

TABLE 3. DRYING TIME AND CONDITIONS FOR REPRESENTATIVE MATERIALS^a—Con.

MATERIAL	TEMPERATURE DEG F	PER CENT RELATIVE HUMIDITY	DRYING TIME
Tanin and other chemicals (spray dried).....	250-300		Instantaneous
Terra Cotta (air drying in conditioned room).....	150-200		12-96 Hrs
Tobacco leaves.....	85-130		12 Hrs
Tobacco stems.....	180-200		12 Hrs
Varnish refrigerator boxes.....	110	35	5-7 Hrs
Varnish steering wheels.....	110-140	25-35	Overnight
Veneer ¼ in. 3-ply.....	120-130	35-40	6-8 Hrs + 2 Hrs acclima- tion
1½ in. 5-ply.....	120-130	35-40	16-18 Hrs + 4 Hrs acclima- tion
1¼ in. 5-ply.....	120-130	35-40	20-24 Hrs + 4 Hrs acclima- tion
Vitreous Enamel sheets before firing.....	170		
Wallboard pasted plywood.....	300		15-20 Min
Wallboard fiber insulating, roller type drier.....	300-385		2½-3 Hrs
Wallboard fiber insulating, truck type drier.....	300-385		24-48 Hrs
Walnuts.....	100		24 Hrs
Wheat, corn, oats, rice, barley.....	180		
Wire cloth Japan.....	200		20 Min
Wool.....	105		

^aSee references at end of chapter.

the common constituents of fuel are shown in Table 4. The heating values of oils are shown in Fig. 7. The sensible heat in Btu contained in the products of combustion of an average fuel oil and various gases is given in Fig. 8. The problem of securing complete combustion in a heater is important, in order to secure efficiency and the absence of soot formation, but unlike the ordinary power or heating boiler, excess air need not be maintained at a minimum in most cases. Excess air is generally admitted either in the heater or before the products go into the drier.

DESIGN

In all drying problems, data regarding temperatures, time, and humidity must be obtained by experiment or previous experience. Experiments are best performed at the temperatures, humidities, and velocities to be actually used in the full sized drier, and with full size samples.

The following nomenclature and explanation of terms will be used in the discussion of drying calculations:

- H = humidity of air, pounds of water vapor per pound of dry air.
 G = pounds of dry air supplied to the drier per unit of time.
 S = pounds of stock dried per unit of time in a continuous drier.
 S' = pounds of stock charged per batch to a discontinuous drier.
 Θ = time.
 Q = total heat supplied to the drier.

t = air temperature.

t' = stock temperature.

t'' = average stock temperature over short time interval, in a batch drier.

t_w = wet-bulb temperature.

s' = specific heat of the stock.

B = total radiation and conduction losses per unit time.

w = pounds of water per pound of dry stock.

r = heat of evaporation of water.

s = humid heat of air, i.e., heat necessary to raise 1 lb of dry air + H lb of steam 1 F.

Subscript (1) designates conditions at the point where the material in question (air or stock) enters and (2) where it leaves the drier.

Air driers may be divided into two classes, those in which *all moisture* evaporated from the stock *leaves the drier as vapor* in the effluent air, and those in which *part or all* of the moisture *is condensed* from the air *in the drying equipment itself*. In any continuously operating drier of the first type the relation between moisture content of the stock and quantity of air required for the drying operation is given by the equation:

$$G(H_2 - H_1) = S(w_1 - w_2) \quad (2)$$

TABLE 4. GAS COMBUSTION CONSTANTS^a

Gas	CHEMICAL FORMULA	MOLECULAR WEIGHT	CU FT PER LB	HEAT OF COMBUSTION		LBS PER LB OF COMBUSTIBLE					
				Btu per Lb		Required for Combustion			Flue Products		
				Gross	Net	O ₂	N ₂	Air	CO ₂	H ₂ O	N ₂
Carbon	C	12.000		14,140	14,140	2.667	8.873	11.540	3.667		8.873
Hydrogen	H ₂	2.015	187.723	61,100	51,643	7.939	26.414	34.353		8.939	26.414
Oxygen	O ₂	32.000	11.819								
Nitrogen	N ₂	28.016	13.443								
Carbon Monoxide	CO	28.000	13.506	4,369	4,369	0.571	1.900	2.471	1.571		1.900
Carbon Dioxide	CO ₂	44.000	8.548								
Methane	CH ₄	16.031	23.565	23,912	21,533	3.992	13.282	17.274	2.745	2.248	13.282
Ethane	C ₂ H ₆	30.046	12.455	22,215	20,312	3.728	12.404	16.132	2.929	1.799	12.404
Propane	C ₃ H ₈	44.062	8.365	21,564	19,834	3.631	12.081	15.712	2.996	1.635	12.081
Sulphur Dioxide	SO ₂	64.060	5.770								
Water Vapor	H ₂ O	18.015	21.017								
Air		28.900	13.063								

^aAll gas volumes corrected to 60 F and 30 in. mercury barometric pressure dry.