3	91.6
	C	89.4	86.4	87.9	90.3	90.4	85.3	88.3	82.1	92.6	88.8	87.6	87.8	89.1	88.1
TCE TO PER-TRI	T/D	56.0	66.9	77.9	83.8	73.9	70.9	77.6	47.7	74.2	61.1	61.0	73.5	64.1	69.4
HCl to HCl Pross.	T/D	19.1	23.1	23.4	26.9	26.7	30.3	35.1	22.1	26.9	36.4	34.3	36.2	33.6	29.6
VDC to VDCM	T/D	18.2	22.3	19.3	22.1	23.5	25.5	39.4	15.7	11.5	42.6	21.7	38.6	30.2	26.0
Tons Cl_2/T TCE		0.598	0.569	0.567	0.535	0.547	0.582	0.589	0.672	0.549	0.585	0.606	0.585	0.568	0.580
Tons EDC/T TCE		0.763	0.741	0.735	0.714	0.705	0.775	0.748	0.842	0.719	0.746	0.756	0.780	0.760	0.752
Tons C_2H_4/T MC															
Tons N_2/T MC		0.074	0.085	0.082	0.110	0.072	0.098	0.089	0.092	0.093	0.083	0.073	0.074	0.061	0.084
Steam (140# Basis) Lbs./T MC		1282	2352	1614	1213	1665	1261	1204	1087	1292	1264	1213	1235	1218	1385
Well Water M Gals/T MC		7.6	9.1	9.4	8.8	10.1	8.7	8.7	17.3	9.7	8.1	8.0	8.2	7.7	9.5
Tons Cell Liquor/T MC		0.478	0.515	0.501	0.501	0.504	0.572	0.623	0.605	0.528	0.570	0.502	0.556	0.486	0.539
Catalyst Lbs./T MC ($FeCl_3$)		3.9	4.9	4.7	4.1	3.0	1.8	2.0	4.6	1.8	2.4	1.2	1.4	5.3	3.1
TPP Lbs./T MC		6.6	7.6	7.2	7.3	6.9	8.0	7.5	7.4	7.8	5.4	2.4	7.2	11.0	7.1
HQMME Lbs./T VDC		1.6	2.2	1.2	1.0	1.2	1.5	1.5	1.1	0.9	1.0	1.5	1.5	1.1	1.3
AIBN Lbs./T TCE		0.279	0.689	0.330	0.356	0.312	0.383	0.422	0.723	0.756	0.316	0.439	0.468	0.183	0.448
"Tri-Ethane" ® Inventory Tons		2449	2671	1986	2077	679	1443	1653	542	910	676	2087	1247	4088	1672
Operating Time	%	96	96	97	97	98	100	97	62	92	100	95	98	100	94

SL 013403

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

"TRI-ETHANE" ® DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
MAN HOURS/T MC PRODUCED														
Production	0.337	0.438	0.390	0.315	0.306	0.359	0.367	0.627	0.361	0.333	0.318	0.288	0.234	0.361
Maintenance	0.231	0.245	0.189	0.152	0.127	0.347	0.227	1.881	0.580	0.548	0.421	0.223	0.246	0.432
Salaried	0.105	0.116	0.113	0.105	0.107	0.123	0.117	0.194	0.116	0.098	0.099	0.085	0.078	0.113
Total	0.673	0.799	0.692	0.572	0.540	0.829	0.711	2.702	1.057	0.979	0.838	0.596	0.558	0.906
Contract Maint. Included in Above	0.008	0.004	0.000	0.000	0.000	0.000	0.005	0.030	0.216	0.312	0.117	0.021	0.075	0.065
MAN HOURS/T "TRI-ETHANE" ® SHIPPED														
Bulk	0.038	0.043	0.036	0.038	0.031	0.046	0.038	0.041	0.037	0.033	0.042	0.026	0.023	0.036
Drum	0.725	0.880	0.928	0.747	0.999	0.841	0.710	0.778	0.767	0.733	0.918	0.792	0.819	0.826
Salaried	0.007	0.010	0.007	0.007	0.006	0.008	0.007	0.010	0.009	0.006	0.007	0.004	0.006	0.007

FORM NO. 209-3

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
"TRI-ETHANE" DEPARTMENT OPERATIONS REPORT

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

MATERIAL BALANCE	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
CARBON - TONS														
TOTAL CARBON IN FEED	1378.0	1433.4	1353.1	1532.4	1472.3	1546.8	1527.1	975.6	1407.0	1691.8	1630.0	1861.6	1970.6	1533.5
CARBON IN PRODUCTION	1295.3	1313.7	1248.9	1463.4	1392.2	1363.6	1386.1	886.0	1235.9	1496.0	1467.7	1592.0	1769.1	1384.6
CARBON LOSS IN PROCESS	82.7	119.7	104.2	69.0	80.1	183.2	141.0	89.6	171.1	195.8	162.3	269.6	201.5	148.9
ACCT. LOSS IN STILL BOTTOMS	8.9	0.0	0.0	0.0	0.0	0.0	0.0	27.7	0.0	0.0	0.0	6.0	0.0	2.8
MISC. ACCT. LOSSES														
UNACCOUNTABLE CARBON LOSS IN PROCESS	73.8	119.7	104.2	69.0	80.1	183.2	141.0	61.9	171.1	195.8	162.3	263.6	201.5	146.1
CARBON LOADING LOSS	25.3	49.0	15.1	28.0	26.1	3.7	36.4	69.5	-16.6	2.0	43.6	24.1	46.8	27.3
TOTAL CARBON LOSS	108.0	168.7	119.3	97.0	106.2	186.9	177.4	159.1	154.5	197.8	205.9	293.7	248.3	176.2
CHLORINE - TONS														
TOTAL CHLORINE IN FEED	8532.6	8765.6	8296.9	9258.5	9054.0	9352.5	9462.1	6086.9	8579.0	10464.3	10203.6	11248.4	11879.1	9387.6
CHLORINE IN PRODUCTION	6260.9	6721.8	6182.5	7341.1	7003.4	6724.9	7113.1	4612.5	6385.0	7566.9	7336.8	7964.4	8315.0	6939.0
CHLORINE LOSS IN PROCESS	2271.7	2043.8	2114.4	1917.4	2050.6	2627.6	2349.0	1474.4	2194.0	2897.4	2866.8	3284.0	3564.1	2448.6
ACCT. LOSS IN STILL BOTTOMS	45.6	0.0	0.0	0.0	0.0	0.0	0	95.0	0.0	0.0	0.0	26.8	0.0	10.2
MISC. ACCT. LOSSES														
LOSS FROM VDC REACTION PLUS OTHER UNACCOUNTABLE LOSSES	1976.2	2043.8	2114.4	1917.4	2050.6	2627.6	2349.0	1379.4	2194.0	2897.4	2866.8	3257.2	3564.1	2438.4
CHLORINE LOADING LOSS	118.8	229.7	71.0	131.3	122.5	17.4	170.9	326.2	-77.9	9.3	204.6	106.7	207.9	126.6
TOTAL CHLORINE LOSS	2390.5	2273.5	2185.4	2048.7	2173.1	2645.0	2519.9	1800.7	2116.1	2906.7	3071.4	3390.7	3772.0	2575.2
TCE REACTOR SYSTEM														
TEMP. BOTTOM °F	193	209	203	212	223	209	208	206	202	215	216	203	196	208
PRESS. TOP PSIG	50	50	48	49	52	51.1	48.9	47.9	48.1	50.1	48.0	49.1	50.0	49.4
EDC ABSORBER														
TEMP. CHILLED HCL °F	11	18	26	18	23	24	40	39	27	23	22	21	24	25
FEED FLOW GPM	12.0	25.8	10.5	9.6	10.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	9.5	12.4
LIGHTS STILL														
TEMP. BOTTOM °F	291	292	291	292	295	297	297	294	287	289	286	282	283	290
VAPOR °F	203	204	203	205	208	210	211	208	199	201	200	192	193	203
FEED FLOW GPM	99	100	100	100	100	99	104	101	103	119	116	110	115	106

SL 013405

FORM I 5A209-4

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
"TRI-ETHANE"® DEPARTMENT OPERATIONS REPORT

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

HEAVIES STILL		1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
TEMP. STEAM	°F	274	265	265	265	268	268	267	268	273	275	277	279	279	271
TOP	°F	236	237	238	237	238	237	237	237	236	236	238	241	241	238
FEED FLOW	GPM	31.1	32.8	31.9	32.7	34.0	33.2	35.6	34.1	31.7	35.0	34.8	37.6	38.2	34.3
VDC REACTOR SYSTEM															
FLOWS TCE FEED	GPM	22.2	22.1	21.9	22.2	23.3	22.2	24.1	22.9	21.0	24.6	24.4	28.3	30.6	24.0
C.L. FEED	GPM	72.7	77.3	78.1	79.4	84.5	80.9	87.3	84.4	79.2	95.6	95.7	101.5	109.2	87.8
BOTTOM COLUMN PRESS.	PSIG.	22.2	21.3	20.6	21.1	22.3	24.3	24.3	23.5	22.6	23.7	22.7	22.7	21.4	22.5
TEMP. BOTTOM	°F	224	228	227	226	226	226	226	228	229	226	225	224	224	226
VAPOR	°F	130	129	128	128	131	132	133	133	131	131	133	134	133	131
MC REACTOR SYSTEM															
FLOWS VDC FEED	GPM	23.0	18.7	18.2	18.2	19.7	15.9	16.9	17.7	18.0	17.9	20.0	20.2	23.3	18.7
HCL FEED	SCFM	613	587	630	587	617	557	563	602	620	623	732	683	843	637
TEMP. VDC VAP. BOTTOM	°F	134	128	133	131	134	134	136	137	135	135	138	145	149	136
BOTTOM	°F	94	95	91	92	93	94	101	101	99	96	98	88	80	94
TOP	°F	89	89	87	85	86	87	89	88	89	87	91	87	83	87
FLASHER SYSTEM															
TEMP.	°F	178	179	181	188	191	191	185	184	182	184	185	188	187	185
Dopp Kettle Temp.	°F	173	171	170	174	172	173	179	174	174	175	175	189	192	176
STRIPPER SYSTEM															
FEED FLOW	GPM	25.8	26.9	27.6	27.8	28.8	24.7	24.6	25.6	26.8	31.8	34.1	32.8	41.2	29.4
TEMP. BOTTOM	°F	229	230	230	229	229	227	228	229	228	229	229	228	232	229
TOP PRESS.	PSIG	20.9	22.0	21.6	21.3	20.9	20.6	21.0	20.9	20.1	20.4	20.6	20.2	22.1	21.0
TOPPING STILL SYSTEM															
TOP TEMP.	°F	167	167	167	167	167	167	167	167	167	167	168	166	172	167
MC PRODUCT															
FLOW	GPM	18.9	17.2	17.7	17.5	18.6	15.9	16.0	18.0	19.2	19.8	22.0	18.3	22.5	18.6

