



DATE February 7, 1984

SUBJECT Incident at VCM-II

The incident occurred shortly after the EC plant was shut down. VCM-II HCl production (from VCM) and consumption (to OHC) had been essentially balanced. When EC shut down, 50-60 TPD of HCl was put to the VCM-II atmospheric scrubber. Apparently a good bit of VCM had been put into the header during the upset at VC-I earlier in the day. When the vinyl hit our scrubber, it vaporized rapidly. The demister was torn apart and blown out the top of the scrubber in many pieces. The scrubber will be inspected during the upcoming outage to assess further damage. At 9:00 AM on 2/7, the scrubber boot was still completely iced up, indicating that it was still completely full of liquid VCM. We were very fortunate the cloud did not find an ignition source.

ATTACHMENTS

Air Monitor Report
PLC Message Report
VCM-II OHC Logbook Entries

DISTRIBUTION

~~F. Ortiz~~
P. Trew

AVERAGE for
24 hr. period

ppm or %

TIME OF
MAX. CONC.

AVERAGE READINGS
VC AREA MONITOR
V.C.

SL 049473

DAILY REPORT 08:00 02/07/1984 R1 - 5.00M R2 - 10.00M R3 - 50.00M

STREAM	Avg CONC	LAST READING	MAX CONC	Tmax	R1	R2	R3	R3
1 AI Pump	2.65M	0.10M	113.53M	21:14	73	5	0	1
2 AL Pump	0.82M	44.47B	19.33M	21:15	77	1	1	0
3 LI. Pump	1.54M	34.24B	53.83M	21:17	74	4	0	1
4 Lact. Inoculum	1.77M	34.60B	51.83M	21:18	75	0	3	1
5 Abs. Conc. Pump	4.81M	43.37B	211.26M	21:19	67	5	5	1
6 P.S. Fe Pump	3.38M	37.70B	88.18M	21:21	64	9	4	1
7 P.S. Rax Pump	0.82M	33.27B	63.14M	21:22	55	9	13	1
8 N.S. NUTS	16.10M	60.83B	975.46M	21:03	58	7	11	2
9 PRODUCT FILTRATE	13.04M	37.74B	641.14M	21:06	60	7	10	1
10 VCM NUTS	34.11M	0.11M	0.19%	21:08	54	7	11	6
11 SHIRT BULLETS	29.41M	0.62M	0.13%	21:27	57	10	9	2
12 SHIRT BULLETS	15.93M	0.13M	744.83M	21:28	75	4	0	2
13 PLANT LAB/CNT. RM	2.67M	0.11M	146.17M	21:12	70	1	1	1
14 S. OF PROD. STN	9.86M	60.58B	568.88M	21:13	66	2	9	1
15	0.00B	0.00B	0.00B	00:00	0	0	0	0

VCM II AREA

AVERAGE READINGS
LOW TEMP STORAGE
V.C.

DAILY REPORT 08:00 02/07/1984 R1 - 5.00M R2 - 10.00M R3 - 50.00M

STREAM	Avg CONC	LAST READING	MAX CONC	Tmax	R1	R2	R3	R3
1	9.88B	0.00B	0.39M	06:15	126	0	0	0
2	0.00B	0.00B	0.00B	00:00	127	0	0	0
3	20.88B	0.00B	0.41M	12:02	126	0	0	0
4	0.22M	0.00B	3.18M	18:24	126	0	0	0
5	74.84B	0.27M	0.77M	07:05	126	0	0	0
6	21.77B	0.00B	0.53M	01:57	126	0	0	0
7	72.75B	0.00B	0.69M	18:28	126	0	0	0
8	54.10B	0.00B	0.83M	06:23	126	0	0	0
9	3.35B	0.00B	0.21M	06:24	125	0	0	0
10	0.00B	0.00B	0.00B	00:00	125	0	0	0
11	0.00B	0.00B	0.00B	00:00	0	0	0	0
12	0.00B	0.00B	0.00B	00:00	0	0	0	0
13	0.00B	0.00B	0.00B	00:00	0	0	0	0
14	0.00B	0.00B	0.00B	00:00	0	0	0	0
15	0.00B	0.00B	0.00B	00:00	0	0	0	0

