

ADDENDUM TO THE OPERATING MANUAL

FLUID CATALYTIC CRACKING UNIT

PLANT 3B

TEXACO INC.

PUGET SOUND PLANT

ESTIMATE 3910

BECHTEL INCORPORATED

HOUSTON, TEXAS

1973

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1. GENERAL
DESCRIPTION

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I - GENERAL DESCRIPTION

A. INTRODUCTION

This addendum to the Operating Manual for the Fluid Catalytic Cracking Unit at the Puget Sound Works of TEXACO Inc., Anacortes, Washington, covers the revamp of the FCC Unit. The principal new equipment for this revamp is:

Reactor Charge Heater

Emergency Box Cooler

Fresh Feed Pumps

B. BASIS OF DESIGN

General

The process design of the FCCU section is based on feeding 30,000 BPSD of hot fresh feed to the charge drum and feed preheat exchangers. Some 6,000 BPSD of hot intermediate recycle gas oil are combined with the fresh feed for a total heater charge of 36,000 BPSD. The heater is designed for 750°F outlet temperature. The emergency box cooler is designed for 36,000 BPSD and 200°F outlet temperature. Process flow conditions for the preheat section are shown on process flow diagram 3-RA-40.

C. DESCRIPTION OF ADDITIONS AND MODIFICATIONS TO THE UNIT

This section describes only additions and significant modifications to the FCC Unit. Reference should be made to the Operating Manual for the FCC Unit for a description of the existing facilities.

Reactor Feed Heat Section (Reference PFD 3-RA-40)

Hot gas oil from the Crude Unit and Deasphalting Unit and/or cool feed from storage are charged through the existing light gas oil-reactor feed exchanger, 3B-E4, and the existing slurry quench-reactor feed exchanger, 3B-E5 A&B. This stream is combined with the hot recycle gas oil and the combined stream is heated in the new reactor charge heater, 3B-F3. The preheated combined stream flows to the reactor feed riser.

A new emergency box cooler is provided. Activation of the pushbutton, or low pressure drop across the spent or regenerated catalyst slide valve, will cause the valve in the line to the feed riser to close, the valve in the

oil line to the emergency box cooler, 3B-E40, to open, and the valve in the service water to the emergency box cooler, 3B-E40, to open. Hot reactor feed will be diverted from the feed riser, through the emergency box cooler, 3B-E40, and the cooled reactor feed flows either to the hot charge drum, 3B-C23, via 3LIC-62VB, or to storage via line 3B-0-1.

2. CONTROL FEATURES

2 - CONTROL FEATURES

A. PRINCIPAL CONTROL FEATURES

This section describes only additions and significant modifications to the FCC Unit controls. Reference should be made to the Operating Manual for the FCC Unit for a description of existing controls.

Reactor Feed Heat Section (Reference P&ID 3-RA-41)

The fresh feed flow controller, 3FRC-30, and the recycle feed flow controllers, 3FRC-11 and 3FRC-302, are left in place. Since a flow controller, 3FIC-600, is provided for the combined fresh feed and recycle streams, the flow controller for the fresh feed stream, or one of the recycle feed streams, must be taken out of service and the related control valve or bypass valve placed in the full open position. The fresh feed flow controller, 3FRC-30, is, preferably, taken out of service as there is no danger of "starving" the combined fresh feed and recycle feed flow controller, 3FIC-600, with the fresh feed flow controller out of service.

Total feed to the feed riser is controlled upstream of the reactor charge heater, 3B-F3, by a master controller, 3FIC-600. The master controller, 3FIC-600, makes equal distribution of the charge to the six coils of the reactor charge heater, 3B-F3, by setting uniform rates on the individual coil flow controllers, 3FFIC-620, 3FFIC-621, 3FFIC-601, 3FFIC-602, 3FFIC-603, and 3FFIC-604. Each heater coil is provided with a low flow switch, 3FSL-620, 3FSL-621, 3FSL-601, 3FSL-602, 3FSL-603, and 3FSL-604. Low flow through any heater coil will actuate common low flow alarm 3FAL-624. A further sustained reduction in flow through any heater coil will cause the fuel supply to the heater to shut off. A momentary reduction in flow through a heater coil will not cause the fuel supply to the heater to shut off, due to the action of time delay relay 3FY-622. Bypass switches 3FHS-620, 3FHS-621, 3FHS-601, 3FHS-602, 3FHS-603, and 3FHS-604 are provided to inhibit the heater fuel shutoff function of each low flow switch. A selector switch, 3FHS-623, allows the flow through any one heater coil to be recorded, 3FR-623.

The combined oil outlet temperature from the reactor charge heater, 3B-F3, is on temperature control, 3TIC-302, by adjustment of the amount of fuel oil or fuel gas to the burners. A selector switch, 3HS-606, provides a convenient means of firing fuel oil or fuel gas, or both. In this latter case, one fuel control valve, 3PV-641 or 3FV-606, is remotely positioned by a hand controller, 3HIC-606, to set a constant firing rate, while the other fuel control valve is automatically positioned by the temperature controller, 3TIC-302, to trim the firing operation as required.

In the event of a power failure, the reactor charge heater outlet temperature transmitter, 3TT-302, will be powered by batteries. If the batteries should fail or weaken, the output signal from the temperature transmitter, 3TT-302, will be low and high heater firing could result. A low temperature switch, 3TSL-302, is provided to prevent this occurrence. If the output signal from the temperature transmitter, 3TT-302, is low, the low temperature switch, 3TSL-302, causes the output signal from the temperature controller, 3TIC-302, to be replaced by the output signal from the hand controller, 3HIC-302. With proper setting of the hand controller, 3HIC-302, high heater firing is avoided.

Emergency Box Cooler

Low pressure drop across the spent catalyst slide valve, PdCL-14A, or low pressure drop across the regenerator catalyst slide valve, PdCL-14B, or activation of the pushbutton will (1) close the riser inlet valve, 3PdCL-14VN, (2) close the recycle gas oil valve, 3FRC-11, (3) close the slurry recycle valve 3FRC-302, (4) open the emergency box cooler process inlet valve, 3PdCV-14VB, (5) open the emergency box cooler water inlet valve, 3PdCL-14VM, (6) open the fresh feed pump discharge bypass valve, 3PdCL-14VH, to the blow-down drum, (7) close the spent catalyst slide valves, 3PdCL-14VF and 3PdCL-14VG, (8) close the regenerated catalyst slide valves, 3PdCL-14VC and 3PdCL-14VD, (9) open emergency steam valve, 3PdCL-14VE, and (10) close slurry quench reactor feed exchangers temperature control valve 3PdCL-14VK.

A light cycle oil line is provided that ties in just downstream of the emergency box cooler process inlet line block valve, 3PdCV-14VB, to permit flushing of the emergency box cooler, 3B-E40, when not in use. Flow of light cycle oil through this line is limited by a restricting orifice, 3FO-608.

3. PREPARATION FOR
OPERATION

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3 - PREPARATIONS FOR OPERATIONS

A. INTRODUCTION

This section describes only those preparations for operations that are necessitated by the addition of the reactor charge heater, 3B-F3. Reference should be made to the Operating Manual for the FCCU for a general description of preparations for operations.

B. DRYING THE REACTOR CHARGE HEATER

The masonry in all heaters, firebrick, or refractory linings, must be dried by slow heating. Damage from cracking and expansion strains will occur if damp settings are heated too rapidly. The vendor's recommended drying procedure should be followed. An alternate procedure is given below:

1. Check that the fuel gas system has been purged, and that it is blinded or otherwise secured against leakage of gas into the heater. Remove blinds in the gas supply header just prior to lighting burners. If natural gas is available, it should be used to dry out the heater.

If fuel gas is not available, fuel oil will be fired to dry out the heater. The fuel oil system must be thoroughly cleaned and charged with fuel oil. The fuel oil circulation should be established. Fuel oil temperature should be approximately 280°F.

2. Break flanges at the oil coil outlets, venting them to atmosphere, or otherwise provide means for venting steam from the coils to the atmosphere.
3. Blowdown condensate drains on atomizing steam lines, snuffing steam lines, and coil steam lines.
4. Purge the heater firebox with steam for at least 15 minutes, to eliminate all combustible gas from the firebox. The damper and air registers should be wide open. A steam plume should be readily noticeable from the top of the stack.
5. Light an alternate pattern of burners. During the drying period, rapid changes in temperature or highly localized temperature must be avoided. The lowest possible burner

flame and maximum number of burners should be used for better heat distribution, while obtaining the desired temperature. The burners should be alternated at hourly intervals, for uniform heat distribution, and the performance of all burners should be verified.

The purpose of the dryout is to eliminate water from the furnace masonry. It follows that maximum ventilation should be provided. The stack dampers should be fully open. All registers of unfired burners should be fully open.

6. During the drying period, the heater arch temperature is used as the point of regulation. Raise the heater temperature at 50 to 75°F per hour to 500°F. Maintain at 500°F for 24 hours. Increase the temperature at 50 to 75°F per hour to 750°F. Maintain at 750°F for 24 hours. Increase the temperature at 50 to 75°F per hour to 1000°F.

At near 500°F, steam should be carefully introduced into the coils. Steam should not be introduced into the coils, particularly in vertically installed coils, until temperatures have progressed above the steam condensation temperature. Introduction of steam into cold coils will cause considerable "water hammer".

The most accurate indication of readiness of a furnace for operation is the shell temperature. When the fires are started in a new furnace, the moisture of the outer surface of the refractory evaporates into the combustion gases, but much of the moisture held deeper in the refractory is driven back into the insulation next to the shell. During this period, the furnace shell remains cold. Then, as heat density in the combustion chamber is increased, the lining heats through and the moisture from the insulation begins to evaporate. This causes the furnace shell to heat up by the generation of steam on the adjacent insulation. When this moisture has been thoroughly evaporated, however, the shell temperature will again fall. If the operator keeps some progressive account of the shell temperature, he will note this rise and fall during the drying out process, and when the shell temperature has decreased to the rated casing temperature, the furnace can be considered ready for operation.

The 1000°F temperature may be maintained for a few hours, and then gradually reduced at not more than 75°F per hour. When the heater has cooled to about 350°F, the steam to the coils may be discontinued. The burners may be extinguished at about 300°F, and further cooling continued by natural draft.

7. Upon completion of drying, the heater coils should be drained, blown out, and flanged up. Everything is left in readiness for process operation.
8. After cooling of the heater, the masonry and internals should be inspected, and repairs made if indicated.

4. STARTUP
PROCEDURE

4 - STARTUP PROCEDURE

A. INTRODUCTION

The procedure given here is for initial startup of the reactor charge heater, 3B-F3, and commissioning of the emergency cooler, 3B-E40, with the existing FCCU in operation. Feed to the FCCU is flowing through the reactor charge heater bypass line. Reference should be made to the Operating Manual for the FCCU for a description of the startup procedure for the existing FCCU.

It is assumed the reactor charge heater, 3B-F3, and the emergency cooler, 3B-E40, have been made ready for operation as described in the preceding Section III. It is assumed that all utilities are available and ready for service.

The reactor charge heater, 3B-F3, and the emergency cooler, 3B-E40, are steam-purged, tightness-tested, and pressured with fuel gas. Reactor charge heater burners are lit on low fire. Oil is gradually diverted from the reactor charge heater bypass line through the reactor charge heater to the reactor riser. When all the oil is flowing through the heater, the feed rate and operating conditions should be adjusted to desired operating levels.

B. STEAM PURGE AND TIGHTNESS-TEST

Introduce steam through the steamout connection at line 3B-0-204-10" and through the steamout connections at each reactor charge heater pass. Purge through the reactor charge heater, 3B-F3, and the emergency cooler, 3B-E40. Vent steam and air at all high point vents. Drain condensate at all low point drains. When the system has been thoroughly purged, close vents and drains and tightness-test the system by gradually increasing the pressure to 100 psig with steam.

C. PRESSURE WITH FUEL GAS

After a successful tightness test, reduce the steam pressure to about 15 psig. Make a temporary connection and pressure the system to about 25 psig with fuel gas while all steam to the system is discontinued. Drain steam condensate from all low point drains. Make sure that all steam condensate is drained, as hot oil is to be introduced into the system.

D. INTRODUCE OIL

The emergency cooler, 3B-E40, is flushed with light cycle oil. The emergency dump system is not put into service at this time. Valving should be arranged such that if relief valve 3PSV-127A operates, it can discharge to storage.

Light a few burners in the reactor charge heater, 3B-F3, and bring the flue gas temperature at the arch to about 300°F. With the master heater flow controller, 3FIC-600, on manual control and the heater pass flow control valves closed, slowly open the block valve in line 3B-0-204-10" and admit oil to the heater inlet header. At this point, it should be recognized that hot oil is introduced into a wet system. The hot oil should be brought in slowly, and with caution. It must be remembered that a volume of water will expand to about 1600 volumes of steam when vaporized at 212°F and at atmospheric pressure. This vaporization takes place with violent force and, when in a closed place, is capable of causing physical damage to piping and equipment.

With the individual pass flow controllers on manual control, slowly admit oil through the heater passes, one pass at a time, to the block valve in the heater discharge header, 3B-0-213-10". Open the block valve in line, 3B-0-215-8", to the emergency cooler and permit the hot oil to flow through the emergency cooler, through the jump over from the emergency cooler discharge line to the emergency tankage (slops) header. After the system is free of water, close the block valve in line, 3B-0-215-8", to the emergency cooler and the block valve in the heater feed line, 3B-0-204-10". Open the block valve in the heater discharge line, 3B-0-219-6", and the block valve in the line to the emergency cooler and permit hot oil to back through the heater discharge line and the emergency cooler to the slops header. After the heater discharge line is free of water, close the block valve in the jump over line to the slops header and isolate the emergency cooler. Close the individual pass flow control valves.

With the individual pass flow controllers receiving their set point from master flow controller 3FIC-600, and with master flow controller 3FIC-600 on manual control, slowly start oil flow through the reactor charge heater, 3B-F3, while reducing flow through the reactor charge heater bypass. Light additional burners and adjust firing as required to maintain the oil temperature to the reactor riser. Commission the emergency dump system to the emergency cooler, 3B-E40.

When all of the oil is passing through the reactor charge heater, 3B-F3, and the heater bypass is closed, place the heater outlet temperature controller, 3TIC-302, and the heater master flow controller, 3FIC-600, on automatic control. Note that when the heater master flow controller is on automatic control, the fresh feed flow controller, 3FRC-30, or one of the recycle feed flow controllers, 3FRC-11 or 3FRC-302, must be taken out of service with the respective control valve or bypass valve in the open position. Adjust feed and recycle flow rates and operating conditions as directed by supervision.

5. OPERATING
VARIABLES

5 - OPERATING VARIABLES

A. INTRODUCTION

Reference should be made to the Operating Manual for the FCCU for a description of the operating variables. The following discussion is limited to the reactor charge heater, 3B-F3.

B. REACTOR CHARGE HEATER FIRING

Control the combined pass outlet temperature of the heater with temperature controller 3TIC-302. This controller resets the pressure controller regulating the fuel gas supply to the gas burners of the heater, or resets the flow controller regulating the fuel oil supply to the fuel oil burners of the heater. During reduced firing rates, it may be necessary to take burners out of service to maintain the design burner fuel gas pressure to avoid burner backfiring. Maintain the burner air and firebox pressure to obtain clear burner flame and the design excess air in the flue gasses. Burner firing must be even, so that there is no flame impingement on the tubes or furnace walls. Flame impingement will cause localized hot spots, and coking or tube failure can result. Visual inspection of the tubes for hot spots must be done routinely, several times per shift.

C. HEATER SOOTBLOWERS

Electrically-driven rotary sootblowers are provided in the convection section of the reactor charge heater, 3B-F3, for cleaning the extended surface tubes during oil firing operations. Steam is used as the blowing medium. The sootblowers should be operated every 8 hours, or on indication of higher stack gas temperature, when oil is being fired. The sootblowers can be operated automatic-sequential or manually. The sootblowers are conveniently operated from the Vulcan EC-15 automatic-sequential controller.

Automatic-Sequential Operation

1. Place the start-run-stop (S-R-S) selector switch in the stop position.
2. Place the 4 toggle switches in the up (auto) position.
3. Place the steam supply selector switch in the auto position. The steam supply valve, 3PV-658, will open. The adjustable time delay (15 minutes maximum) for warmup will run out before blower operation will begin. High pressure switch 3PSH-658, downstream of the steam supply valve, must be satisfied before the sootblowers will sequence.

4. Place the start-run-stop (S-R-S) selector switch in the start position and hold momentarily, then release. The blowers will then operate in sequence.
5. On completion of the sootblowing cycle, the unit will shut down. Place the steam supply switch in the close position. Open the circuit breaker to remove power supply to the controller.

Individual Manual Operation

The sootblowers can be operated individually in any sequence from the Vulcan EC-15 automatic-sequential controller or from the sootblower location.