SL 013406

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

PERCHLORETHYLENE — TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
Records Per Prod.	T/D	213.3	246.4	233.8	234.7	180.6	224.2	203.1	197.2	188.2	202.8	179.7	195.4	247.6	211.1
Shipments	T/D	208.9	190.9	285.8	263.9	264.1	244.2	172.8	228.8	153.6	259.6	98.9	246.4	196.5	217.1
Inventory	Tons	4732.3	7421.2	6016.2	5112.1	2610.3	1992.0	2896.4	1916.0	2985.9	1282.6	3791.8	2259.4	3841.7	3510.5
Rec rds Tri Prod.	T/D	264.6	313.6	260.8	270.1	228.3	298.7	250.7	260.2	217.8	281.7	180.2	239.8	245.9	254.0
Shipments	T/D	265.7	162.4	254.9	425.1	262.3	274.9	237.8	232.6	233.0	274.0	209.5	193.8	237.4	249.8
Inventory	Tons	3525.2	7190.3	7353.9	2545.5	1524.8	2263.1	2649.2	3506.6	3035.6	3268.4	2359.8	3741.1	4005.8	3620.3
Area Per Prod.	T/D	215.4	250.9	235.9	247.2	175.3	234.9	196.7	213.0	175.9	211.2	183.2	221.6	242.9	215.7
EDC	T/T														
Cl_2	T/T	0.070	0.093	0.071	0.086	0.116	0.082	0.107	0.084	0.078	0.067	0.085	0.036	0.046	0.079
NH_3	Lbs./T	6.4	8.2	7.2	3.3	9.5	9.0	8.9	8.2	8.2	7.6	7.4	9.2	6.9	7.8
Area Tri Prod.	T/D	265.9	316.3	261.4	265.4	239.6	301.9	258.4	253.5	239.4	255.4	209.1	248.4	249.1	258.2
EDC	T/T														
Cl_2	T/T	0.044	0.058	0.045	0.054	0.073	0.052	0.068	0.053	0.049	0.042	0.054	0.022	0.029	0.050
NH_3	Lbs./T	6.4	8.3	7.3	3.3	9.6	9.3	8.6	8.4	8.7	7.4	7.6	8.9	7.0	7.9
Total Area Prod. O_2	T/T	0.160	0.149	0.163	0.155	0.165	0.169	0.197	0.167	0.190	0.161	0.184	0.150	0.184	0.170
N_2	T/T	0.086	0.072	0.091	0.098	0.115	0.072	0.109	0.119	0.144	0.112	0.149	0.122	0.115	0.110
Catalyst	Lbs./T	2.87	2.09	3.04	1.73	3.76	1.63	4.21	3.11	3.10	4.02	7.21	5.09	5.21	3.68
400 # Stm.(actual)	Lbs./T	4859	4548	4883	4561	5204	4374	5231	5286	5874	5041	5694	4819	4605	5010
KWH/T		56.3	62.0	68.8	69.0	85.4	64.3	82.5	81.5	99.8	83.5	94.9	74.3	83.9	79.2
Total Stillbottoms	T/T	0.272	0.251	0.305	0.239	0.392	0.243	0.353	0.383	0.365	0.265	0.340	0.267	0.256	0.305
MAN HRS./T RECORDS PROD.															
Production		0.186	0.171	0.196	0.212	0.278	0.192	0.239	0.218	0.285	0.242	0.306	0.246	0.233	0.235
Maintenance		0.318	0.208	0.292	0.313	0.468	0.293	0.384	0.353	0.496	0.500	0.655	0.440	0.452	0.404
Salaried		0.060	0.052	0.060	0.056	0.074	0.055	0.062	0.064	0.071	0.060	0.079	0.056	0.060	0.062
Total		0.564	0.431	0.548	0.581	0.820	0.540	0.685	0.635	0.852	0.802	1.040	0.742	0.745	0.701
Contract Man Hrs. Included		0.003	0.000	0.000	0.047	0.004	0.000	0.013	0.062	0.003	0.018	0.000	0.000	0.032	0.015
MAN HRS./T SHIPPED															
Bulk		0.028	0.044	0.029	0.025	0.022	0.032	0.032	0.036	0.041	0.027	0.045	0.036	0.035	0.034
Drum		0.699	0.863	0.862	0.748	0.729	0.760	0.660	0.749	0.920	0.757	0.725	0.857	0.977	0.801
Salaried		0.005	0.008	0.005	0.003	0.004	0.005	0.005	0.006	0.007	0.004	0.007	0.005	0.006	0.005
TCE T/T PER AREA PROD.		0.919	0.938	0.877	0.871	0.850	0.897	0.814	0.919	0.943	0.842	0.906	0.845	0.938	0.887
TCE T/T TRI AREA PROD.		1.165	1.185	1.107	1.099	1.073	1.133	1.028	1.160	1.190	1.063	1.144	1.067	1.185	1.120

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

PERCHLORETHYLENE — TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

YIELDS	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
Area Production Basis + Trans.									*					
Cl_2	88.1	88.5	87.5	84.7	83.4	86.2	84.8	84.8	82.1	86.4	83.7	93.3	90.3	86.3
C	88.7	91.2	89.5	88.9	86.6	89.4	85.8	85.6	83.0	85.5	83.1	90.2	86.3	87.1
Records Production Basis + Trans														
Cl_2	87.6	87.8	87.3	83.9	82.8	84.8	84.7	83.8	81.1	88.3	79.7	89.1	90.5	85.3
C	88.4	90.4	89.2	88.1	85.4	87.7	85.4	84.8	81.1	88.5	77.6	85.3	86.4	85.8

RECOVERED HCl TO 8002 & 8003

SL 013408

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

* Corrected Values

FORM 5A 210-3

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

PERCHLORETHYLENE-TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

MATERIAL BALANCE	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
CARBON - TONS														
TOTAL CARBON IN FEED	3444.8	4141.1	3347.2	3748.8	3374.0	3882.6	3660.8	3927.3	3503.0	3562.0	3251.4	3317.7	3752.2	3622.3
CARBON IN UNSTAB. PRODUCT	3059.9	3778.8	2996.4	3332.8	2921.3	3471.5	3140.4	3361.9	3046.7	3044.3	2702.6	2993.1	3238.0	3169.0
PROCESS LOSS BY DIFFERENCE	384.9	362.3	350.8	416.0	452.7	411.1	520.4	565.4	456.3	517.7	548.8	324.6	514.2	453.3
ACCOUNTABLE PROCESS LOSSES														
REACTOR	364.9	342.3	330.8	394.0	432.7	391.1	500.4	545.4	436.2	497.7	528.8	304.6	494.2	433.3
MISCELLANEOUS	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0
SUB TOTAL	384.9	362.3	350.8	416.0	452.7	411.1	520.4	565.4	456.3	517.7	548.8	324.6	514.2	453.3
CARBON LOADING LOSS	16.6	26.1	22.6	28.2	20.7	-2.9	19.0	22.9	82.0	-50.3	22.3	170.6	10.3	30.9
TOTAL CARBON LOSSES	401.5	388.5	373.4	444.2	473.4	408.2	539.4	588.3	538.3	467.4	571.1	495.2	524.5	484.2
CHLORINE - TONS														
TOTAL CHLORINE IN FEED	22489.8	27621.1	21643.0	24272.4	21390.6	25528.2	22717.2	24815.3	21636.9	22017.9	20635.2	21081.3	23861.5	23101.7
CHLORINE IN UNSTAB. PRODUCT	19786.5	24433.7	18947.8	20568.4	17844.6	22019.9	19274.7	21035.0	18227.4	19033.9	17269.0	19660.3	21547.9	19988.6
PROCESS LOSS BY DIFFERENCE	2703.3	3187.4	2695.2	3704.0	3546.0	3508.3	3442.5	3780.3	3409.5	2984.0	3366.2	1421.0	2313.6	3113.1
ACCOUNTABLE PROCESS LOSSES														
REACTOR	2603.4	3087.3	2595.2	3604.0	3446.0	3408.3	3342.5	3680.3	3309.5	2884.0	3266.2	1321.0	2213.6	3013.2
MISCELLANEOUS	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0
SUB TOTAL	2703.4	3187.4	2695.2	3704.0	3546.0	3508.3	3442.5	3780.3	3409.5	2984.0	3366.2	1421.0	2313.6	3113.2
CHLORINE LOADING LOSS	86.2	141.0	120.9	207.5	48.7	27.7	86.6	186.5	309.3	-259.2	135.8	921.5	26.2	162.7
TOTAL CHLORINE LOSS	2789.5	3328.3	2816.1	3911.5	3594.7	3536.0	3529.1	3966.8	3718.8	2724.8	3502.1	2342.5	2339.8	3275.8

SL 013409

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

FORM NO. 210. 4. CONFIDENTIAL: Subject to Protective Order of 14th Judicial District Court No. 91-1145