VAPOR DETECTOR 21:01	43.5	NORTH PROCESS AREA LOW
VAPOR DETECTOR 21:01	47.0	DELUGE DV-9 CONFIRMED OPEN
VAPOR DETECTOR 21:01	51.2	6B-13 THROUGH 19, DOW FURNACE, AND SHIFT STG SCS BYPASSED
VAPOR DETECTOR 21:01	58.7	FURNACE AREA 6A-1 THROUGH 8 AND SCS SYSTEM BYPASSED

VAPOR DETECTOR 21:02	06.2	HYDROSHIELD/REF AREA 6A-9/12 AND FURN SCS BYPASSED
VAPOR DETECTOR 21:02	13.2	VCM/EDC SOUTH AREA 6A-14 BYPASSED
VAPOR DETECTOR 21:02	20.5	VCM/EDC MID AREA 6A-15 THROUGH 17 BYPASSED
VAPOR DETECTOR 21:02	27.9	VCM/EDC NORTH AREA 6A-18 THROUGH 20 BYPASSED
VAPOR DETECTOR 21:02	35.2	CONTROL ROOM VAPOR DETECTOR 6A-24 BYPASSED
VAPOR DETECTOR 21:02	42.6	LAB FRESH AIR VAPOR DETECTOR 6A-23 BYPASSED
VAPOR DETECTOR 21:02	49.3	SOUTH PROCESS AREA LOW
VAPOR DETECTOR 21:02	52.5	HIGH TRIP INITIATED TO DELUGE DV-6 EDC AREA
VAPOR DETECTOR 21:02	55.7	HIGH TRIP INITIATED TO DELUGE DV-7 OHC AREA
VAPOR DETECTOR 21:02	58.9	HIGH TRIP INITIATED TO DELUGE DV-8 OHC AREA
VAPOR DETECTOR 21:05	38.8	DELUGE DV-8 CONFIRMED OPEN
VAPOR DETECTOR 21:07	28.9	DELUGE OFF DV-7 THROUGH DV-14
VAPOR DETECTOR 21:07	36.2	12 SWITCHGEAR ROOM LOW
VAPOR DETECTOR 21:07	41.7	12 SWITCHGEAR ROOM HIGH TRIP INITIATED
		HIGH TRIP INITIATED TO DOW FURNACE

VCM II PLC Alarm
Report

2/6/84 starting
@ 21:01

SL 049474

12 OHC REACTOR 21:12	04.0	02/HCL FLOW RATIO WARNING
VAPOR DETECTOR 21:55	14.1	NORTH PROCESS AREA LOW
11 OHC REACTOR 21:59	49.0	SCS OFF KEYED BYPASS
12 OHC REACTOR 21:59	54.1	SCS SYSTEM OFF KEYED BYPASS
22:00		

12 OHC REACTOR 22:14	31.6	SCS KEY BYPASSED
11 OHC REACTOR 22:31	43.0	SCS KEY BYPASSED
11 OHC REACTOR 22:38	24.4	SCS OFF KEYED BYPASS
12 OHC REACTOR 22:38	29.6	SCS SYSTEM OFF KEYED BYPASS
VAPOR DETECTOR 22:42	13.6	FURNACE AREA 6A-1 THROUGH 8 AND SCS SYSTEM OFF BYPASS

493		
VAPOR DETECTOR 22:42	23.7	HYDROSHIELD/REFER AREA 6A-9/12 AND SCS OFF BYPASS
VAPOR DETECTOR 22:42	31.3	VCM/EDC SOUTH AREA 6A-14 OFF BYPASS
VAPOR DETECTOR 22:42	38.3	VCM/EDC MID AREA 6A-15 THROUGH 17 OFF BYPASS
VAPOR DETECTOR 22:42	45.7	VCM/EDC NORTH AREA 6A-18 THROUGH 20 OFF BYPASS
VAPOR DETECTOR 22:42	53.2	CONTROL ROOM VAPOR DETECTOR 6A-24 OFF BYPASS
VAPOR DETECTOR 22:43	00.7	LAB FRESH AIR VAPOR DETECTOR 6A-23 OFF BYPASS
VAPOR DETECTOR 22:43	08.2	TB-13 THROUGH 19, DOW FURNACE, AND SHIFT STG SCS OFF BYPASS
23:00		

VAPOR DETECTOR 23:27	05.9	NORTH PROCESS AREA LOW
VAPOR DETECTOR 23:33	02.5	NORTH PROCESS AREA LOW

top piping off of the primary being pulled. We should have been able to route this flow in some manner to keep the structure from icing up and becoming hazardous to us and the reactor operation. It is intended not to have these little surprises surface, but when they do we need to deal with them or if possible.

