Monsanto

Anniston Plant

TECHNICAL SERVICES DEPARTMENT

MONTHLY REPORT

Anniston

C. K. Eastman
A. J. Koenig
J. C. Landwehr
L. J. Boesch
G. W. Miller
W. B. Papageorge
W. F. Taffee
H. L. Williams

General Offices

H. C. Carder
W. R. Robirds
D. Danna (5)
P. B. Hodges
D. B. Hosmer (2)
W. A. Kuhn
C. F. Luecke
N. L. Sample
J. E. Smith
R. J. Stratmeyer
H. S. Trail

OTHER LOCATIONS

D. W. Jackson-WGK
T. M. Patrick-
So.2nd.St.
A. H. Forsten-
Alvin,Texas

Summary

January, 1969

Cost Improvement Results

	Actual	Target	% of Target
1968	453,720	492,600	92.3%
1969		574,075	
January	Estimated Actual 13,430	18,450	73%

Organic Division

Solid Aroclor projects transmitted were:

1. Yield improvement instrumentation
2. Montar 5 flaking
3. Solid Aroclor in Liquid Aroclor system. Installation is 90% complete.

Liquid Aroclor capacity falls to 36 M lbs/yr. as Solid Aroclor is made in the Liquid Aroclor system.

Preliminary work indicates 0.05% Biphenyl content of Santowax C can be attained. FDA approval of Aroclor 5460 needs low chlorinated Biphenyl content.

Second HB-40 autoclave capacity sufficient to meet 1969 forecasted product demand.

HCL

Agricultural Division

Staley Grade HCl project continues to be expedited. Installation of entrainment knock-out pot has been targeted for 3/1/69 to help alleviate current difficulties in making water white acid.

Sulfur Recovery purification process was reviewed and first plant Project Safety Review was held. Project description package in preparation for transmitting to CED week of February 3.

DSW 551400

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Agricultural Division (Continued)

Parathion Recovery unit dismantled for inspection.

Tentative amendment submitted for approval for testing increased Acetone Recovery from condensation reactors.

Design and Drafting

Staley Grade Acid drawings forwarded for review. Solid Aroclor instrumentation (ph. II) design complete, drafting underway.

CED Liaison

Biphenyl/Aroclor bag flattener guards designed. This completes work in this area.

J. C. Landwehr

jw

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D

ORGANIC DIVISION
1969 TSD COST IMPROVEMENT

	ANNUAL	JAN	FEB	MAR	APR	MAY	JUN	JUL	AUG	SEP	OCT	NOV	DEC
Sol.Aro. LI-Still SpG. AFE 3015	TAR				2250	2250	2250	2250	2250	2250	2250	2250	2250
	ACT												
Sp.Solid Aro. Lower 5060	TAR	2600	2600	2600	2600	2600	2600	2600	2600	2600	-	-	-
	ACT	1500											
Sol.Aro.-Still Coolout temp. AFE 3015	TAR				160	170	160	170	160	170	160	170	160
	ACT												
Sol.Aro.-Chlor'tor Batch End AFE 3015	TAR				390	390	390	390	390	390	390	390	390
	ACT												
SW/R Composition AFE 3016	TAR					2750	2750	2750	2750	2750	2750	2750	2750
	ACT												
Solid Aro. Montar 5 Flake AFE 2949	TAR					1080	1080	1080	1080	1080	1080	1080	1080
	ACT												
Sol.Aro. Blend 4465	TAR	2500	2500	2500	2500	2500	2500	2500	2500	2500	2500	2500	2500
	ACT	1690											
Sol.Aro.-Vertical Still Cond. AFE 2324	TAR	70	80	70	80	70							
	ACT	70											
Sol.Aro.Cl_2 T/C Dock AFE 2342	TAR			940	940	950							
	ACT												
Cl_2 Plt.Down No Unload CED 1831	TAR						950	940	950	940	950	940	950
	ACT												
Solid Aro.-Flake & Drum CED 1430	TAR	3000	3000	5000	5000	5000	5000	5000	5000	5000	5000	5000	5000
	ACT	0											
Liq.Aro. 48-53 M #/yr. AFE 2545	TAR	3000	3000	-	-	-	-	-	-	-	-	-	-
	ACT	0											
Liq.Aro.-No.2 Still Entrain Sep. AFE 3093	TAR										3000	3000	
	ACT												
Liq.Aro.-Montar Disposal AFE 2952	TAR			1080	1080	1080	1080	1080	1080	1080	1080	1080	1080
	ACT												
Warehouse CEA 1452	TAR	2000	3000	3000	3000	3000	3000	3000	3000	3000	3000	3000	3000
	ACT	2000											
Liq.Aro.New Burners #3 Still	TAR			1500	1500	1500	1500	1500	1500	1500	1500	1500	1500
	ACT												
Biphenyl Relocate No. 1 Preheat CEA 1892	TAR	500	500	500	500	500	500	500	500	500	500	500	500
	ACT	1500											
HB-40 2 A/C's AFE 3102	TAR	3000	3000	3000	3000	3000	3000	3000	3000	3000	3000	3000	3000
	ACT	2230											

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ORGANIC DIVISION
1969 TSD COST IMPROVEMENT