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

SL 013410

PERCHLORETHYLENE-TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

REACTOR NO. 1	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
ON STREAM TIME *HRS.	8272	744	646	714	616	730	682	736	740	641	674	672	606	8201
TEMP. °F VAPORIZER LIQUOR	336	380	377	390	351	386	359	385	372	370	377	363	384	374
DOWTHERM OUT	460	450	455	569	552	578	500	468	470	447	522	503	515	502
SEC. COND. DISCH	33	32	27	30	34	50	35	36	41	39	40	27	24	34
CATALYST CHARGED * LBS.	111537	4698	4292	2389	12512	5082	13892	13784	5472	20823	29305	10026	14118	136393
CATALYST FROM CENTRIFIX * LBS.	111537	4698	4292	2389	12512	5082	13892	13784	5472	20823	29305	10026	14118	136393
FLOW GPM Organic	18.0	21.9	20.9	20.4	19.3	22.8	20.6	21.7	20.3	19.1	19.3	17.6	17.1	20.1
SCFH Cl_2	1419	3100	3600	3300	3600	3100	3140	2780	1700	1700	1100	2500	1900	2626
O_2	13100	13800	16200	12600	11400	13200	12500	14090	13400	12000	14600	14600	13000	13449
PER.TRI RATIO	0.92	0.85	1.04	1.15	1.15	0.98	0.94	0.89	1.02	0.93	1.60	1.43	1.49	1.12
PER & TRI IN CRUDE %	85.83	83.69	77.23	88.67	82.29	80.65	76.60	82.10	82.60	82.00	84.40	84.30	87.20	82.64
REACTOR NO. 2														
ON STREAM TIME * HRS.	7963	680	650	684	698	710	662	742	524	570	690	569	676	7855
TEMP. °F VAPORIZER LIQUOR	356	376	394	381	369	384	362	379	364	360	374	375	376	374
DOWTHERM OUT	526	520	485	537	607	580	520	604	571	541	609	576	519	556
SEC. COND. DISCH.	38	33	32	37	35	51	42	41	48	43	35	29	28	38
CATALYST CHARGED * LBS.	136569	10648	6392	9914	12862	6132	18092	10284	7572	6123	13905	16676	11468	130068
CATALYST FROM CENTRIFIX * LBS.	136569	10648	6392	9914	12862	6132	18092	10284	7572	6123	13905	16676	11468	130068
FLOW GPM Organic	17.0	19.4	19.0	16.8	15.6	17.7	18.5	16.5	13.4	15.2	16.9	15.9	14.4	16.6
SCFH Cl_2	2501	4300	1800	3500	3600	3200	3571	2912	3000	2350	2000	2700	1900	2903
O_2	15900	17100	20900	15900	12500	15500	16400	16480	14900	15100	15500	17100	18400	16315
PER-TRI RATIO	0.90	1.69	1.27	1.06	1.21	0.95	0.94	0.70	0.81	0.90	1.26	0.88	1.52	1.10
PER & TRI IN CRUDE %	87.79	81.80	90.22	86.95	80.61	80.01	78.90	84.10	86.80	86.00	80.00	80.10	89.00	83.71

*Totals

FORM [redacted]SA 210. 5

CONFIDENTIAL: Subject to Protective Order of 14th Judicial District Court No. 91-1145

[redacted] PPG [redacted] DUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

SL 013411

PERCHLORETHYLENE - TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

REACTOR NO. 3	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
On Stream Time * Hrs.	8223	742	532	734	692	682	667	714	702	686	584	639	663	8037
Temp. °F Vaporizer Liquor	338	367	366	356	342	358	351	347	356	361	347	373	379	359
Downtherm Out	495	456	464	525	560	499	479	576	582	541	602	567	520	531
Sec. Cond. Disch.	31	25	24	28	29	49	32	34	31	32	30	23	27	30
Catalyst Charged Lbs. *	88216	6448	11992	7289	9362	5082	13892	6434	6872	11198	7255	10026	20218	116068
Catalyst from Centrifix Lbs. *	88216	6448	11992	7289	9362	5082	13892	6434	6872	11198	7255	10026	20218	116068
Flow GPM Organic	18.4	18.2	16.8	16.2	15.6	16.4	15.1	15.8	15.2	13.7	11.9	13.7	13.7	15.2
SCFH Cl_2	1944	3000	3500	3700	3300	3400	3700	2200	2180	2270	2900	800	800	2646
O_2	16400	16700	13500	16200	13900	16800	15000	16500	16400	16400	13000	19500	17500	16000
Per-Tri Ratio	0.94	0.87	1.03	1.48	1.16	1.05	1.17	0.90	1.02	1.30	1.02	1.00	0.96	1.08
Per & Tri in Crude %	85.89	85.25	81.78	91.49	86.19	85.38	77.40	87.6	86.2	86.9	85.4	86.0	86.4	85.5
REACTOR NO. 4														
On Stream Time *Hrs.	8325	726	616	744	692	734	690	672	715	720	655	634	670	8268
Temp. °F Vaporizer Liquor	352	354	362	361	328	358	338	348	350	362	349	362	370	354
Downtherm Out	490	451	475	585	588	508	536	517	541	521	603	562	485	531
Sec. Cond. Disch.	41	55	55	52	53	61	60	53	52	47	50	29	44	51
Catalyst Charged Lbs.*	77320	10298	10942	4489	7262	5082	5142	10284	10372	6648	14955	17726	12868	116068
Catalyst from Centrifix Lbs.*	77320	10298	10942	4489	7262	5082	5142	10284	10372	6648	14955	17726	12868	116068
Flow GPM Organic	18.0	19.5	18.7	18.6	15.7	19.4	18.4	16.6	16.8	17.0	14.3	15.4	18.4	17.4
SCFH Cl_2	1952	2900	3200	3000	3600	2600	2760	2700	2400	1260	2500	1400	600	2400
O_2	13700	16700	16400	16600	13600	18300	16100	14600	16800	16500	12600	13600	16700	15700
Per-Tri Ratio	1.01	1.00	1.15	1.22	1.26	1.44	1.41	1.05	1.02	1.13	0.86	1.18	1.14	1.16
Per & Tri in Crude %	88.37	86.10	87.81	91.56	89.88	90.95	87.00	89.0	86.9	87.7	85.0	87.8	89.3	88.19

*Totals

FC..... NO. ... 21...

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

PERCHLORETHYLENE - TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

REACTOR NO. 5	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
ON STREAM TIME * HRS.	8346	728	650	728	700	729	714	716	583	660	686	662	664	8220
TEMP. F VAPORIZER LIQUOR	350	320	320	324	294	302	298	320	326	379	368	370	380	333
DOWTHERM UT	520	462	469	509	624	607	506	490	521	500	523	495	500	517
SEC. COND. DISCH.	49	43	42	47	47	60	54	55	58	51	53	43	40	49
CATALYST CHARGED * LBS.	89333	4698	8842	3439	4812	5782	6542	4334	9672	11548	22306	17376	20918	120269
CATALYST FROM CENTRIFIX * LBS.	89333	4698	8842	3439	4812	5782	6542	4334	9672	11548	22306	17376	20918	120269
FL # GPM Organic	16.4	18.6	18.7	16.2	14.7	19.8	18.3	16.5	15.2	19.2	15.0	17.3	19.4	17.4
SCFH Cl_2	2785	3800	2700	3500	3700	3700	3720	2200	1700	2370	1600	300	-	2663
2	13700	15400	15800	13300	10600	13000	14300	13900	13600	16700	13300	13800	12500	13850
Per-Tri Ratio	0.92	0.89	1.11	1.43	1.32	0.91	1.30	0.80	1.32	1.21	1.32	1.09	0.98	1.14
Per + Tri in Crude %	90.11	89.48	88.47	91.73	86.92	85.16	82.90	83.9	86.3	84.5	85.2	80.5	81.2	85.5

SL 013412

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No. 91-1145

*Totals

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PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

SL 013413

PERCHLORETHYLENE - TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

REFRIGERATED BRINE	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
Temp. °F #1 Warm (in)														
#1 Cold (out)														
#2 Warm (in)	6	5	5	4	4	25	5	6	4	1	4	(1	(0	5
#2 Cold (out)	2	-4	-5	3	-6	21	-3	-3	-3	-4	-4	-6	-5	-2
PER STILL #1														
Feed GPM	7.6	7.9	8.4	9.0	7.5	8.6	8.5	7.1	7.2	8.0	9.8	7.8	8.9	8.2
Reflux GPM	13.7	13.3	14.3	14.1	13.7	14.0	14.1	14.2	14.7	10.5	11.2	15.0	14.6	13.6
Recycle GPM	0.21	(0.1	0.4	0.1	0.5	0.6	0.7	0.4	0.6	0.8	0.7	1.0	0.5	0.5
Pot Temp °F	287	288	289	290	285	285	285	288	293	291	284	283	280	287
Overhead Temp °F	257	258	262	264	246	248	246	247	251	243	242	238	245	249
PER STILL #2														
Feed GPM	16.2	19.3	18.0	19.6	14.6	17.3	18.0	18.2	17.7	20.3	20.1	19.6	22.0	18.7
Reflux GPM	24.8	22.7	23.5	19.6	18.6	16.5	17.9	17.9	18.4	18.7	17.8	18.6	17.4	19.0
Recycle GPM	1.5	1.8	2.9	3.8	3.0	3.9	4.5	3.9	4.3	5.6	5.2	5.1	4.7	4.1
Pot Temp °F	293	294	296	294	290	283	290	290	292	302	301	299	294	294
Overhead Temp °F	248	253	260	261	252	255	251	252	254	253	246	252	251	253
TRI STILL #1														
Feed GPM	14.8	17.5	17.0	14.8	13.6	16.5	15.5	17.0	16.8	51.5	14.6	15.6	15.1	15.8
Reflux GPM	66.0	63.7	62.6	54.3	53.2	52.2	56.8	55.0	61.4	58.6	54.3	56.2	57.5	58.0
Recycle GPM	2.76	3.4	4.4	3.1	3.1	4.2	3.9	4.6	4.4	3.2	2.8	2.8	2.6	3.5
Bottoms GPM	17.1	18.2	15.3	14.9	13.1	15.6	13.8	15.8	16.5	15.1	13.8	14.2	14.8	15.1
Pot Temp °F	234	233	233	229	230	229	232	230	231	229	228	227	228	229
Overhead Temp °F	160	158	160	170	166	172	169	172	173	166	162	162	163	166
TRI STILL #2														
Feed GPM	23.2	28.4	26.5	24.0	22.8	29.0	27.3	28.6	28.1	25.6	24.3	25.2	26.1	26.3
Reflux GPM	101.2	98.8	93.9	82.5	82.9	84.3	92.9	95.2	100.2	100.4	93.9	87.6	95.6	92.3
Recycle GPM	4.7	5.6	7.0	5.0	5.1	6.2	6.3	6.7	6.0	6.1	4.7	5.0	4.5	5.7
Bottoms GPM	18.2	23.0	18.7	18.6	18.6	23.6	21.0	21.2	22.4	20.1	20.6	19.5	20.6	20.7
Pot Temp °F	226	237	236	234	235	235	237	234	236	237	235	227	234	235
Overhead Temp °F	147	147	154	162	158	159	157	162	163	162	158	160	160	158
DH STILL #1														
Temp. °F Pot	181	179	180	184	182	185	181	187	185	185	184	177	182	183
Overhead	148	144	141	147	142	147	142	150	151	148	148	142	143	146
Pot Pressure PSIG	1.70	1.68	1.68	1.70	1.66	1.68	1.70	1.68	1.78	1.66	1.48	1.52	1.49	1.64

