



~~for IAH to Ethyl Pasadena~~
DEPARTMENT OF HEALTH & HUMAN SERVICES

Public Health Service

Centers for Disease Control
National Institute for
Occupational Safety & Health
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February 16, 1983

Don Johnson
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FEB 24 1983

F.Y. Attention
File: Houston

Mr. Gilbert B. Meyers
Ethyl Corporation
Corporate Medical Department
451 Florida Boulevard
Baton Rouge, Louisiana 70801

Dear Mr. Meyers:

Enclosed is a copy of the draft report of the industrial hygiene survey conducted during the tetraethyl lead study at the Ethyl Corporation in Pasadena, Texas, on April 7-10, 1980. A copy has also been forwarded to the Plant Manager of the Pasadena plant for review and comments.

If you have any questions, you may contact me at (513) 684-3255.

Sincerely yours,

Virginia Ringenborg
Virginia Ringenborg
Industrial Hygienist
Industrial Hygiene Section
Industrywide Studies Branch
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1 Enclosure

SURVEY REPORT OF
ETHYL CORPORATION
PASADENA, TEXAS 77501

SURVEY CONDUCTED BY:
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DATE OF SURVEY:
April 7-10, 1980

REPORT WRITTEN BY:
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DATE OF REPORT:
January 19, 1983

REPORT #:
115.10

Industrial Hygiene Section
Industrywide Studies Branch
Division of Surveillance, Hazard Evaluations and Field Studies
National Institute for Occupational Safety and Health
Centers for Disease Control
Cincinnati, Ohio

Purpose of Survey:

The purpose of the industrial hygiene survey was to determine the Ethyl Corporation employees' exposure to tetraethyl lead (TEL), inorganic lead (Pb), ethylene dibromide (EDB), ethylene dichloride (EDC), and ethyl chloride.

**Employer Representative
Contacted:**

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**Employee Representative
Contacted:**

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**Standard Industrial
Classification of Company:**

2869

Disclaimer

Mention of company names or products does not constitute endorsement by NIOSH.

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Abstract

An industrial hygiene survey was conducted at the Ethyl Corporation to estimate worker exposure to tetraethyl lead (TEL) and other air contaminants in the TEL manufacturing and blending units. Personal and area samples were collected for tetraethyl lead, inorganic lead, ethylene dibromide, ethylene dichloride and ethyl chloride.

Tetraethyl lead sampling results ranged from 0.011 to 0.159 mg/m³, and inorganic lead (Pb) sampling results ranged from 0.0027 to 0.869 mg/m³. Ten percent of the TEL and inorganic lead personal samples were above the OSHA Permissible Exposure Limit (PEL) of 0.075 milligrams per cubic meter (mg/m³) for TEL and 0.05 mg/m³ for inorganic lead. Approximately 6.5% of the inorganic Pb samples were above the NIOSH recommended standard of 0.10 mg/m³. However, Ethyl employees wore protective clothing and respirators which had been quantitatively fit tested. Levels of ethylene dibromide (EDB), ethylene dichloride (EDC), and ethyl chloride personal samples averaged 0.064, 0.068, and 0.295 mg/m³; the OSHA standards are 154, 202, and 2600 mg/m³, respectively. NIOSH recommended standards are 1 mg/m³ as a ceiling level for EDB and 20 mg/m³ as a Time Weighted Average (TWA) for EDC.

See results section
EC 3011
12/1/74
WJ

Introduction

Under the Occupational Safety and Health Act of 1970 (set forth by the 91st Congress, S.9123, Public Law 91-596) the National Institute for Occupational Safety and Health (NIOSH) was given the authority and responsibility for conducting and reporting on field research studies in industry. Section 20(a)7 states that NIOSH shall conduct and publish industrywide studies of the effects of chronic low level exposure to industrial materials, processes, and stresses on the potential for illness, disease or loss of functional capacity in the aging adult.

Manufacture of tetraethyl lead for use as a gasoline additive began in 1923. By 1924, commercial activities were stopped due to TEL intoxication of workers.² An extensive investigation conducted by the U.S. Public Health Service revealed that if adequate precautions were taken in TEL's manufacture and addition to gasoline, the use of TEL should not endanger workers' health.³ Industry developed more hygienic work practices and better technology, began clinical surveillance of TEL workers, and resumed production of TEL in 1926.² Several years later (and as late as the 1970's), TEL intoxication was observed in employees engaged in cleaning and repairing large gasoline storage tanks. It was discovered that most of these cases were due to laxness in wearing of safety apparel, especially air supplied respirators.¹

In June, 1978, NIOSH responded to a Health Hazard Evaluation (HHE) request at the Ethyl Corporation plant in Pasadena, Texas. The request was prompted by the occurrence of three cases of multiple myeloma among long-term plant employees who had been exposed to TEL. These cases were diagnosed between 1971 and 1976.

To assist in the Health Hazard Evaluation, an investigation was conducted by NIOSH epidemiologists. The incidence of multiple myeloma among workers at the Pasadena plant was determined to be approximately 15 times that expected by using race-specific data from the Third National Cancer Survey (1969-1971) and the State of Connecticut (1970), and the person-years calculated for workers employed a minimum of one year. These results prompted NIOSH to undertake a combined retrospective cohort mortality study and industrial hygiene evaluation of workers at the Ethyl Corporation plant in Pasadena, Texas.

This industrial hygiene survey was performed on April 7-10, 1980, to determine the TEL plant employees' exposure to TEL, inorganic lead (Pb), ethylene dibromide (EDB), ethylene dichloride (EDC), and ethyl chloride. The exposure data will be used in conjunction with the ongoing epidemiological retrospective cohort mortality study. This data represents exposure at the time of this survey and may not be indicative of past exposure. ✓

Plant Description

The Ethyl Corporation is comprised of eight buildings on 400 acres of land in Pasadena, Texas. (The major plant buildings and processes may be seen in Figure A-1.) The plant was built in 1952 principally for production of the motor fuel antiknock compound tetraethyl lead (TEL). Several other processes operating at the facility produced linear alcohols, linear olefins, diethyl aniline, ethyl chloride, ethylene dichloride, and aluminum alkyls. Production of vinyl chloride monomer was begun in 1965 and terminated in 1975.

Much of the Pasadena plant and its operations were open to the environment. The TEL process, however, was enclosed, and laminar flow ventilation systems and air sampling monitors were added to the process areas to reduce worker exposures. The TEL building contained four floors. The alloy area occupied part of the first three floors on the southwest end of the building. The lead-sodium alloy and ethyl chloride were charged from the fourth floor to the autoclaves on the third floor. The steam stills were located on the second floor, the blending area occupied a three floor area on the north end of the building, and the recovery furnaces were located on the ground floor along the east side of the building.

The entire TEL process was manually operated until 1960 when half of the process was automated. This included automatic charge pot filling and conveying to the autoclave charging station; however, manual operations were still required in the actual autoclave charging. The TEL production at this plant was closed down in 1981.

Description of Industrial Hygiene, Safety and Medical Programs

Industrial Hygiene

Ethyl Corporation employed a staff of seven industrial hygienists at corporate headquarters in Baton Rouge, Louisiana, with one hygienist located at the Pasadena plant. The hygienists conducted a comprehensive quarterly monitoring program to check for exposures to physical agents, TEL, and chemicals used in the TEL and other processes. All process areas were provided with forced air (general) ventilation and local exhaust ventilation.