1. Perform steps 1 through 3 of the automatic-sequential operation procedure, or place the steam supply selector switch in the open position.
2. Manual operation of a sootblower from the controller is accomplished by depressing the three-way toggle switch for the desired sootblower. Blowing will stop when the selected blower completes its cycle.
3. Manual operation of a sootblower at the sootblower location is accomplished by operation of the pushbutton in the sootblower housing.
4. After manual operation, return the steam supply selector switch to the off position.

Automatic-Sequential Controller

In addition to the control and switching functions described above, the Vulcan EC-15 automatic-sequential controller has the following features:

1. A light labeled "CO" to indicate that the controller is operating.
2. A light labeled "LV" to indicate that power has been lost.
3. A light labeled "RF" to indicate that a sootblower has failed to rotate.
4. A light labeled "LHP" to indicate that the steam header has not come up to pressure.
5. A light for each sootblower to indicate operation of that sootblower.
6. An ammeter to indicate the power consumption of the operating sootblower.

D. EMERGENCY COOLER

Valving in the piping to and from the emergency cooler is arranged such that oil can freely flow through the cooler to storage in the event emergency valve 3PdCV-14VB opens. During periods of cold weather, steam should be utilized to prevent freezing of water in the cooler.

6. SHUTDOWN
PROCEDURE

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6 - SHUTTING DOWN PROCEDURE

A. INTRODUCTION

Reference should be made to the Operating Manual for the FCCU for a description of shutting down procedures. The following discussion is limited to the reactor charge heater, 3B-F3, and the emergency cooler, 3B-E40.

During normal shutdowns, firing of the reactor charge heater is reduced as feed rate is reduced and then discontinued. The heater is steamed out in conjunction with the remainder of the FCCU. A procedure for heater decoking is given at the end of this section.

During an emergency shutdown, firing of the reactor charge heater, 3B-F3, may be stopped by operation of emergency shutdown switch 3HS-601. Oil feed may be diverted from the reactor riser to the emergency cooler, 3B-E40, by operation of the emergency pushbutton.

B. HEATER DECOKING

The FCCU need not necessarily be taken out of service for heater decoking. The FCCU can be returned to the operating mode that was used before the reactor charge heater was installed. The reactor charge heater can then be isolated, purged with steam and decoked as described in the following paragraphs. After heater decoking, the heater is returned to service by the procedures given in Section 4.

Means are provided for steam-air decoking the tubes in the 3B-F3 reactor charge heater.

The typical decoking manifolds are shown on P&ID 3-RA-41.

Internal coke deposition may be removed from heater tubes by steam-air decoking. This is accomplished in two consecutive operations. The spalling operation is removal of coke by cracking and fragmentizing the coke by external heating of the tubes, and blowing the loosened coke from the coils. The burning operation is removal of coke by controlled combustion, (i.e., burning,) of coke with air in the presence of steam, which carries the products of combustion from the coils. The decoking procedure is described in four steps:

Preparation

Coke Spalling

Coke Burning

Cleanup

Preparation

1. The tubes are steamed free of oil, in the normal manner, at shutdown.
2. The appropriate decoking manifold arrangement is connected to the coils.

4. Verify that all tube hangers and guides are present and in good condition; if not, repair or replace as required before proceeding with decoking operations.
5. Verify that plant air, steam, and service water are available to the manifold.

Spalling

1. Establish service water flows as quench water to the quench drum, 3B-C40.
2. The burners shall be lighted with nonluminous flames, if possible. It is advantageous to light the fires during the afternoon, so that the burning portion of the decoking operation can take place at night when red spots on the tubes can more easily be detected. Operate with a minimum amount of excess air, so as to reduce external tube oxidation.
3. Establish steam flow through the coils. Initially, a high flow rate should be maintained to flush oil that may still be deposited on the coke. The rate will be decreased during coke spalling to prevent erosion by coke particles.
4. Increase the bridgwall temperature at a rate of approximately 300°F per hour to 1100-1150°F, with a maximum temperature of 1300°F.
5. Increase steam flow through the coil being decoked to produce a mass velocity of 18 pounds/square foot/second.
6. If spalling has not started at the above temperature, the following steps will be taken until spalling does start:
 - a. Reverse the flow through the coil.
 - b. Alternately decrease and increase steam flow.
 - c. Lower flue gas temperature by 100-200°F.
 - d. Add a small amount of air, for not more than 5 minutes, then be sure to close off the air.
7. The rate of spalling is determined by observing the quenched effluent. Spalling rate is judged by appearance of quench water stream.
 - a. Light grey - containing soot or fine coke particles.
 - b. Dark grey to black - containing increased size and quantity of coke.

8. When heavy spalling starts, decrease steam flow to prevent erosion. The amount of steam flow rate is dependent on operator's judgment; the pressure in coil inlet and observation of the effluent is the guide. As effluent darkens, steam flow is decreased and inlet pressure observed. As effluent becomes lighter, steam flow is increased and the observed inlet pressure may be a guide for flow adjustment. High velocity may produce fine dust. This is determined by reducing steam flow for 10 to 15 minutes and observing the effluent. Should find dust continue, further reduce the steam flow to make sure the dust is not produced by high velocity.
9. Continue spalling operation until assured that spalling has stopped.

Burning

1. Reduce the radiant section flue gas outlet temperature about 50-100°F.
2. Reduce the steam flow to produce a rate of 5650 LB/HR.
3. Gradually introduce air to the coils at a quantity equal to one-tenth of the weight of the steam, i.e., 5650 LB/HR. Observe the appearance of the tubes. Do not permit the tubes' temperature to exceed 1250-1300°F., i.e., dark red color. Decrease air flow, if necessary, to avoid high temperature. With a good coke burning operation, the progress of the burn can be observed by tube color. As the burning coke in the tube progresses, the tube temperature, hence red color, also progresses.

Do not allow the tubes to attain a cherry red color. If the temperature rises, decrease the air flow.

4. After about one hour of burning, the flow is reversed. If coke burn is heavy, it is advisable to periodically increase the steam flow for short periods, to avoid plugging.
5. The effluent is observed throughout the burning operation. The appearance of the effluent during spalling and burning indicates the progress.
 - a. Greyish-milky is the appearance before and after decoking.
 - b. Light grey appearance indicates fine soot particles.
 - c. Dark grey to black indicates larger particle size and greater volume of coke.
 - d. A reddish-brown color appears during coke burning and blowing out period.

6. When coke burning is completed, the reddish-brown color disappears and decoking is completed.

Cleanup

1. Upon completion of coke burning, discontinue air flow.
2. Temporarily increase the steam flow to full line pressure. Hold for a few minutes, and then reverse in direction. Repeat this three or four times, to remove all loose ash and scale.
3. Maintain low steam flow and decrease firing at approximately 500°F per hour rate, as indicated by radiant section outlet flue gas. When radiant tube metal temperature has dropped to 500°F, stop steam flow.
4. At 400-450°F radiant section outlet flue gas temperature, discontinue firing. Follow plant safety practices in discontinuing heater firing. Discontinue steam to tubes.
5. Flush the tubes thoroughly with service water. A hydrostatic test of the tubes may be made following the water flush.
6. Upon completion of the water wash, the tubes are dried. Re-establish the air flow to remove water. Relight several burners to bring the radiant section flue gas temperature to around 400°F.
7. Intermittently discontinue water quench and observe the blowoff line effluent. In this manner, it may be determined when coil is dry.
8. After completion of drying, discontinue heater firing. Follow the plant safety practices in discontinuing the heater firing. Stop air flow.
9. Disconnect the decoking manifold from the heater coils. Replace the removable normal crossovers and swingout spools. Also turn the Figure 8 blinds to normal. The heater is made ready for normal service.

7. APPENDIX

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7. APPENDIX

7.1 Process and Utility Diagrams

7.2 Vessel Drawings

7.3 Combustion Equipment

7.4 Heat Exchangers

7.5 Pump Data and Curves

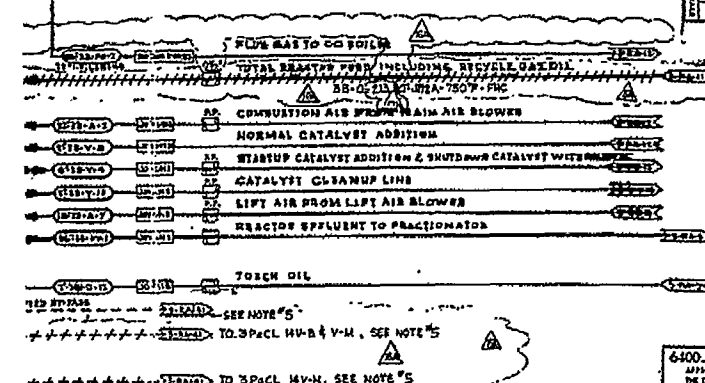
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7.1 PROCESS AND
UTILITY DIAGRAMS

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LEGEND		
PIPING SYMBOLS		
	GATE VALVE	CHECK VALVE
	CLOSE VALVE	
	INDICATOR FOR PRESSURE CONNECTION	 VALVE WITH BLAST PROOF 3/8" BIRTH "O"
	CONTROL VALVE ELECTRICALLY OPERATED	 CONTROL VALVE OPERATING IN SUB-PULPIT
	EMPTY RELIEF VALVE	 ABNORMAL UNIT OUTSTATION, A-04B- SEE DETAIL "A"
	INSTRUMENTED TO REMAIN ISOLATION UNCHANGED	 LOCAL UNIT IN-STATION, A-04B- SEE DETAIL "A"
	TRACED CODE LIFTING FROM INSTRUMENTED LINE	
INSTRUMENT SYMBOLS		
	LOCAL MOUNTED	 TRANSMITTER NEUTRON FLUX, CAP L-10-100, FUEL-TAP
	BOARD MOUNTED	 TRANSMITTER OF PRESSURE SWITCHER BOARD MOUNTED
	INTERLOCK ELEMENT SIGNAL CIRCUIT FROM AIR TIME	 IDENTIFYING ELEMENT
	NEUTRON LEAD	 CAPILLARY TUBING
	PLANT NUMBER	
	INSTRUMENT IDENTIFICATION INSTRUMENT NUMBER	
INSTRUMENT IDENTIFICATION		
ALL INSTRUMENTS ARE CODED IN ACCORDANCE WITH I.E.A. STANDARDS EXCEPT AS NOTED		
LINE IDENTIFICATION		
	SUPPLY	
	RETURN	

[illegible][illegible]

1000-10-10-10	1000000	NAME: C. CHAM
BECHTEL CORPORATION SAN FRANCISCO		
★	THE TEXAS COMPANY PUREX SODIUM WORKS	★
PROCESS PIPING & INSTRUMENT DIAGRAM REACTOR & GENERATOR SECTION FLUID CATALYTIC CRACKING UNIT		
RECEIVED	2025	2025

BECHTEL - 10055 TEXACO EST. - 39K

SYMBOLS

 EXISTING
 NEW
 REMOVE
 RELOCATE
 NOT USED - DO NOT REMOVE
 DENOTES TIE-IN NUMBERS

NOTES

1. REVISIONS OF MAJOR SYSTEMS ARE DESIGNATED BY THE SYMBOLS SHOWN ABOVE, MAJOR REVISIONS ARE REQUIRED AND INCLUDE A TRIANGULAR REVISION MARK.
2. PIPING SERVICE SPECIFICATION FOR NEW LINES IS IN ACCORDANCE WITH GEMS J-108-24E
3. LINE NUMBER SUFFIXES FOR INSULATION ON NEW LINES ARE IDENTIFIED AS FOLLOWS:
 - PP - PERSONNEL PROTECTION
 - CC - COLD CONSERVATION
 - PHC - PARTIAL HEAT CONSERVATION
 - PHC - FULL HEAT CONSERVATION
 - OTC - OPERATING TEMPERATURE CONTROL
 - ST - STEAM TRACED
 - NI - NO INSULATION
4. REPLACE EXISTING 10" LINE TO INLET OF DISTON OPERATED VALVE, SPCL-14B WITH NEW 8" PIPE & VALVE, 38-14C-14BN. EXISTING VALVE SPCL-14B WILL BE INSTALLED IN EMERGENCY COOLER INLET LINE. SEE DWG. 38-14A-1.
5. PUSH BUTTON OR LOW PRESSURE DROP SIGNAL ACROSS THE SPENT CATALYST OR REGENERATOR COOLER SLIDE VALVE WILL AUTOMATICALLY CLOSE INLET VALVE TO RISER AND WILL PERFORM THE FOLLOWING ACTIONS SHOWN ON DWG. 38-14A-1: OPEN PROCESS VALVE TO EMERGENCY COOLER, OPEN WATER VALVE TO EMERGENCY COOLER, CLOSE THE SLURRY REAGILE CONTROL VALVE & CLOSE RECYCLE GAS OIL TO 38-FB AT 38-1C-1.

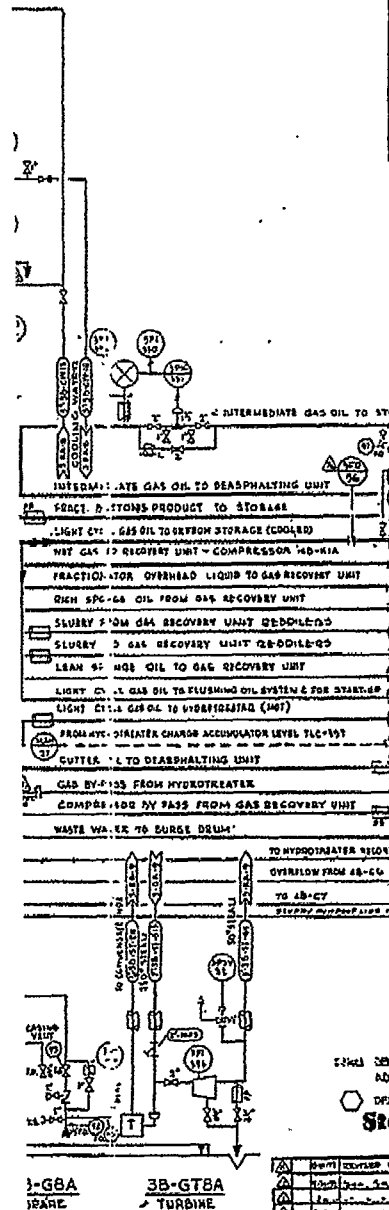
LINE IDENTIFICATION

1A = 0-422-8"-112A-N)

TEXACO PLANT NUMBER TEXACO SERVICE SYMBOL SIZE INSULATION REQUIREMENTS
NUMBER NUMBER TEXACO PIPING MATERIAL SERVICE SPECIFICATION

[illegible]

WA-TEX 000894



LEGEND	
ITEM NUMBERS	
28	5CH 80 DIAMLESS PIPE
57	36 FABRICATED STEEL PIPE 1/4" WALL
165	600" SCD. NEEDLE TYPE GLOBE VALVE
201	120" SCD. BROOKS GATE VALVE
219-15	
227-15	600" SW. F.8 GATE VALVE
289	1300" 6401 COCK RELIANCE MODEL 301
600	180" FLOD C.S. GATE VALVE XCF, 12" H. CHTR C.S.
602	180" FLOD. O.S. GATE VALVE XCF, MOHL T & S
607	180" FLOD. C.S. GATE VALVE XCF, MC. JESION & SO
611	800" FLOD. O.S. GATE VALVE XCF, CHAIN 32X
611-7-N	300" FLOD. 104. XND GATE VALVE E J.
619	300" FLOD. 104. XND GATE VALVE XCF, PAC 3350-D
611-7-31	300" FLOD. SCH. 40C. GATE VALVE. ORG.
763	600" FLOD. P.8 BLOWOFF VALVE XCF.
860	
900	180" FLOD. C.S. LUS. PLUG XCF, WR OPR.
907	180" FLOD. C.S. LUS. PLUG XCF. GATE OPR.
1001	
1003	500" FLOD. C.S. "V" STRAINER XCF.
1308	
1330	SAMPLE COOLER PER ENG SD-BL-164
1701	130" FLOD BELLOW TYPE EXPANSION JOINT XCF.
430	200" P.8 LARGE DIAMETER WELD NECK FLANGE
4702	

LEGEND		
DIPILIG		SYMBOLS
	GATE VALVE	SPECTACLE BLIND
	GLOBE VALVE	PLUG COCK
	CHECK VALVE	FLANGE
HAND CONTROL VALVE		TRIPARTITE TEE
STRAINER		SPECIALIZED BLIND FLANGE
CONTROL VALVE		ANGLE VALVE
A/C AIR PRESSURE SWITCH		EQUIPMENT CONTROL VALVE
SAFETY VALVE		ABOVE CONTROL VALVE
STEAM TRACED SEWER		STEAM TRACED SEWER
INSTRUMENT		SYMBOLS
	LOCAL MOUNTED	TRANSMITTER
BOARD MOUNTED		PURGE SWITCH/CONTROL VALVE
POSTURE LINE		ELECTRICAL LEAD
INSTRUMENT ABOVE		CAPILLARY TUBING
PLANT NUMBER INSTRUMENT IDENTIFICATION INSTRUMENT NUMBER		
INSTRUMENT IDENTIFICATION		
ALL INSTRUMENTS ARE CODED IN ACCORDANCE WITH I.S. 8. STANDARD SPECIFICATIONS FOR RELAYS REFER TO Dwg. No. 90-84-4.		
LINE IDENTIFICATION		
GAS LINE	WATER LINE	