	ANNUAL	JAN	FEB	MAR	APR	MAY	JUN	JUL	AUG	SEP	OCT	NOV	DEC
BiØ Improve Tower Treat. AFE 3155	TAR					450	450	450	450	450	450	450	450
	ACT												
Improve Plt. Power Factor	TAR					900	900	900	900	900	900	900	900
	ACT												
Central Air System	TAR									1000	1000	1000	1000
	ACT												
Optimize Rx Time PNP	TAR		2500	2500	2500	2500	2500	2500	2500	2500	2500	2500	2500
	ACT												
Reduce Mole Ratio NaOH/PNCB PNP	TAR				4000	4000	4000	4000	4000	4000	4000	4000	4000
	ACT												
New Wash Water Pump - PNP AFE 2998	TAR					50	50	50	50	50	50	50	50
	ACT												
Automatic pH Control PNP	TAR										500	500	500
	ACT												
HCl Filter Pump	TAR	330	330	340									
	ACT	330											
New Blow Tank HCl	TAR	200	200	200	200	200	200						
	ACT	200											
150,000 Gal.-HCl Storage Tank AFE 2468	TAR				1760	1760	1780	1760	1760	1780	1760	1760	1780
	ACT												
Produce Staley Grade Acid AFE 3076	TAR							780	780	790	780	780	790
	ACT												
Cl_2 Plt. Shutdown CEA 1831	TAR						8880	8880	8880	8880	8880	8880	8880
	ACT												
Hg Recover from Residue	TAR	250	250	250	250								
	ACT	3910											
Hg Wash Tank AFE 2802	TAR	250	250	250	250								
	ACT	0											
	TAR												
	ACT												
	TAR												
	ACT												

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AG DIVISION
1969 TSD COST IMPROVEMENT

		ANNUAL	JAN	FEB	MAR	APR	MAY	JUN	JUL	AUG	SEP	OCT	NOV	DEC
Cooling Tower Repiping AFE 2598	TAR					420	420	410	410	420	420	410	420	420
	ACT	5,000												
Optimize N_2 & Cl_2 Levels	TAR					6600	6700	6700	6600	6700	6700			
	ACT	40,000												
Increase Waste Acid Sales	TAR					400	300	300	400	300	300	400	300	300
	ACT	4,000												
Chlorinator R.I. AFE 2244	TAR								250	250	250	250	250	250
	ACT	3,000												
EVOP Condensation Rx.	TAR		750	750	500							500	750	750
	ACT	4,000	0											
Cl_2 Unloading CEA 1831	TAR								5000	5000	5000	2000	2000	2000
	ACT	42,000												
Recycle Wash Water AFE 2960	TAR								290	290	290	290	290	290
	ACT	3,500												
Parathion Recovery AFE 2655	TAR											5800	5800	5800
	ACT	70,000												
Reduce Acetone Losses	TAR											4300	4300	4300
	ACT	51,600												
Formulations AFE 2897	TAR					1600	1600	1600	1600	1600	1600			
	ACT	9,600												
Change Cooling H_2O Item 737 AFE 3067	TAR					125	125	125	125	125	125	125	125	125
	ACT	1,500												
Well H_2O to Jets	TAR											500	500	500
	ACT	6,000												
	TAR													
	ACT													
	TAR													
	ACT													
	TAR													
	ACT													
	TAR													
	ACT													

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AROCLOR E. E. Bowles, C. R. McIlwain, (V. R. Haupt)

Evaluate Quaterphenyl-Polyphenyl Effects on Solid Aroclor Yields	1969 Savings - $63,200 NFC - $14,000	TSD Objective B-8 (a)

Design package for installing nuclear gage instruments transmitted to Planning and Scheduling week of January 27. Project will increase Solid Aroclor 5460 yield. Second part of project, Still Condenser Coolant Control, will be transmitted by 3-1-69.

Make Solid Aroclor in Liquid Aroclor System	Meet 1969 Forecast	TSD Objective B-8 (b)

Design package transmitted to P & S January 8. Piping was installed week of January 27. Some tracing and insulation work remains.

Demonsatrate Montar 5 Flaking	Savings - $11,500 NFC - $10,000	TSD Objective B-8 (c)

Transmitted to P & S 2/3/69. Project will allow flaking of Montar 5 on old Solid Aroclor flaker. Justification is drum savings.

Debottleneck Liquid Aroclor Stills	Evaluation	TSD Objective B-8 (i)

The use of a portion of the Liquid Aroclor system by the Solid Aroclor Department will reduce the Anniston Plant Liquid Aroclor capacity by 28%. Starting in February the capacity of the Anniston liquid system will be 3,000 M lbs./month.

Project 3093 to install an entrainment separator on No. 2 still has been approved for $4,500. Drafting is scheduled for second quarter 1969 with completion targeted for December, 1969.

Other means of increasing the capacity of remaining liquid system components are being evaluated.

Drum Flushing	Quality NFC - $60,000	TSD Job No. 872

A progress report was issued in Janaury, 1969. No further work is planned on this project until priority is established by the Business Group.

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BIPHENYL-SANTOWAX W. G. Niemeyer, J. W. McGee (V. R. Haupt)

Debottleneck Biphenyl Stills to 87.6 M lbs/yr.	Capacity Increase	TSD Objective B-7 (a)

Santowax C surge tank and column feed pump have been set. The revised stairway was installed over the new Santowax C surge tank. Related piping is in progress. Santowax area piping to be completed in February.