Safety Program

A formal safety program in which all employees were involved, was under the direction of the Safety and Health Supervisor, Robert Mack. Under this program, descriptive literature on Ethyl's products was provided as well as protective clothing such as slicker suits, gloves, chemically impervious safety boots, goggles, hard hats, and respirators (which included quarter-face, half-face, and full-face). Ethyl also had a quantitative respirator fit testing (QNFT) program.

Facilities for changing clothes and taking showers were provided and use of these facilities was mandatory. The change area consisted of clean and "dirty" sides with showers in between. Laundry facilities were also provided by the company, and personal respirators were cleaned in that area. Safety showers were installed throughout the TEL building as well as a kerosene shower in the clothes change area for personnel exposed to TEL liquid.

Medical Program

The Ethyl Corporation, Pasadena plant, employed one full-time physician and a full-time licensed nurse. There was also an employee on each shift with formal first aid training; these employees were designated to provide emergency medical treatment. Preplacement (which replaced preemployment) and annual physical examinations were required for all employees and included a chest x-ray, hearing and visual acuity tests, lung function test, urinalysis, blood chemistry analysis, and an electrocardiogram (ECG) for those 40 years of age and over.

In addition, urine samples were collected approximately every 2-6 months and blood samples collected every 6 months; these samples were analyzed for total lead. If an employee's lead level was elevated (above 40 ug/100g of blood), the individual was removed from the TEL area until his lead level returned to an acceptable level (below 40 ug/100g of blood).

Past analyses have revealed increased blood and urine lead levels with lead intoxication symptoms in some employees. These results as well as any injuries (10 lost-time accidents during 1979), complaints, and other examinations handled by the plant clinic were noted in the employees' medical records. These medical records have been retained from the time the plant opened in 1952 for all employees who have worked at the Pasadena facility.

Description of the Workforce

This plant employed 1200 people at the time of this survey; 1000 in production and 200 in administration. As of 1978, 14% of these employees were black, 5% of Hispanic origin, and 4% female. Women with child bearing potential were not permitted to work in the TEL area due to the possible harmful effects of inorganic lead on the fetus. Production was continuous over three shifts; with 125 employees per shift in the TEL plant. The union representing the Ethyl employees was the Oil, Chemical, and Atomic Workers Union (OCAW), Local 16000.

The main area evaluated during this survey was the TEL manufacturing and blending unit. Fourteen people, excluding maintenance employees, worked in this unit on each shift. Variations in numbers were caused by addition or deletion of trainees per shift. The breakdown of workers by area per shift during the survey was as follows:

<u>Area</u>	<u>Number of Workers</u>
Furnaces	3 furnace operators 1 relief man 1 furnace foreman
Alloy area	1 hopper booth operator 1 charge pot operator
Main Building	1 4th floor operator 1 3rd floor operator 2 2nd floor operators
Blender area	2 blender operators 1 blender foreman

EC 3015

Process Description

Tetraethyl lead is generally made by reacting a lead-sodium alloy with ethyl chloride in an autoclave. (See Appendix, Figures A-1 and A-2 for a description of the TEL process.) The crude product is purified by vacuum distillation and water washing.⁴

The Ethyl TEL process, a multireactor continuous batch operation, was housed in a four story enclosed structure. The alloy area occupied part of the first three floors on the southwest end of the TEL building where the lead-sodium alloy [90% lead (Pb) and 10% sodium (Na)] was prepared in an alloy pot. The liquid alloy was transferred to a drum caster where it was cast, oil cooled to solidify, and crushed. All operations were carried out in a nitrogen atmosphere. The crushed alloy (in flake form) was moved by a vibrating conveyor to a hopper on the fourth floor. The hopper was purged with nitrogen and filled with the flaked alloy by either the manual "A" or automated "B" process. From there the crushed alloy was charged into a horizontal autoclave (with approximately 100 pounds per square inch (psi) of pressure and safety valve) which was located on the third floor. After the autoclave was charged with the alloy, ethyl chloride was fed slowly into the autoclave where part of it was vaporized by heat evolved from the reaction. The vaporized ethyl chloride was condensed in a reflux condenser and returned to the autoclave. Vaporization supplemented by circulation of a coolant in the autoclave jacket kept the reactants at 65-75°C and 50-60 psi. Any gaseous by-products were vented through the reflux condenser. Various catalysts, such as aldehydes, acids, ketones, esters, etc., were used in concentrations of 1 to 2% to speed up the reaction.

When the reaction was completed, the autoclave was vented into a steam still located on the second floor. (Each still was opened and checked prior to loading and before dumping bottoms.) Caustics, fatty acid, and hot water were used in the stills to vaporize the last traces of ethyl chloride, to decrease the surface tension, and to distill the TEL from the spongy metallic mass. (Sodium sulfide, sulfur, and caustic were combined to produce sodium thiosulfate which when mixed with ferric chloride and added to the stills prevents "balling" of the solid material). The tetraethyl lead and water were removed from the top of the stills and placed in a settling tank where the water was drawn off the top.

The lead-salt sludge and water remaining in the stills were dumped out the bottom to a sludge pit. The slurry from the still was washed free of sodium chloride and passed (under slight vacuum) through the dryer twice before being resmelted in three recovery furnaces located on the east side of the ground floor. In the furnaces, impurities were skimmed off before going to the melting pot. Seventy-five percent of the Pb used was recovered (and reused) since only about 25% of the lead fed into the autoclave was consumed in the process reaction.

The crude TEL from the still was aereated, washed, filtered, and pumped to the blending area which was located on three floors on the north side of the building. There, under a nitrogen blanket, the ethylene dibromide, ethylene dichloride, and kerosene were automatically metered into the blender and the dyes, Automate orange-2 (oil soluble) and Ethyl red 105 (granular), were manually added through a chute to the crude TEL.

Mixed lead alkyls (MLA) and tetramethyl lead are also manufactured; these compounds and TEL are mixed according to customer specifications and shipped to refineries for use as gasoline additives.

Potential Exposures and Controls Used

The TEL process could be divided into ^{five} ~~four~~ ^{furnace} main areas: alloy, autoclave, steam still, recovery, and blending areas, among which the exposure potential varied. Elemental lead (Pb) exposure was possible throughout the TEL process by inhalation or skin absorption; however, the potential for Pb exposure was greatest in the alloy and recovery (furnace) areas. If system leaks occurred in the autoclave or steam stills, exposure (by inhalation) to lead, ethyl chloride, catalysts, and TEL was possible. Exposure to ethylene dibromide, ethylene dichloride, kerosene, and dyes such as Automate orange-2 and Ethyl red 105 was also possible (by inhalation) in the blending area. Potential exposure was reduced by ventilation systems, protective clothing, and respirators used as control measures in the various TEL process areas.