[illegible]

SERVICE DESIGNATION	
0	HYDROCARBON LIQUID OR VAPOR FUEL OIL & GAS
0Y	HYDROCARBON, CATALYST, PRESENT
10	WASTE WATER, SPILL WATER
17	STEAM & CONDENSATE
6W	COOLING WATER
74	SERVICE WATER, TEST WATER
8F	BOILER FEEDWATER

REFERENCES		DRAWINGS	
PROCESS REGD. AMBITION & RUGGERATION	SECTION	FEED	5-0-0
PROCESS REGD. WASTE WATER STRIPPER	SECTION	FEED	5-0-0
UTILITY REGD. WASTE WATER TREAT	FEED		5-0-0
UTILITY REGD. 374. COND. & DOLLAR FEED	WATER FEED		5-0-0
PROCESS REGD. COMPACTION	FEED	MS. RECOVERY PLANT	
PROCESS REGD. ADSORPTION	FEED	FEED	4-0-1
PROCESS REGD. SPLITTING	FEED	FEED	4-0-1
FEED. TREATMENT & INTERCONNECTING	LINE	SHEET NO. 2	2-0-0
PROCESS REGD. BLOWDOWN	FEED		1-0-0
LIST OF REVISIONS TO THIS DRAWING			
FEED	GLAND OIL & FLUSHING OIL		4-0-1

NOTES

1. FOR LETTER CODE FOR STEAM TRACED LINES, SEE TABLE X, SPECIFICATION M-2, USE INSULATION THICKNESS SHOWN ON LINE TABLE UNLESS NOTED

[illegible]

BECHTEL CORPORATION SAN FRANCISCO		
	THE BECHTEL COMPANY PUGET SOUND WORKS	
PROCESS PIPING & INSTRUMENT DIAGRAM FRACTIONATION SECTION FLUID CATALYTIC CRACKING UNIT		
	FIG. No. 2525	DRAWING No. 3-RA-514

12/11/67 10009 TEACO EDT. 5710

SYMBOLS

	EXISTING
	NEW
	REMOVE
	RELOCATE
	NOT USED - DO NOT REMOVE
	REMOVES TIE-IN NUMBERS

NOTES

1. REVISIONS OF MAJOR SYSTEMS ARE DESIGNATED BY THE SYMBOLS SHOWN ABOVE. MINOR REVISIONS ARE CIRCLED AND INCLUDE A TRIANGULAR REVISION MARK.
2. PIPING SERVICE SPECIFICATIONS FOR NEW LINES ARE IN ACCORDANCE WITH GEMS J-208 TABLE 7.
3. LINE NO. SUFFERS FOR INSULATION ON NEW LINES ARE IDENTIFIED AS FOLLOWS:
 PP PERSONNEL PROTECTION
 SLD SOIL CONSERVATION
 PUC PARTIAL HEAT CONSERVATION
 ENC FULL HEAT CONSERVATION
 DTC OPERATING TEMPERATURE CONTROL
 ST STEAM TRACED & INSULATED
 NI NO INSULATION
4. PUSH BUTTON OR LOW PRESSURE DROP SIGNAL - ACROSS THE SPENT CATALYST OR REGENERATOR INLET AND VALVE WILL AUTOMATICALLY OPEN VALVE TO EMERGENCY COOLER, CLOSE INLET VALVE TO REGENERATOR INLET AND OPEN EMERGENCY COOLER WATER BYPASS VALVE. CLOSE THE SPENT REGENERATOR CATALYST VALVE AND REGENERATOR GAS OIL TO DRY-FS AT DRY-FS-11.

LINE IDENTIFICATION

1A-0-432-0-113A-N1

TERACO PLANT NUMBER TERACO SERVICE SYMBOL SIZE NUMBER INSULATION REQUIREMENTS TERACO PIPING MATERIAL SERVICE SPECIFICATION

1A

WA-TEX 000895

[illegible]

BECHTEL HOUSTON			
	TEXACO INC. PUREST SOUND PLANE		
PROCESS PIPING & INST DIAGRAM FRACTIONATION SECTION - FLUID CATALYTIC CRACKING UNIT			
	with the BECHTEL 50000 THERMEX - 3010	Draw No 3-RA-5	No. 8



○ DENOTES TIE-IN NUMBERS
DENOTES PIPING EQUIPMENT+
INSTRUMENTS ADDED ON C-1110.

REFERENCE DRAWINGS		
PROCESS P&ID, REACTOR & REGENERATION SECT. FEED		3-21-A
PROCESS P&ID, REACTOR SECTION FEED		3-21-B
PROCESS P&ID, MIXER WATER SPRING SECTION FEED		3-21-C
PROCESS P&ID, COMBUSTION SECTION GAS DECOUPLING		3-21-D
PROCESS P&ID, REGENERATOR SECTION GAS DECOUPLING		3-21-E
PROCESS P&ID, DISTILLATION & TREATING, SECT. GAS DECOUPLING		4-24-B
PROCESS P&ID, MIXER WATER TREATMENT SECTION FEED		3-21-F
PROCESS P&ID, CO. DRYER SECTION FEED		3-21-G
PROCESS P&ID, CATALYST STORAGE SECT. FEED		3-21-H
FLUE GASES DOMESTIC DRYER & COOLING WATER DTD.		3-21-J
PIPE, INSULATION OVERALL		22-22-F

DRAWING STATUS			
DRAWING	ISSUE NO.	DATE	
DESIGN OF PLANT	1	18/11/81	
PRELIMINARY ENGINEERING	5	18/11/81	
CONSTRUCTION	3	18/11/81	
DESIGN OF PLANT FOR CONSTRUCTION			

6400 12
APPROVED BY
THE TEXAS CO.
TX 75116 7-57-57

LINE IDENTIFICATION

TA-Q-437-6-313A-NI

INSULATION REQUIREMENTS

TEXACO PIPING MATERIAL SERVICE SPECIFICATION

TEXACO PLANT NUMBER

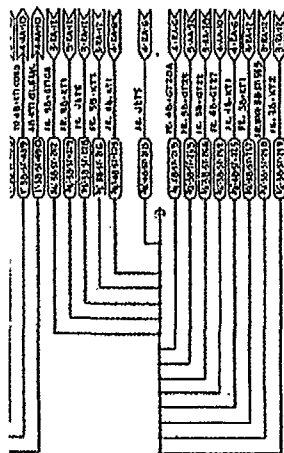
TEXACO SERVICE SIMLOC

SIZE

NUMBER

70

WA-TEX 000896



:TAIL "2"

[illegible]

BECHTEL 10075
TEXACO EST. 9510

SYMBOLS

EXISTING
 NEW
 REMOVE
 RELOCATE
 NOT USED - DO NOT REMOVE
 DEMOTES TIE IN NUMBERS

NOTES

- REVISIONS OF MAJOR SYSTEMS ARE DESIGNATED BY THE SYMBOLS SHOWN ABOVE. MINOR REVISIONS ARE CIRCLED AND INCLUDE A TRIANGULAR REVISION MARK.
- PIPING SERVICE SPECIFICATIONS FOR NEW LINES ARE IN ACCORDANCE WITH GEMS J-2DB, TABLE 7.
- LINE NO. SUFFICES FOR INSULATION ON NEW LINES ARE IDENTIFIED AS FOLLOWS:
 PP PERSONNEL PROTECTION
 CC COLD CONSERVATION
 PHC PARTIAL HEAT CONSERVATION
 FHC FULL HEAT CONSERVATION
 DTC OPERATING TEMPERATURE CONTROL
 ST STEAM TRACED & INSULATED
 NI NO INSULATION

LINE IDENTIFICATION

1A - 9 - 421 - 313A - H

TEXACO NUMBER	SERVICE SYMBOL	SIZE	NUMBER

INSULATION
REQUIREMENTS
TEXACO PIPING MATERIAL
SERVICE SPECIFICATION

REV	DATE	DESCRIPTION	BY	CHKD	APPD
1/1	4/14	REVISIONS FOR THERMAL STRESS ON			
2/1	4/14	ADDED THERMAL STRESS			
3/1	4/14	UNITS INST. FOR INST. 3			
4/1	4/14	REMOVED DB-11 THERMALIZATION			
5/1	4/14	ADDED LINE INST. 2			
6/1	4/14	FIELD UNIT SYSTEMS			
7/1	4/14	REMOVED PER DRAWING			
8/1	4/14	REMOVED PER DRAWING			
9/1	4/14	ISSUED FOR CONSTRUCTION			
10/1	4/14	ISSUED FOR CONSTRUCTION			
11/1	4/14	ISSUED FOR CONSTRUCTION			
12/1	4/14	ISSUED FOR CONSTRUCTION			

BECHTEL

HOUSTON

TEXACO INC.

PORT SOUND PLANT

TEXACO INC.

PORT SOUND PLANT

UTILITY PIPING & INST. DIAGRAM

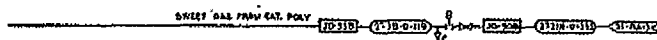
STM. COND. & BOILER FEED WATER

FCCU & GAS RECOVERY UNIT

Job No. _____

Draw No. _____

3-RA-9



REFERENCE DRAWINGS		
PROCESS FLOW, MINERAL ENRICHMENT UNIT, P.F.M.		1-10-1
UTILITY P.L.D., MAIN SYSTEM, P.C.C.U.		3-10-1
UTILITY P.L.D., S.M. CONDENSATE WATER, P.C.C.U.		3-10-2
UTILITY P.L.D., FLOWDOWN, T. PUMPED WATER, P.C.C.U.		3-10-3
PROCESS P.L.D., S.M. STORAGE MTS, P.C.C.U. ON-SITE UNIT		1-10-1
PROCESS P.L.D., S.M. BOILER SYSTEM, P.C.C.U.		1-10-2
PROCESS P.L.D., MAIN TREATMENT MTS, ACCU		3-10-7
LIST OF NAVIGATIONS TO THIS DRAWING		1-10-13
UTILITY P.L.D., DISTILLATION & TREATING MTS, GAS RECOVERY		4-10-2
P.L.D., FANCLAKE & INTERCOMINGING UNITS		2-10-2
UTILITY DISTRIBUTION		3-10-4

[illegible]

Stearns-Roger

DRAWING STATUS			
DRAWING NO.	ISSUE NO.	DATE	
947510700001	1	3/2/78	
947510700002	1	3/2/78	
FOR CONSTRUCTION			
FOR CONSTRUCTION			

APPROVED BY
THE DEAS CO.
Tel: 011 2 2-23-67

BECHTEL CORPORATION SAN FRANCISCO			
 THE TEXAS COMPANY FURST BOWNE WORKS			
UTILITY PIPING & INSTRUMENT DIAGRAM PLANT, INSTRUMENT & AERATION AID, FUEL OIL & GAS FGCU & GAS RECOVERY UNIT			
	2525	3-RA-11X	

BECHTEL - 10025 TEXACO EAST 3210

SYMBOLS

EXISTING
NEW
REMOVE
RELOCATE
NOT USED, DO NOT REMOVE
CNOTES TIE-IN NUMBERS

Notes

1. REVISION OF MAJOR SYSTEMS ARE DESIGNATED BY THE SYMBOL SHOWN ABOVE. MAJOR REVISIONS ARE CIRCLED AND INCLUDE A TRIANGULAR REVISION MARK.
2. PIPING SYMBOLS SPECIFICATIONS FOR NEW LINES ARE IN ACCORDANCE WITH ANSI J-208, TABLE 2.
3. LWA NUMBER SUFFICES FOR INSULATION ARE IDENTIFIED AS FOLLOWS:
 - PP PERSONNEL PROTECTION
 - CC COLD CONSERVATION
 - PHG PARTIAL HEAT CONSERVATION
 - FHG FULL HEAT CONSERVATION
 - OTC OPERATING TEMPERATURE CONTROL
 - ST STEAM TRACED
 - NI NO INSULATION

LINE IDENTIFICATION

1A-O-22-A-112A-NI

TEXACO PLANT NUMBER TEXACO SERVICE SYMBOL SIZE INSULATION REQUIREMENTS
TEXACO PIPING MATERIAL SERVICE SPECIFICATION

WA-TEX 000899

[illegible]

BECHTEL
HOUSTON

TEXACO INC.
PURET SOUND PLANT

UTILITY PIPING & INST DIAGRAM
PLT, INST & AERATION AIR FUEL OIL & GAS
FCCU & GAS RECOVERY UNIT

	Date Rec. RECEIVED - MOBILE TELETYPE UNIT - MOBILE	Date Rec. 3-14-44	Date Rec. 3-14-44
	3-14-44	3-14-44	3-14-44

EQUIPMENT LIST PLANT 3

3B-C1	EXTRACTOR
3B-C2	OVERHEAD ACCUMULATOR
3B-C3	AIR SURGE DRUM
3B-C4	REDUCT STOMPER
3B-C5	CONDENSATE FLASH DRUM
3B-C6	HOT CATALYST STORAGE HOPPER
3B-C7	FRESH CATALYST STORAGE HOPPER
3B-C8	WASTE WATER SURGE DRUM
3B-C9	WASTE WATER STRIPPER
3B-C10	AIR WATER CONTACT TOWER
3B-C11	AIR WATER SEPARATOR
3B-C12	CATALYST RINS HOPPER
3B-C13	REACTOR
3B-C14	REGENERATOR
3B-C15	FUEL GAS KICKOUT DRUM
3B-C16	INT. BOILER BLOWDOWN DRUM
3B-C17	CONT. BOILER BLOWDOWN DRUM
3B-C18	BLOWDOWN DRUM
3B-C19	SMALL TANK
3B-C20	BY PASS SEAL TANK
(SEE BELOW FOR T.D. CONT.)	
3B-D1	CONDENSATE STORAGE
3B-D2	PHOSPHATE MIXING
3B-D3	COMPRESSOR LUBE OIL MAKEUP
3B-E1A-K	FRAC. OVERHEAD CONDENSERS
3B-E2	INTERMEDIATE REFLUX STR. COND.
3B-E3	SLURRY QUENCH STR. COND.
3B-E4	FRESH FEED L.O.O. EXCHANGER
3B-E5A1B	FRESH FEED PREHEATER
3B-E6A1B	LIGHT GAS OIL COOLER
3B-E7	INTERMEDIATE GAS OIL COOLER
3B-E8	100% NEW EXCHANGER
3B-E9	FRACTIONATOR BOTTOMS EXCHANGER
3B-E10	SURFACE CONDENSER (AIR NUMBER TUBES)
3B-E11	FRAC. REFLUX SPY EXCHANGER
3B-E12	WATERWATER FEED STR. EXCHANGER
3B-E13	W.W. STRIPPER REFLUX COOLER
3B-E14A1B	WATERWATER COOLER
3B-E15	EMERGENCY COOLING COIL
3B-E16A1B	LUBE OIL COOLERS (3B-E16A)
3B-E17A1B	LUBE OIL COOLERS (3B-E17A)
3B-E18A1B	LUBE OIL COOLERS (3B-E18A)
3B-F1	AIR HEATER
3B-F2	CO BOILER
3B-G50	FRESH FEED
3B-G50A	COMMON SPARE (3B-G50) 3B-G50
3B-G52A	FRAC. COND. REFLUX & SPARE
3B-G51A	SLURRY QUENCH & SPARE
3B-G54A	INTERMEDIATE REFLUX & SPARE
3B-G55	LIGHT GAS OIL
3B-G56A	COMMON SPARE (3B-G55) 3B-G56
3B-G57	RECYCLE GAS OIL
3B-G58	INTERMEDIATE GAS OIL PRODUCT
3B-G59A1B	FRAC. BOTTOMS FEED & SPARE
3B-G60A1B	SLURRY WATER & SPARE
3B-G61A1B	MAIN AIR BLOWDOWN COND. & SPARE
3B-G62A1B	WASTE WATER STRIPPER FEED
3B-G63A1B	COMMON SPARE (3B-G62) 3B-G63
3B-G64A1B	WASTE WATER STRIPPER BOTTOMS FEED
3B-G65A1B	WASTE WATER STRIPPER REFLUX
3B-G66A1B	PREHEATER REFLUX WATER & SPARE
3B-G67A1B	FLOR OIL
3B-G68A1B	FEED (BLOWDOWN) PUMP
3B-G69A1B	PHOSPHATE INJECTION
3B-G70A1B	PHOSPHATE INJECTION
3B-G71A1B	PHOSPHATE INJECTION
3B-G72A1B	LUBE OIL COOLERS (3B-G72A)
3B-G73A1B	LUBE OIL COOLERS (3B-G73A)
3B-G74A1B	LUBE OIL COOLERS (3B-G74A)
3B-G75A1B	CO BOILER WASH WATER
3B-G76A1B	CONDENSATE RETURN
3B-G77A1B	SOUR GAS K.O. DRUM PUMP
3B-H1	AIR EJECTORS & CONDENSERS
3B-I1	MAIN AIR BLOWER
3B-I2	LIFT AIR BLOWER
3B-K1A	FORCED DRAFT FAN & SPARE
3B-T1	ELEVATOR (P.E.C. STRUCTURE)