2-6-84 ~~Down~~ Reuse freeze precaution list if needed.
 Wintree
 Monro
 Reiky

- ① Added 1 drum of Aged P/T to #5 RX.
- ② Computer calculated 1.2 gals of 2020 & 2.7 gals of 2040. Failed to add to CT. Shipped 2 gals 2020 & 3 gals 2040. Note Kamag: We have had to manually add chemicals to CT. When computer would add, we kept our CT spec at closer ranges. We have also had computer read out to have added 29.0 gals of chemical. Is there something that our E... people can do to correct this problem.

Picked up 10 Tons #5 RX.

NOTE: 2015 put low pressure condenser back in service.

2030 EC Down, 50 Ton HCL in system. Have to lower HCL scrubber set point 69" → 65" to get HCL back to VCM II. Cont. next page.

2101 DV-9 tripped. Several high vapor detector alarms in unit, all over. HCl scrubber valve wide open & just barely holding line pressure, DV 8 tripped. Had to cut Vinyl rates quickly to get scrubber valve in control. Looks like some one hit us hard with C_2H_4 or mints in HCl, whatever it was vapor detectors picked it up good.

By $\approx$ 2120 all Vapor detectors clear & DV's reset. Scrubber valve in range Vinyl cutting further to get off scrubber. #6 Rx out of cooling room.

Got High vapor detector trip for #2 SGR point out but everything looks O.K. Door latch does not hold but blower will still come on in manual mode. It is not needed as air conditioner seems to be holding SGR pressure. Called L. Mason, said will check it in the morning.

- 2-7-84 ① Shift Supervisor notified of trouble with 1st shift scrubber & he said that EPA was notified
 Noward ② Rates #5Rx 258 HCL #6Rx 257 HCL Floyd
 Hoyer ③ Shot fed 2 gal 2020 & 3 gal 2040 to Ct.
 Sanford ④ Added 1 drum ni-doped cat to #6 Rx
 ⑤ Cut 10 tons HCL on #5Rx
 ⑥ " 65 ton HCL on #6Rx For Absorbers
 ⑦ Absorbers could not take it right now
 had to raise 55 tons HCL on #6Rx
 KAY to get HCL off scrubber.



TO See Distribution

DATE February 13, 1984

FROM F. Ortiz

SUBJECT VCM Plant Absorber Upset

Location: VCM I

Description of Upset:

On February 6, 1984 Vinyl Chloride, HCl and EDC migrated from the VCM I plant absorber into the Plant B HCl system.

Cause:

1. The loss of lean oil to the absorber. Both pumps had mechanical problems. See Maintenance Foreman's report attached.
2. The introduction of VCM rework to the bottom of the absorber.
3. The introduction of recycle from the Product Still into the bottom of the absorber.

The VCM Stripper steam flow was off. However the recycle EDC from the product still input enough energy to counter-measure the refrigeration available. Only the absorber upper intercooler and absorber condenser was available. The lower intercooler was out for repairs. See the VCM I Foreman's report for details.

Duration:

The lean oil flow was lost from 11:10 A.M. to 3:50 P.M. The organic evolution is speculated to have occurred from 12:00 P.M. until 3:50 P.M.

Quantity:

A total of 12.3 tons of VCM migrated from the absorber into the HCl system. It is estimated that 7.19 tons traveled toward VCM II and 5.104 tons were fed to the Ethyl Chloride plant. See basis for the split in the appendix.

Environmental Impact:

The VCM that entered the EC reactor left the EC plant as byproducts. No releases to the atmosphere were made through the Ethyl Chloride Plant.

The 7.19 tons that traveled to VCM II was distributed as follows:

- a. It is speculated that approximately 2 tons was fed to OHC reactors, due to the slight unbalance on the HCl at VCM II. No environmental consequences.

Therefore

- b. ~~5.19~~ 5.19 tons remained in the HCl system.

Conclusion:

Part or all (it is impossible to say for sure) of the 5.19 tons of VCM that remained in the HCl system as condensed liquid was released when the HCl PCV to the VC-II scrubber was opened. The PCV opened at 21:01 on the 6th. Some liquid VCM trapped in the boot of the scrubber continued to evaporate during the day of the 7th.