No. 1 Furnace Upgrade Liaison (CEA-1892)	Capacity Increase	TSD Objective B-7 (c)

The 300,000 gallon benzene storage tank is complete and was hydrotested on January 28. Three small leaks were found and will be repaired on February 3. Piping work in the tank area is in progress.

Improve Santowax R Quality with New Distillation Column	Quality	TSD Objective B-7 (d)

The quality of the Santowax R overhead product continues to swing as expected. We cannot expect consistent Santowax R quality until additional instrumentation is installed on Project No. 3016. Delivery on some instruments ordered on Project 3016 has been delayed. Unless Purchasing can expedite these items the project will not be installed until March 1969.

Santowax with Low Biphenyl Content for FDA Solid Aroclor	Quality	TSD Objective B-7 (b)

A 16 hour plant test run was made to determine if the biphenyl content in Santowax C could be reduced to 0.05% or less. The test indicated that it can be done; however, more work is planned to demonstrate consistent long term limits of capability.

HB-40 V. R. Haupt

Installation of 2nd Autoclave to meet Product Forecast	Savings - $36 M NFC - $16 M	TSD Objective B-12 (b)

Routine operation of the larger autoclave with larger batch sizes indicates 900 M lbs/mo. capacity using the one larger autoclave. Hydrogen supply prevents operating both autoclaves at the same time. This demonstrated rate will meet 1969's product forecast now and when hydrogen source is changed to Biphenyl department by-product upon shutdown of the Chlorine department in May.

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CHLORINE D. W. Dudley (A. G. McCarty)

Reduce Mercury Usuage to 0.75 lbs. Hg/Ton Cl_2	Savings $1,700	TSD Objective B-6 (b)

Mercury-acid wash tank now in operation. Mercury "butter" is being accumulated in wash tank. To date no "butter" has been acid washed. Project is anticipated to achieve full savings of $1,700 before plant shutdown.

Brine Dechlorination	Saving - 0	TSD Objective B-6 (c)

No further work is anticipated on this project before plant shutdown.

Central Chlorine Unloading	CED Liaison Savings - $53,300	TSD Objective CEA 1831

Design is 90 % complete. Construction slated to begin in first week of February. Project start-up still estimated as May 1, 1969.

HCl O. J. Norris, G. L. Moore (A. G. McCarty)

Production of Staley Grade Acid	Increased Sales Savings - $9,400	TSD Objective B-10 (c)

Project 3076 given top priority in drafting during January. Review drawings have been completed and project transmittal is scheduled for 2/7/69. Portion of project to install catch tank in HCl gas line will be expedited: - most optimistic date for installation - 3/1/69; most probable 3/15/69. This catch tank will allow gas by-pass purge valve to be closed contributing to as high as 800,000 lb/mo. increased recovery. Coaleser will be ready for intermediate organics removal, installation 5/1/69 as scheduled.

Muriatic Acid Storage	Savings - $21,200	TSD Job No. 497

Tank construction complete. Rubber lining will be completed as soon as warmer weather permits.

PNP O. J. Norris, G. L. Moore (A. G. McCarty)

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Debottleneck to 1.8 M#/mo.	Capacity Savings - $27,500	TSD Job No. 482

Random reactor letdown problem appeared and was corrected around the middle of the month. Main cure for problem this occasion appears to be reduction in condensor temperature to 100°C. Small PNCB charge (7400#) was also used. Presently charge is up to 7600# and letdown continue excellent. PR&D testing to

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PNP (Continued)

establish a base operation point on % organics, % NaPNP, etc. in charge tank temporarily delayed until cause for data spread (8.8% to 21.3% on organics) is established. This information is critical to determining exact nature of the randomly recurring letdown problem.

Study of Molar Ratio NaOH/PNCB	Savings - $36,000	TSD Objective B-9 (c)

Approved tentative ammendment received from St. Louis. However, on agreement between TSD and production has been reached to hold tests until rate capabilities for Niran requirements are met.

Revise MIP

Plant review completed 1/9/69. Final draft being typed prior to final review with TPM.

NIRAN K. G. Hale, D. W. Dudley, (A. G. McCarty)

Demonstrate Parathion Recovery	Savings - $17,500 10-15% Reduced C.O.D. Load	TSD Objective B-5 (a)

Work began in late January to remove coalescer for inspection of elements. Coalescer will be pulled the first week in February. One vendor proposal for a pre-coat type filter has been received and will be evaluated in early February.

Parathion Formulations	Savings - $10,000	TSD Job No. 845

Increase in sales forecasts for formulated Parathions from 369 M gallons to 417 M gallons in 1969 has necessitated a crash project to increase blending capability. Project is slated for start-up April 1. Project schedule and rush notification was issued January 24. Project proceeding as scheduled.

Acetone Recovery	Savings - $12,900	TSD Job No. 869

Tentative amendment to Niran process of January, 1969 to recover $50,000/yr. in acetone and reduce C.O.D. waste load 40-50% was submitted for approval 1/10/69. Early approval of the amendment will enable plant test on Niran prior to turn-around.