EQUIPMENT LIST PLANT 4

4B-C1	ABSORBER DE-ETHANIZER
4B-C2	SPONGE COLUMN
4B-C3	DEBUTANIZER COLUMN
4B-C4	SPLITTER COLUMN
4B-C5	STEAM CONDENSATE DRUM
4B-C6	INTERSTAGE SEPARATOR
4B-C7	2ND STAGE SEPARATOR
4B-C8	WATER DRAFF POT
4B-C9	DEBUTANIZER OVERHEAD ACCUMULATOR
4B-C10	SPLITTER OVERHEAD ACCUMULATOR
4B-C11	HEAVY FCC GASO CAUSTIC TREATER
4B-C12	LIGHT FCC GASO CAUSTIC TREATER
4B-C13	GUM INHIBITOR DRUM
4B-C14	CORROSION INHIBITOR DRUM
4B-C15	JOHNSON ELECTRAP
4B-C16	ABSORBER K.O. POT
4B-C17	DOCTOR SOLUTION MIXING TANK
4B-C18	GAS COMPRESSOR INTERCOOLER
4B-C19	GAS COMPRESSOR AFTERCOOLER
4B-C20	ABSORPTION OIL COOLER
4B-C21	ABSORBER 1ST INTERCOOLER
4B-C22	LIGHT FCC GASOLINE RECOOLER
4B-C23	ABSORBER 2ND INTERCOOLER
4B-C24	ABSORBER STEAM RECOILER
4B-C25	DEBUTANIZER OVERHEAD CONDENSER
4B-C26	DEBUTANIZER RECOILER
4B-C27	GASO SPLITTER OIL CONDENSER (LIGHT)
4B-C28	GASO SPLITTER RECOILERS
4B-C29	HEAVY FCC GASO COOLER
4B-C30	LIGHT FCC GASO COOLER
4B-C31	SURFACE COND. GAS COMP. TUBS
4B-C32	INHIBITOR DRUM HEATER
4B-C33	HEAVY FCC GASOLINE AFTER COOLER
4B-C34	LUBE OIL COOLERS (4B-C34A)
4B-C35	SPLITTER BOTTOMS EXCHANGER
4B-C36	ABSORBER 3RD INTERCOOLER
4B-C37	INTERSTAGE SEPARATOR LIQUID & SPARE
4B-C38	2ND STAGE SEPARATOR LIQUID & SPARE
4B-C39	LEAN SPONGE OIL & SPARE
4B-C40	ABSORBER 1ST INTERCOOLER CIRC.
4B-C41	COMMON SPARE FOR C39 & C40
4B-C42	ABSORBER 2ND INTERCOOLER CIRC.
4B-C43	ABSORBER REBOILER & SPARE
4B-C44	RECIRCULATED LEAN OIL
4B-C45	DEBUTANIZER PROD.
4B-C46	COMMON SPARE FOR C45 & C46
4B-C47	SPLITTER BOTTOMS
4B-C48	COMMON SPARE FOR C47 & C48
4B-C49	SPLITTER PRODUCT & PRODUCT
4B-C50	NR 1 CAUSTIC CIRCULATING
4B-C51	NR 2 CAUSTIC CIRCULATING
4B-G18	DRINATOR BLEND INJECTION (PROPORTION)
4B-G19	INHIBITOR CIRCULATING
4B-G20A1B	COMPRESSOR TUBE COND. & SPARE
4B-G21A1B	DEBUTANIZER REFLUX & SPARE
4B-G22	CORROSION INHIBITOR INJECTION
4B-G23	CORROSION INHIBITOR INJECTION
4B-G24	DOCTOR SOLUTION INJECTION
4B-G25	NR 1 CAUSTIC CIRCULATING
4B-G26	NR 2 CAUSTIC CIRCULATING
4B-G27A1B	LUBE OIL (4B-G27A)
4B-G28	WATER INJECTION (TO 4B-G28)
4B-H1	AIR EJECTORS & CONDENSERS
4B-K1A	1ST STAGE GAS COMPRESSOR
4B-K1B	2ND STAGE GAS COMPRESSOR
4B-K2	FRESH REFRIGERATION SYSTEM
4B-K2A	ABSORPTION OIL CHILLER
4B-K2B	BUTANE REFRIGERANT CONDENSER

NOTE: ALL HORIZONTAL VESSELS ARE LOCATED TO SEAM-LINE AT 1/2 OF VESSEL

SCALE 1/4" = 1' 0"

NO.	DESCRIPTION	DATE	BY	CHKD.	APP'D.	REV.	DATE	BY	CHKD.	APP'D.
1	ISSUED FOR CONSTRUCTION									
2	ISSUED FOR CONSTRUCTION									
3	ISSUED FOR CONSTRUCTION									
4	ISSUED FOR CONSTRUCTION									
5	ISSUED FOR CONSTRUCTION									
6	ISSUED FOR CONSTRUCTION									
7	ISSUED FOR CONSTRUCTION									
8	ISSUED FOR CONSTRUCTION									
9	ISSUED FOR CONSTRUCTION									
10	ISSUED FOR CONSTRUCTION									

BECHTEL CORPORATION
SAN FRANCISCO

THE TEXAS COMPANY
PUGET SOUND WORKS

PLOT PLAN
FLUID CAT CRACKER & GAS RECOVERY UNIT

2525 3-RA-14



BECHTEL		HOUSTON	
TEXACO INC.		PUGET SOUND PLANT	
PLOT PLAN			
FLUID CAT CRACKER & GAS RECOVERY UNIT			
DATE	REV.	DATE	REV.
11/11/51	1	11/11/51	1
11/11/51	2	11/11/51	2
11/11/51	3	11/11/51	3
11/11/51	4	11/11/51	4
11/11/51	5	11/11/51	5
11/11/51	6	11/11/51	6
11/11/51	7	11/11/51	7
11/11/51	8	11/11/51	8
11/11/51	9	11/11/51	9
11/11/51	10	11/11/51	10

WA-TEX 000900

NOTES

1. THIS FC (NEW) CONTROLS TOTAL FLOW BY RESETTNG INDIVIDUAL HEATER COIL FLOW CONTROLLERS (NEW)
2. NORMAL OPERATION WITH 250 B/H HCGO RECYCLE AND NO HCGO RECYCLE. ALTERNATE CASE WITH 250 B/H HCGO RECYCLE AND NO HCGO RECYCLE.
3. PUSHBUTTON OR LOW PRESSURE DROP SIGNAL ACROSS THE SPENT OR REGENERATED CATALYST. SLOW VALVE AUTOMATICALLY OPENS VALVES IN LINES TO EMERGENCY COOLER AND CLOSES INLET VALVE TO RISER. THE EXISTING VALVE AT THE RISER WILL BE RELOCATED AS THE EMERGENCY COOLER VALVE AND A NEW VALVE WILL BE INSTALLED AT THE RISER.
4. NORMAL OPERATION- HOT FEED FROM CRUDE AND DEASPHALTING UNITS.
ALTERNATE OPERATION- COLD FEED FROM STORAGE.
5. STREAM 7 PROPERTIES ARE FROM TEXACO TEST RUN.
6. STREAM 8 PROPERTIES ARE FROM TEXACO'S NEW DESIGN.

SERVICE WATER

TO STORAGE

OR P&CL 14A & B

TO FEED RISER

TO LIGHT GAS OIL
PRODUCT COOLERS

TO FRACTIONATOR

HCGO TO GAS RECOVERY
UNIT REBOILERS

SYMBOLS

- EXISTING
- ++++ NEW
- REMOVE
- RELOCATE
- NOT USED
- DO NOT REMOVE
- REPLACE

NOTICE

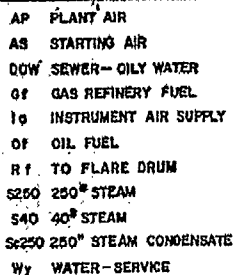
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		TEXACO INC. ENGINEERING DEPARTMENT HOUSTON, TEXAS		
PROCESS FLOW DIAGRAM FCC UNIT REACTOR FEED HEAT AND EMERGENCY COOLING				
INITIALS	DATES	SCALE:		
BY DATE	BY DATE	NUMBER ASSIGNED	DATE	
BY DATE	BY DATE	TRACING RECORD ENTERED		
APPROVED		JOB		REVISIONS
3-RA-40				

WA-TEX 000901

UTILITY LEGEND

TEXACO EST. -3910



NOTES

1. LOCATE TOGETHER.
2. FOR HEATER DECKING SEE DETAIL "X"
3. PUSH BUTTON OR LOW PRESSURE DROP SIGNAL ACROSS THE SPENT CATALYST OR REGENERATOR CATALYST SLIDE VALVE WILL AUTOMATICALLY OPEN VALVE TO EMERGENCY COOLER, CLOSE INLET VALVE TO RISER SHOWN ON DWG. 3-RA-4, OPEN EMERGENCY COOLER WATER SHUTOFF VALVE, CLOSE THE SLURRY RECYCLE CONTROL VALVE AND CLOSE RECYCLE GAS OIL TO 3B-F3 AT 3PRC-11.
4. RELOCATE EXISTING FCC RISER INLET VALVE 3P4CL 14VB AS CLOSE TO TEE AS POSSIBLE. PIPE FROM TEE TO VALVE TO BE 9 CR
5. CAN USE EXISTING TURBINE 3B-67IA
6. ADJUSTABLE ORIFICE IN PNEUMATIC LINE TO EFFECT SLOW OPENING AND CLOSING OF VALVE 3P4CL 14V-M.
7. ANGLE OF INTERSECTION SHOULD BE 45° OR LESS
8. REPLACE EXISTING FCC INLET PIPING WITH 9CR PIPE
- 9.
10. LINE NUMBER SUFFIXES FOR INSULATION ARE IDENTIFIED AS FOLLOWS:
PP - PERSONNEL PROTECTION
CC - COLD CONSERVATION
PH - PARTIAL HEAT CONSERVATION
FHG - FULL HEAT CONSERVATION
OTC - OPERATING TEMPERATURE CONTROL
ST - STEAM TRACED & INSULATED
NI - NO INSULATION
11. UNLESS OTHERWISE SPECIFIED, THE VALVE SELECTION SHALL BE BY THE CONTRACTOR GEMS.
12. REFER TO GEMS J-10, PARA.513 FOR TEXACO'S PHILOSOPHY WITH REGARDS TO BLINDS TO BE SUPPLIED BY THE CONTRACTOR. PARTICULAR ATTENTION SHOULD BE GIVEN TO THE MODIFICATION OF PARA.513.1 WHICH COVERS SHUTDOWN BLINDS.
13. RELIEF VALVES 3-PSV-74&75 REQUIRE "P" SIZE ORIFICE
14. TRANSFER LINE PRESSURE DROP MUST BE CHECKED BY CONTRACTOR AFTER HEATER SELECTION HAS BEEN MADE

NOTICE

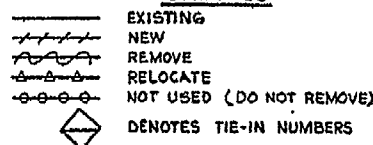
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TEXACO INC.
ENGINEERING DEPARTMENT
HOUSTON, TEXAS

ENGINEERING FLOW DIAGRAM
FEED PREHEAT
FLUID CATALYTIC CRACKING UNIT

INITIALS	DATE	SCALE: NONE
PROPERTY BY	NUMBER ASSIGNED	DATE
ISSUED BY	TRACING RECORD ENTERED	
TRACING CODE		3-RA-41

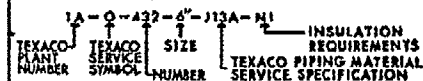
SYMBOLS



NOTES

15. REVISIONS OF MAJOR SYSTEMS ARE DESIGNATED BY THE SYMBOLS SHOWN ABOVE. MINOR REVISIONS ARE CIRCLED AND INCLUDE A TRIANGULAR REVISION MARK.
16. PIPING SERVICE SPECIFICATIONS FOR NEW LINES ARE IN ACCORDANCE WITH GEMS J-208 TABLE 7.
17. LINE NUMBER SUFFIXES FOR INSULATION ARE IDENTIFIED AS FOLLOWS:
- | | |
|-----|-------------------------------|
| PP | PERSONNEL PROTECTION |
| CC | COLD CONSERVATION |
| PHC | PARTIAL HEAT CONSERVATION |
| FHC | FULL HEAT CONSERVATION |
| OTC | OPERATING TEMPERATURE CONTROL |
| ST | STEAM TRACED |
| NI | NO INSULATION |

LINE IDENTIFICATION

[illegible]

SCALE NONE	DENIED
------------	--------

GRAPHIC

BECHTEL
HOUSTON



TEXACO INC.
PUGET SOUND PLANT



PROCESS PIPING & INST. DIAGRAM
FEED PREHEAT
FLUID CATALYTIC CRACKING UNIT

	Job No.	Comp. No.	Plan.
	BECHTEL - 10086	3-RA-41	11A
	TERMINAL DIST. - 2010		

3B-E40	EMERGENCY COOLER
3B-F3	REACTOR CHARGE HEATER
3B-C40	QUENCH DRUM



WA-TEX 000903

NOTICE

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PLOT PLAN
FCCU HEATER & EMERGENCY COOLER

INITIALS	DATE		SCALE:	
SEARCHED	INDEXED	NUMBER ASSIGNED		DATE
SERIALIZED	FILED	TRACING RECORD ENTERED		2-17-71
FBI - MEMPHIS		3-AA-42		
FBI - JACKSON				

RECHTEL
HOUSTON

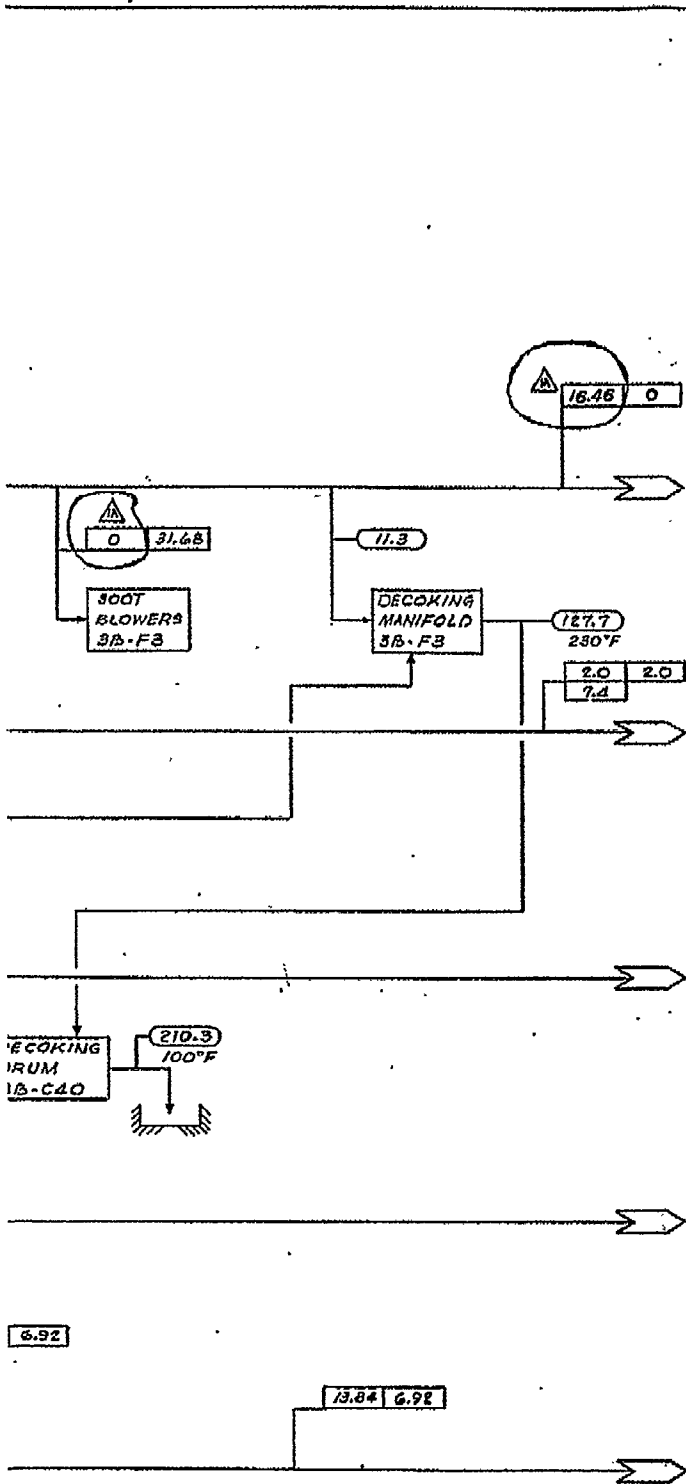


TEXACO INC.
PUGET SOUND PLANT



PLOT PLAN
FCCU HEATER & EMERGENCY COOLER

	Job No.	Draw No.	Rev.
	BECHTEL - 30006 TERRACE EXT - 3910	3-RA-42	5A



LEGEND

1	2
3	

1 - NORMAL OPERATION FIRING HEATER ON FUEL GAS;

2 - NORMAL OPERATION FIRING HEATER ON FUEL OIL;

3 - SPARE FRESH FEED PUMP OPERATING.