Recommendations to Avoid Reoccurrence:

1. Review the incident with all VCM plant operators and front line supervision.
2. Have a policy to cut the HCl flow from the VCM absorbers to the HCl system should its temperature reach 100° for more than 15 minutes. The policy should be incorporated in the SOP manual. Warning notes should be installed on the appropriate temperature recorder.
3. The incident should be incorporated as part of the regular situation response for the VCM operators.
4. Have the VCM II scrubber inlet boots level switch checked. It did not activate during the incident.

/ds

SL 049478

CHEMICALS

INTEROFFICE / LAKE CHARLES

TO F. Ortiz

DATE February 7, 1984

FROM L. Ware

SUBJECT Lean Oil Pumps VC I

The #1 lean oil pump was pulled at VC I on the morning of 2/6/84. The seal had failed and the EDC that escaped was introduced into the bearing housing. The pump repair required a new seal, bearings, gaskets, and oil seals.

I was notified of the needed repairs by C. Brazitis prior to 7:30 AM. I responded by borrowing Randy Hutchins, a machinist from J. Warden at VCM II. The pump repairs and installation was complete at 3:30 PM.

At approximately 11:00 AM, 2/6/84, I was notified that the #2 lean oil pump had failed. The pump was pulled by R. Burgess. He found that the outboard bearing had frozen up. The necessary repairs and installation was completed on overtime by Burgess at approximately 8:00 PM.

F. Ortiz communicated the urgency of the lean oil pumps' situation to me some time near noon on 2/6/84. I relayed this to Hutchins and he responded with a positive effort.

/bb

SL 049479

TO F. Ortiz

DATE February 7, 1984

FROM J. Gustin

SUBJECT EC Plant Upset

On the morning of 2/6/84, I was informed by the EC operator that he was having problems getting catalyst into the EC reactor. Several attempts were made to shock the catalyst pot to free the catalyst. These attempts were only partially successful. It is not unusual to experience this type of problem. In addition, an incident that occurred on the previous shift led us to believe the catalyst pot was more than likely plugged. Shortly after the lean oil pump shut down in VC I, the operator cleared the catalyst pot of organics. This allowed him to open the pot and with the aid of a board physically broke the surface crust on top of the catalyst. The catalyst pot was then put back in service and it appeared the problem was somewhat resolved. Several heat peaks were witnessed indicating the reactor was indeed getting catalyst. At approximately 2:30 PM the operator started experiencing what was thought to be catalyst addition problems again. The day operator held over to assist the evening operator in trying to unplug what was thought to be a plugged catalyst pot. Pressure in the EC reactor continued to rise slowly. At 8:30 PM the operator cut feeds from the reactor and put the plant on recycle.

Unfortunately, the symptoms of low catalyst levels in the reactor and "foreign" organic feeds to the reactor will be about the same. The vinyl and HCl mix being fed to the reactor will go to DCE in a liquid bed with ferric chloride catalyst. Any EDC fed will act as a heavy and accumulate in the heavy still. Therefore, with the feed mix we were getting it would be very difficult to determine foreign feeds because they would not appear in any of the "in-plant" analysis we sample for.

/bb

SL 049480

CHEMICALS

INTEROFFICE / LAKE CHARLES

TO F. Ortiz DATE February 7, 1984
FROM C. Brazitis SUBJECT Abnormal Operating Incident On
2/6/84

Situation Prior To Incident: VCM I was processing 115 TPD VC from TE II. The furnaces, quench tower and heavies still are down. Day tank rework is going to the bottom of the absorber. Vinyl production is going into the reworking tank. The product still LCV is in service to the heavies still feed tank. Heavies feed tank material is being recycled by the heavies feed pumps back to the bottom of the absorber. The #1 lean oil pump was pulled earlier on day shift for a seal leak that occurred on graveyard shift. The #2 lean oil pump was running but it was reported to be tight when first put on line earlier. The HCl absorbers were consuming VC produced HCl and VCM I is open to the HCl system. The lower intercooler is out of service to replace a pump suction valve. Operations relatively stable.

Incident: At 11:10 AM the #2 lean oil pump tripped off the line. After quick investigation it was realized that the pump had frozen up and would remain inoperable. At this time the transfer from TE II was backed down over a period of several minutes. Once the transfer was blocked off an attempt was made to line up the off gas from the VC absorber to the scrubber. The HCl absorbers had been blocked off when lean oil could not be restored. The scrubber was not able to handle the off gas and would pressurize up to 10-15 psig so the off gas was left in the HCl system. It was thought that at this time there was still HCl evolution from the system. In fact, the incinerator vent system was tripped by WTU at one point for about 10 minutes and most likely this with the result of problems caused by the high vent load due to scrubbing the off gas. The system was left in the HCl header.