Production and Toxicity of Substances Monitored

Tetraethyl Lead (TEL)

Tetraethyl lead is an antiknock compound that has been manufactured and used as an additive for gasoline since 1923.¹ Only very small quantities (i.e. approximately 2 cubic centimeters per gallon of gasoline) are needed to raise the efficiency of the fuel so that it burns more evenly.⁵

TEL, a colorless oily liquid, is a slightly volatile organic Pb compound that is insoluble in water but soluble in fats and their solvents. The solubility factor allows TEL to be absorbed into the blood stream via contact with skin, inhalation of vapors or ingestion of the liquid. TEL is then deposited in the fatty tissues of the body, especially the central nervous system (CNS). (A study by Cremer¹ showed that TEL was readily converted in the liver to triethyl lead, and that triethyl lead, not TEL, caused the CNS effects.) Early signs and symptoms associated with TEL intoxication may include: insomnia, disturbing dreams, anorexia (loss of appetite), nausea, vomiting, metallic taste in the mouth, headache, irritability and nervous anxiety, palor, tremors, slow pulse, low temperature, exaggerated reflexes, change in bowel habits, and weight loss. As the state of TEL intoxication increases, the signs and symptoms are exaggerated and the subject may suffer an acute anxiety state progressing to a state of mania typical of acute toxic psychosis; coma and death may follow. ^{5,6,7}

Although the lead content of the blood is the best indicator of inorganic Pb poisoning, the concentration of Pb in the blood may be only slightly elevated or within normal range when TEL intoxication occurs. Urine levels, however, may be elevated in both cases; but urine levels usually are appreciably higher in TEL intoxication since lead, absorbed in this form, is more rapidly excreted.⁸

The Occupational Safety and Health Administration (OSHA) Permissible Exposure Limit (PEL) for TEL is 0.075 milligrams per cubic meter (mg/m^3) for an 8-hour time weighted average (TWA). The Immediately Dangerous to Life or Health (IDLH) level set by OSHA is $40\text{-mg}/\text{m}^3$.⁹ The American Conference of Governmental Hygienists (ACGIH) recommends a Threshold Limit Value (TLV) of $0.1\text{ mg}/\text{m}^3$ for an 8-hour TWA.⁹ (See Appendix, Table A-1.)

Lead

Inorganic Pb is ubiquitous in the environment and can be found in measurable amounts in all adult body tissues and fluids. Lead is used in many industrial processes, one of which is tetraethyl lead. In most of these processes the main routes of occupational exposure to Pb are inhalation and ingestion. Either type of exposure may result in Pb absorption (5-10% of ingested Pb; 30-50% of inhaled Pb)¹⁰ and distribution throughout the body. The effects of Pb absorption have been described by Mayers¹¹ as follows: loss of appetite, metallic taste in the mouth, constipation, anemia, pallor, malaise, weakness, insomnia, headache, nervous irritability, muscle and joint pains, fine tremors, encephalopathy, and colic. Other effects include damage to the reproductive system and inhibition of heme synthesis (which would decrease oxygen (O_2) transport in the body).¹²

An indirect indicator of Pb exposure is the blood lead (PbB) level. Prevention of adverse health effects from exposure to Pb throughout a working lifetime requires that the PbB level be maintained at or below 40 ug/100g of blood. Average PbB levels are <20 ug Pb/100g of blood for 50% of the population and <35 ug Pb/100g of blood for 98% of the population.¹² Urinalysis may also be used to indirectly determine the amount of Pb exposure. Under certain circumstances, although not a regular procedure, analysis of feces may be conducted to give an approximate measurement of the amount of Pb ingested (including that from the upper respiratory tract).

The OSHA Standard (PEL) for Pb is 0.05 mg/ μ^3 ; NIOSH recommends a TWA of 0.1 mg/ m^3 ; and ACGIH recommends a TLV of 0.15 mg/ m^3 and a Short Term Exposure Limit (STEL, up to 15 minutes) of 0.45 mg/ m^3 .^{9,13} (See Appendix, Table A-1.)

Ethylene dibromide (EDB) and Ethylene dichloride (EDC)

Ethylene dibromide and Ethylene dichloride are added to TEL in order to prevent the deposition of lead in the exhaust sections of the engine. The ethylene halide converts the lead oxide formed during combustion into the volatile lead halide.¹⁴

Both EDB and EDC are toxic by inhalation, ingestion, and skin absorption, and are strong irritants to the eyes and skin.¹⁵ Exposure to EDB vapor concentrations above the standard may cause injury to the lungs, liver, and kidneys as well as CNS depression and death (due to pneumonia resulting from injury to the lungs).¹⁶ NIOSH recommends that EDB be treated as a potential carcinogen.¹⁷ Exposure to EDC vapor concentrations above the standard may cause mental confusion, dizziness, nausea, and vomiting. Liver, kidney, and adrenal injuries may also occur.¹⁶

The OSHA standards for EDB are: 20 parts per million (ppm) PEL, 30 ppm as a ceiling level, 50 ppm maximum peak for five minutes, and 400 ppm IDLH level.^{18,9} (See Appendix, Table A-1.) NIOSH recommends a 15 minute ceiling limit of 1 mg/m³.⁹ ACGIH lists EDB as a substance that is suspect of inducing cancer in man; however, environmental conditions have not been sufficiently defined to assign a TLV.¹³

The OSHA standards for EDC are: 50 ppm PEL, 100 ppm as a ceiling concentration, 200 ppm maximum duration for 5 minutes in any 3 hours, and 1000 ppm IDLH level.^{18,9} NIOSH recommends that the PEL be reduced to 5 ppm per 10-hour workday and the ceiling level be reduced to 15 ppm averaged over a 15 minute period.⁹ ACGIH recommends a TLV of 10 ppm and a STEL of 15 ppm.¹³ (See Appendix, Table A-1.)

Ethyl chloride

Ethyl chloride and a lead-sodium alloy are fed into an autoclave; the resultant chemical reaction produces TEL. Afterwards, any remaining trace of ethyl chloride is vaporized and removed.⁴

The major problems involved in handling ethyl chloride are fire and explosion.¹⁹ Healthwise, it may cause eye irritation, stomach cramps, dizziness and incoordination, liver and kidney damage, cardiac arrhythmias, and cardiac arrest.^{9,20}

The OSHA standards for ethyl chloride are 1000 ppm (2600 mg/m³) PEL and 20,000 ppm IDLH level.^{18,9} ACGIH recommends a TLV of 1000 ppm and a STEL of 1,250 ppm (3,250 mg/m³).¹³ (See Appendix, Table A-1.)

Survey Methods

General

Area and personal air samples were collected at the TEL (process) plant over the four following work shifts:

4-8-80	7:30am to 3:30pm
4-8/9-80	11:30pm to 7:30am
4-9-80	3:30pm to 11:30pm
4-10-80	7:30am to 3:30pm

Only the automated half of the process was in operation at the time of the survey; monitoring for inorganic lead and TEL was conducted in all areas of this process. However, monitoring of ethyl chloride was conducted only in the TEL manufacturing area and monitoring of EDB and EDC was conducted only in the blending area.

Tetraethyl lead (TEL)

Area and personal TEL samples were collected at a flow rate of approximately 1.25 liters per minute (Lpm) for 6-8 hours per shift using MSA Model G pumps. Sampling media were changed at least once during each shift and consisted of an 0.8 micron AA Millipore filter backed up with an XAD-2 resin tube. The filter collected the inorganic lead fraction and the XAD-2 resin tube collected the TEL (organic lead) fraction.

Chemical analysis for TEL was performed using NIOSH Method No. S383.²¹ TEL was desorbed from the resin with pentane, separated, and analyzed by using a gas chromatograph with a photoionization detector.

Inorganic Lead (Pb)

Personal and area Pb samples were collected on 0.8 micron AA Millipore filters in line with MSA Model G pumps. The flow rate was 1.0 Lpm with a collection time of 6-8 hours per shift.

Analysis of lead was performed using NIOSH Method SCP No. S-341.²² The sample filters were wet ashed with nitric and perchloric acids to insure their complete oxidation. The ashed samples were diluted to a final volume of 25 milliliters (mL) and analyzed by atomic absorption spectrophotometry.