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PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

PERCHLORETHYLENE - TRICHLORETHYLENE DEPARTMENT OPERATIONS REPORT

-Continued	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
DH STILL #2														
Temp. °F Pot	202	201	203	207	202	195	198	202	199	202	200	208	207	202
Overhead	143	135	133	140	136	142	142	147	145	141	139	142	139	140
Pot Pressure PSIG	1.64	1.66	1.61	1.66	1.60	1.67	1.67	1.65	1.77	1.72	1.57	1.43	1.30	1.61
PER-TRI STILL														
Feed GPM	67.6	81.3	77.5	73.0	64.5	82.5	76.2	75.2	76.6	78.1	74.3	74.1	76.9	75.8
Reflux GPM	54.8	64.3	61.6	61.1	56.7	69.0	66.0	66.9	68.3	66.8	59.4	63.2	60.0	63.6
Pot Temp. °F	292	283	298	294	292	301	295	298	291	295	290	289	295	293
Overhead Temp. °F	190	189	187	189	189	196	193	194	193	192	192	193	197	192
HEAVIES STILL														
Feed GPM	29.4	33.5	32.5	36.5	31.4	35.3	34.0	30.8	30.7	34.9	34.4	32.1	34.7	33.4
Reflux GPM	309.2	362.7	360.6	330.8	265.5	288.5	342.3	318.9	326.1	299.4	305.6	303.5	319.1	318.6
Temp °F Top	261	265	265	264	252	255	259	258	256	254	256	261	260	259
Pot	323	333	328	318	301	306	321	315	303	306	307	316	313	314
NEUTRALIZATION & DRYING														
#1 PER														
NH_3 PSIG	3.7	4.0	3.9	4.0	3.7	4.8	5.0	3.7	2.7	2.4	2.4	2.9	4.0	3.6
Product to Stg. GPM	11.7	9.1	6.3	7.3	8.6	10.3	9.6	5.6	6.4	10.5	20.7	10.7	12.4	9.8
#2 PER														
NH_3 PSIG	5.9	6.1	6.2	6.9	7.4	5.8	4.9	5.1	5.5	3.2	3.9	3.1	3.7	5.2
Product to Stg. GPM	21.4	26.2	24.3	28.4	25.9	27.2	24.2	25.1	22.3	26.1	27.4	24.5	27.4	25.8
-TRI-														
NH_3 PSIG	3.37	2.9	2.6	1.9	1.9	2.55	3.10	3.16	2.33	1.85	2.20	2.3	2.3	2.4
Product to Stg. GPM	55.0	32.0	26.2	28.8	27.5	33.1	30.5	34.0	31.8	27.3	26.0	28.2	30.4	29.6

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No. 91-1145

SL 013414

FORM [redacted]45A 211-1

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

HYDROGEN CHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	AVG.
62A DRY HCL														
HCL SOLD T/D														
CHLORINE TO 62A T/D														
HYDROGEN TO 62A MCF/D														
CL_2 EFFICIENCY %														
EXCESS H_2 %														
TONS CL_2/TON HCL SOLD														
MCF H_2/TON HCL SOLD														
KWH/TON														
WELL WATER M GAL/TON														
H_2SO_4 LBS/TON														
MAN HOURS/TON HCL														
PRODUCTION														
MAINTENANCE														
SALARIED														
TOTAL														
CONTRACT MAINT. INCLUDED IN ABOVE														

SL 013415

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No. 91-1145

Form 95A 21-2

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

SL 013416

HYDROGEN CHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
PRESSURE														
Comp. Disch. PSIG														
Comp. Suction "H_2O														
TEMPERATURE °F														
No. 1 Burner														
Gas from Primary														
Gas from Secondary														
No. 2 Burner														
Gas from Primary														
Gas from Secondary														
No. 5 Burner														
Gas from Primary														
Gas from Secondary														
No. 5 Comp. Disch. °F														
Cell Liquor #/Ton HCl														
Well Water to HCl GPM														
OPERATING TIME *														
No. 1 Burner														
No. 2 Burner														
No. 5 Burner														
COMPRESSORS #1 *	6741	59	345	632	338	684	146	475	707	488	358	595	594	5421
#2 *	7669	730	76	497	469	308	683	744	634	720	744	315	214	6134
#3 *	3180	664	345	333	452	438	578	231	0	232	352	305	588	4518
#4 *	7188	35	0	363	108	0	0	0	0	0	0	0	0	506
#5 *	2543	0	0	0	0	0	0	0	0	0	57	659	744	1460
#6 *	7826	35	0	0	0	0	370	15	0	0	121	0	0	541
#7 *	7895	709	626	689	628	744	356	654	597	696	579	487	744	7509
#8 *														
No. 1 Stripper *	7404	35	0	375	145	0	0	0	0	0	0	0	0	555
No. 2 Stripper *	6927	0	0	0	0	0	0	0	0	0	0	0	0	0

CONFIDENTIAL:
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*Totals

FORM NO. 6A 211-3

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

HYDROGEN CHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG.
62B - WET HCl														
Wet HCl Produced T/D	97.9	39.3	37.0	53.6	45.3	47.5	19.4	32.5	17.6	5.2	2.8	10.7	8.9	26.6
N_2 T/T	0.046	0.158	0.169	0.105	0.147	0.119	0.258	0.199	0.640	1.272	2.579	0.547	0.908	0.592
Steam (Actual) M lbs./T	2831	225	0	1293	592	0	0	0	0	0	0	476	0	646
Well Water M Gals/T	4.2	-	-	-	-	-	-	-	-	-	-	-	-	-
H_2SO_4 lbs./T	0.3	0.6	0.4	0.4	0.4	0.7	1.0	0.9	1.4	6.7	0.0	0.0	0.0	1.0
KWH/Ton	10.4	24.6	28.9	18.0	22.0	20.4	51.5	29.8	54.8	190.7	343.9	93.8	109.0	82.3
HCl (as Muriatic Acid)														
Captive Use T/D	46.2	36.5	51.7	46.3	54.3	47.2	41.2	37.3	28.6	38.9	34.7	38.7	30.6	40.5
Shipped T/D	1.2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
ACID Strong Wt. %	31.95	32.79	31.30	32.24	31.57	30.04	30.78	30.47	30.96	30.95	32.52	32.39	30.05	31.34
Weak Wt. %														

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SL 013417

FORM N)A 211-4

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

HYDROGEN CHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG
62B WET HCL														
REFRIGERATION UNIT														
PRESSURE PSIG														
SUCTION	-20.5	-18.6	-	21.2	-21.6	-	-	-	-	-	-23.0	-21.8	-22.0	-21.4
DISCHARGE	11.4	8.4	-	10.0	8.8	-	-	-	-	-	8.8	8.2	8.5	8.8
SEAL	30.1	30.0	-	30.0	30.0	-	-	-	-	-	29.9	30.5	30.3	30.1
TEMPERATURES °F														
BRINE IN	32	38	-	28	25	-	-	-	-	-	19	28	31	28
BRINE OUT	33	38	-	25	21	-	-	-	-	-	15	24	27	25
AMPS	158	144	-	153	143	-	-	-	-	-	146	144	145	146
NO. 1 STRIPPER														
FLOWS														
STRONG ACID FEED GPM	46.8	43.8	-	38.0	36.3	-	-	-	-	-	-	-	-	39.4
STEAM LBS/HR	8881	9131	-	6674	6469	-	-	-	-	-	-	-	-	7425
TEMPERATURES °F														
TOP	230	226	-	226	230	-	-	-	-	-	-	-	-	227
Gas from Cooler	44	40	-	42	38	-	-	-	-	-	-	-	-	40
NO. 2 STRIPPER														
FLOWS														
STRONG ACID FEED GPM	43.4	0												
STEAM LBS/HR	6793	0												
TEMPERATURES °F														
TOP	244	-												
Gas from Cooler	44	-												
MAN HOURS/TON HCL														
PRODUCTION	0.135	0.346	0.365	0.242	0.314	0.291	0.690	0.372	0.519	1.990	3.233	0.917	1.079	0.863
MAINTENANCE	0.090	0.016	0.069	0.289	0.038	0.066	0.022	0.191	0.190	1.272	0.756	0.219	0.406	0.294
SALARIED	0.034	0.087	0.092	0.060	0.078	0.072	0.165	0.105	0.193	0.610	1.266	0.285	0.384	0.283
TOTAL	0.259	0.449	0.526	0.591	0.430	0.429	0.877	0.668	0.902	3.872	5.255	1.421	1.869	1.440
CONTRACT MAINT. INCLUDED IN ABOVE	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000