The absorber became relatively hot quickly and by noon the off gas temperature was 85°F and still rising. At this time there was an HCl flow on the chart showing on off gas flow. Also, the absorber bottoms flow had diminished and was very near non-existent. The product still feed tank level was decreasing and the heavies still feed tank level was increasing. The stripper steam flow had been cut to zero by the automatic temperature control. The absorber eventually leveled off with tray 35 temperature of 136°F and overhead temperature of 120°F.

The #1 lean oil pump was finished and given back to Operations at approximately 3:30 PM. The pump was put on line at about 3:50 PM. Shortly after this the product still bottoms was routed to the product still feed tank and steam was cut on the product still because of a low level in the still. When the lean oil flow was established the absorber began to cool off slowly and the system pressure began to fall, eventually reaching a low of 60 psig. The system was

SL 049481

F. Ortiz
February 7, 1984
Page 2

blocked off from the HCl system. As the product still fed tank level and product still levels were re-established, steam was introduced back to the product still slowly. Shortly after 4:00 PM the absorber bottoms flow was re-established as the absorber cooled off. Steam was put back to the stripper. By 6:00 PM the system temperature profiles were such that some transfer from TE II was started. The system pressure was allowed to come up to 78# and then it was unblocked to the HCl system.

Attachments

/bb

SL 049482

Appendix

Estimate of VCM Release at VCM II

- ① Integrated flow on the HCL chart out of VCM I during V₁
 $R = 250,000 \text{ SCF}$

$$R = R' \sqrt{\frac{P_{act}}{P_{avg}}} \times \frac{T_{on}}{T_{act}} \sqrt{\frac{Sp_{gr} \text{ HCL}}{Sp_{gr} \text{ VCM}}}$$

$$= 250,000 \sqrt{\frac{94.7}{94.7} \times \frac{-22 + 460}{120 + 460}} \sqrt{\frac{1.28}{2.155}}$$

$$R = 167,434.29 \text{ SCF}$$

Duration of Incident 4.1333 Hrs.

VCM flow out of VCM I = 40,508.62 SCFH.

Amount of VCM Assume Ideality

$$\frac{167,434.29 (14.7) (61.5)}{10.73 \times 520 \times 2,000} = 13.7 \text{ Tons.}$$

VCM from VCM absorber into the HCL system

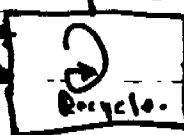
$$= 13.7 \text{ Tons.}$$

II Using Records Number and No Accumulation.

Balance from 7:30 AM to 7:30 AM.

↑ 12.3 Tons Losses.

Tri Ethane Tank
77.8 Tons.



D.T.W.K.

65.5 Tons
Products

Say HCl flow to EC = 45062.5 SCFH

Ucm flow to EC = X

$$\text{Total Flow} = (45062.5 + X) \sqrt{\frac{M_{\text{Ucm}}}{M_{\text{HCl}} = 1}}$$

Assume Ucm flow is 15,000 SCFH

$$R' = 45062.5 + 15,000 = 60062.5 \text{ SCFH}$$

$$M_{\text{Ucm gas}} = 62.5 \frac{15,000}{60062.5} + 36.5 \left(\frac{45062.5}{60062.5} \right)$$

$$M_{\text{Ucm gas}} = 42.98$$

$$R = 60,062.5 \sqrt{\frac{42.98}{36.5}} = 65,179.77$$

65179 SCFH ≈ 65,000 SCFH Trial Sum

The Ucm flow to EC = 15000 SCFH

$$\text{Ucm flow to EC} = \frac{15,000 (14.7) (4.133 \text{ hrs}) (62.5)}{10.73 (520) (2,000)}$$

$$= 5.104 \text{ TONS to EC}$$

$$\text{Ucm towards Ucm II } 12.3 - 5.104 = 7.19 \text{ To}$$

Since Ucm II was running unbalance by 2 TPD

it's ~~possible~~ possible that OHC was fed

As much of 2 TONS of Ucm.