Ethylene dibromide (EDB) and Ethylene dichloride (EDC)

Area and personal EDB and EDC samples were obtained using standard 150 milligram (mg) charcoal tubes in line with MDA Accuhaler (Model 808) low-flow pumps [20 cubic centimeters minute (cc/min) limiting orifice]. Samples were collected for a period of 6-8 hours per shift.

The samples were analyzed for EDB and EDC by using a modification of NIOSH Method S-104.²³ Each sample was separated into A and B sections and each section was desorbed with 1 mL of carbon disulfide containing 1 microliter per milliliter (ul/mL) dodecane as an internal standard. Each section was analyzed by using a gas chromatograph.

Ethyl chloride

Area and personal ethyl chloride samples were collected using charcoal tubes (600 mg) in line with MDA Accuhaler (Model 808) low-flow pumps (20 cc/min limiting orifice). Sampling was conducted for 6-8 hours per shift.

The charcoal tube samples were analyzed for ethyl chloride by using a modification of NIOSH Method S-105.²⁴ Ethyl chloride was desorbed from the charcoal with 2 mLs of carbon disulfide containing 1 uL/mL octane as an internal standard. The sample analysis was completed on a gas chromatograph by flame ionization detection.

Statistical Methods

Summary statistics such as arithmetic mean, standard deviation, geometric mean, geometric standard deviation, and 95% confidence limits of geometric means were calculated by different job titles for TEL, Pb, EDB, EDC and ethyl chloride.

Due to the small number of samples in each statistical grouping, the statistical analysis was judged not to be descriptive of the exposure data. This analysis may be seen in the Appendix, Tables A-2 through A-6.

Results and Discussion

All 8-hour TWA area TEL sample results and most 8-hour TWA personal TEL sample results were below the OSHA standard of 0.075 mg/m^3 and ACGIH TLV of 0.15 mg/m^3 . However, 6 of 60 TEL personal samples were above the OSHA standard and ranged from 0.092 to 0.159 mg/m^3 ; five were above the ACGIH TLV. (See Table 1 and Appendix, Table A-8.) Although these levels were above the OSHA standard, the employees were required to wear respirators and protective clothing, which if properly used and maintained would decrease the actual exposure level.

For lead, the 8-hour TWA area sampling results ranged from 0.003 to 0.006 mg/m^3 which is below the OSHA standard of 0.05 mg/m^3 , the NIOSH recommended standard of 0.1 mg/m^3 , and ACGIH TLV of 0.15 mg/m^3 . Four of 60 TWA personal sampling results were above the NIOSH recommended standard and ranged from 0.118 to 0.869 mg/m^3 ; six were above the OSHA standard and ranged from 0.057 to 0.869 mg/m^3 . (See Table 2 and Appendix, Table A-9.)

All area and personal EDB and EDC sample results were below the analytical limit of detection of 0.01 mg/sample . (See Appendix, Tables A-10 and A-11.) For ethyl chloride, all 8-hour TWA area and personal sampling results were well below the OSHA standard and ACGIH TLV of 2600 mg/m^3 and ranged from 0.138 to 0.572 mg/m^3 . (See Appendix, Table A-12.)

Conclusions

Worker exposure to TEL, Pb, EDB, EDC, and ethyl chloride was assessed at the Ethyl Corporation. The employees' exposure to EDB, EDC and ethyl chloride was judged not to constitute a health hazard since all area and personal levels found were well below the OSHA standards and NIOSH recommended standards (for EDB and EDC).

Due to physical contact with TEL and Pb containing substances and to malfunctioning of equipment (e.g. system leaks), the potential existed for an appreciable exposure to TEL and/or Pb. However, since the employees wore protective equipment, their actual personal exposure was probably below the OSHA standards of 0.075 mg/m^3 for TEL and 0.05 mg/m^3 for Pb.

TABLE 1

Worker Exposure Levels for Tetraethyl Lead (TEL)
Greater Than the OSHA Standard ^(a) (0.075 mg/m³) 4/8-10/80

Date	Shift	Job Title	TEL TWA Concentration (mg/m ³)
4/8	1	3rd Floor Operator	0.141
4/8	3	4th Floor Operator	0.109
4/9	2	Blender Operator	>0.094
4/9	2	4th Floor Operator	0.159
4/9	2	Furnace Operator	0.137
4/10	1	2nd Floor Operator	0.092

a) Data have not been corrected for temperature and pressure variation; maximum deviation would be within $\pm 1\%$ of actual values.

TABLE 2

Worker Exposure Levels for Lead (Pb)
Greater Than the OSHA Standard ^(a) (0.050 mg/m³) 4/8-10/80

Date	Shift	Job Title	Pb TWA Concentration (mg/m ³)
4/8	1	Carpenter (Sludge pit)	0.118
4/8	3	Alloy Charge Pot Operator	0.869
4/8	3	B-2 Furnace Operator	0.198*
4/9	2	Chief Operator	0.091
4/9	2	Alloy Charge Pot Operator	0.167
4/10	1	Alloy Charge Pot Operator	0.057

a) Data have not been corrected for temperature and pressure variation; maximum deviation would be within $\pm 1\%$ of actual values.

* Furnace B-2 started leaking Pb resulting in Pb fumes.

Recommendations

1. Continue to emphasize the respirator fit testing program.
 2. Continue the industrial hygiene and biological monitoring programs.
 3. Better maintain equipment to reduce system leaks.
-
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APPENDIX A