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No. 91-1145

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FORM N

SL 013419

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
ETHYL CHLORIDE DEPARTMENT OPERATIONS REPORT

CONFIDENTIA
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

GENERAL DEPARTMENT	1973 AVG	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG
ETHYL CHLORIDE PRODUCTION T/D	168.2	175.4	89.7	148.4	141.2	172.3	183.8	165.7	139.1	160.0	152.3	140.7	183.5	154.3
EC AREA PRODUCTION T/D	168.6	175.7	80.6	148.3	142.0	172.7	184.5	167.1	144.8	154.7	152.1	140.9	183.6	153.9
EC SHIPMENTS T/D	169.3	139.7	136.4	123.8	153.0	176.4	158.7	152.4	171.0	157.5	174.0	120.5	170.3	152.8
HCL TO EC T/D	105.2	110.9	50.9	92.5	87.8	112.5	114.2	104.7	84.9	93.8	98.2	91.8	114.6	96.4
ETHYLENE TO EC T/D	76.0	79.0	36.3	67.0	64.3	79.8	85.0	79.2	69.5	73.0	73.0	66.3	84.7	71.4
PURITY %	99.92	99.87	99.92	99.91	99.94	99.97	99.95	99.93	99.95	99.91	99.86	99.94	99.88	99.92
HCL EFFICIENCY %	91.0	89.8	90.1	90.9	91.8	87.4	91.8	90.0	96.8	93.6	88.0	87.4	91.1	90.7
CARBON EFFICIENCY %	96.8	97.0	97.0	96.5	96.2	94.6	94.7	91.3	90.9	92.4	91.0	92.8	94.6	94.1
EXCESS HCL T/D	6.5	8.3	3.7	5.4	4.1	8.7	3.6	1.7	-5.4	-1.1	3.4	5.6	4.4	3.5
EXCESS HCL %	6.6	8.1	12.0	6.2	4.9	8.4	3.3	1.6	-6.0	-1.2	3.6	6.4	4.0	4.3
HCL TO EC TONS/TON EC PROD	0.624	0.631	0.632	0.623	0.617	0.651	0.619	0.631	0.586	0.606	0.645	0.651	0.623	0.626
C_2H_4 TO EC TONS/TON EC	0.450	0.449	0.450	0.451	0.452	0.462	0.461	0.478	0.479	0.472	0.479	0.470	0.461	0.464
N_2 TO EC TONS/TON EC	0.040	0.052	0.157	0.058	0.055	0.042	0.039	0.046	0.073	0.067	0.069	0.064	0.045	0.064
$FrCl_3$ LBS/TON EC	8.4	9.5	8.8	7.7	9.9	7.9	9.3	9.8	10.2	9.6	11.1	9.8	7.2	9.2
STEAM LBS/TON EC	1102	1120	1182	1182	1139	1074	1052	1242	1116	1622	1703	1728	1567	1311
WELL WATER M GALS/TON EC	1.529	1.358	1.816	1.957	2.041	1.680	1.553	1.616	1.692	1.723	1.759	1.702	1.457	1.696
KWH/TON EC	93.0	79.2	95.3	95.9	90.6	70.1	72.6	81.2	88.1	87.0	95.5	89.2	90.3	86.2
MAN HOURS/TON EC														
PRODUCTION	0.212	0.238	0.508	0.266	0.300	0.244	0.226	0.188	0.199	0.195	0.180	0.196	0.146	0.240
MAINTENANCE	0.197	0.154	0.841	0.151	0.221	0.134	0.096	0.115	0.316	0.183	0.132	0.167	0.069	0.215
SALARIED	0.076	0.074	0.163	0.084	0.095	0.076	0.066	0.079	0.090	0.079	0.090	0.083	0.071	0.088
TOTAL	0.485	0.466	1.512	0.501	0.616	0.454	0.388	0.382	0.605	0.457	0.402	0.446	0.286	0.543
CONTRACT MAINT. INCLUDED IN ABOVE	0.035	0.000	0.000	0.000	0.007	0.000	0.000	0.000	0.000	0.020	0.000	0.000	0.000	0.002
an Hours/T EC Shipped														
Bulk	0.025	0.030	0.025	0.034	0.025	0.027	0.051	0.041	0.025	0.038	0.020	0.030	0.022	0.031
Salaried	0.002	0.003	0.002	0.003	0.002	0.002	0.004	0.004	0.003	0.004	0.002	0.002	0.002	0.003

FORM [redacted]5A 212-2

PPG I[redacted]USTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

ETHYL CHLORIDE DEPARTMENT OPERATIONS REPORT

MATERIAL BALANCE	1973 AVG	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG
CHLORINE — TONS														
TOTAL CHLORINE IN FEED	3112.0	3343.2	1386.6	2788.7	2560.3	3390.3	3331.5	3155.3	2560.2	2737.0	2961.2	2676.9	3453.1	2862.0
CHLORINE IN PRODUCTION + Tons.	2832.8	3003.6	1249.2	2535.9	2350.0	2964.9	3058.5	2839.4	2479.2	2563.3	2605.0	2340.4	3144.5	2594.5
CHLORINE LOSS IN PROCESS	279.2	339.6	137.4	252.8	210.3	425.4	273.0	315.9	81.0	173.7	356.2	336.5	308.6	267.5
BLOWDOWN FROM HEAVIES STILL	15.3	11.4	8.9	9.6	8.7	22.9	17.8	17.6	12.6	12.9	13.9	17.0	15.9	14.1
UNACCOUNTABLE PROCESS LOSS	263.9	328.2	128.6	243.2	201.6	402.5	255.2	298.3	68.4	160.8	342.3	139.5	292.7	253.4
CHLORINE LOADING LOSS	7.2	5.1	5.6	-0.6	13.4	7.2	10.7	-24.9	93.9	-73.5	-3.6	3.9	3.0	3.3
TOTAL CHLORINE LOSS	286.4	344.7	143.1	252.2	223.7	432.6	283.7	291.0	174.9	100.2	352.6	340.4	311.6	270.8
CARBON — TONS														
TOTAL CARBON IN FEED	1979.0	2095.8	870.7	1778.3	1653.0	2118.9	2184.9	2102.9	1844.3	1876.2	1937.4	1704.1	2249.1	1868.0
CARBON IN PRODUCTION + Tons.	1916.4	2032.9	844.6	1716.4	1590.6	2004.2	2068.7	1920.3	1677.3	1734.2	1762.2	1582.2	2127.2	1755.1
CARBON LOSS IN PROCESS	62.6	62.9	26.1	61.9	62.4	114.7	116.2	182.6	167.0	142.0	175.2	121.9	121.9	112.9
BLOWDOWN FROM HEAVIES STILL	7.1	5.3	4.1	4.4	4.0	10.6	8.2	8.1	5.8	6.0	6.4	7.8	7.3	6.5
UNACCOUNTABLE PROCESS LOSS	55.5	57.6	22.0	57.5	58.3	104.1	108.0	174.5	161.2	136.0	168.7	114.0	114.6	106.4
CARBON LOADING LOSS	4.9	3.5	3.8	-0.4	9.0	4.9	7.2	-16.8	63.6	-52.5	-2.5	2.6	2.0	2.0
TOTAL CARBON LOSS	67.5	66.4	29.9	61.5	71.4	119.6	123.4	165.8	230.6	89.5	172.7	124.6	123.9	114.9

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PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

ETHYL CHLORIDE DEPARTMENT OPERATIONS REPORT

REACTOR	1973 AVG	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 AVG
PRESSURE PSIG	125	128	106	106	101	116	119	122	112	113	113	96	103	111
TEMPERATURE °F	136	133	120	126	123	125	131	133	126	127	131	122	128	127
FLASHER														
TEMPERATURE °F														
BOTTOM	159	159	154	141	151	158	159	162	160	163	160	165	160	158
TOP	136	138	135	126	133	137	138	142	136	136	139	137	135	136
PRIMARY STRIPPER														
PRESSURE PSIG	86	86	83	74	81	85	87	90	84	84	87	85	83	84
TEMPERATURE °F														
TOP	109	112	116	103	106	114	113	115	111	113	107	108	108	111
BOTTOM	150	152	148	138	144	149	150	152	147	148	150	149	146	148
HEAVIES STILL														
FEED RATE GPM	43.5	43.1	36.2	42.6	48.0	43.0	43.1	42.6	43.8	38.8	38.2	37.0	42.2	41.6
REFLUX GPM	19.6	17.4	18.1	19.9	19.0	20.6	20.0	20.0	20.0	20.0	20.1	20.5	20.0	19.6
STEAM (ACTUAL) LBS/HR	3959	4186	3354	3859	3952	3818	4022	4793	3631	3504	3605	3552	4001	3856
TEMPERATURE °F														
TOP	146	147	146	147	149	148	146	145	146	145	144	146	146	146
BOTTOM	191	187	184	183	181	184	188	184	187	190	184	184	185	185
SECONDARY STRIPPER														
PRESSURE PSIG	73	74	73	71	74	73	74	73	73	74	73	72	73	73
TEMPERATURE °F														
TOP	153	154	153	152	149	152	153	152	154	154	153	150	150	152
BOTTOM	154	154	153	151	154	152	153	153	154	154	152	151	151	153

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
VINYL CHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
VC Records Production	T/D	416.5	266.9	135.4	335.8	371.0	496.9	568.2	437.0	446.4	438.0	409.2	343.8	417.0	388.8
VC Area Production	T/D	421.9	269.4	138.4	337.8	374.9	489.9	566.3	435.7	449.0	441.5	410.8	342.3	417,6	389.5
VC Shipments	T/D	427.6	173.2	283.7	216.4	418.2	559.2	469.6	423.4	470.6	332.0	480.2	313.5	574.4	392.9
YIELDS															
Area Prod. + Trans. Credits															
Basis	Cl_2	99.7	99.9	95.9	101.0	99.8	99.2	98.5	98.6	99.3	99.2	99.1	98.1	98.8	99.0
	C	99.3	99.9	95.2	100.6	99.3	98.7	98.1	98.1	98.9	98.8	98.7	97.7	98.5	98.5
Records Prod. + Trans. Credits															
Basis	Cl_2	98.9	99.5	94.9	100.6	99.3	98.5	98.7	98.4	99.1	98.8	98.9	98.3	98.7	98.6
	C	98.1	99.0	93.1	100.0	98.3	97.4	98.4	97.8	98.4	98.0	98.3	98.1	98.4	97.9
HCl By-Product Prod.	T/D	246.2	156.6	80.7	197.0	218.5	289.7	330.1	254.8	261.8	257.3	239.5	199.5	243.4	227.4
HCl By-Prod. Utilized	T/D	241.0	153.6	82.1	188.5	216.5	281.9	321.0	246.8	256.4	260.7	232.4	192.2	246.4	223.2
HCl By-Prod. Utilization	%	97.9	98.1	101.7	95.6	99.0	97.3	97.2	96.9	98.0	101.3	97.0	96.4	101.2	98.3
Heavies Still Bottoms Prod.	T/D	9.7	3.5	7.9	8.4	15.7	17.0	16.2	14.6	14.5	14.3	11.4	11.0	9.7	12.0
Dopp Kettle Waste	Lbs./T VC	6.87	9.13	11.8	7.3	4.0	8.7	5.1	7.6	5.3	6.2	7.2	6.1	6.6	7.1
EDC Consumption	T/D	682.9	429.9	237.6	539.0	611.6	811.8	928.0	718.2	731.3	720.0	668.9	564.7	679.9	636.7
EDC Consumption	T/T VC	1.62	1.60	1.72	1.60	1.63	1.63	1.64	1.64	1.63	1.63	1.63	1.65	1.63	1.64
Cl_2 Consumption	Lbs./T VC	6.34	6.93	6.37	4.38	5.88	3.73	5.46	5.35	5.73	6.45	8.06	2.87	2.61	5.32
Steam Consumption	Lbs./T	3664	4384	4594	3761	3867	3462	3154	3932	3886	3362	4099	3024	3812	3778
Gas Consumption	MCF/T	4.66	4.67	5.35	5.15	5.50	4.89	4.60	5.46	5.38	5.35	5.47	4.35	5.32	5.12
Well Water Used	M Gals./T	0.93	2.78	3.61	2.09	1.80	1.31	1.29	1.86	1.76	1.71	2.02	1.81	1.50	1.96
Nitrogen Used	Lbs./T	41.1	75.2	311.6	61.1	75.9	66.1	58.2	59.6	48.4	89.4	56.2	87.6	67.8	88.1
Power Consumption	KWH/T	71.2	108.4	31.1	74.8	70.5	69.2	67.4	80.5	72.5	70.5	77.0	58.4	73.0	71.1