TEMP °F

DESIGN-DECOCKING OPERATION

ALL FIGURES IN 1000#/HR. EXCEPT AS NOTED

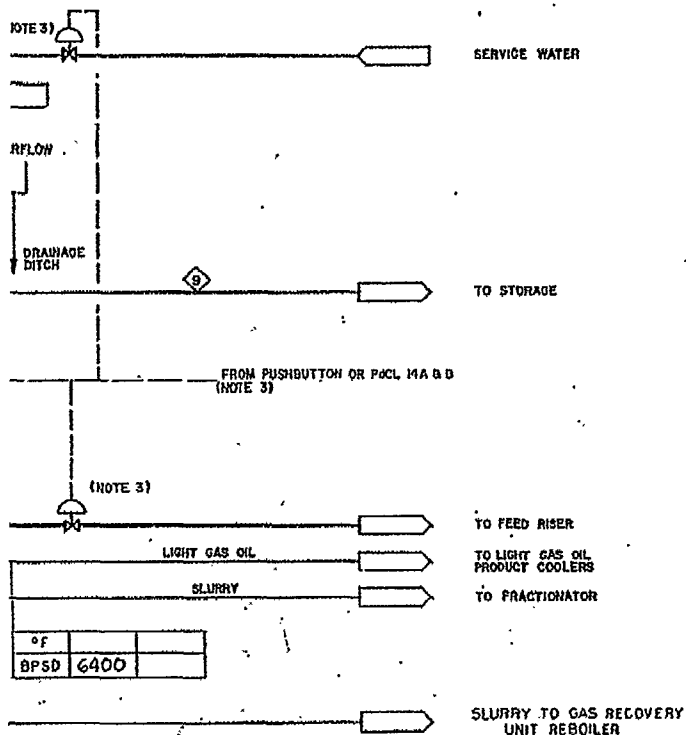


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SCALE		DESIGNED		DRAWN	
BECHTEL HOUSTON TEXACO INC. PUGET SOUND PLANT					
UTILITY USAGE DIAGRAM FCCU UNIT PLANT 3B					
DATE: 10006 TEXACO EST - 3910		3-RA-43		1A	

WA-TEX 000904

ER



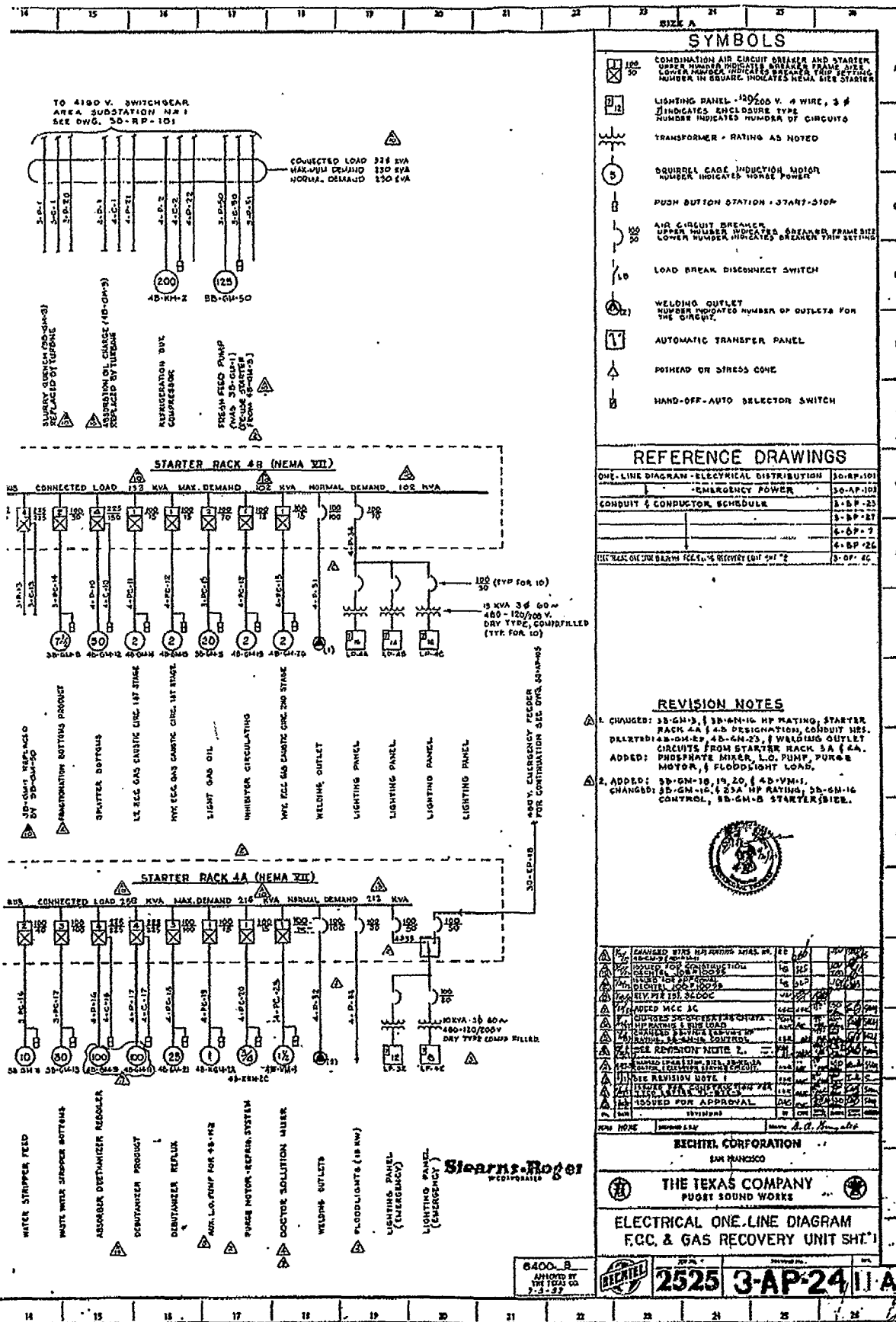
NOTES

1. THIS FC (NEW) CONTROLS TOTAL FLOW BY RESETTNG INDIVIDUAL HEATER COIL FLOW-CONTROLLERS (NEW)
2. NORMAL OPERATION WITH 250 B/H ICGO RECYCLE AND NO HCGO RECYCLE. ALTERNATE CASE WITH 250 B/H HCGO RECYCLE AND NO ICGO RECYCLE.
3. PUSHBUTTON OR LOW PRESSURE DROP SIGNAL ACROSS THE SPENT OR REGENERATED CATALYST SLIDE VALVE AUTOMATICALLY OPENS VALVES IN LINES TO EMERGENCY COOLER AND CLOSSES INLET VALVE TO RISER. THE EXISTING VALVE AT THE RISER WILL BE RELOCATED AS THE EMERGENCY COOLER VALVE AND A NEW VALVE WILL BE INSTALLED AT THE RISER.
4. NORMAL OPERATION-HOT FEED FROM CRUDE AND DEASPHALTING UNITS. ALTERNATE OPERATION- COLD FEED FROM STORAGE.
5. STREAM 7 PROPERTIES ARE FROM TEXACO TEST RUN.
6. STREAM 8 PROPERTIES ARE FROM TEXACO'S NEW DESIGN.
7. T1 LOCATED ON LCGO STRIPPER OUTLET

WA-TEX 000905

△									
△									
△									
△	4/12	ISSUED FOR INFORMATION							
△	4/12	ISSUED FOR APPROVAL	LH						
No.	Date	Revisions	By	CHKD	CHKD	CHKD	CHKD	CHKD	CHKD
SCALE		DESIGNED		DRAWN					
BECHTEL HOUSTON									
TEXACO INC. PUGET SOUND PLANT									
FLAG FLOW DIAGRAM REACTOR FEED HEAT AND EMERGENCY COOLING FCC UNIT									
Job No.		Draw No.		Rev.					
BECHTEL - 100905		3-RA-44		1A					
TEXACO INC. - 2619									

10



WA-TEX 000906

7.2 VESSEL DRAWINGS

TABLE OF CONTENTS
SECTION 7.2 VESSEL DRAWINGS

Decoking Quench Drum - 3B-C4D

3-DC-40

ELEVATION

WA-TEX 000909

△	2/21/72	ADDED INSULATION (RP)	5/2	R	R	TAN	2/21/72
		RELEASED FOR CONSTR.					
		REY. FULLJET NOZZ. MODEL#					
△	2/28/72	ADDED: ORIENT. CHGD	1/0	5/2	R	TAN	2/28/72
		NOZZLE N3 FROM C"	H				
△	2/28/72	ISSUED FOR PURCHASE	1/4	5/2	R	TAN	2/28/72
		RELEASED SHELL AND					
		HEAD MATERIAL					
△	2/28/72	ISSUED FOR QUOTES	1/4	5/2		20% L	2/28/72
		STUBS	ST	CONC	DEPT	ENGR	ARCH

[illegible]

7.3 COMBUSTION
EQUIPMENT

TABLE OF CONTENTS
SECTION 7.3 COMBUSTION EQUIPMENT

Data Sheet for 3B-F3

3B-F3	General Arrangement	V.P.10095-F-01-HAC-40-6
	Combination Oil and Gas Burner	V.P.10095-F-01-HAC-67-2

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PROCESS DESIGN CONDITIONS

Remarks and Special Requirements:

* 1. Distillation Data or Composition Attached
 2. SELLERS PRESSURE DROP CALCULATIONS SHALL NOT TAKE CREDIT
 FOR STATIC HEAD BETWEEN HEATER INLETS AND OUTLETS.
 * Items So Designated To Be Filled In By Buyer I.B.P. 400°F

SHEET 1 OF 60

MECHANICAL DESIGN CONDITIONS

General

*Plot Limitations

*Tube Limitations

*Required Drawings

*Structural Design Data: Wind Load

*List of Applicable Standards or Specifications: 1.

2.

*Stack Limitations

Other Limitations

Seismic Factor

3.

4. SEE ATTACHMENT

Coil Design

*Heater Section

RADIANT CONVECTION

*Service

PROCESS

*Design Pressure, psig

150

*Design Fluid Temperature, Deg F

750

*Corrosion Allowance: Tubes

1/8"

Fittings

1/8"

Hydrostatic Test Pressure, psig

550

Number of Passes/Tubes per pass

6 / 18

6 / 12

Overall Tube Length, Ft

33'-0

27'-0

Effective Tube Length, Ft

34'-0

26'-0

Bare Tubes: Number

108

18

Total Exposed Surface, Sq Ft

4260

552

Extended Surface Tubes: Number

54

Total Exposed Surface, Sq. Ft.

14,000

Tube Spacing, Center to Center, In. (Staggered) (In Line)

8

8

Tube Center to Furnace Wall, In. Min

6

*Stress Relieve

Yes - 241 MAX

*Weld Inspection Requirements, X-Ray or Other

Yes - 100%

Tubes

Vertical or Horizontal

VERT

HORIZ

*Tube Material (ASTM Specification and Grade)

A-200 GR T-9

Outside Diameter, In

4.5

Wall Thickness, (Minimum) (Average), In

0.265

Maximum Tube Wall Temperature, Deg F (Calculated)/(Design)

/900

/900

Inside Film Coefficient (Calculated) (Based on Outside Surface)

Design Basis for Tube Wall Thickness

CEMS H-1M7

Description of Extended Surface:

Type

—

FINS

Fin or Stud Material

—

11% CR & 13-8

Fin or Stud Dimensions

HEIGHT X THICKNESS

—

1 x 0.105

Fin or Stud Spacing

NO PER INCH

—

3

Maximum Fin or Stud Temperature

—

N.A.

Extension Ratio

—

Plug-Type Headers

Manufacturer and Type

*Material (ASTM Specification and Grade)

Nominal Rating

*Location

*Welded or Rolled

NONE

Return Bends

Manufacturer and Type

120° WELDED RETURN BEND

*Material (ASTM Specification and Grade)

9% CR-1% MO

Nominal Rating or Schedule

TO SUIT TUBE

*Location

FIREBOX

HEADER BOX

MECHANICAL DESIGN CONDITIONS (CONT'D)

Coil Design (Cont'd)

	RADIANT	CONVECTION
	Process	Process
* Heater Section		
* Service		
Terminals		
* Manufacturer and Type	FLANGED	FLANGED
* Material (ASTM Specification and Grade)	A-182GRF9	A-182GRF9
Nominal Rating	To Suit Tube	To Suit Tube
* Location	OUTSIDE F.B.	OUTSIDE H.B.
* Welded or Rolled	WELDED	WELDED
Flange: Size and Rating	150# R.F.	150# R.F.
Location	SEE NOTE 1	
Stress Group To Complete		
* Nozzle Movement:		
* Direction		
* External Nozzle Load		
* Direction		
* Pipe Load Supported By Heater		
* Special Support Brackets Required		
Comments		
.....		
.....		
.....		

Crossovers

* Welded or Flanged	WELDED	-
* Pipe Material (ASTM Specification and Grade)	A-200 GRT9	-
Pipe Size and Wall Thickness	4.5 x 0.265	-
Location	INTERNAL	-
Flange Rating		-

Tube Supports

Ends, Top, Bottom:		
Material	A-447 TP11	
Thickness		
Type and Thickness of Insulation		
Insulation Reinforcement		
Intermediate:		
Material	A-447 TP11	
Spacing, Ft	13'-0	
Type and Thickness of Coating		
Guides: Location	BOTTOM	
Material	1 1/2 SCH 80 25-12 PIPE	

Notes

- 1) RADIANT OUTLETS ARE TO BE GROUPE

H&C SFE FORM 376C-8/71

DS-3-F-1.

2

DSF 3 12 6

WA-TEX 000914

MECHANICAL DESIGN CONDITIONS (CONT'D)

Header Boxes

Location: CONVECTION SECTION Material: CARBON STEEL Thickness: 3/16
 Insulation: Material: CASTABLE, LHV 1:2:4 MIX Thickness: 2
 Anchoring Material: CARBON STEEL CHAIN LINK FENCING
 Are Header Box Doors Bolted or Hinged? BOLTED

Burners

Manufacturer and Type: JOHN ZINK - COND GAS & OIL - MAX Size: 24 Number: 7
 Location: RADIANT FLOOR
 Size and Type of Pilots: 3/4" - GAS - 1-PER BURNER
 Heat Release per Burner at Design Excess Air and Draft: (MM Btu per hour)
 Normal: 14,000,000 Minimum: 7,000,000 Maximum: 16,800,000
 Minimum Distance Burner Centerline to Tube Centerline:
 Horizontal: 6'-0" MIN. Vertical: N.A.

Settings:

Exposed Vertical Walls:

Thickness: _____ Hot-Face Temperature: Design _____ Calculated _____
 Wall Construction: _____
 Outside Casing: Thickness: _____ Material: _____ Outside Temperature: _____
 Tieback Design and Material: _____ Spacing: _____
 Support: Material: _____
 Method of Fastening Tiebacks to Structure: _____

Shielded Vertical Walls:

Thickness: 5 Hot-Face Temperature: Design 2000 Calculated 1200
 Wall Construction: CASTABLE, LHV 1:2:4 MIX
 Outside Casing: Thickness: 1/4 MIN Material: CARBON STEEL Outside Temperature: _____
 Tieback Design and Material: V-CLIPS, SS TYPE 304 Spacing: 1'
 Support: Material: _____
 Method of Fastening Tiebacks to Structure: WELDING

Arch:

Thickness: 6" Hot-Face Temperature: Design 2000 Calculated _____
 Arch Construction: CASTABLE, L.H.V. 1:2:4 MIX
 Outside Casing: Thickness: 1/4" Material: CARBON STEEL Outside Temperature: 4200
 Tieback Design and Material: V-CLIPS, SS TYPE 304 Spacing: _____
 Support: Material: _____
 Method of Fastening Tiebacks to Structure: WELDING

Floor:

Thickness: 6" Hot-Face Temperature: Design 2000 Calculated _____
 Floor Construction: CASTABLE, LHV 1:2:4 MIX
 Minimum Floor Elevation: _____
 Outside Casing: Thickness: 1/4" Material: CARBON STEEL Outside Temperature: 4200

Convection Section:

Thickness: 5 Design Hot-Face Temperature: 2000
 Construction: CASTABLE, L.H.V. 1:2:4 MIX
 Outside Casing: Thickness: 3/16 Material: CARBON STEEL Outside Temperature: 4200

MECHANICAL DESIGN CONDITIONS (CONT'D)

Settings (Cont'd)

Tieback Design and Material V-CLIPS SS TYPE 304

Support Material

Method of Fastening Tiebacks to Structure WELDING

Internal Well:

Type NONE

Dimensions

Material

Stack

Number ONE

Self-Supporting or Guyed SELF SUPPORT

Location TOP OF HEATER

Material CARBON STEEL A-36

Thickness

Minimum Thickness 1/4"

Inside Metal Diameter 6'-6" EXIT 4'-3"

Height Above Grade 182'-5"

Stack Length 122'-9"

Lining: Material

Thickness

Type of Material or Reinforcement

Extent of Lining NONE

Dampers

Location: Stack or Bottom Air Plenum

STACK

Material CARBON STEEL - 1/4 MIN

Multiple or Single Leaf

MULTIPLE

Description of Provision for Operation from Grade

WINCH

Hot Ducts, Breaching, Flues, and Collectors

Material CARBON STEEL - 1/4 THICK

ASTM Specification

A-36

Size

Insulation: Type CASTABLE - LHV 1, 2, 4 MIX

Thickness 1 1/2"

Type of Anchoring Material

CARBON STEEL CHAIN LINK FENCING

Size of Access Door into Breaching

NONE

Cold Air Duct and Plenum

Material CARBON STEEL - 1/4 THICK

ASTM Specification

Size

Miscellaneous

Overall Dimensions of Furnace

"CONN INLET, RAD OUTLET"

Platforms: Location

BOTT RAD - SOOTBLOWERS - DECOKING CONN - STACK

Width: Min.