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NIRAN (Continued)

Sulfur Recovery from Residue	$500,000/yr. Savings 40% Reduction in SO_2	TSD Objective B-5 (d)

Anniston TSD is preparing a package transmittal for the Sulfur Recovery Project. The package will include the pilot separation test report, the report by Bird Machine Company, the PR&D process report, and a transmittal write-up covering additional details (objectives, facilities, etc.).

The first plant safety review for selection of locations was held on 1/21/69. The PR&D process report was reviewed in plant on 1/17/69.

Submerged Pump for Refractive Index Control of Chlorination	Savings $1,500 (Potential Automation)	TSD Objective B-5 (c)

Submerged pump was pulled and inspected due to potential glass damage upon starting if pump was corroded. Still no evidence of corrosion. The pump will be re-installed by mid-February. Tests will begin by late February.

Fume Collection System in Parathion Department	Reduce Atmospheric Corrosion	TSD Objective F-10

A new fan of Atlac 382 to replace damaged, PVC coated original, has been ordered. Scheduled shipment date is 3/1/69. Transmittal on new foundation and transition pieces to adapt new fan is scheduled for 2/15/69.

ENGINEERING DESIGN AND SERVICES

Mechanical/Electrical/Instrument Design and Drafting — J. C. Price, J. A. Veazey, R. L. Brewer, J. K. Rennie, V. T. Langdon, (W. F. Taffee)

Issued design package for AFE 3036, acidic spring water sewer. TSD guideline for control of TSD Mechanical expense budget was reviewed and approved.

Projects were approved for modification of agitator interlocks in Parathion department ($9700.00 total) and automatic alcohol feed to Thio Acid reactors ($3860.00 total). Design is scheduled for fourth quarter 1969.

E & I design was completed for Staley-Grade Acid and for Solid Aroclor Instrumentation (Phase II).

A meeting was held with George Hunt, Electrical section of S&PP, to define scope of S&PP recommendation to test electrical feeders, interlocks, etc.

Design packages transmitted to Maintenance to cover P_2S_5 conveyor access ladder, deluge system at soda ash tank (Niran), PNP reactor and acidifier agitator alarms and Niran cubicle sight windows.

UTILITIES ENGINEERING J. C. Price (W. F. Taffee)

Forwarded AFE 3155, Improve Biphenyl Cooling Tower Treatment, for approval. Estimated savings $5400/yr. Evaluation completed and AFE 2821, Steam Meters, issued covering four (4) new meters in distribution system which are required for accurate utilities cost control in departments. Forwarded review drawings for AFE 2988 - Biphenyl Gas Meter, and AFE 3067 - Cooling Water on Niran Item 737.

PLANT IMPROVEMENT G. C. Goodwin (W. F. Taffee)

Design package covering lights on 5th street forwarded to Maintenance for construction.

POLLUTION CONTROL E. G. Wright (W. F. Taffee)

Reporting	Pollution Abatement	TSD Objective F-1

A method was devised with Accounting whereby pollution control expenditures are kept up to date. The 1968 figures are available and can be transmitted to Paul Hodges as soon as forms are received from St. Louis.

A.I.A. Meeting	Community and Govt. Relations	TSD Objective F-2

Attended meeting of Associated Industries of Alabama January 22. Meeting was to discuss the A.I.A.'s position in the upcoming congressional session.

Waste Audits	Pollution Abatement	TSD Objective F-3

Visited the W. G. Krummrich plant to observe flow measurement technique using lithium chloride dilution method. We will use this method for determining flows during waste audits. Also visited J. F. Queeny plant to discuss their experience in departmental waste audits.

Air Sampling Program	Pollution Abatement	TSD Objective F-3

Initial testing of trial SO_2 analyzer indicates interference from other acidic compounds. Additional investigation underway.

Contact with Regulatory Agencies	Community and Govt. Relations	TSD Objective F-2

Visited Anniston sewage treatment plant twice. They are continuing to experience occasional difficulty in handling their total solids load. Invited chemist from the city plant to our laboratory to observe demonstration by vendor of Polymers for increasing clarification effeciency.

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POLLUTION CONTROL (Continued)

Install Solids Removal Equipment at Waste Treatment Plant	Pollution Abatement	TSD Job No. 808

Project revision forwarded to management in January. Some preliminary screening tests were run on some polymers which might be used as a filter aid.

Choccolocco Creek Biological Survey	Pollution Abatement	TSD Objective F-4

Drs. Gunning and Suttkus of Tulane University completed low water phase of continuing survey of Choccolocco Creek during week of January 26, 1969. Their report is expected in March.

Waste Treatment

All wastes were effectively treated during January, although there are indications that we are very near the upper limit of our treatment plant capacity. Some problems were also encountered due to the high solids loading at City Waste Treatment. Average daily values for Monsanto's effluent are as follows:

	Average Daily	Specifications
PNP	1 ppm	5.0
COD	< 8 ppm	< 200
Parathion	.08 ppm	1.0
BOD	5.0 ppm	< 200

PROCESS AND QUALITY ANALYSIS W. B. Dunlap

Quality

The Plant Quality Score was 89.5, down 5.0 from December, with YTD (January only) score of 89.5 against a target of 95.0 minimum. Below average levels continued in Liquid Aroclors and Niran, with excellent uniformity in Caustics and PNP. Studies relating product quality with raw materials are continuing in P_2S_5 and PNP.