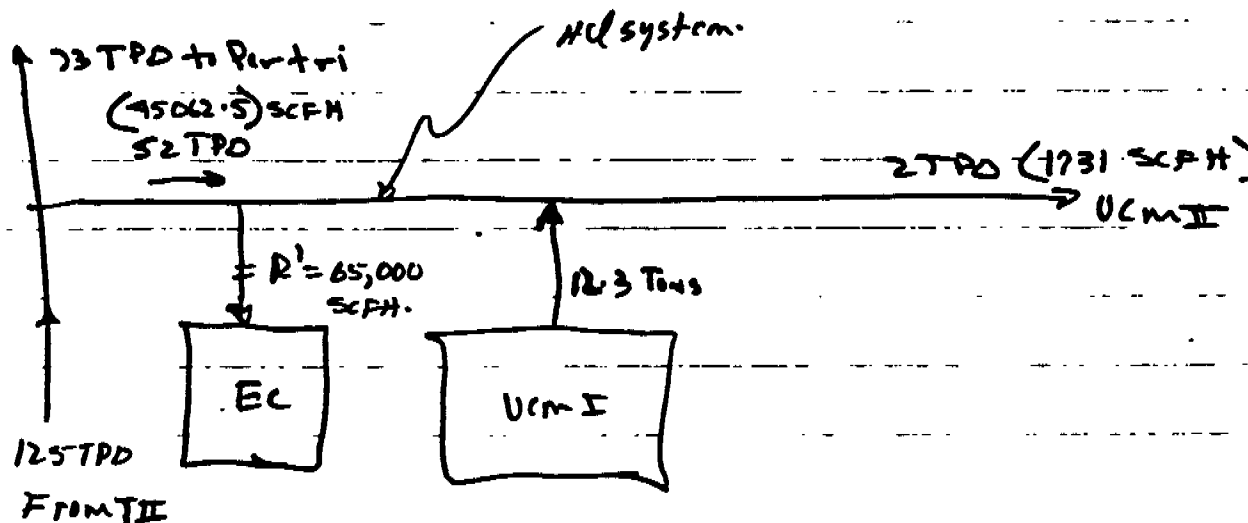
SL 049484

Second Method Shows 12.3 Tons.

The 13.7 Tons figure is lost because since also has some HCl. Also the sudden drop of pressure on the Absorber after Lemn oil was introduced caused back flow some Ucm Back to the Absorber.

How much went to EC plant and how much to Ucm II.

For the 6th the balance look like follow.