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PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
VINYL CHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
MAN HOURS/TON VC PROD.														
Production	0.144	0.236	0.515	0.195	0.175	0.127	0.116	0.154	0.143	0.146	0.165	0.187	0.146	0.192
Maintenance	0.102	0.155	1.256	0.098	0.136	0.138	0.081	0.062	0.046	0.090	0.110	0.273	0.070	0.210
Salaried	0.039	0.063	0.124	0.048	0.047	0.034	0.028	0.039	0.038	0.036	0.043	0.044	0.041	0.049
Total	0.285	0.454	1.895	0.341	0.358	0.299	0.225	0.255	0.227	0.272	0.318	0.504	0.257	0.451
Contract Man Hours included	0.029	0.000	0.000	0.013	0.015	0.041	0.000	0.000	0.000	0.006	0.000	0.002	0.009	0.007
MAN HOURS/T VC SHIPPED														
Bulk	0.021	0.040	0.023	0.028	0.024	0.019	0.027	0.023	0.025	0.020	0.028	0.028	0.021	0.026
Salaried	0.002	0.004	0.002	0.002	0.002	0.002	0.002	0.002	0.003	0.002	0.002	0.002	0.002	0.002

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CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

VINYL CHLORIDE DEPARTMENT OPERATIONS REPORT

PROCESS CONDITIONS	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
VAPORIZING FURNACE														
EDC FEED TEMP. °F	329	326	322	308	316	307	287	324	322	313	315	315	314	314
FURNACE BRIDGEWALL TEMP. °F	1308	1232	1241	1244	1261	1253	1320	1289	1288	1306	1281	1369	1344	1286
Δ P AVG., PASSES #1 & #2 PSI	193	209	211	170	182	198	206	205	202	214	217	205	202	202
CRACKING FURNACE FEED TEMP. °F	401	450	450	376	386	398	404	392	396	401	398	388	392	403
CRACKING FURNACE #1														
FURNACE BRIDGE WALL TEMP. °F	1290	1357	1255	1258	1285	1266	1371	1340	1341	1281	1287	1284	1242	1297
Δ P AVG., PASSES #1, #2, #3 & #4 PSI	126	137	141	113	122	141	146	140	141	150	150	130	128	137
AVG PASS OUTLET TEMP., PASSES #1, #2, #3, & #4 °F	904	936	920	913	886	870	926	912	904	844	842	878	842	889
CRACKING FURNACE #2														
FURNACE BRIDGEWALL TEMP. °F	1229	–	–	1201	1225	1261	1308	1273	1263	1265	1272	1250	1210	1253
Δ P AVG. PASSES #1, #2, #3 & #4 PSI	125	–	–	112	119	134	143	142	134	135	140	123	120	130
AVG. PASS OUTLET TEMP. PASSES #1, #2, #3 & #4 °F	877	–	–	873	870	893	922	908	908	882	876	874	837	884
QUENCH TOWER														
TOP TEMP °F	275	269	267	275	272	274	278	285	281	281	278	275	274	276
TOP PRESS. PSIG	91	84	86	88	91	97	102	98	95	96	93	91	89	93

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No. 91-1145

FORM NO. A 213-4

PPG INDUSTRIES

CHEMICAL DIVISION

LAKE CHARLES, LOUISIANA

VINYL CHLORIDE DEPARTMENT OPERATIONS REPORT

PROCESS CONDITIONS	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
ABSORBER COLUMN														
SEC. QUENCH COND. GAS														
FEED TEMP. °F	159	142	145	166	151	140	148	168	181	178	183	159	160	160
BOTTOM LIQ. TEMP. °F	123	127	128	110	119	123	127	136	136	137	138	124	126	128
TRAY #7 TEMP. °F	66	55	65	80	76	81	95	81	76	70	76	71	64	74
TRAY #12 TEMP. °F	55	53	56	59	57	61	65	58	59	57	56	56	55	58
TRAY #35 TEMP. °F	19	39	40	27	24	19	23	19	20	18	18	20	24	24
LIQ. FROM UPPER INTERCOOLER														
TEMP. °F	45	52	53	44	49	49	42	43	45	44	41	44	44	46
LIQ FROM LOWER INTERCOOLER														
TEMP. °F	(0	-1	-1	(0	(1	0	0	(0	(0	-1	(0	2	2	(0
LEAN OIL TO ABSORBER TEMP. °F	-26	-26	-26	-25	-25	-25	-22	-26	-22	-24	-24	-26	-27	-25
LEAN OIL FLOW AVG. GPM	166	150	150	162	173	184	195	173	180	180	180	175	163	172
ABSORBER TOP PRESSURE PSIG	78	77	77	79	79	79	80	75	80	80	80	80	80	79
STRIPPER COLUMN														
QUENCH LIQ. FEED TEMP. °F	133	118	119	125	126	133	142	151	139	139	136	123	123	131
BOTTOM LIQ. TEMP. °F	218	225	220	209	210	211	208	219	219	219	221	215	217	216
STRIPPER TOP TEMP. °F	125	133	132	125	123	122	123	129	129	129	131	119	122	126
BOTTOM PRESS PSIG	94	86	90	93	94	97	100	95	96	97	94	96	94	94
PRODUCT STILL COLUMN														
LIQUID FEED TEMP. °F	222	229	224	214	216	218	215	227	232	229	226	223	224	223
BOTTOM LIQ TEMP. °F	326	319	321	319	318	323	324	321	322	322	320	321	319	321
TRAY #19 TEMP. °F	240	247	248	229	239	244	243	244	241	241	241	240	242	242
TOP TEMP. °F	109	106	107	102	106	109	110	109	111	111	109	109	106	108
STILL TOP PRESSURE PSIG	85	81	84	77	81	87	88	86	88	88	86	86	82	85

SL 013425

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No 91-1145

FORM NO. A 213-5

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

VINYL CHLORIDE DEPARTMENT OPERATIONS REPORT

PROCESS CONDITIONS	1973 Avg.	JAN	FEB	MAR	APR	MAY	JUNE	JULY	AUG	SEP	OCT	NOV	DEC	1974 Avg.
HEAVIES STILL COLUMN														
LIQ FEED TEMP. °F	174	177	175	157	173	176	178	179	190	207	212	143	149	176
BOTTOM LIQ. TEMP. °F	239	235	234	235	238	239	239	238	240	241	242	236	238	238
TOP TEMP. °F	201	196	196	199	199	201	199	201	202	201	200	201	200	200
TOP PRESSURE PSIG	1.28	2.41	2.26	1.80	1.05	1.01	1.63	.82	1.11	0.97	0.84	1.00	0.99	1.32
REFRIGERATION														
FIRST STAGE SUCTION TEMP. °F	-29	-28	-29	-33	-31	-33	-35	-36	-34	-33	-33	-33	-36	-33
SECOND STAGE SUCTION TEMP. °F	-4	-5	-5	-5	-5	-5	-7	-8	-7	-7	-6	-4	-6	-6
THIRD STAGE SUCTION TEMP. °F	34	34	42	33	42	57	55	63	40	50	45	39	40	45
FOURTH STAGE SUCTION PRESS. PSIG	57	46	47	54	60	63	64	62	62	61	63	57	56	58
COMPRESSOR #1 - AMPS @ 2400V	213	191	197	201	200	252	243	231	222	214	240	224	229	220
DISCHARGE PRESS PSIG	124	115	121	118	118	132	137	132	132	128	126	124	132	126
DISCHARGE TEMP. °F	183	184	190	182	188	191	190	200	190	195	186	180	188	189
COMPRESSOR #2 - AMPS @ 2400V	228	212	215	221	218	231	256	240	222	220	229	222	233	227
DISCHARGE PRESS PSIG	130	121	126	124	124	136	142	136	137	132	130	128	136	131
DISCHARGE TEMP. °F	180	186	183	176	182	191	189	196	186	193	189	186	190	187
PRODUCT STORAGE														
DAY TANKS - AVG. TEMP. °F	69	56	56	70	73	77	82	82	87	76	69	60	54	70
AVG. PRESS. PSIG	36	26	27	36	36	39	40	51	50	44	40	33	30	38
SPHERES - AVG. TEMP. °F	68	55	60	62	69	77	80	82	79	75	70	58	54	68
AVG. PRESS PSIG	44	36	40	42	45	50	56	56	53	52	53	41	38	47
MISCELLANEOUS														
HCl BY-PRODUCT TO DISTRIBUTION.														
TEMP. °F	-18	-21	-21	-21	-23	-24	-24	-24	-22	-23	-20	-19	-20	-22
COOLING TOWER WATER TO PLANT.														
TEMP. °F	87	85	87	85	84	88	89	90	91	88	85	83	84	87