P_2S_5 Raw Material and Process Surveillance	Potential Savings $50,000	TSD Objective C-1 Job 877

Job number assigned with work to start in 1st quarter. Correlation of raw materials with P_2S_5 quality being conducted by Production Supervisor.

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PROCESS AND QUALITY ANALYSIS (Continued)

Parathions - Correlate Intermediate and Parathion Isomers	Potential Savings $88,000	TSD Objective C-2 Job 878

Job number assigned with work in progress. Laboratory has set up routine analysis of Parathion isomers, and a determination of isomer content of extremely low-assay intermediate.

PNP - Monitor Critical Process Variables	Potential Savings $60,000	TSD Objective C-3 Job 879

Job number assigned with work in progress. Process variables are being explored in team effort with Process Engineer and Laboratory through a testing-surveillance study.

Solid Aroclors - Statistical Surveillance of Critical Variables	Potential Savings $50,000	TSD Objective C-4 880

Job number assigned to replace TSD Job 831. Work is planned to start in second quarter following installation of control equipment.

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PLANT LABORATORIES G. W. Miller

PROCESS RESEARCH AND DEVELOPMENT J. T. Bell

For the month, 94 working days of the possible 95 were directed toward the projects outlined in the 1969 PR&D Program. At present, all projects appear to be progressing as planned. The study of Blend Scavenger Refinement (Aroclor) may be excluded from the program and replaced by an investigation to recover the benzene value of quaterphenyls and higher homologs by an aluminum chloride catalyzed rearrangement.

HB-40 Biphenyl Hydrogen Purification	Alternate Hydrogen Source	J. L. Brown

The investigation has been terminated and the pilot unit returned to Chemical Design, Inc.

p-Nitrophenol	Reduce Cycle Times	W. H. Howard J. T. Bell

Analysis of samples taken from the PNP charge tank during 10 batches of constant charges, reaction times etc., has been undertaken to establish variations present in material levels. Analysis of 216 recycle water is to be included with the projected completion date scheduled for 2-14-69.

Aroclor 1272	Sample Preparation for Sales	G. L. Arnett

A 30 lb. sample has been prepared. A comparison of Iron and Aluminum chlorination catalysts were completed along with material balance studies. A report is under preparation and project completion will be in advance of the 2-10-69 projected date.

Sulfur Recovery	Sulfur Refinement for Reuse	I. Ransaw W. H. Howard

A report has been prepared and is in the process of being issued. An investigation into the chlorination of wash water to lower waste treatment has been initiated.

Blend Scavenger Refinement (Aroclor)	Improved Aroclor Electrical Properties	J. L. Brown

Techniques to improve the electrical properties of phenyl glycidyl ether have as yet been unsuccessful. Absorption on Porocel and Silica Gel resulted in no improvement and the use of a 500 volt d.c. potential for the removal of ionic contamination resulted in only slight improvement. Analysis indicates that the concentration of chloride, sodium and potassium ions is very low or nonexistent.

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PLANT LABORATORIES (Continued)

ANALYTICAL AND QUALITY CONTROL S. O. Kemp

A series of 20 samples were analyzed by GLC to determine yield loss from the Biphenyl/Santowax still.

Analytical difficulties involving HB-40 sales to General Cable Corporation are being resolved and no business loss is anticipated. Special tests and specifications were agreed to by Mr. S. Mickeloski of the General Cable research labs, Bayonne, N. J. during a recent visit by R. N. Brell and G. W. Miller.

Complaint Report

Quality

Number	Material	Customer	Reason
1-A-69	Muriatic Acid	Merck	Color

YTD Quality Complaints/100 Shipments 0.17 Target 0.20

Service

None

YTD Service Complaints/100 Shipments 0.0 Target 0.20

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COMMUNITY RELATIONS, PERSONNEL, RECRUITING, AND DEVELOPMENT

Personnel

1. V. R. Haupt, G. W. Miller, and J. T. Bell met in St. Louis for meeting on Solid Aroclor Research Tuesday, January 7.

2. W. G. Niemeyer promoted to TSD Senior Engineer effective February 1, 1969.

Recruiting

1. Mr. T. W. Lawrence, MS Chemical Engineer graduate in 1965 from Auburn University, accepted an offer for position as Process Engineer.

Development

1. J. C. Landwehr attended TSD Superintendents' Conference January 13 and 14.

2. J. C. Landwehr went to St. Louis on January 20 for the initial chairman meeting for the 1969 Innovation Exchange Program, Wednesday, January 22.

3. W. F. Taffee attended annual meeting of Coosa-Alabama River Improvement Association in Montgomery, Wednesday, January 22.

4. E. G. Wright attended a meeting of the Air and Water Resources Committee, Associated Industries of Alabama in Birmingham, Wednesday, January 22.