FIG. A-1
Flow Chart of Ethyl Corp.
Tetraethyl Lead, Process and Plants

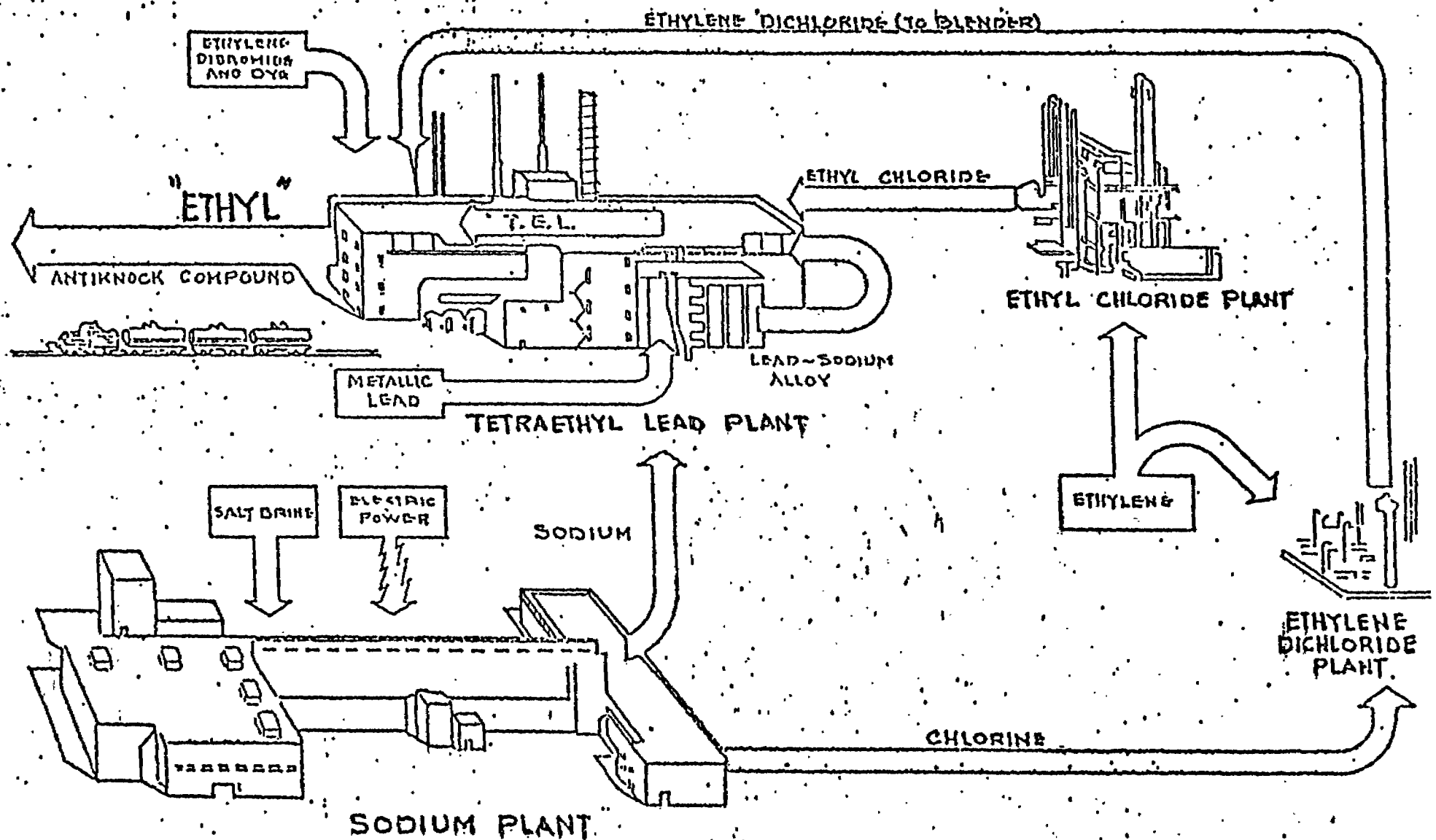


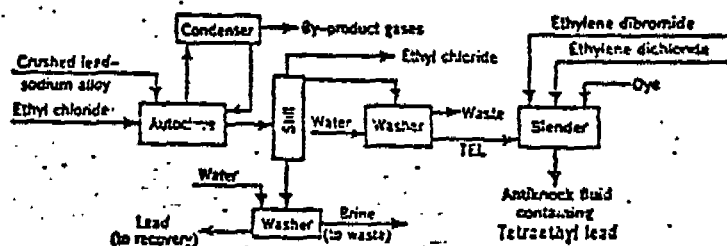
FIGURE A-2

Process Flow, Reaction, and Material Requirements

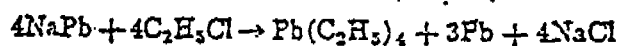
TETRAETHYLLEAD
(LEAD TETRAETHYL, TEL)



From Ethyl Chloride and Lead-Sodium Alloy



Reaction



85-90% yield (based on sodium)

Material Requirements

Basis—1 metric ton tetraethyllead

Sodium	325 kg
Lead (theoretical)	640 kg
Ethyl chloride (theoretical)	798 kg
Catalyst	7.5 to 25 kg
Ferric chloride	Small
Sodium thiosulfate	Small

TABLE A-1

Applicable Standards of Substances Monitored

On April 8-10, 1980

Substance Monitored	OSHA Standard		NIOSH Recommended Standard		ACGIH Recommended Standard	
	PEL	IDLH	TWA	Ceiling	TLV	STEL
TEL	0.075 mg/m ³	40 mg/m ³			0.1 mg/m ³	
Pb	0.05 mg/m ³	Variable	0.1 mg/m ³		0.15 mg/m ³	0.45 mg/m ³
EDB	20 ppm 154 mg/m ³ (30 ppm ceiling)	400 ppm		0.13 ppm 1 mg/m ³	*	
EDC	50 ppm 202 mg/m ³ (100 ppm ceiling) **	1000 ppm	5 ppm/ 10 hr shift	15 ppm/ (15 min.)	40 mg/m ³	60 mg/m ³
Ethyl chloride	1000 ppm 2600 mg/m ³	20,000 ppm			1000 ppm 2600 mg/m ³	1250 ppm 3250 mg/m ³

* Is suspect of inducing cancer in man; environmental conditions have not been sufficiently defined to assign a TLV.

** 200 ppm for five minute - peak for any three hour period.

TABLE A-2

SUMMARY STATISTICS
ETHYL CORPORATION
PASADENA, TX
APRIL 8-10, 1980

REAGENT

TETRA ETHYL LEAD

JOB TITLE	N	MAX	MIN	MEAN	STANDARD DEVIATION	STANDARD ERROR	GEOMETRIC MEAN	GEOMETRIC STANDARD DEVIATION	95% LOWER CONFIDENCE LIMIT	95% UPPER CONFIDENCE LIMIT
CHIEF OPERATOR	3	0.030	0.011	0.018	0.010	0.006	0.016	1.705	0.004	0.062
+ 2ND FLOOR OPERATOR	8	0.092	0.023	0.039	0.024	0.008	0.034	1.624	0.023	0.051
+ 3RD FLOOR OPERATOR	4	0.141	0.025	0.056	0.057	0.028	0.041	2.280	0.011	0.152
4TH FLOOR OPERATOR	5	0.159	0.024	0.076	0.058	0.026	0.057	2.381	0.020	0.169
+ BLENDER OPERATOR	6	0.108	0.018	0.055	0.034	0.014	0.046	1.935	0.023	0.092
+ ALLOY CHARGE POT OPERATOR	4	0.039	0.017	0.027	0.009	0.005	0.026	1.402	0.015	0.044
+ ALLOY HOPPER BOOTH OPERATOR	3	0.027	0.017	0.022	0.005	0.003	0.022	1.290	0.012	0.041
+ A FURNACE OPERATOR	4	0.137	0.025	0.055	0.054	0.027	0.042	2.212	0.012	0.148
+ B-1 FURNACE OPERATOR	3	0.082	0.026	0.048	0.030	0.017	0.042	1.801	0.010	0.182
+ FURNACE RELIEF OPERATOR	2	0.030	0.024	0.027	0.004	0.003	0.027	1.178	0.006	0.118
+ FURNACE BREAKER	1	0.018	0.018	0.018	.	.	0.018	.	.	.
+ PIPEFITTER (FURNACE AREA)	3	0.027	0.023	0.025	0.002	0.001	0.025	1.093	0.020	0.031
CARPENTER (SLUDGE PIT)	1	0.030	0.030	0.030	.	.	0.030	.	.	.
+ 2ND FLOOR OPERATOR (TRAINEE)	1	0.024	0.024	0.024	.	.	0.024	.	.	.
+ BLENDER FOREMAN	2	0.032	0.027	0.030	0.004	0.003	0.029	1.128	0.010	0.087
+ B-2 FURNACE OPERATOR	2	0.082	0.023	0.053	0.041	0.029	0.044	2.418	0.000	122.084
+ FURNACE SWINGMAN	1	0.027	0.027	0.027	.	.	0.027	.	.	.
+ ELECTRICIAN	2	0.024	0.012	0.018	0.008	0.006	0.017	1.627	0.000	1.348

NOTE: UNITS FOR THIS TABLE ARE IN: MILLIGRAMS PER CUBIC METER
+ MORE THAN 50% OF THE VALUES USED TO COMPUTE THIS STATISTIC
WERE BELOW THE LIMIT OF DETECTION