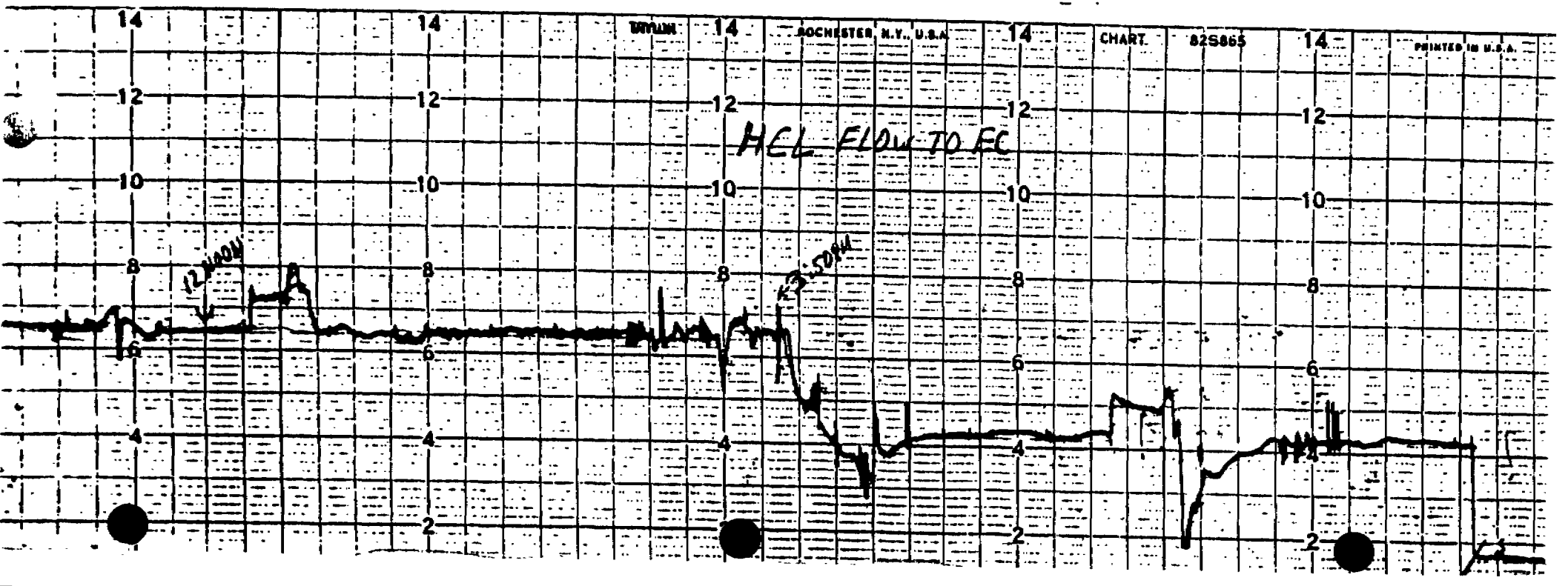
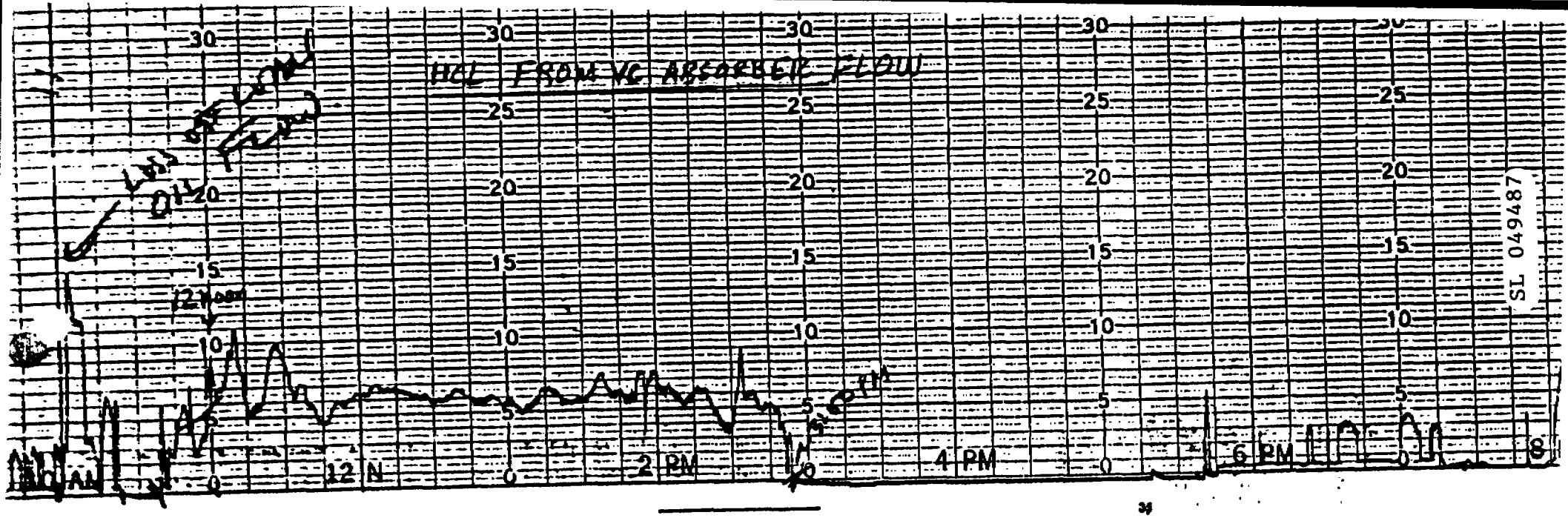
~~Flow~~ Flow to EC HCl + Ucm = $6.5 \times 10,000 = 65,000$
↑
Per-ch.

$$R = R' \sqrt{\frac{MW_{g_1}}{MW_{HCl}}}$$

So VCM that stay in loader was
Approximately 5.19 Tons.

Is Impossible to say how much went
to the scribbles. No more than 5.19 T.

SL 049486



Revised: 12/15/84 887670 TS

ENVIRONMENTAL UPSET REPORT

ROUTING - OPERATIONS

General Foreman
Production Superintendent
Operations Superintendent
Plant Manager
Environmental Control

SUBJECT: EC VENTS TO EC SCRUBBER
FROM: JERRY GUSTIN

Please complete the following questionnaire and forward as soon as possible.
[This report must be received by the Environmental Control Department within five (5) calendar days of the incident.]