SL 013426

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
OHC-EDC DEPARTMENT OPERATIONS REPORT

CONFIDENTIAL:
Subject to Protective Order
of 14th Judicial District Court
No. 91-1145

GENERAL DEPARTMENT		1973 Avg.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 Avg.
OHC-EDC Production	T/D	262.1	294.5	210.3	274.1	293.9	412.9	465.4	357.8	390.8	438.6	366.0	362.0	436.0	358.5
HCL to OHC-EDC	T/D	197.6	224.6	157.2	205.9	227.7	312.5	351.3	275.3	303.9	338.3	283.3	279.9	331.7	274.3
HCL Consumed	T/T EDC	0.754	0.762	0.747	0.751	0.756	0.756	0.754	0.769	0.777	0.771	0.774	0.773	0.760	0.763
Purchased C_2H_4 to OHC-EDC	T/D	75.6	85.4	61.6	80.7	87.7	120.3	142.4	104.4	117.8	127.1	107.0	104.0	125.3	105.3
% C_2H_4 Purity		99.92	99.87	99.92	99.91	99.94	99.97	99.95	99.93	99.95	99.91	99.86	99.94	99.88	99.92
YIELD	%														
Cl_2 Basis		97.8	96.6	98.6	98.1	98.2	97.4	97.6	95.7	94.7	95.5	95.2	95.3	96.9	96.6
C_2H_4 Basis		98.2	92.5	91.8	92.5	95.0	94.2	90.7	94.0	91.7	95.3	94.5	95.3	95.4	93.6
Excess C_2H_4	%	1.9	2.4	3.4	3.9	2.8	2.8	8.0	2.9	6.3	2.2	3.2	1.4	1.4	3.4
Excess C_2H_4	T/M	41.2	60.9	56.2	93.5	70.6	102.4	315.1	92.6	217.4	82.2	101.3	42.7	53.4	107.4
Excess C_2H_4	Lbs/T EDC	10.7	13.3	19.1	22.0	15.6	16.0	45.1	16.7	35.9	12.5	17.9	7.8	7.9	19.2
Oxygen to OHC-EDC	T/D	50.1	57.5	39.5	52.4	55.1	75.8	85.1	75.8	79.4	74.7	72.7	69.9	81.1	68.3
Oxygen to OHC-EDC	T/T EDC	0.191	0.195	0.187	0.191	0.183	0.183	0.182	0.211	0.203	0.170	0.198	0.193	0.186	0.190
Excess O_2	%	15.6	16.7	12.6	15.9	10.4	10.5	10.4	25.4	19.1	0.7	17.0	13.8	11.5	13.7
Excess O_2	T/M	205.4	255.3	124.0	222.8	155.3	223.4	241.6	476.4	395.5	15.2	327.3	254.4	258.8	245.8
Excess O_2	Lbs/T EDC	51.8	57.8	42.1	52.4	34.4	34.9	34.6	86.8	65.3	2.3	57.7	46.9	38.3	46.1
CRUDE EDC INVENTORY	TONS	228.4	240.6	531.8	407.4	679.3	361.9	457.5	571.3	410.7	420.5	400.9	474.7	240.3	433.1
For Per-Tri Feed	TONS	46.7	89.7	200.8	27.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	26.5
For EDC Still No. 2 Feed	TONS	183.7	150.9	331.0	40.3	381.9	52.3	62.4	24.4	13.8	54.9	54.9	36.8	0.0	100.3
For Tetra Feed	Tons	-	-	-	340.1	297.4	309.6	395.1	546.9	396.9	365.6	346.0	437.9	240.3	306.3
Transferred to Per-Tri	TONS					499.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	41.6
Transferred to EDC Still No. 2	TONS	82.7	0.0	0.0	588.4	2231.5	2463.3	4064.2	1788.6	4027.2	4888.8	3498.8	5403.7	4479.1	2786.1
Transferred to Tetra	TONS	7854.0	8863.9	5309.2	8327.8	5786.5	10632	9782.6	9100.3	8242.1	8180.6	7786.2	5329.5	9252.2	8049.5
MAN HOURS/TON EDC PRODUCED															
Production		0.177	0.199	0.334	0.205	0.199	0.144	0.108	0.152	0.134	0.114	0.144	0.152	0.121	0.167
Maintenance		0.250	0.105	0.404	0.207	0.236	0.135	0.135	0.261	0.216	0.160	0.266	0.240	0.248	0.218
Salaried		0.086	0.077	0.109	0.079	0.078	0.055	0.046	0.063	0.058	0.049	0.065	0.056	0.052	0.065
Total		0.513	0.381	0.847	0.491	0.513	0.334	0.289	0.476	0.408	0.323	0.475	0.448	0.421	0.450
Contract Man Hours Included		0.001	0.000	0.000	0.000	0.022	0.000	0.000	0.043	0.010	0.000	0.000	0.000	0.020	0.008

SL 013427

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

SL 013428

OXYHYDROCHLORINATION OPERATIONS

OHC-EDC REACTOR #1		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
On-Stream Time *	Hrs.	5249	688	522	384	532	696	676	296	404	682	704	668	288	6540
Top Pressure	psig	23	25	20	24	21	22	21	21	20	16	13	16	15	20
Dowtherm Temp.(From)	°F	346	348	367	342	-	-	-	348	366	480	398	388	397	382
(Into)	°F	313	303	335	314	-	-	-	314	337	351	372	362	374	340
Reactor Temp.															
Catalyst Bottom	°F	596	589	586	590	617	624	580	563	591	577	583	586	580	589
Middle	°F	539	543	529	539	534	535	526	546	538	542	534	541	539	537
Top	°F	521	526	513	514	504	510	514	516	511	-	519	525	521	516
Vapor Space	°F	520	526	513	512	505	511	518	528	515	525	521	526	523	519
Refrig. Cond. Outlet	°F	55	43	43	48	-	-	-	63	61	41	56	44	60	51
FEEDS C_2H_4	schf	47384	48400	41500	47100	43100	41900	40600	38200	34800	33700	29600	31700	31400	38500
O_2	schf	27546	29200	24700	28700	25200	25300	24700	27600	23800	23300	20400	23500	22700	24900
HCl	schf	97390	101700	88600	100600	85700	88600	89000	95800	86100	83700	70400	78700	76100	87100
RECYCLE ANALYSIS(Vol. %)															
CO_2	%	28.6	32.8	30.9	31.5	27.2	27.7	32.6	35.2	32.8	30.3	43.3	38.5	40.7	33.6
C_2H_4	%	54.2	51.2	51.7	51.4	48.0	47.5	50.0	39.1	40.0	50.5	38.7	47.1	48.2	47.0
O_2	%	2.7	1.8	2.0	2.0	1.6	1.6	2.0	2.9	2.7	3.0	2.8	2.7	3.1	2.4
Catalyst Charged	Lbs.	10725	11669	0	17522	106	15839	15891	4268	7493	6348	22110	18910	3260	7714
REACTOR #2															
On-Stream Time *	Hrs.	5269	736	512	708	72	0	676	604	648	608	464	536	690	6254
Top Pressure	psig	23	24	19	19	14	-	21	20	12	16	15	13	18	17
Dowtherm Temp.(From)	°F	352	356	364	377	-	-	-	326	383	379	381	396	375	371
(Into)	°F	315	316	117	346	-	-	-	302	356	350	352	366	339	340
Reactor Temp.							-								
Catalyst Bottom	°F	580	571	596	576	596	-	580	593	598	580	594	589	586	587
Middle	°F	529	534	525	521	520	-	526	522	529	533	532	532	545	529
Top	°F	518	527	509	508	505	-	514	507	511	510	518	520	533	518
Vapor Space	°F	520	528	513	513	509	-	518	511	512	513	520	522	535	518
Refrig. Cond. Outlet	°F	55	43	45	45	-	-	-	65	62	43	52	45	49	50
FEEDS C_2H_4	schf	47249	46500	41700	38400	32300	-	40600	38600	31100	34700	34900	33800	40200	37500
O_2	schf	25808	26400	23100	22300	19400	-	24700	23600	18300	21000	20300	20100	25000	22200
HCl	schf	99500	97700	87200	84000	72800	-	89000	86900	65300	79000	72500	70700	82500	80700
RECYCLE ANALYSIS(Vol. %)							-								
CO_2	%	29.5	31.9	28.8	35.7	35.7	-	32.6	39.8	41.0	43.3	40.9	40.4	43.5	37.6
C_2H_4	%	54.5	53.5	53.3	52.7	52.7	-	50.0	42.4	43.7	43.3	46.9	46.0	38.4	47.5
O_2	%	2.8	2.3	2.2	3.2	3.1	-	2.0	2.0	2.4	3.1	2.8	2.7	2.3	2.6
Catalyst Charged	Lbs.	10907	12641	0	32308	14	-	15891	8537	7493	5660	4950	8680	5580	9250

Totals*

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
OXYHYDROCHLORINATION OPERATIONS

CHC-EDC REACTOR #3		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
On-Stream Time *	Hrs.					584	744	632	600	690	720	608	480	712	5870
Top Pressure	psig					17.8	25.1	20.1	19.1	20.8	15.8	16.7	21.3	20.4	19.7
Dowtherm Temp. (From)	°F					-	-	-	383	389	395	412	385	381	391
(Into)	°F					-	-	-	364	369	374	395	363	361	371
Reactor Temp.															
Catalyst Bottom	°F					525	520	539	542	532	530	534	530	537	532
Middle	°F					519	512	527	527	529	512	527	527	532	524
Top	°F					509	513	498	487	508	506	520	522	520	509
Vapor Space	°F					503	502	491	480	502	500	515	518	512	503
Refrig. Cond. Outlet	°F					-	-	-	62	61	42	60	46	46	53
FEEDS C_2H_4	schf					71500	92500	82200	81000	83400	73300	76100	89900	88100	82000
O_2	schf					41700	56300	52000	49900	50800	43100	43400	48400	50100	48400
HCl	schf					153300	195500	167900	165300	170200	142900	155300	165400	188000	167100
RECYCLE ANALYSIS (Vol. %)															
CO_2	%					37.2	39.9	51.4	47.6	44.6	48.2	48.4	50.2	57.2	47.2
C_2H_4	%					35.2	31.7	39.3	35.7	35.6	38.8	35.3	32.0	28.9	34.7
O_2	%					2.0	2.0	2.7	3.0	1.3	3.0	2.8	2.7	2.4	2.4
Catalyst Charged	Lbs.					118	16931	14818	8537	14985	6702	22560	30530	31620	15978