TABLE A-2 (Cont)

SUMMARY STATISTICS
ETHYL CORPORATION
PASADENA, TX
APRIL 8-10, 1980

APRIL 8-10, 1980

REAGENT		TETRA ETHYL LEAD								
JOB TITLE	N	MAX	MIN	MEAN	STANDARD DEVIATION	STANDARD ERROR	GEOMETRIC MEAN	GEOMETRIC STANDARD DEVIATION	95% LOWER CONFIDENCE LIMIT	95% UPPER CONFIDENCE LIMIT
+ MACHINIST	1	0.024	0.024	0.024	.	.	0.024	.	.	.
+ OUTSIDE MACHINIST (FURNACE AREA)	2	0.057	0.026	0.041	0.021	0.015	0.039	1.722	0.000	5.077
+ OUTSIDE MACHINIST (1ST FLOOR ALLOY)	1	0.035	0.035	0.035	.	.	0.035	.	.	.
+ BLENDER TRAINEE	1	0.042	0.042	0.042	.	.	0.042	.	.	.
+ MLA OPERATOR	1	0.027	0.027	0.027	.	.	0.027	.	.	.
+ TEL OFFICE	1	0.013	0.013	0.013	.	.	0.013	.	.	.
+ CHANGE ROOM (CONTAMINATED SIDE)	1	0.017	0.017	0.017	.	.	0.017	.	.	.
+ CHANGE ROOM (CLEAN SIDE)	1	0.015	0.015	0.015	.	.	0.015	.	.	.
+ IH OFFICE	1	0.015	0.015	0.015	.	.	0.015	.	.	.
+ BREAK AREA	1	0.013	0.013	0.013	.	.	0.013	.	.	.

NOTE: UNITS FOR THIS TABLE ARE IN: MILLIGRAMS PER CUBIC METER
+ MORE THAN 50% OF THE VALUES USED TO COMPUTE THIS STATISTIC
WERE BELOW THE LIMIT OF DETECTION

EC 3034

TABLE A-3

SUMMARY STATISTICS
ETHYL CORPORATION
PASADENA, TX
APRIL 8-10, 1980

REAGENT	LEAD										
JOB TITLE	N	MAX	MIN	MEAN	STANDARD DEVIATION	STANDARD ERROR	GEOMETRIC MEAN	GEOMETRIC STANDARD DEVIATION	95% LOWER CONFIDENCE LIMIT	95% UPPER CONFIDENCE LIMIT	
+ 2ND FLOOR OPERATOR	8	12.876	2.576	6.093	4.130	1.460	5.024	1.926	2.905	8.689	
+ 3RD FLOOR OPERATOR	4	5.590	3.048	4.406	1.061	0.530	4.303	1.292	2.864	6.466	
+ 4TH FLOOR OPERATOR	5	5.427	3.004	4.107	1.015	0.454	4.005	1.287	2.927	5.481	
+ BLENDER OPERATOR	6	11.445	3.218	6.350	3.020	1.233	5.807	1.583	3.587	9.402	
ALLOY CHARGE POT OPERATOR	4	869.499	3.936	274.214	402.625	201.313	75.379	9.645	2.047	2775.283	
ALLOY HOPPER BOOTH OPERATOR	3	18.322	3.740	12.001	7.482	4.320	9.849	2.339	1.193	81.286	
A FURNACE OPERATOR	4	30.661	14.485	23.901	6.792	3.396	23.056	1.382	13.777	38.585	
B-1 FURNACE OPERATOR	3	32.771	6.580	17.755	13.512	7.801	14.423	2.233	1.960	106.135	
FURNACE RELIEF OPERATOR	2	46.895	25.017	35.956	15.470	10.939	34.252	1.559	0.632	1854.942	
FURNACE BREAKER	1	37.111	37.111	37.111	.	.	37.111	.	.	.	
PIPEFITTER (FURNACE AREA)	2	24.727	9.137	16.932	11.024	7.795	15.031	2.022	0.027	8391.651	
CARPENTER (SLUDGE PIT)	1	118.296	118.296	118.296	.	.	118.296	.	.	.	
2ND FLOOR OPERATOR (TRAINEE)	1	5.414	5.414	5.414	.	.	5.414	.	.	.	
+ BLENDER FOREMAN	EC 3035 2	3.617	3.051	3.334	0.400	0.283	3.322	1.128	1.127	9.789	
B-2 FURNACE OPERATOR	2	198.268	45.558	121.913	107.982	76.355	95.040	2.829	0.008	1085191.324	
FURNACE SWINGMAN	1	20.075	20.075	20.075	.	.	20.075	.	.	.	
ELECTRICIAN	2	21.584	4.516	13.050	12.068	8.534	9.873	3.022	0.000	204307.023	
MACHINIST	1	12.804	12.804	12.804	.	.	12.804	.	.	.	

NOTE: UNITS FOR THIS TABLE ARE IN: MICROGRAMS PER CUBIC METER
+ MORE THAN 50% OF THE VALUES USED TO COMPUTE THIS STATISTIC
WERE BELOW THE LIMIT OF DETECTION

TABLE A-3 (cont)

SUMMARY STATISTICS
ETHYL CORPORATION
PASADENA, TX
APRIL 8-10, 1980

APRIL 8-10, 1980

REAGENT	LEAD									
JOB TITLE	N	MAX	MIN	MEAN	STANDARD DEVIATION	STANDARD ERROR	GEOMETRIC MEAN	GEOMETRIC STANDARD DEVIATION	95% LOWER CONFIDENCE LIMIT	95% UPPER CONFIDENCE LIMIT
OUTSIDE MACHINIST (FURNACE AREA)	2	24.728	4.928	14.828	14.000	9.900	11.039	3.128	9.000	311304.352
OUTSIDE MACHINIST (1ST FLOOR ALLOY)	1	12.372	12.372	12.372	.	.	12.372	.	.	.
+ BLENDER TRAINEE	1	4.316	4.316	4.316	.	.	4.316	.	.	.
MLA OPERATOR	1	12.302	12.302	12.302	.	.	12.302	.	.	.
+ TEL OFFICE	1	4.827	4.827	4.827	.	.	4.827	.	.	.
+ CHANGE ROOM (CONTAMINATED SIDE)	1	6.249	6.249	6.249	.	.	6.249	.	.	.
+ CHANGE ROOM (CLEAN SIDE)	1	5.687	5.687	5.687	.	.	5.687	.	.	.
+ IH OFFICE	1	5.462	5.462	5.462	.	.	5.462	.	.	.