1. DATE OF INCIDENT: 2/5/84
2. SOURCE OF RELEASE: ETHYL CHLORIDE UNIT
3. TIME AND DURATION: 2-5-84 at 11:30pm UNTIL 2:45pm 2-6-84
4. WEATHER CONDITIONS (Circle One): Clear Partly Cloudy Cloudy Rain
5. WIND SPEED AND DIRECTION (if a gas release): _____ mph
6. HAZARDOUS MATERIAL RELEASED: ETHYL CHLORIDE - ETHYLENE
7. ESTIMATED QUANTITY RELEASED: 100 lbs
8. CAUSE OF RELEASE: LOSS OF NUMBER 6 AND NO. 7 ~~EC~~ VENT COMPRESSOR.
9. IMMEDIATE ACTION TAKEN: VENTS WERE SWITCHED TO EC SCRUBBER
10. ACTION PLANS TO PREVENT REOCCURRENCE: BOTH COMPRESSORS ARE BEING REPAIRED. ONE COMPRESSOR ACTS AS A SPARE.
11. NOTIFICATION MADE (Who, When): PHILLIP TROW 9AM 2-6-84
Not reported, EC plant vent is reported in EIQ as
A startup vent.

687670 TS

ENVIRONMENTAL UPSET REPORT

10. People/Agencies notified: OPERATIONS NOTIFIED TWO SHIFT
ENGINEER. Minor leak not reported. Operations
instructor to document in fixed post monitoring records.

067670 TS



PPG INDUSTRIES, INC. INDUSTRIAL CHEMICAL DIVISION P. O. BOX 1000 LAKE CHARLES, LA. 70602

January 16, 1984

Mr. Tom Coerver
Department of Natural Resources
Air Quality Division
P. O. Box 44066, Capitol Station
Baton Rouge, LA 70804

RE: EC Plant Vent

Dear Mr. Coerver:

In accordance with Section 17.11 of the Louisiana Air Quality Regulations, this letter is the follow-up to my telephone report of January 3, 1984, regarding the venting of the Ethyl Chloride process waste gas vent on that date.

At approximately 7:30 p.m. on 1/3/84, the EC plant vent was diverted to the emergency scrubber due to plugging of the EC Vent Recirculation Cooler. The cooler is utilized to reduce heat generated during the compression of the vent stream. After many attempts to unplug the cooler, the cooler had to be taken out-of-service and hydroblasted. The cooler remained out-of-service until 1/6/84 at 11:30 p.m. From 1/3 to 1/6 the EC process waste gases were controlled by scrubbing with water in a packed tower. During the time that the vents were being scrubbed the amount of hydrocarbons released to the atmosphere has been estimated to be 500 pounds.

If you should have any questions concerning this incident please call me at (318) 491-4576.

Respectively,

A handwritten signature in dark ink, appearing to read 'Philip S. Trew'. The signature is written in a cursive, flowing style.

Philip S. Trew
Environmental Control Specialist

/bh

cc: Mr. Joe Withers

bcc: E. J. Tullier
Francisco Ortiz
File #109.8

RECEIVED

JAN 13 1984

ENVIRONMENTAL UPSET REPORT

ROUTING - OPERATIONS

General Foreman
Production Superintendent
Operations Superintendent
Plant Manager
Environmental Control

SUBJECT: ROUTING EC PLANT VENT TO EC SCRABBERFROM: JERRY GUSTIN

Please complete the following questionnaire and forward as soon as possible.
[This report must be received by the Environmental Control Department within five (5) calendar days of the incident.]

1. DATE OF INCIDENT: 1-3-84 7:30 pm
2. SOURCE OF RELEASE: EC PLANT
3. TIME AND DURATION: 1-3-84 (7:30 pm) TO 1-4-84 (11:30 pm)
4. WEATHER CONDITIONS (Circle One): Clear Partly Cloudy Cloudy Rain
5. WIND SPEED AND DIRECTION (if a gas release): _____ mph
6. HAZARDOUS MATERIAL RELEASED: ETHYL CHLORIDE
7. ESTIMATED QUANTITY RELEASED: 500 lbs
8. CAUSE OF RELEASE: PLUGGED COOLER
9. IMMEDIATE ACTION TAKEN: SHUT DOWN VENT COMPRESSOR AND
ROUTED VENT TO SCRABBER.
10. ACTION PLANS TO PREVENT REOCCURRENCE: CLEAN COOLER ON A
ROUTINE BASIS WHEN THE EC UNIT IS SHUT DOWN
11. NOTIFICATION MADE (Who, When): P. TREW 1-4-84
Reported to DNR. After report was made, due to the
EC vent being listed in the EIO, we probably did not need
to place a emergency report.

Environmental File # 107.8

SL 049491