2'-6"

3'-0"

3'-0" CLEAR

Type of Floor

1/4" CHECKERED PLATE

Stairs: Location

TO BOTTOM RADIANT PLATFORM

Ladders: Location

1) FROM GRADE TO SOOTBLOWER PLATE W/ STEP-OFF AT RAD. PLATE

2) SOOTBLOWER PLATE TO DECOKING CONN 3) SOOTBLOWER PLATE TO STACK PLATE

Access Doors: Location and Size

1) FLOOR

2) STACK

Observation Doors: Location and Size

1) 7-OBS DOORS RAD. 2) 6-RAD FLOOR PEEPS

Miscellaneous Connections (Number and Size):

Draft 1" - 150# RF - 6

Flue Gas Sample 1" - 150# RF - 4

Temperature 1 1/2" - 150# RF - 8

Smothering Steam 2" IPS - 6

Header Box Drain 1" - IPS - 2

Stack Drain 1 1/2" IPS - 1

Coil Drains NONE

Other

MECHANICAL DESIGN CONDITIONS (CONT'D)

Painting and Galvanizing Requirements: HEATER STEEL: SURFACE PREP. SSPC-SP3,
PAIN 1.5 MILS MIN. DFT., To. FEDERAL SPEC TT-P-86, TYPE II
2) PLATFORMS, LADDERS, STAIRS AND LIGHT STRUCTURAL-
GALVANIZED PER SPEC S-2M
3) STACKS, METALLIZED ON EXTERIOR USING THE METCO 120 SYSTEM

Are Painter's Trolley and Rail Included? NONE
 Extent of Tube-Handling Facilities NONE
 Explosion Doors: Location and Size 2 - 18" x 18"
 Special Equipment (Soot Blowers, Air Preheaters, Noise Suppressors, Fans, Etc.)
1) 18 - TUBE SKIN THERMOCOUPLES
2) 4 - ROTARY SOOTBLOWERS W/ AUTOMATIC CONTROL PANEL
3) 1 - NOISE PLENUM

COMBUSTION DESIGN CONDITIONS

Type of Fuel	OIL	GAS
* Excess Air: Percent	30%	20%
* Guaranteed Efficiency: Percent (LHV) (See Note)	81.0	
* Calculated Efficiency: Percent (LHV)	82.0	
* Radiation Loss: Percent of Heat Release (LHV)	1.5	
* Flue Gas Temperature, Deg F: Leaving Radiant Section	1530	
* Flue Gas Temperature, Deg F: Leaving Convection Section	670	650
* Flue Gas Mass Velocity Through Convection Section Lb/Sq Ft/Sec	0.44	0.40
* Draft at Bridge Wall, In. H ₂ O 30% EXCESS AIR & 120% OF DESIGN	0.10	
* Draft at Burners, In. H ₂ O	0.45	
* Ambient Air Temperature, Deg F	60	
* Altitude, Ft Above Sea Level	95	
* Calculated Heat Release, MM Btu per Hr (LHV)	98.8	
* Volumetric Heat Release, Btu per Hr per Cu Ft		

Note: A fuel saving of _____ MM Btu per hr will offset a \$1,000 increase in furnace cost (erected).

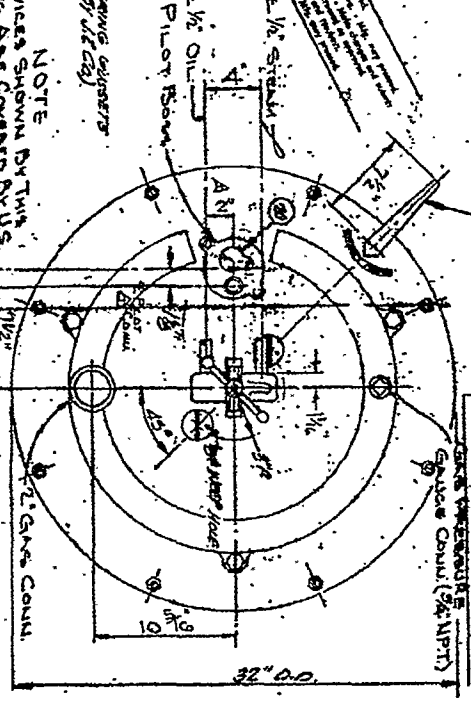
A tube side pressure decrease of _____ psi will offset a \$1,000 increase in furnace cost (erected).

FUEL CHARACTERISTICS

Type of Fuel	OIL		GAS	
	MAX.	NORM. MIN.	MAX.	NORM. MIN.
* Heating Value: HHV	18,560		1713	1211
* Heating Value: LHV	17,000		1542	1090
* See Fuel Data Sheet				
REFINERY FUEL GAS:				
PRESSURE PSIG	70	60	47	
SPECIFIC GRAVITY	1.095	0.83	0.64	
FUEL OIL:				
PRESSURE PSIG	250	235	200	
TEMP °F	310	280	250	
API GRAVITY	12	10	10	
VISCOSITY SSU @ 70°F	95-102	150-170	280-320	
SULFUR, PERCENT (BY WT)		1.2		

FUEL PRESSURES ARE UPSTREAM OF CONTROL VALVE

7-2-2 SPE FORM 370F (5/77)



MOUNTING DETAIL

22

Header 3B-F3

[illegible]

7.4 HEAT EXCHANGERS

TABLE OF CONTENTS
SECTION 7.4 HEAT EXCHANGERS

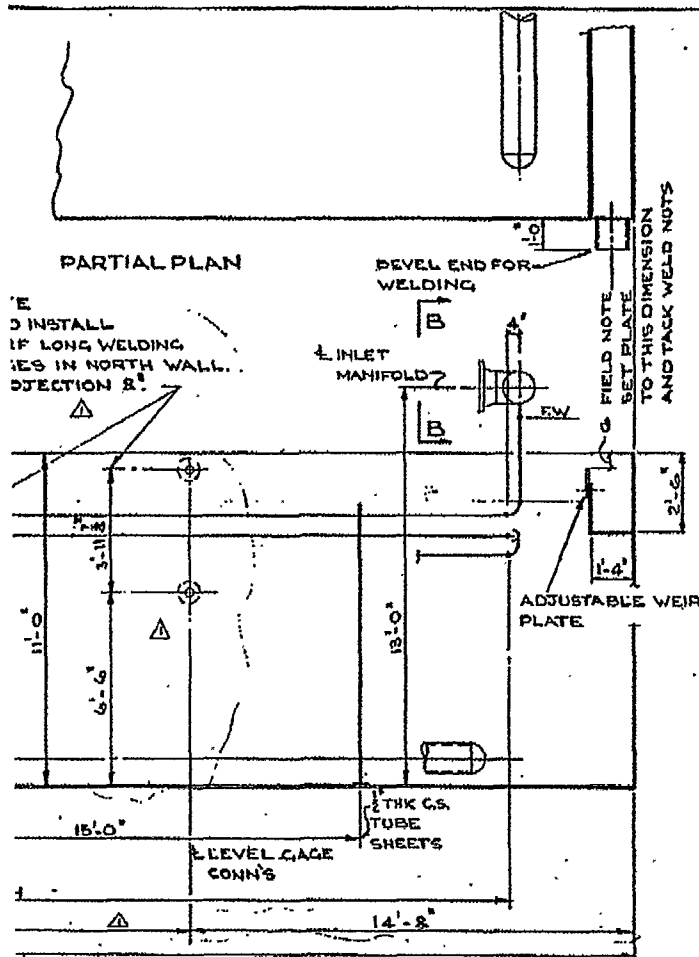
Data Sheet	Emergency Cooler	3B-E40
3B-E40	Emergency Cooler	3-DE-1

EXCHANGER SPECIFICATION SHEET

1	CUSTOMER AND PROJECT LOCATION TEXACO INC.		EXCHANGER MFR. SEATTI CO.	
2	PLANT PUGET SOUND		REQ. NO. E-61	
3	EXCHANGER NO. 3B-E40		ITEM NO. 1	
4	SERVICE OF UNIT EMERGENCY COOLER			
5	SIZE	TYPE	CONNECTED IN	SERIES
6	SURFACE PER UNIT 11,000	EFF. 44 SHELLS PER UNIT ONE	SURFACE PER SHELL	EFF. 44 GR.
PERFORMANCE OF ONE UNIT				
7	FLUID CIRCULATED WATER		TUBE SIDE GAS OIL	
8	TOTAL FLUID ENTERING 1,800,000	473,371		
9	VAPOR			
10	LIQUID	473,371		
11	STEAM			
12	NON-CONDENSIBLES			
13	FLUID VAPORIZED OR CONDENSED			
14	STEAM CONDENSED			
15	GRAVITY - LIQUID API	25.6		
16	VISCOSITY - LIQUID CP	0.44 @ 750°F 1.5 @ 380°F		
17	MOLECULAR WEIGHT - VAPORS			
18	SPECIFIC HEAT - LIQUIDS	BTU/°F		BTU/°F
19	LATENT HEAT - VAPORS	BTU/°F		BTU/°F
20	TEMPERATURE IN 50	°F		750
21	TEMPERATURE OUT 150	°F		250
22	OPERATING PRESSURE PSIG			
23	NUMBER OF PASSES	6		
24	VELOCITY	FT/SEC		5.8
25	PRESSURE DROP ALLOW/GALC	#/SQ IN.		20/20
26	FOULING RESISTANCE MIN			
27				
28	HEAT EXCHANGED - BTU/HR 180,000,000	M.T.D. (CORRECTED)		325
29	TRANSFER RATE - SERVICE 50	CLEAN		ACTUAL FOULING FACTOR
CONSTRUCTION				
30	DESIGN PRESSURE	#/SQ IN.		150
31	TEST PRESSURE	#/SQ IN.		315
32	DESIGN TEMPERATURE	°F		800
33	TUBES C.S. A-53 Gr B NO 234	O.D. 0.45		LENGTH 40'-0"
34	SHELL	I.D. O.D.		PITCH 8" A-B-C
35	SHELL COVER	THICKNESS		
36	CHANNEL	FLOATING HEAD COVER		
37	TUBE SHEETS - STATIONARY C.S. 1/2" THK	CHANNEL COVER		
38	BAFFLES - CROSS	FLOATING		
39	BAFFLE - LONG	THICKNESS		
40	TUBE SUPPORTS	THICKNESS		
41	GASKETS	THICKNESS		
42	CONNECTIONS - SHELL - IN	OUT		RATING
43	-CHANNEL-IN	OUT		RATING
44	CORROSION ALLOWANCE - SHELL SIDE	TUBE SIDE		
45	CODE REQUIREMENTS	TENA CLASS		SPEC. E-109
46	WEIGHTS - EACH SHELL	BUNDLE		FULL OF WATER
47	NOTE INDICATE AFTER EACH PART WHETHER STRESS RELIEVED (S R) AND WHETHER RADIOGRAPHED (X-R)			
48	REMARKS - FOR ADDITIONAL INFORMATION SEE DRAWING 10095-3-DE-1			
49				
50				
51				

REV.	DATE	DESCRIPTION
1	3-1-77	ISSUED FOR CONSTRUCTION

JOB NO.	DRWG. NO.	REV.
10095	DS-3-E-19	0



PARTIAL ELEVATION OF SOUTH WALL

DRAIN CONNECTION
PER TEXACO STD
DWG. 75-2574-4 (DET. B)
VALVE & SCRD
FITTINGS BY
BECHTEL

LIST OF MATERIAL

ITEM	QUAN	DESCRIPTION	ORDER NO
1	ONE	EMERGENCY EXCHANGER	E-61

GENERAL NOTES

- FOR LOCATION SEE PLOT PLAN DRAWING 3-RA-42
- BOX TO BE FABRICATED FROM $\frac{1}{4}$ " C.S. & SHIPPED TO SITE IN SECTIONS: FLOOR IN TWO SECTIONS, END WALLS & SIDE WALLS, IN COMPLETE PANELS.

REFERENCE DRAWINGS

PLOT PLAN	3-RA-42
FOUNDATION DETAIL	

ADDED INST CONNECTIONS	ML	CL	MS
ISSUED FOR PURCHASE/CONSTRUCTION	PL	AS	MS
BY	CHK	APP	CHK
DATE			

BECHTEL CORPORATION
SAN FRANCISCO HOUSTON NEW YORK

TEXACO INC.
PUGET SOUND PLANT

ARRANGEMENT OF
EMERGENCY EXCHANGER
3B-E40

	JOB No. BECHTEL - 10005 TEXACO EST - 3010	DRAWING No. 3-DE-1	REV. 1
--	---	-----------------------	-----------

WA-TEX 000923

7.5 PUMPS

TABLE OF CONTENTS
SECTION 7.5 PUMP DATA AND CURVES

Summary Table 7.5-1

Data Sheets - All Pumps

Pump Curves - All Pumps

Table 7.5-1
Centrifugal Pump Summary Sheet
Plant 3B FCC Unit
Anacortes, Washington

Service	Performance Data					Construction Data					Driver Data								
	Flow Temp ° F	GPH @ P.T. Design	Design Flow		Sp. GR @ P.T.	NPSH Feet Required	B.H.P.		Max Wk'g PR PSIG	Material Impeller		No. of Stages	Shaft Seal	Rated H.P.	Type	Full Load Amps			
			Suction	Discharge			Design	Max		Case	Rated						Max.		
Overhead Reflux	100	690	6	63	0.75	7.0	32	36	266	C.I.	C.I.	7-1/16	7-1/2	1	Mech.	3550	36	Turb	-
Slurry Quench	675	2380	11	84	0.76	8.0	142	175	300	11-13 Cr.	11-13 Cr.	15-3/8	16-1/2	1	Pecked	1750	156	Turb	-
Fresh Feed	410	1018	3	130	0.78	9.0	105.5	117	667	Steel	C.I.	10-3/4	13-1/4	1	Mech.	3600	125	Motor	16.8
Spare	410	1018	3	130	0.78	9.0	105.5	117	667	Steel	C.I.	10-3/4	13-1/4	1	Mech.	3550	117	Turb	-

APPLICABLE TO: PROPOSALS ☐ PURCHASE ☐ AS BUILT ☐
NOTE () INDICATES INFORMATION TO BE COMPLETED BY PURCHASER:
☐ BY MANUFACTURER

JOB NO. 10095 ITEM NO. 3B-G50
PURCHASE ORDER NO. 10095-G01
REQUISITION NO. 10095-G01
INQUIRY NO. _____
DATE _____ REVISION _____

FOR	<u>TEXACO INC.</u>	SITE	<u>PUGET SOUND</u>
UNIT	<u>FLUID CATALYTIC CRACKING</u>	SERVICE	<u>FCC FRESH FEED</u>
NO. PUMPS REQ'D	<u>2</u>	NO. MOTORS REQ'D	<u>1</u>
	ITEM NO. <u>28-650</u>	PROVIDED BY	<u>PUMP MAINTD BY FIELD</u>
	NO. TURBINES REQ'D	ITEM NO. <u>28-650A</u>	PROVIDED BY
			<u>EXISTING</u>
PUMP MFR	<u>BYRON JACKSON</u>	SIZE AND TYPE	<u>4X6X13/4H DST</u>
		SERIAL NO.	<u>731-H-0013/12</u>

OPERATING CONDITIONS, EACH PUMP				PERFORMANCE	
LIQUID	<u>FCC FEED</u>	U.S. GPM at PT. NOR.	<u>1018</u>	RATED	PROPOSAL CURVE NO. <u>2771-1</u>
		DISCH. PRESS. PSIG	<u>130</u>		RPM <u>3550</u> NPSHR (WATER) <u>9</u>
PT. F. NOR.	<u>410</u>	MAX. SUCT. PRESS. PSIG	<u>MAX.</u>	RATED	EFF. <u>71%</u> BHP RATED <u>105.5</u>
SP GR at PT.	<u>0.78</u>	DIFF. PRESS. PSI	<u>126.6</u>		MAX. BHP RATED IMP <u>11.7</u>
VAP PRESS. at PT. PSIA	<u>11.8</u>	DIFF. HEAD, FT	<u>375</u>		MAX HEAD RATED IMP <u>480</u>
VIS. at PT. SS#	<u>CP 10</u>	NPSHA FT.	<u>2. CORRECTED</u>		MIN. CONTINUOUS GPM <u>110</u>
CORR/EROS CAUSED BY		HYD. HP			ROTATION (VIEWED FROM CPLG END) <u>CCW</u>