NOTE: UNITS FOR THIS TABLE ARE IN: MICROGRAMS PER CUBIC METER
+ MORE THAN 50% OF THE VALUES USED TO COMPUTE THIS STATISTIC
WERE BELOW THE LIMIT OF DETECTION

TABLE A-4

SUMMARY STATISTICS
ETHYL CORPORATION
PASADENA, TX
APRIL 8-10, 1980

REAGENT ETHYLENE DIBROMIDE

JOB TITLE	N	MAX	MIN	MEAN	STANDARD DEVIATION	STANDARD ERROR	GEOMETRIC MEAN	GEOMETRIC STANDARD DEVIATION	95% LOWER CONFIDENCE LIMIT	95% UPPER CONFIDENCE LIMIT
+ BLENDER TRAINEE	1	0.054	0.054	0.054			0.054			
+ MLA OPERATOR	1	0.062	0.062	0.062			0.062			
+ 2ND FLOOR BLENDING	3	0.065	0.056	0.061	0.005	0.003	0.061	1.080	0.050	0.073
+ 3RD FLOOR BLENDING	3	0.070	0.054	0.060	0.008	0.005	0.060	1.143	0.043	0.083
+ 1ST FLOOR BLENDING	3	0.072	0.049	0.058	0.012	0.007	0.057	1.228	0.034	0.096
+ EDB	1	0.123	0.123	0.123			0.123			
+ EDC	1	0.055	0.055	0.055			0.055			

NOTE: UNITS FOR THIS TABLE ARE IN: MILLIGRAMS PER CUBIC METER
+ MORE THAN 50% OF THE VALUES USED TO COMPUTE THIS STATISTIC
WERE BELOW THE LIMIT OF DETECTION

EC 3037

TABLE A-5

SUMMARY STATISTICS
ETHYL CORPORATION
PASADENA, TX
APRIL 8-10, 1980

EC 3038

REAGENT ETHYLENE DICHLORIDE

JOB TITLE	N	MAX	MIN	MEAN	STANDARD DEVIATION	STANDARD ERROR	GEOMETRIC MEAN	GEOMETRIC STANDARD DEVIATION	95% LOWER CONFIDENCE LIMIT	95% UPPER CONFIDENCE LIMIT
+ BLENDER TRAINEE.	1	0.054	0.054	0.054	.	.	0.054	.	.	.
+ MLA OPERATOR	1	0.062	0.062	0.062	.	.	0.062	.	.	.
+ 2ND FLOOR BLENDING	3	0.065	0.056	0.061	0.005	0.003	0.061	1.080	0.050	0.073
+ 3RD FLOOR BLENDING	3	0.070	0.054	0.060	0.008	0.005	0.060	1.143	0.043	0.083
+ 1ST FLOOR BLENDING	3	0.072	0.049	0.058	0.012	0.007	0.057	1.228	0.034	0.096
+ EDB	1	0.123	0.123	0.123	.	.	0.123	.	.	.
+ EDC	1	0.055	0.055	0.055	.	.	0.055	.	.	.
+ BLENDER OPERATOR	1	0.073	0.073	0.073	.	.	0.073	.	.	.

NOTE: UNITS FOR THIS TABLE ARE IN: MICROGRAMS PER CUBIC METER
+ MORE THAN 50% OF THE VALUES USED TO COMPUTE THIS STATISTIC
WERE BELOW THE LIMIT OF DETECTION

TABLE A-6

SUMMARY STATISTICS
ETHYL CORPORATION
PASADENA, TX
APRIL 8-10, 1980

EC 3039

H REAGENT

ETHYL CHLORIDE

JOB TITLE	N	MAX	MIN	MEAN	STANDARD DEVIATION	STANDARD ERROR	GEOMETRIC MEAN	GEOMETRIC STANDARD DEVIATION	95% LOWER CONFIDENCE LIMIT	95% UPPER CONFIDENCE LIMIT
+ B-7	1	0.198	0.198	0.198	.	.	0.198	.	.	.
+ B-15	1	0.265	0.265	0.265	.	.	0.265	.	.	.
+ B-1	1	0.299	0.299	0.299	.	.	0.299	.	.	.
+ B-8	2	0.208	0.142	0.175	0.047	0.033	0.172	1.310	0.015	1.941
+ B-12	1	0.239	0.239	0.239	.	.	0.239	.	.	.
+ B-9	2	0.488	0.166	0.327	0.227	0.161	0.285	2.139	0.000	264.100
+ B-4	2	0.280	0.180	0.230	0.071	0.050	0.224	1.367	0.013	3.730
+ B-3	1	0.206	0.206	0.206	.	.	0.206	.	.	.
+ B-13	1	0.138	0.138	0.138	.	.	0.138	.	.	.
+ B-6	1	0.317	0.317	0.317	.	.	0.317	.	.	.
+ B-2	1	0.572	0.572	0.572	.	.	0.572	.	.	.
+ B-5	1	0.239	0.239	0.239	.	.	0.239	.	.	.

NOTE: UNITS FOR THIS TABLE ARE IN: MILLIGRAMS PER CUBIC METER
+ MORE THAN 50% OF THE VALUES USED TO COMPUTE THIS STATISTIC
WERE BELOW THE LIMIT OF DETECTION

TABLE A-7

Notation for the following sample data tables;

Data have not been corrected for temperature and pressure variation; maximum deviation would be within $\pm 1\%$ of actual values.

TABLE A-8

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT

TETRA ETHYL LEAD

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
3281	CHIEF OPERATOR	08	1	115	160.991	< 0.013	< 0.083	
3361	CHIEF OPERATOR	08	1	200	279.984	< 0.013	< 0.048	< 0.030
3441	3RD FLOOR OPERATOR	08	1	136	139.079	0.015	0.109	
3521	3RD FLOOR OPERATOR	08	1	209	213.731	0.035	0.162	0.141
3781	4TH FLOOR OPERATOR	08	1	140	184.869	0.017	0.091	
3861	4TH FLOOR OPERATOR	08	1	214	286.835	0.013	0.046	0.064
3770	4TH FLOOR OPERATOR	10	1	265	357.824	< 0.013	< 0.037	
3850	4TH FLOOR OPERATOR	10	1	150	202.542	< 0.013	< 0.066	< 0.024
4171	2ND FLOOR OPERATOR	08	1	159	200.487	< 0.013	< 0.066	< 0.033
4251	PIPEFITTER (FURNACE AREA)	08	1	201	259.432	< 0.013	< 0.051	
4331	PIPEFITTER (FURNACE AREA)	08	1	175	225.874	< 0.013	< 0.059	< 0.027
4671	CARPENTER (SLUDGE PIT)	08	1	314	439.575	0.013	0.030	0.030
4751	BLENDER OPERATOR	08	1	301	364.595	< 0.013	< 0.036	< 0.018
5221	ALLOY CHARGE POT OPERATOR	08	1	293	381.087	< 0.013	< 0.035	< 0.017
5301	FURNACE BREAKER	08	1	322	377.244	< 0.013	< 0.035	< 0.018
5481	ALLOY HOPPER BOOTH OPERATOR	08	1	297	401.033	< 0.013	< 0.033	< 0.017
5561	FURNACE RELIEF OPERATOR	08	1	207	250.735	< 0.013	< 0.053	
5641	FURNACE RELIEF OPERATOR	08	1	156	188.960	< 0.013	< 0.070	< 0.030