Totals#

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

OXYHYDROCHLORINATION OPERATIONS

OHC-EDC PLANT DATA	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
Refrigerated Brine Temp.														
Warm °F	51	40	39	42	-	-	-	59	58	37	53	42	46	46
Cold °F	50	39	38	38	-	-	-	58	57	34	53	40	45	45
Chloral Treatment Feeds														
Organic (gpm	30.5	30.2	21.8	32.3	31.2	48.5	55.1	35.6	40.1	48.0	47.3	46.9	52.0	40.8
Cell Liquor (gpm	3.6	-	3.48	4.41	4.97	5.38	5.18	4.96	5.15	5.18	5.9	6.0	6.0	5.2
Drying Still No. 1														
Temp. Bottom °F	183	184	183	185	-	-	-	102	178	187	185	184	182	174
Vapor Outlet °F	163	165	165	-	-	-	-	97	160	170	165	162	158	155
Press. Bottom psig	2.0	2.2	2.0	2.5	-	-	2.0	2.6	2.5	3.4	2.9	1.1	1.8	2.3
Lights Still Feed (gpm	10.6	9.7	11.3	11.4	13.5	16.4	21.5	12.2	19.5	29.4	20.2	29.5	29.9	18.7
Reflux (gpm	24.7	26.2	26.5	26.6	25.5	24.5	25.0	18.6	18.1	18.9	21.3	22.8	22.9	23.1
Temp. Bottom °F	201	206	206	204	-	-	-	204	208	209	205	207	212	207
Overhead °F	164	169	168	167	-	-	-	178	180	184	182	183	185	177
30# Steam Produced Lbs.	1164	1901	1048	1493	0	0	2895	1078	1239	2230	1667	2607	1427	1465
Electric Power (KWH/T EDC)	108.2	93.3	119.0	114.3	108.9	85.0	79.5	100.6	85.5	82.2	95.3	81.8	73.1	86.8
Well Water (M Gal/T EDC)	0.544	0.142	0.305	0.235	0.243	0.070	0.021	0.054	0.090	0.060	0.070	0.046	0.066	0.117
Natural Gas (MCF/T EDC)	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
Nitrogen (T/T EDC)	0.108	0.092	0.143	0.122	0.106	0.062	0.071	0.104	0.102	0.080	0.107	0.106	0.086	0.098
Catalyst (Lb./T EDC)	2.03	2.61	-	6.22	-	2.56	3.11	1.94	2.47	1.42	4.41	5.35	2.99	3.31
Drying Still No. 2														
Temp. Bottom °F				-	-	-	-	-	190	188	183	189	189	188
Vapor Outlet °F				-	-	-	-	-	173	166	168	170	169	169
Press. Bottom PSIG				1.3	2.4	2.9	2.8	2.3	3.07	3.1	1.9	1.8	1.7	2.3

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

VINYLIDENE CHLORIDE DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT		1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
No. of Batches															
Highest Reactor Temp. Avg.	°F														
Avg. Time of Reaction															
Reactor Feed	GPM														
Still Pressure	PSIG	16.9	16.3	15.8	15.9	20.7	19.6	20.0	21.3	16.1	17.5	16.4	16.8	18.4	17.9
Still Top Temp.	°F	111	97	94	98	104	114	122	117	134	120	120	109	105	111
Reboiler Steam Flow	#/Hr.	704	560	470	480	640	900	1100	970	730	1000	836	995	822	792
Reboiler Temp.	°F	136	132	131	130	140	137	141	138	138	136	134	129	127	134
Bottoms to VDC	Roto. %	40	36	25	29	32	36	33	29	32	28	22	26	27	30
MAN HOURS/TON															
Production		0.747	0.681	0.725	0.587	0.502	0.480	0.327	0.809	1.154	0.316	0.650	0.320	0.434	0.582
Maintenance		0.200	0.102	0.000	0.041	0.951	0.105	0.008	0.008	1.144	0.202	0.132	0.129	0.010	0.236
Supervision															
Total															
Contract Man Hours/T inc.		0.000													
Production	Tons/Day	18.2	22.1	19.3	22.1	23.5	25.5	39.4	15.7	11.5	42.6	21.7	38.6	30.2	26.0
Shipped	Tons/Day	18.0	20.0	23.7	20.3	30.4	26.7	30.7	24.5	7.1	40.2	27.1	26.6	33.2	25.9
MPN	#/Ton VDCM						1.1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.1
HCHME	#/Ton VDCM	2.2	2.9	6.8	-2.7	1.1	1.3	1.8	-0.2	3.2	1.1	1.6	0.9	0.6	1.5

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PPG INDUSTRIES
CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA

WASTE RECOVERY DEPARTMENT OPERATIONS REPORT

GENERAL DEPARTMENT	1973 AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1974 AVG.
Total Received from: T/D														
EDC	-	5.5	5.1	9.5	5.8	5.6	3.4	3.3	3.0	7.2	5.3	4.7	7.0	5.4
TCE	-	0.0	0.0	0.0	0.0	0.0	0.0	4.0	0.0	0.0	0.0	1.1	0.0	0.4
EC	-	0.5	0.5	0.5	0.4	1.1	0.9	0.8	0.6	0.6	0.7	0.8	0.8	0.7
VC	-	3.5	7.9	8.4	15.7	17.0	16.3	14.6	14.5	14.3	11.5	11.1	9.7	12.0
P/T	-	142.7	152.0	122.6	163.0	130.7	160.7	179.1	151.9	124.1	133.6	125.9	126.2	142.7
CONOCO	-	23.4	22.1	20.5	25.2	21.0	22.1	21.5	24.0	24.6	18.0	18.2	16.5	21.4
Puerto Rican Tank	-	0.0	2.8	52.4	14.8	10.9	0.0	11.9	6.1	25.4	35.0	49.3	6.9	18.0
TOTAL	-	175.6	190.4	213.9	224.9	186.3	203.4	251.6	211.2	224.1	227.9	211.1	195.6	209.7
Transferred to P/T T/D	-	137.0	202.5	190.3	193.1	156.9	174.6	218.2	128.3	179.4	176.7	180.8	147.9	173.8
LOSS Tons	-	322.2	659.0	731.5	805.0	997.7	701.8	695.1	1732.4	618.2	791.2	816.2	590.3	788.4
POT TEMPERATURES °F														
No. 1 Kettle	-	329	319	325	323	326	325	330	307	294	287	268	288	310
No. 2 Kettle	-	324	322	320	312	328	313	321	280	-	267	231	206	293
OVERHEAD TEMPERATURES °F														
No. 1 Kettle	-	305	297	297	291	300	294	301	279	277	270	269	271	288
No. 2 Kettle	-	308	302	298	292	296	296	304	290	299	296	295	293	297
YEILDS Cl	88.0	94.6	86.5	89.1	87.9	82.0	88.4	90.5	84.4*	89.6	87.6	87.0	88.1	88.0
C	86.9	91.6	93.6	88.4	88.7	86.1	88.9	90.1	81.9	89.0	87.1	87.4	91.0	88.7

* Corrected Values

PPG INDUSTRIES

CHEMICAL DIVISION
LAKE CHARLES, LOUISIANA
INCINERATOR OPERATIONS REPORT

GENERAL DEPARTMENT	AVG.	JAN.	FEB.	MAR.	APR.	MAY	JUNE	JULY	AUG.	SEP.	OCT.	NOV.	DEC.	1971 AVG.
VENT FLOWS MCF/Day														
No. 1 EDC			41.5	45.9	31.7	129.3	170.1	25.9	15.4	0.0	0.0	0.0	4.2	42.2
No. 2 EDC			196.2	178.2	172.2	175.7	197.0	153.3	241.0	167.0	236.7	212.2	221.8	195.6
P/T			1191.4	1455.0	1418.5	1256.8	1496.3	1257.3	1335.5	1336.5	1178.4	1058.4	1260.1	1294.9
OHC			188.5	191.0	241.6	321.0	395.1	288.5	416.8	451.2	307.8	279.2	357.1	312.5
LIQUID FLOWS Cl LBS./Day														
EDC			-	-	-	-	-	-	-	-	-	-	-	-
Waste Recovery			-	-	64689	53356	84064	68607	79738	91144	66673	75324	97751	75705
MC			-	-	-	-	-	-	-	-	-	-	-	-
EC			-	-	-	-	-	-	-	-	-	-	-	-
VC			-	-	-	-	-	-	-	-	-	-	-	-
NO. 1 INCINERATOR														
Waste Gas MCF/Day			194.2	922.0	0.0	772.9	18.0	75.2	0.0	0.0	0.0	584.9	1160.8	338.9
Natural Gas MCF/Day			235.1	213.0	266.9	266.0	317.0	229.8	323.0	223.0	247.1	224.7	184.1	248.2
Lake Water GPM			702.9	685.4	574.9	646.8	433.1	453.0	481.2	402.8	501.4	423.6	377.1	516.6
Temperature °F			2045	2199	2500	2461	2457	2508	2470	2576	2507	2490	2468	2426
Operating Hours*											736	653	673	-
HCl in Aqueous Sol. Tons				1083	594	1058	695	1050	1184	1365	1041	1162	801	1003
NO. 2 INCINERATOR														
Waste Gas MCF/Day			1832.9	2090.7	2149.0	1308.4	2407.7	1985.6	2316.7	23194	1886.3	1160.0	960.4	1856.1
Natural Gas MCF/Day			178.8	225.4	189.2	131.6	192.3	229.9	225.9	221.0	229.0	215.6	315.6	214.0
Lake Water GPM			669.7	695.3	601.6	543.0	516.8	411.9	511.8	525.7	700.1	453.5	395.1	547.7
Temperature °F			2469	2431	2518	2388	2500	2465	2490	2549	2509	2427	2458	2473
Operating Hours*										-	734	570	744	-
HCl in Aqueous Sol. Tons			2186	1763	2240	1270	1827	1296	1545	1750	1654	1080	704	1574

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*Totals