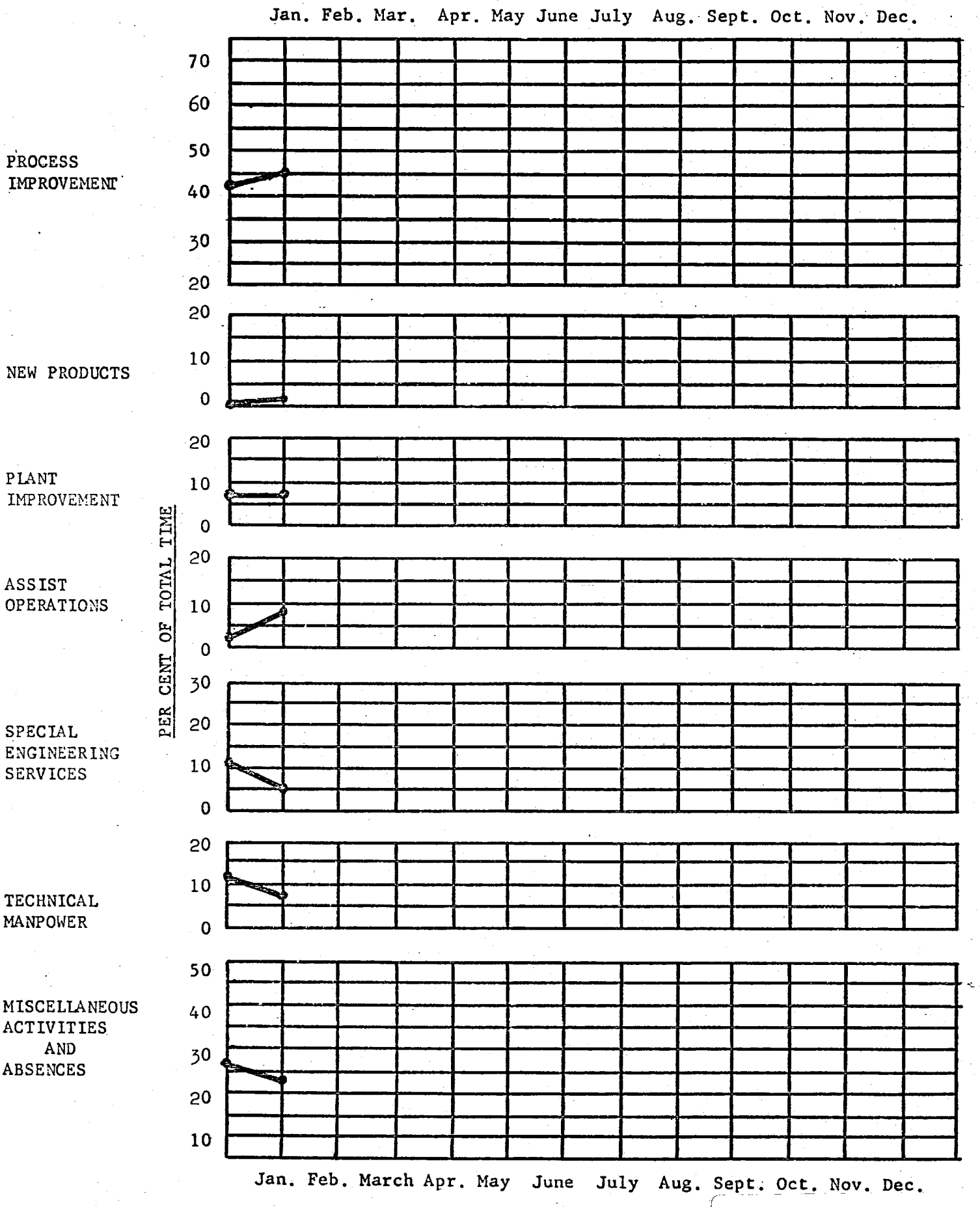
Visitors

1. Director of Manufacturing for the Ag Division Crop Protector Business Group, W. R. Robirds, D. E. Cayard, and B. B. Blocker visited.

2. TSD participated with accounting in a review of visibility of Central Division Computer System, R. F. Brooks and M. Tesson from Queeny.