CONSTRUCTION					SHOP TESTS	
NOZZLES	SIZE	RATING	FACING	LOCATION	☒ NON-WIT PERF	☐ WIT PERF
SUCTION	6	300#	RF	TOP	☐ NON-WIT HYDRO	☒ WIT HYDRO
DISCHARGE	4	300#	RF	TOP	☐ NPSH REQ'D	☐ WIT NPSH

CASE-MOUNT ☒ CENTERLINE ☐ FOOT ☐ BRACKET ☐ VERT (TYPE) _____

SPLIT ☐ AXIAL ☒ RAD. TYPE VOLUTE ☐ SGL ☐ DBL ☐ DIFFUSER

PRESS ☐ MAX. ALLOW. 667 PSIG 60 F. ☐ HYDRO TEST 1000 PSIG

CONNECT ☒ VENT ☐ BRAIN ☐ GAGE

IMPELLER DIA ☐ RATED 10 9/16 ☐ MAX 13 1/4 ☐ TYPE D.5

MOUNT ☐ BETWEEN BRGS ☒ OVERHUNG ☐ WEAR. WG. DIAM./CLINC. 0.023

BEARINGS-TYPE ☐ RADIAL ND-3214LR ☐ THRUST ND 45312LIA

LUBE ☐ RING OIL ☐ FLOOD ☐ OIL MIST ☒ DELINGER ☐ PRESSURE

COUPLING ☐ MRF FAST ☐ MODEL B

DRIVER HALF MTD BY: ☐ PUMP MFR ☐ DRIVER MFR ☒ PURCHASER

PACKING: ☐ MFR & TYPE _____ ☐ SIZE/NO. OF RINGS _____

MECH. SEAL: ☐ MFR & MODEL BW-QB ☐ API CLASS CODE B5TEJ

☐ MFR CODE QB-2500-504K

SHOP TESTS	
☒ NON-WIT PERF	☐ WIT PERF
☐ NON-WIT HYDRO	☒ WIT HYDRO
☐ NPSH REQ'D	☐ WIT NPSH
☒ SHOP INSPECTION	
☐ DISMANT & INSP AFTER TEST	
☐ OTHER	

MATERIALS	
API CASE/TRIM CLASS	○
GEMS	P-2M7
GEMS	P-2B1
CASE	- F25E4

BASEPLATE. ☐ ESOR

VERTICAL PUMPS

AUXILIARY PIPING

☐ C.W. PIPE PLAN F ☐ CU: ☐ S.S.: ☐ TUBING: ☐ PIPE

☐ TOTAL COOLING WATER REQ'D, GPM 210 ☐ SIGHT F.I. REQ'D

☐ PACKING COOLING INJECTION REQ'D: ☐ TOTAL GPM ☐ PSIG

☐ SEAL FLUSH PIPE PLAN 21 ☒ C.S. ☐ S.S. ☐ TUBING ☒ PIPE SCH 80 WELD SOCK

☐ EXTERNAL SEAL FLUSH FLUID ☐ GPM ☐ PSIG

☐ AUXILIARY SEAL PLAN... ☐ C.S. ☐ S.S. ☐ TUBING ☐ PIPE

☐ AUX. SEAL QUENCH FLUID: WATER QUENCH PIPING BY PUMP MFR

PIT OR SUMP DEPTH ☐ _____

MIN. SUBMERGENCE REQ'D. ☐ _____

COLUMN PIPE ☐ FLANGED ☐ THREADED

LINE SHAFT ☐ OPEN ☐ ENCLOSED

BRGs ☐ BOWL _____ ☐ LINE SHAFT

BRG LUBE ☐ WATER ☐ OIL ☐ GREASE

FLOAT & ROD ☐ CS ☐ SS ☐ BRZ ☐ NONE

FLOAT SWITCH ☐ _____

PUMP THRUST. LB ☐ UP ☐ DOWN

MOTOR DRIVER

HP 125 RPM 3600 FRAME 405MS VOLTS/PHASE/CYCLES 4000 V-3P-60
MFR. A.C. BEARINGS BALL LUBE AS
TYPE HORIZ. INSUL. B FULL LOAD AMPS 16.8
ENC. TEFC TEMP RISE C. 80 LOCKED MOTOR AMPS 110
VHS VSS VERT. THRUST CAP. LB. SERVICE FACTOR 1.0

APPROX WT. PUMP & BASE 2000
MOTOR 2320 TURBINE

API STANDARD 610 GOVERNS UNLESS OTHERWISE NOTED

	3	1-22-74	ISSUED FOR CONSTRUCTION							
	2	1/15/73	REVISED SEAL FLUSH PLAN	UT				JOB NO	DRAWING NO	REV.
	1	12/26/72	ISSUED FOR PURCHASE	UT	704			10095	DS-38-G-1	3
	0	10/2/72	ISSUED FOR QUOTATION	UT						
	NO	DATE						SHEET ..	1	OF .. 1



WA-TEX 000927

CENTRIFUGAL PUMP DATA SHEET

APPLICABLE TO: PROPOSALS ☐ PURCHASE ☐ AS BUILT ☐
 NOTE () INDICATES INFORMATION TO BE COMPLETED BY PURCHASER:
☐ BY MANUFACTURER

JOB NO. 10095 ITEM NO. 3B-G2
 PURCHASE ORDER NO. _____
 REQUISITION NO. _____
 INQUIRY NO. _____
 DATE _____ REVISION _____

FOR TEACO, INC. SITE PUGET SOUND
 UNIT ECC UNIT SERVICE OVERHEAD REFLUX
 NO. PUMPS REQ'D _____ NO. MOTORS REQ'D _____ ITEM NO. _____ PROVIDED BY _____ MTD BY _____
 NO. TURBINES REQ'D 1 ITEM NO. 3B-G2 PROVIDED BY _____ MTD BY _____
 PUMP MFR UNITED SIZE AND TYPE 4" TC-AA SERIAL NO. 74799/800 SPARE

OPERATING CONDITIONS, EACH PUMP				PERFORMANCE	
LIQUID <u>GASOLINE</u>	U.S. GPM @ PT. NOR. <u>690</u>	RATED _____	DISCH. PRESS., PSIG <u>62.6</u>	PROPOSAL CURVE NO. _____	
PT. F. NOR <u>100</u>	MAX _____	SUCT. PRESS., PSIG MAX _____	RATED <u>6.0</u>	RPM <u>3550</u> NPSHR (WATER) _____	
SP GR @ PT <u>0.75</u>	DIFF. PRESS., PSI <u>56.6</u>			EFF. <u>73.5</u> BHP RATED <u>32</u>	
VAP PRESS. @ PT. PSIA <u>16.2</u>	DIFF. HEAD, FT <u>174</u>			MAX. BHP RATED IMP <u>36</u>	
VIS. @ PT. Sgs _____	CP <u>75</u> NPSHA, FT <u>15</u>			MAX. HEAD RATED IMP <u>210</u>	
CORR/EROS CAUSED BY _____ HYD. HP _____				MIN. CONTINUOUS GPM _____	
				ROTATION (VIEWED FROM CPLG END) <u>CCW</u>	

CONSTRUCTION					SHOP TESTS
NOZZLES	SIZE	RATING	FACING	LOCATION	☐ NON-WIT PERF ☐ WIT PERF
SUCTION	<u>6"</u>	<u>250#</u>	<u>FF</u>	<u>TOP</u>	☐ NON-WIT HYDRO ☐ WIT HYDRO
DISCHARGE	<u>4"</u>	<u>250#</u>	<u>FF</u>	<u>TOP</u>	☐ NPSH REQ'D ☐ WIT NPSH
CASE-MOUNT ☒ CENTERLINE ☐ FOOT ☐ BRACKET ☐ VENT. (TYPE) _____					☐ SHOP INSPECTION
SPLIT ☐ AXIAL ☒ RAD: TYPE VOLUTE ☐ SGL ☒ DBL ☐ DIFFUSER					☐ DISMANT & INSP AFTER TEST
PRESS ☐ MAX ALLOW. <u>266.6</u> PSIG <u>60.0</u> F. ☐ HYDRO TEST <u>400</u> PSIG					☐ OTHER _____
CONNECT ☒ VENT ☒ FRAIN ☐ GAGE					
IMPELLER DIA <u>7 1/16</u> ☒ RATED <u>7 1/2</u> ☐ MAX. <u>7 1/2</u> ☐ TYPE: _____					
MOUNT ☐ BETWEEN BRGS ☒ OVERHUNG ☐ WEAR. RG DIAM./CLRNC _____					
BEARINGS-TYPE ☒ RADIAL <u>BALL</u> ☒ THRUST <u>BALL</u>					
LUBE ☒ RING OIL ☐ FLOOD ☐ OIL MIST ☐ FLINGER ☐ PRESSURE					
COUPLING ☒ MRF <u>EALK</u> ☐ MODEL <u>SPACER TYPE</u>					
DRIVER HALF MTD BY ☐ PUMP MFR ☐ DRIVER MFR ☐ PURCHASER					
PACKING ☐ MFR & TYPE _____ ☐ SIZE/NO. OF RINGS <u>8-3/8"</u>					
MECH SEAL ☐ MFR & MODEL _____ ☐ AM CLASS CODE _____					
☐ MFR CODE _____					

AUXILIARY PIPING				VERTICAL PUMPS
☐ CW PIPE PLAN	☐ CU: ☐ S.S. ☐ TUBING: ☐ PIPE			PIT OR SUMP DEPTH _____
☐ TOTAL COOLING WATER REQ'D, GPM _____	☐ SIGHT F.I. REQ'D _____			MIN. SUBMERGENCE REQ'D ☐ _____
☐ PACKING COOLING INJECTION REQ'D: ☐ TOTAL GPM ☐ PSIG				COLUMN PIPE ☐ FLANGED ☐ THREADED
☐ SEAL FLUSH PIPE PLAN ☐ C.S. ☐ S.S. ☐ TUBING ☐ PIPE				LINE SHAFT ☐ OPEN ☐ ENCLOSED
☐ EXTERNAL SEAL FLUSH FLUID _____ ☐ GPM _____ ☐ PSIG _____				BRGS. ☐ BOWL _____ ☐ LINE SHAFT
☐ AUXILIARY SEAL PLAN _____ ☐ C.S. ☐ S.S. ☐ TUBING ☐ PIPE				BRG. LUBE ☐ WATER ☐ OIL ☐ GREASE
☐ AUX. SEAL QUENCH FLUID _____				FLOAT & ROD ☐ C.S. ☐ S.S. ☐ BRZ ☐ NONE
				FLOAT SWITCH ☐ _____
				PUMP THRUST, LB ☐ UP _____ ☐ DOWN _____

MOTOR DRIVER				APPROX. WT. PUMP & BASE
HP _____	RPM _____	FRAME _____	VOLTS/PHASE/CYCLES _____	MOTOR _____ TURBINE _____
MFR _____	BEARINGS _____	LUBE _____		
TYPE _____	INSUL _____	FULL LOAD AMPS _____		
ENC _____	TEMP INSE C _____	LOCKED MOTOR AMPS _____		
☐ VHS ☐ VSS	VERT THRUST CAP. LB _____	SERVICE FACTOR _____		

API STANDARD 610 GOVERNS UNLESS OTHERWISE NOTED. (1) EXISTING PUMP-INSTALLED NEW
TURBINE DRIVER.

FORM NO. 130 (REVISED APRIL 71)



JOB NO.	DRAWING NO.	REV.
10095	DS-3-G-2	0
SHEET 1 OF 1		

WA-TEX 000928

CENTRIFUGAL PUMP DATA SHEET

APPLICABLE TO: PROPOSALS ☐ PURCHASE ☐ AS BUILT ☐
 NOTE () INDICATES INFORMATION TO BE COMPLETED BY PURCHASER:
☐ BY MANUFACTURER

JOB NO. 10095 ITEM NO. 3B-G3
 PURCHASE ORDER NO. _____
 REQUISITION NO. _____
 INQUIRY NO. _____
 DATE _____ REVISION _____

FOR TEXACO, INC. SITE PUGET SOUND
 UNIT FCC UNIT SERVICE SLURRY QUENCH PUMP
 NO. PUMPS REQ'D _____ NO. MOTORS REQ'D _____ ITEM NO. _____ PROVIDED BY _____ MTD BY _____
 NO. TURBINES REQ'D 1 ITEM NO. 3B-GT3 PROVIDED BY _____ MTD BY _____
 PUMP MFR BINGHAM SIZE AND TYPE 8X10 1/2 CF-H-S SERIAL NO. 33086/87

OPERATING CONDITIONS, EACH PUMP				PERFORMANCE	
LIQUID <u>SLURRY OIL</u>	U.S. GPM at PT. NOR. <u>2380</u>	RATED _____	DISCH. PRESS. PSIG <u>83.7</u>	PROPOSAL CURVE NO. _____	RPM <u>1760</u> NPSH (WATER) <u>27</u>
PT. F. NOR. <u>675</u> MAX.	SUCT. PRESS. PSIG MAX. _____	RATED <u>11</u>	DIFF. PRESS. PSI <u>72.7</u>	EFF. <u>71</u> BHP RATED <u>142</u>	MAX. BHP RATED IMP <u>175</u>
SP GR. at PT. <u>0.763</u>	DIFF. HEAD. FT. <u>220</u>		VAP. PRESS. at PT. PSIA <u>17</u>	MAX. HEAD RATED IMP <u>250</u>	MIN. CONTINUOUS GPM _____
VIS. at PT. <u>43 CSAP</u>	NPSH _A FT. <u>27</u>		COMB/EROS CAUSED BY _____	HYD. HP _____	ROTATION (VIEWED FROM CPLG END) <u>CCW</u>

CONSTRUCTION					SHOP TESTS	
NOZZLES	SIZE	RATING	FACING	LOCATION	☐ NON-WIT PERF	☐ WIT PERF
SUCTION	<u>10"</u>	<u>300"</u>	<u>RT</u>	<u>END</u>	☐ NON-WIT HYDRO	☐ WIT HYDRO
DISCHARGE	<u>8"</u>	<u>300"</u>	<u>RS</u>	<u>TOP</u>	☐ NPSH REQ'D	☐ WIT NPSH
CASE-MOUNT ☒ CENTERLINE ☐ FOOT ☐ BRACKET ☐ VERT. (TYPE) _____					☐ SHOP INSPECTION	
SPLIT ☐ AXIAL ☐ RAD: TYPE VOLUTE ☐ SGL ☒ DBL ☐ DIFFUSER					☐ DISMANT & INSP AFTER TEST	
PRESS ☐ MAX ALLOW. <u>300</u> PSIG <u>60°</u> F. ☐ HYDRO TEST <u>450</u> PSIG					☐ OTHER _____	
CONNECT ☒ VENT ☐ DRAIN ☐ GAGE						
IMPELLER DIA ☐ RATED <u>15 3/8</u> ☐ MAX. <u>16 1/2</u> ☐ TYPE <u>CLOSED</u>						
MOUNT ☐ BETWEEN BRGS ☒ OVERHUNG ☐ WEAR. RS. DIAM./CLING _____						
BEARINGS-TYPE ☐ RADIAL <u>BALL</u> ☐ THRUST <u>BALL</u>						
LUBE ☒ RING OIL ☐ FLOOD ☐ OIL MIST ☐ FLINGER ☐ PRESSURE						
COUPLING ☐ MRF <u>FALK</u> ☐ MODEL <u>SPACER TYPE</u>						
DRIVER HALF MTD BY: ☐ PUMP MFR ☐ DRIVER MFR ☐ PURCHASER						
PACKING: ☐ MFR & TYPE _____ ☐ SIZE/NO. OF RINGS _____						
MECH. SEAL ☐ MFR & MODEL _____ API CLASS. CODE _____						
☐ MFR CODE _____						

AUXILIARY PIPING		VERTICAL PUMPS	
☐ C.W. PIPE PLAN	☐ CU: ☐ S.S.; ☐ TUBING: ☐ PIPE	PIT OR SUMP DEPTH ☐ _____	MIN. SUBMERGENCE REQ'D ☐ _____
☐ TOTAL COOLING WATER REQ'D, GPM _____	☐ SIGHT FL. REQ'D _____	COLUMN PIPE: ☐ FLANGED ☐ THREADED	LINE SHAFT ☐ OPEN ☐ ENCLOSED
☐ PACKING COOLING INJECTION REQ'D: ☐ TOTAL GPM _____ ☐ PSIG _____	☐ SEAL FLUSH PIPE PLAN _____ ☐ C.S. ☐ S.S. ☐ TUBING ☐ PIPE _____	BRGS: ☐ BOWL _____ ☐ LINE SHAFT _____	BRG LUBE ☐ WATER ☐ OIL ☐ GREASE _____
☐ EXTERNAL SEAL FLUSH FLUID _____ ☐ GPM _____ ☐ PSIG _____	☐ AUXILIARY SEAL PLAN _____ ☐ C.S. ☐ S.S. ☐ TUBING ☐ PIPE _____	FLOAT & ROD ☐ CS ☐ SS ☐ BRZ ☐ NONE	FLOAT SWITCH ☐ _____
☐ AUX. SEAL QUENCH FLUID _____		PUMP THRUST, LB ☐ UP _____ ☐ DOWN _____	

MOTOR DRIVER			
HP _____	RPM _____	FRAME _____	VOLTS/PHASE/CYCLES _____
MFR. _____	BEARINGS _____	LUBE _____	
TYPE _____	INSUL _____	FULL LOAD AMPS _____	
ENC _____	TEMP RISE, C _____	LOCKED MOTOR AMPS _____	
☐ VHS ☐ VSS	VERT. THRUST CAP., LB _____	SERVICE FACTOR _____	

API STANDARD 610 GOVERNS UNLESS OTHERWISE NOTED. (1) EXISTING PUMP-INSTALLED NEW
TURBINE DRIVER.

