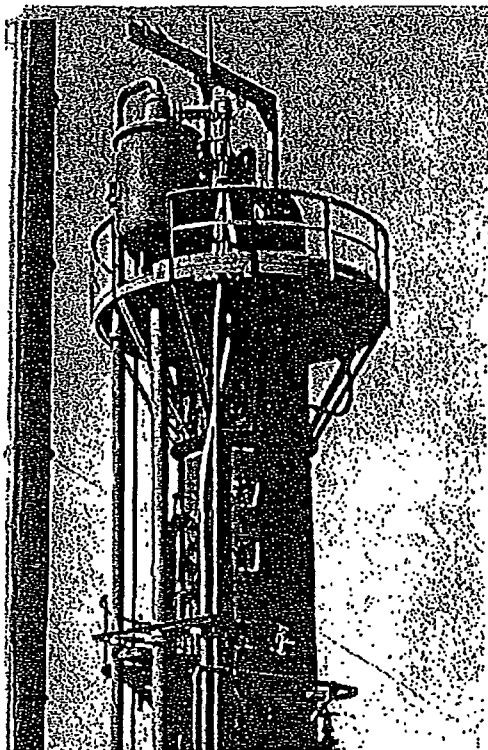




is injected into the system, together with fresh water to wash out the residual brine and soluble salts, and from there through another series of exchangers and into a heater or furnace. The hot oils, from the heater, flow into a fractionating tower operating at substantially atmospheric pressure, which is designed to separate the straight-run gasoline, kerosene, and gas oil fractions. The gas oil, or reduced crude, from the bottom of the atmospheric tower is then reheated and introduced into the second-stage tower, which is operated under a vacuum for the production of gas oil for charge to the catalytic cracking unit, and asphalt. The vacuum tower is equipped with an Elliott three-stage steam jet ejector maintaining 15 Hg absolute pressure when handling 2000 lb per hr of 250 F gas, consisting of 1000 lb per hr steam, plus 400 lb per hr condensable hydrocarbon vapor, plus 600 lb per hr of air or equivalent noncondensable gases.

Fluid Catalytic Cracking Unit:

The fluid catalytic cracking process has the ability to produce greater yields of gasoline of a high-octane rating than the thermal cracking process. In the fluid process, finely divided catalyst is suspended in gas, or vapor, or air, so



The Elliott multi-stage, turbine-driven centrifugal blower which was installed in connection with the fluid catalytic unit. It is rated 30,000 cfm, compressing air to a discharge pressure of 26 psig. It is operated 24 hours a day at 4750 rpm by the Elliott direct-connected 3140-hp steam turbine.