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DISTRIBUTION OF TIME BY TECHNICAL SERVICE

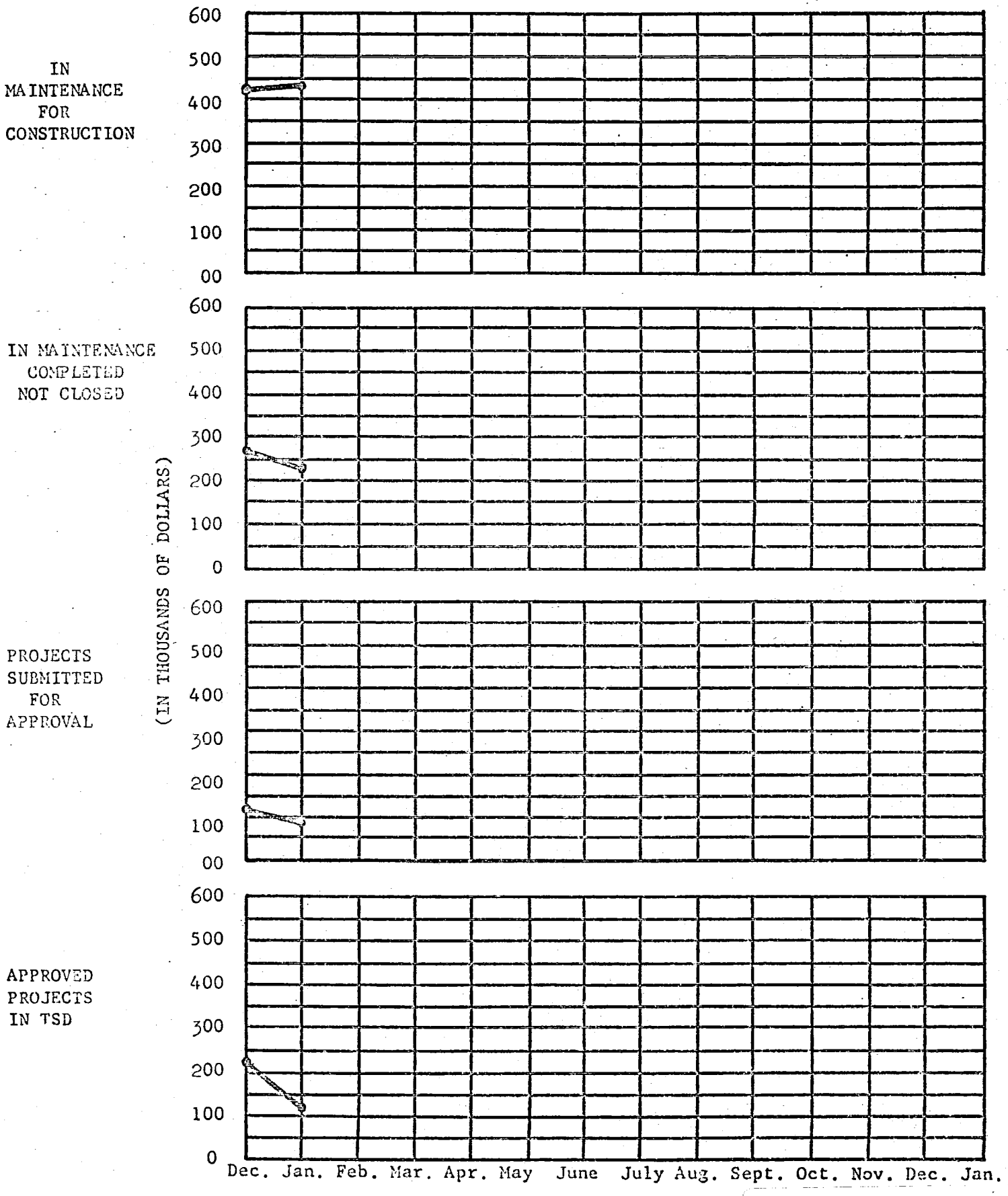


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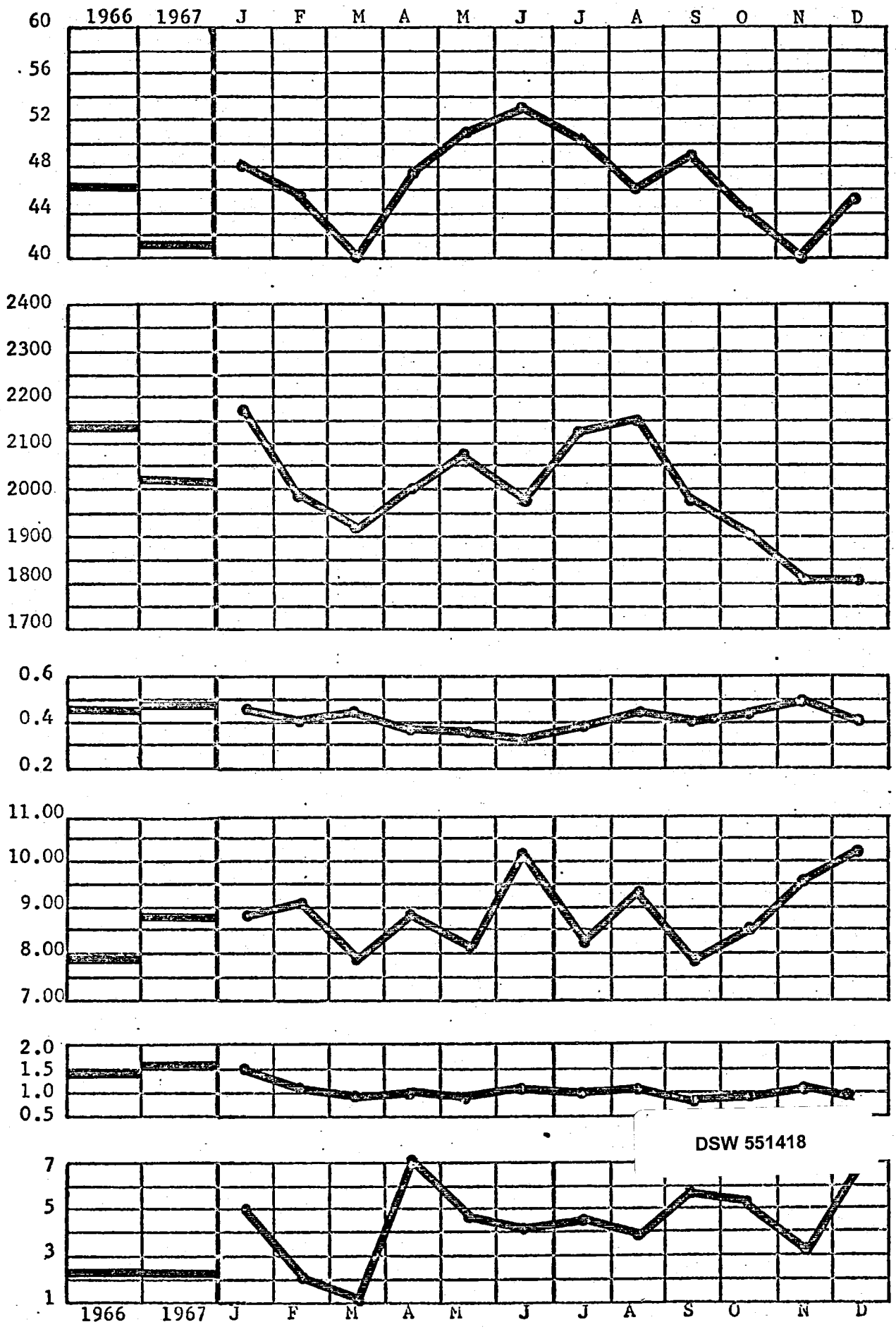
TSD PROJECT SUMMARY