FORM NO 130 REVISED APRIL 71



JOB NO.	DRAWING NO.	REV.
10095	DS-3-G-3	0
NO.	DATE	SHEET 1 OF 1

WA-TEX 000929

7.6 INSTRUMENTS

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Control Valve Data Sheets	

TABLE 7.6-1
RELIEF VALVE SUMMARY SHEET
PLANT 3B FCC UNIT
ANACORTES, WASHINGTON

<u>Tag No.</u>	<u>Service</u>	<u>Size</u>	<u>Set Press</u>
3PSV-127A	3B-F3	6" x 3"	114 PSIG
3PSV-127B	"	"	"
3PSV-630	3B-GT3	3" x 4"	300 PSIG
3PSV-634	3B-GT2	1-1/2" x 2-1/2"	65 PSIG

TABLE 7.6-2
 RESTRICTION ORIFICE SUMMARY SHEET
 PLANT 3B FCC Unit
 ANACORTES, WASHINGTON

<u>Tag No.</u>	<u>Service</u>	<u>Location</u>	<u>Line Size</u>	<u>Orifice Size</u>	<u>Flow Rate</u>
3FO-608	Lt. Cycle Oil	3B-0-218	2"	0.433	-
3FO-610	Flushing Oil	4B-0-372	2"	0.433	-
3FO-611	Fuel Oil	3B-0-228	1-1/2"	0.234	14 GPM

WA-TEX 000935

TABLE 7.6-3
FLOW ELEMENT SUMMARY SHEET
PLANT 3B FCC UNIT
ANACORTES, WASHINGTON

Flow Element No.	Service	Orifice Size	Line Size	Meter Coefficient
3FE-600	3B-F3 Feed	6.773	10" Sch 40	300 BPH
3FE-601	" "	2.489	4" Sch 80	40 BPH
3FE-602	" "	"	"	"
3FE-603	" "	"	"	"
3FE-604	" "	"	"	"
3FE-607	Fuel Gas to 3B-F3	3.681	6" Sch 40	20000 SCFH
3FE-620	3B-F3 Feed	2.489	4" Sch 80	40 BPH
3FE-621	" "	"	"	"

TABLE 7.6-4
ALARM AND SHUTDOWN SETTINGS
PLANT 3B FCC UNIT
ANACORTES, WASHINGTON

Alarm No.	Switch No.	Service	Switch Location	Switch Function	Switch Activates at	Switch Actuated by:	Switch Set Point	Remarks
3TAH-300	3TSH-300	3B-F3 Heater	IN TR-300	High Temp.		Mechanical		
3TAL-302	3TSL-302	3B-F3 Outlet	Main Panel	Low Temp.	5.4 PSIG	Inst. Air	5.4 PSIG	In Bristol Recorder
3TAH-304	3TSH-304	3B-E40 Outlet	Main Panel	High Temp.		Thermocouple	750°F	
3TAH-305	3TSH-305	3B-F3 Stack	Main Panel	High Temp.		Thermocouple	750°F	
3PALL-600	3PSLI-600	3B-F3 F.O. HDR.	Main Panel	Low Pressure	5.4 PSIG	Inst. Air	5.4 PSIG	
3HA-601	3HS-601	3B-F3 Heater	Main Panel	Shutdown Alarm		P/B		
3PAL-602	3PSL-602	3B-F3 Fuel Oil	Main Panel	Shutdown Alarm	5.4 PSIG	Inst. Air	5.4 PSIG	
3FAL-606	3FSL-606	3B-F3 Feed	Main Panel	Low Flow		Inst. Air		
3FALL-606	3FSL-606	3B-F3 Feed	Main Panel	Shutdown Alarm		Inst. Air		
3PAL-607	3PSL-607	3B-F3 Fuel Gas	Main Panel	Low Press	5.4 PSIG	Inst. Air	5.4 PSIG	
3FALL-622	3FY-622	3B-FB Heater	Main Panel	Shutdown Alarm		Relay Cont.		
3FAL-624	3FSL-620	3B-F3-Pass #1	Main Panel	Low Flow	5.4 PSIG	Inst. Air	5.4 PSIG	
3FAL-624	3FSL-621	3B-F3-Pass #2	Main Panel	Low Flow	5.4 PSIG	Inst. Air	5.4 PSIG	
3FAL-624	3FSL-601	3B-F3-Pass #3	Main Panel	Low Flow	5.4 PSIG	Inst. Air	5.4 PSIG	
3FAL-624	3FSL-602	3B-F3-Pass #4	Main Panel	Low Flow	5.4 PSIG	Inst. Air	5.4 PSIG	
3FAL-624	3FSL-603	3B-F3-Pass #5	Main Panel	Low Flow	5.4 PSIG	Inst. Air	5.4 PSIG	
3FAL-624	3FSL-604	3B-F3-Pass #6	Main Panel	Low Flow	5.4 PSIG	Inst. Air	5.4 PSIG	
3FAL-641	3PSL-641	3B-F3 Fuel Gas	Main Panel	Low Press	5.4 PSIG	Inst. Air	5.4 PSIG	
3PAL-679	3PSL-679	Soot Blower Purge	Main Panel	Low Press		Inst. Air		

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FORM NO. 1-65 (12/64)

		FLUID																							
		INLET PSIG	MIN.	OPER.	MAX.																				
		OUTLET PSIG	MIN.	OPER.	MAX.	100									200										
		INLET TEMP. °F	OPER.		MAX.	521								280											
SERVICE CONDITIONS		OPER. SP. GR.	VAPOR MOL. WT.		0.735									12.92											
		Tot °F or % FLASH	OPER. VISC. C.P.			54									6.6P										
		CRIT. PRESS. P _c	VAPOR PRESS. P _v																						
		OPER. FLOW	SIZING FLOW		145	300									13	18									
		MIN. FLOW	MAX. FLOW																						
		FLOW UNITS	ΔP SIZING		GPM	25									GPM	110									
		ΔP SHUT OFF	ΔP MIN.		150										300										
		Cv @ SIZING ΔP & FLOW	MIN. Cv		616										1.64										
		Cv-VALVE SELECTED	FACTORS		12.9										3.22										
								Km = 59								Km = 70									
VALVE BODY		SIZE	TYPE		2" GLDGE									1" GLDGE											
		PRESS. RATING	CONNECTIONS		300	RT																			
		MATERIAL	CLASS		C.S.																				
		BONNET TYPE	BOLTS		ERT	STD									PLAIN	STD.									
		PACKING	TYPE	MAT'L	TEFLON	ROBUST																			
		LUBRICATOR	ISOL. VALVE		YES	YES																			
TRIM		PORT SIZE	NO. OF PORTS		FULL	BLD								3/8"	1										
		CHARACTER.	PLUG TYPE		LIN.	CAGE									= 90	M. FORM									
		GUIDE TYPE	TRIM SPEC.			A																			
		ACTION PUSH TO	OPEN-CLOSE	FLOW: OPENS-CLOSES		CLOSE	CLOSE							CLOSE	OPEN										
ACTUATOR		ACTUATOR TYPE				DIAP.																			
		MOTIVE POWER	LINEAR / ROTARY		RIC	LIN.																			
		PRESS./VOLTAGE	POS. ON POWER FAIL		-	3									-	C									
		THRUST OR TORQUE REQ.	SHUT OFF OPER.																						
		SIZE	MAX. OUTPUT		40										30										
		MANUAL O'RIDE	POS. FEEDBACK TYPE		-	-																			
		POSITIONER OUTPUT	SINGLE/DUAL		3-15	S																			
		INPUT SIGNAL	SUPPLY PSIG		3-15	20									3-15	-									
		BY-PASS	GAUGES		YES	YES																			
MISC.																									
		AIRSET MTD & PIPED				YES																			
		M. R. / P. O. NUMBER				J-411																			
		MANUFACTURER				FISHER																			
GENERAL		MODEL NO.				657 ED								667 ES											
		P. & I. D. NUMBER				3-PA-41								3-PA-41											
		SERVICE				REACTOR FEED								FUEL OIL TO REACTOR											
		LINE SIZE - NO. - SPEC.				4" J117A				4" J117A				4" J117A				4" J117A				2" J113A			
		INSTRUMENT TAG NO.				3FV-601				3FV-602				3FV-603				3FV-604				3FV-606			
NO.		1 3-17-62, REVISION								JT 10															
		2 1-31-75 ISSUED FOR PURCHASE								1-10-78															
		REVISIONS																							
ORIGIN R&C ENG.						CONTROL VALVES								JOB NO. 10095 DATA SHEET NUMBER REV. DS-3-126 4											
						TEXACO EST 3910 PULP & PAPER PLANT 30553																			

WA-TEX 000938

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FORM NO. 1050 (8/69)

SERVICE CONDITIONS		FLUID		INLET PRIG		MIN. OPER. MAX.		250		30		60					
		OUTLET PRIG		MIN. OPER. MAX.		247		8		15							
INLET TEMP. °F		OPER. MAX.		500		70		70									
OPER. SP. GR.		Vapor MOL. WT.		-		13		60		8.3		24.1					
TEMP °F or % FLASH		OPER. VISC. CP.		94°F													
CRIT. PRESS. P _c		VAPOR PRESS. P _v															
OPER. FLOW		SIZING FLOW		7450		10400		31000		108M		151M					
MIN. FLOW		MAX. FLOW															
FLOW UNITS		ΔP SIZING		18/HR		3		6PM		32		52FH		4H			
ΔP SHUT OFF		ΔP MIN.		150		C=21		60		75							
Cv @ SIZING ΔP & FLOW		MIN. Cv		Cv=200				767		1920							
Cv-VALVE SELECTED		FACTORS		Cv=255				843		19600							
				C1=30.4		KM=1.85		C1=34.4									
NOISE - DBA				44.6				87		ARBITRARY SIZING							
SIZE		TYPE		3" GLOBE		3" GLOBE		2" GLOBE		3" BALL		2" BALL					
PRESS. RATING		CONNECTIONS		3" RF													
MATERIAL		CLASS		3.5													
BONNET TYPE		BOLTS		5/8" 5-7C		P.A.N 5-7C											
PACKING		TYPE		TEFLON		TEFLON											
LUBRICATOR		ISOL. VALVE		YES		YES											
PORT SIZE		NO. OF PORTS		FILL 1		FILL 3				FULL 1							
CHARACTER.		PLUG TYPE		2.5. CAGE		LIN T.P.		MOD CAGE		CAGE		BALL					
GUIDE TYPE		TRIM SPEC.		A		C											
ACTION PUSH TO		FLOW: OPENS-CLOSES		CLOSE OPEN													
ACTUATOR TYPE				P.O.P.		DIAP.											
MOTIVE POWER		LINEAR / ROTARY		AIR LIN.													
PRESS./VOLTAGE		POS. ON POWER FAIL		-		C											
THRUST OR TORQUE REQ.		SHUT OFF OPER.															
SIZE		MAX. OUTPUT		40		60		40									
MANUAL O'RIDE		POS. FEEDBACK TYPE		-		-											
POSITIONER OUTPUT		SINGLE/DUAL		-		-		3-15		5		-		-			
INPUT SIGNAL		SUPPLY PRIG		ON-OFF 60		-		3-15		20		ON-OFF 60					
BY-PASS		GAUGES		-		-											
MISC.				SIDE MOUNT				FISHER 650									
				HANDWHEEL				60° JATOL									
PURCH.				BIRSET MTO 3 PIPED		YES											
				M. R. / P. O. NUMBER		J-411											
				MANUFACTURER		FISHER											
				MODEL NO.		471-5-6V-ES		657 A		667 A		521-55-D-25					
				P. & I. D. NUMBER		3-FA-41		3-FA-41		3-FA-41		3-FA-41					
				SERVICE		3-FA-41		3-FA-41		3-FA-41		3-FA-41					
						3-FA-41		3-FA-41		3-FA-41		3-FA-41					
				LINE SIZE - NO. - SPEC.		3" J34		10" J03B		6" J16		6" J16		2" J13A			
				INSTRUMENT TAG NO.		32V-643		32VSL-4VM		32V-641		32V-607		32V-604			
				1 3-775		GEN REVISION		JTB									
				0 1-3175		ISSUED FOR PLE-MASE		JTB									
				NO. DATE		REVISIONS											
				ORIGIN R&C ENG.				CONTROL VALVES		JOB NO. 10095		DATA SHEET NUMBER		REV.			
												DS-3-127		1			

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SERVICE CONDITIONS		FLUID		STEAM			
INLET PSIG	MIN. OPER. MAX.			40	250	100	
OUTLET PSIG	MIN. OPER. MAX.			36		75	
INLET TEMP. °F	OPER. MAX.			150	500	521	
OPER. SP. GR.	VAPOR MOL. WT.			0.65	10	0.735	-
Tot °F or % FLASH	OPER. VISC. C.P.						
CRIT. PRESS. P _c	VAPOR PRESS. P _v						
OPER. FLOW	SIZING FLOW			1400	2000	8000	11200
MIN. FLOW	MAX. FLOW						
FLOW UNITS	ΔP SIZING			4	1/4	70	GPM
ΔP SHUT OFF	ΔP MIN.						150
Cv @ SIZING ΔP & FLOW	MIN. Cv			840	670		52
Cv-VALVE SELECTED	FACTORS			843	675		72.9
				K _m = .75			K _m = .59
					C _v = 32		
SIZE	TYPE	8" GLOBE	8" GLOBE	1 1/2" GLOBE	2" GLOBE		
PRESS. RATING	CONNECTIONS	300# RF			300# RF		
MATERIAL	CLASS		5/8" B. C.S.	C.S.	C.S.		
BONNET TYPE	BOLTS		EXT STD		EXT STD		
PACKING	TYPE MAT'L		Teflon		Teflon		
LUBRICATOR	ISOL. VALVE		YES	YES	YES	YES	
PORT SIZE	NO. OF PORTS		FULL 2		RED BALD		
CHARACTER.	PLUG TYPE		LINE T.P.	Q.D. CAGE	LINE CAGE		
GUIDE TYPE	TRIM SPEC.		E	A	A		
ACTION PUSH TO	FLOW: OPENS-CLOSES		CLOSE OPEN	CLOSE OPEN	CLOSE OPEN		
			P.O.P.	DIAP.			
MOTIVE POWER	LINEAR / ROTARY		AIR LIN				
PRESS./VOLTAGE	POS. ON POWER FAIL				C		0
THRUST OR TORQUE REQ.	SHUT OFF OPER.						
SIZE	MAX. OUTPUT		86	40	40		
MANUAL O'RIDE	POS. FEEDBACK TYPE						
POSITIONER OUTPUT	SINGLE/DUAL		3-15 S		3-15 S		
INPUT SIGNAL	SUPPLY PSIG		3-15 70	IN-OFF 60	3-15 70		
BY-PASS	GAUGES		YES YES	NO NO	YES YES		
MISC.		REMOVE EXISTING VALVE ON P. 10					
AIRSET MTD & PIPED		2-FA-4. NEW	YES	YES	YES		
M. R. / P. O. NUMBER		SAME, SAME	J-411	J-411	J-411		
MANUFACTURER			FISHER	FISHER	FISHER		
MODEL NO.		TAG NO.	476D-A	657 ED	657 ED		657 ED
P. & I. D. NUMBER			3-RA-41	3-RA-41	3-RA-41		
SERVICE			REACTOR FEED TO 3R-E-40	FEED TO RX RISER	SYM TO 500T BLOWER		REACTOR FEED TO E-3
LINE SIZE - NO. - SPEC.			10" J14B	10" J113A	2" J34	4" J117A	4" J117A
INSTRUMENT TAG NO.			3PCL-14VB	3PCL-14VM	3PV-65B	3FV-620	3FV-621
NO.	DATE	REVISIONS					
2	10-24-73	REVISED 3PCL-14VN	JTL				
1	3-7-73	CON. REVISION	JT				
0	11-31-73	ISSUED FOR PURCHASE	J. TA				
ORIGIN R&C ENG.	CONTROL VALVES				JOB NO. 10095	DATA SHEET NUMBER REV.	
	BECHTEL				10095	DS-J-120	2