

1. Well water is the most desirable since its temperature is high even in the winter and thus a large amount of heat may be removed in relation to the weight of water handled.

2. Air may be used but its specific heat is low and its temperature uncertain. When the most heat is needed, the temperature of the air is lowest, thus resulting in the least favorable temperature combination.

3. It has been proposed to obtain heat by freezing water, but this is still in the theoretical stage.

Some of the other factors which act as limitations are the large temperature spread when using air as a source of heat and when attempting to cool with even moderately low outside temperatures, the frequent disparity between the size of the cooling load and heating load requiring extra equipment for a complete heating load, and the relatively high initial cost of equipment at present available for the reverse cycle in comparison with that available for heating by conventional means.

Because of these limitations, the present application of the system is largely limited to temperate climates, such as Florida and Southern California, or to heating only for intermediate seasons, or to other localities which have peculiar advantages as, for instance, the ready availability of well water. In these locations it is frequently possible to do all of the heating necessary with the refrigeration equipment so that the extra cost is only that of reversing the functions of the condenser and evaporator.

ICE SYSTEMS

Ice may be used for chilling water for air conditioning work, but its application is limited because of the cost of ice and the difficulty of handling it. While not impossible, the direct cooling of air by ice is rather impractical. The most general method of cooling water with ice is to spray the water over the surface of the ice, insuring as much contact as possible, and approximating the same performance as the Baudelot type of cooler. This cold water is then circulated through cooling coils in the air by means of a pump.

PROBLEMS IN PRACTICE

1 ● Electrically driven dichlorodifluoromethane condensing units are to be used in an air conditioning system, requiring 20 tons refrigerating capacity for conditions of maximum load. An overall analysis of the seasons operating conditions shows an average load factor of 62.5 per cent, and allowing for variable time intervals of operation of refrigeration units installed, three-quarters of the operating season, or 750 hr, would require operation of the equipment at one-half load, and one-quarter of the operating season or 250 hr full load capacity of the refrigeration equipment would be required.

The increased first cost of 2-10 hp, 10 ton condensing units over 1-20 hp, 20 ton condensing unit is, \$830.00 installed price, to the customer.

The increased first cost of a 2-speed compressor motor of 20 hp size over a constant speed 20 hp size motor including increased starter cost is \$210.00. The efficiency of the 2-speed motor above is 83 per cent at full load speed, and 79 per cent for full load at $\frac{1}{2}$ speed. At $\frac{1}{2}$ speed, full load is $\frac{1}{2}$ total bhp of full load speed.

Discuss the considerations involved in making a decision as to whether a single unit with a 20 hp motor of the 2 speed type would be used in preference to 2-10 hp constant speed units.

The cost of 2-10 hp 10 ton units in excess of 1-20 hp, 20 ton unit with 2-speed motor, is \$830.00-\$210.00 or \$620.00, increased first cost. At 15 per cent fixed charges, this represents an increased annual cost of \$93.00 for 2 compressors over one compressor. The advantage of 2 compressors instead of one compressor on an installation of this type, is in the breakdown service provided in the event one compressor is shut down for repairs the system could be operated at one-half capacity utilizing the duplicate machine. The motor efficiency of the constant speed unit would be higher at full load than would be the efficiency of the 2-speed motor at low speed. Offsetting this latter advantage however, is the fact that the condenser on the condensing unit would provide a lower refrigerant condensing temperature for $\frac{1}{2}$ load operation with the same final condensing water temperature than would be the case with duplicate units each furnished with its own compressor and condenser. Operation at a lower condensing temperature would provide for a power saving compensating for the lower efficiency of the 2-speed motor when operated at slow speeds. It is, in a case of this kind, purely a question as to whether or not the purchaser would deem an investment of \$620.00 more and an increased fixed charge of \$93.00 a year, advisable to get breakdown service through the installation of duplicate units. In most cases, this increased first cost would not be warranted because of the fact that satisfactory indoor conditions could not be obtained at full load if only one-half the refrigeration capacity were available.

2 ● For condensing purposes, an air conditioning system uses city water which has an average 70 F supply temperature. The following table lists the number of hours per year during which definite wet-bulb temperatures and corresponding refrigeration rates pertain.

Wet-Bulb Temperature F	No. of Hours per Year	Refrigeration Required Tons
80	6	284
79 - 75	100	233
74 - 70	277	183
69 - 65	330	157
64 - 60	277	144
59 - 55	158	79
54 - 50	52	37
Total 1200 hours		

If the power requirements of a dichlorodifluoromethane refrigeration system are in accordance with the following data on partial load operation, determine the seasonal power cost at 2 cents per kw-hr:

Tons of Refrigeration Kw per ton	284	233	183	157	144	79	37
	0.89	0.89	0.87	0.86	0.86	0.93	0.97

Seasonal power cost:

WET-BULB TEMPERATURE F	TON-HOURS	KWHR
80	6 × 284 = 1,704	1,704 × 0.89 = 1,517
79 - 75	100 × 233 = 23,300	23,300 × 0.89 = 20,750
74 - 70	277 × 183 = 50,700	50,700 × 0.87 = 44,100
69 - 65	330 × 157 = 51,800	51,800 × 0.86 = 44,500
64 - 60	277 × 144 = 39,900	39,900 × 0.86 = 34,300
59 - 55	158 × 79 = 12,500	12,500 × 0.93 = 11,600
54 - 50	52 × 37 = 1,920	1,920 × 0.97 = 1,860
Totals	181,824 ton-hours	158,627 kw-hr

The 158,627 kw-hr at 2 cents per kw-hr will cost \$3,173.

The average consumption will be $\frac{158,627 \text{ kw-hr}}{181,824 \text{ ton-hours}} = 0.873 \text{ kw per ton}$.