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LABORATORY ADMINISTRATION

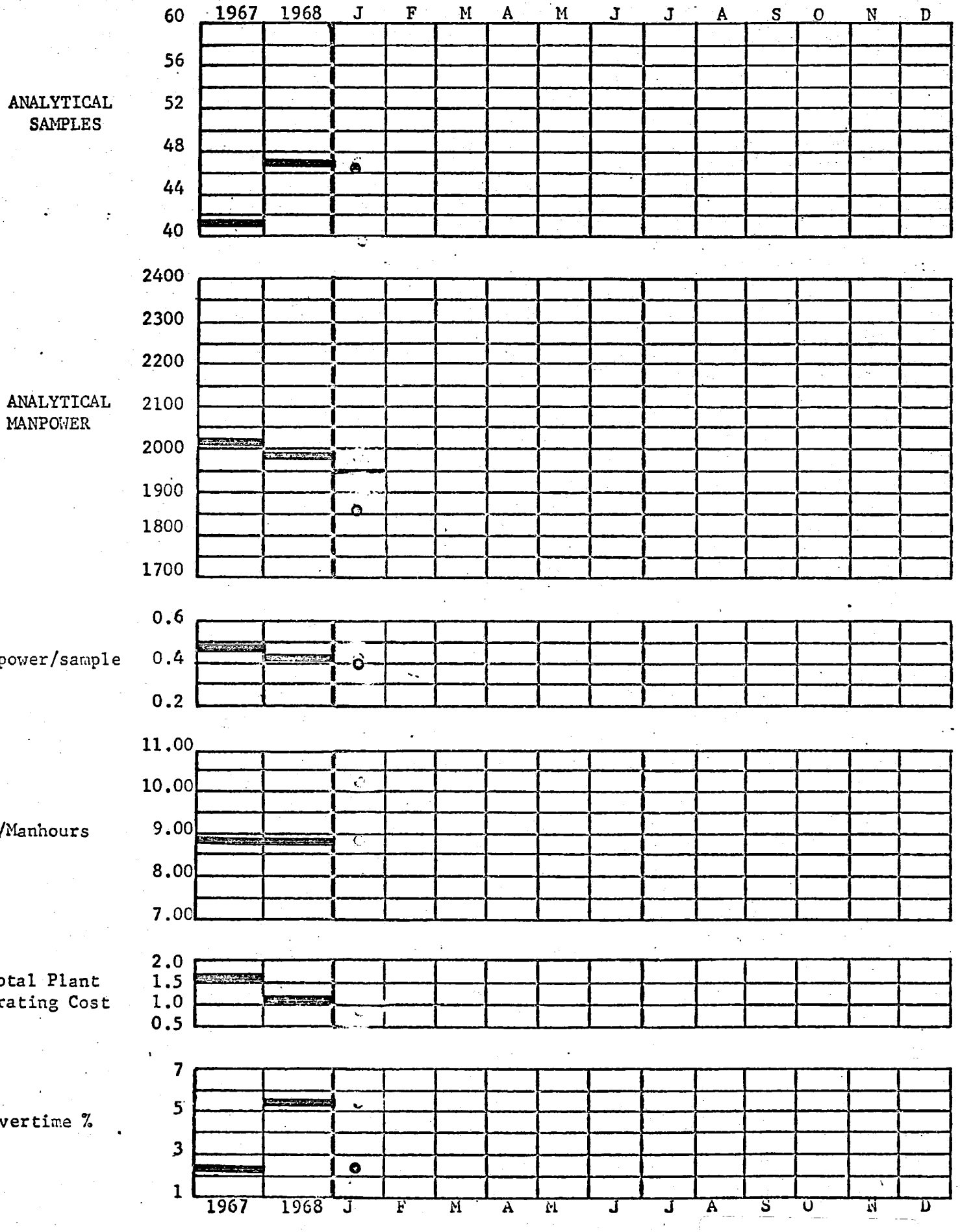


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LABORATORY ADMINISTRATION

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