EC 3041

TABLE (A-1) (Cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

H REAGENT TETRA ETHYL LEAD

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
5721	A FURNACE OPERATOR	08	1	215	268.964	< 0.013	< 0.049	
5801	A FURNACE OPERATOR	08	1	150	187.649	< 0.013	< 0.071	< 0.029
6111	B-1 FURNACE OPERATOR	08	1	210	264.794	0.031	0.116	
6031	B-1 FURNACE OPERATOR	08	1	153	192.921	< 0.013	< 0.069	< 0.082
2620	A FURNACE OPERATOR	10	1	226	271.505	< 0.013	< 0.049	
2700	A FURNACE OPERATOR	10	1	162	194.619	< 0.013	< 0.068	
2720	A FURNACE OPERATOR	10	1	162	194.619	< 0.013	< 0.068	< 0.030
6371	2ND FLOOR OPERATOR	08	1	111	128.942	< 0.013	< 0.103	
6451	2ND FLOOR OPERATOR	08	1	222	257.883	< 0.013	< 0.052	< 0.034
4660	2ND FLOOR OPERATOR	10	1	229	331.950	0.025	0.077	
4580	2ND FLOOR OPERATOR	10	1	188	272.518	< 0.013	< 0.049	< 0.053
6611	BLENDER OPERATOR	08	1	221	243.557	0.024	0.098	
6531	BLENDER OPERATOR	08	1	110	121.227	< 0.013	< 0.110	< 0.084
8720	2ND FLOOR OPERATOR	08	3	280	386.418	< 0.013	< 0.034	
8800	2ND FLOOR OPERATOR	08	3	142	195.969	< 0.013	< 0.068	< 0.023
0011	4TH FLOOR OPERATOR	08	3	254	320.274	0.040	0.125	
0271	4TH FLOOR OPERATOR	08	3	142	179.051	0.014	0.080	0.109
0351	BLENDER OPERATOR	08	3	122	146.565	< 0.013	< 0.091	
0431	BLENDER OPERATOR	08	3	266	319.559	< 0.013	< 0.042	< 0.029
0511	CHIEF OPERATOR	08	3	412	597.221	< 0.013	< 0.022	< 0.011
0771	3RD FLOOR OPERATOR	08	3	252	300.239	< 0.013	< 0.044	
0851	3RD FLOOR OPERATOR	08	3	161	191.819	< 0.013	< 0.069	< 0.027
1081	2ND FLOOR OPERATOR (TRAINEE)	08	3	257	334.264	< 0.013	< 0.040	
1161	2ND FLOOR OPERATOR (TRAINEE)	08	3	169	219.808	< 0.013	< 0.061	

EC 3042

TABLE A-8 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT

TETRA ETHYL LEAD

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
1241	2ND FLOOR OPERATOR	08	3	253	329.061	< 0.013	< 0.040	< 0.024
1321	2ND FLOOR OPERATOR	08	3	174	226.311	< 0.013	< 0.059	< 0.024
1401	MLA OPERATOR	08	3	183	238.016	< 0.013	< 0.056	< 0.027
1581	MLA OPERATOR	08	3	192	249.722	< 0.013	< 0.053	< 0.027
1661	BLENDER FOREMAN	08	3	126	163.880	< 0.013	< 0.081	< 0.027
1741	BLENDER FOREMAN	08	3	252	327.760	< 0.013	< 0.041	< 0.027
1821	ALLOY CHARGE POT OPERATOR	08	3	204	267.355	< 0.013	< 0.050	< 0.024
2051	ALLOY CHARGE POT OPERATOR	08	3	226	296.188	< 0.013	< 0.045	< 0.023
2131	B-2 FURNACE OPERATOR	08	3	204	257.228	< 0.013	< 0.052	< 0.023
2211	B-2 FURNACE OPERATOR	08	3	245	308.926	< 0.013	< 0.043	< 0.025
2471	A FURNACE OPERATOR	08	3	258	302.264	< 0.013	< 0.044	< 0.025
2551	A FURNACE OPERATOR	08	3	191	223.769	< 0.013	< 0.059	< 0.024
2631	ALLOY HOPPER BOOTH OPERATOR	08	3	172	215.171	< 0.013	< 0.062	< 0.013
2711	ALLOY HOPPER BOOTH OPERATOR	08	3	274	342.772	< 0.013	< 0.039	< 0.024
3021	FURNACE RELIEF OPERATOR	08	3	201	245.463	< 0.013	< 0.054	< 0.024
3101	FURNACE RELIEF OPERATOR	08	3	253	308.966	< 0.013	< 0.043	< 0.024
4740	CHIEF OPERATOR	09	2	417	505.104	< 0.013	< 0.026	< 0.013
4820	2ND FLOOR OPERATOR	09	2	197	254.269	< 0.013	< 0.052	< 0.024
5050	2ND FLOOR OPERATOR	09	2	226	291.700	< 0.013	< 0.046	< 0.024
5130	BLENDER FOREMAN	09	2	121	141.759	< 0.013	< 0.094	

TABLE A-8 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT

TETRA ETHYL LEAD

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
5210	BLENDER FOREMAN	09	2	233	272.975	< 0.013	< 0.049	< 0.032
5470	3RD FLOOR OPERATOR	09	2	194	206.096	< 0.013	< 0.065	
5550	3RD FLOOR OPERATOR	09	2	227	241.154	< 0.013	< 0.055	< 0.030
5630	BLENDER OPERATOR	09	2	177	196.823	< 0.014	< 0.069	
5710	BLENDER OPERATOR	09	2	225	250.199	< 0.013	< 0.053	< 0.045
6020	2ND FLOOR OPERATOR	09	2	206	247.478	< 0.013	< 0.054	
6100	2ND FLOOR OPERATOR	09	2	218	261.895	< 0.013	< 0.051	< 0.026
6280	ALLOY CHARGE POT OPERATOR	09	2	191	267.385	< 0.017	< 0.064	
6360	ALLOY CHARGE POT OPERATOR	09	2	237	331.781	< 0.013	< 0.040	< 0.039
6440	BLENDER OPERATOR	09	2	111	135.554	< 0.043	< 0.314	
6520	BLENDER OPERATOR	09	2	261	318.735	< 0.013	< 0.042	< 0.108
6600	4TH FLOOR OPERATOR	09	2	157	210.435	< 0.013	< 0.063	
6780	4TH FLOOR OPERATOR	09	2	259	347.151	< 0.013	< 0.038	< 0.024
6860	ALLOY HOPPER BOOTH OPERATOR	09	2	217	245.612	< 0.013	< 0.054	
7170	ALLOY HOPPER BOOTH OPERATOR	09	2	217	245.612	< 0.013	< 0.054	< 0.027
7250	4TH FLOOR OPERATOR	09	2	191	210.495	0.058	0.276	
7330	4TH FLOOR OPERATOR	09	2	227	250.169	0.015	0.060	0.159
7670	D-2 FURNACE OPERATOR	09	2	184	158.936	0.024	0.150	
7410	D-2 FURNACE OPERATOR	09	2	248	214.218	< 0.013	< 0.062	< 0.082
7750	A FURNACE OPERATOR	09	2	252	317.752	0.069	0.217	
7830	A FURNACE OPERATOR	09	2	186	234.532	< 0.013	< 0.057	0.137
8060	D-1 FURNACE	09	2	203	173.332	< 0.013	< 0.077	

TABLE A-6 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT TETRA ETHYL LEAD									
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)	
8140	OPERATOR B-1 FURNACE OPERATOR	09	2	242	206.632	< 0.013	< 0.064		
								< 0.035	
0000	PIPEFITTER (FURNACE AREA)	10	1	196	247.141	< 0.013	< 0.054		
0130	PIPEFITTER (FURNACE AREA)	10	1	238	300.100	< 0.013	< 0.044		
								< 0.024	
0260	MACHINIST	10	1	199	248.948	< 0.013	< 0.053		
0340	MACHINIST	10	1	238	297.737	< 0.013	< 0.045		
								< 0.024	
0500	B-1 FURNACE OPERATOR	10	1	139	175.268	< 0.013	< 0.076		
0680	B-1 FURNACE OPERATOR	10	1	260	327.840	< 0.013	< 0.041		
								< 0.026	
0760	3RD FLOOR OPERATOR	10	1	187	243.219	< 0.013	< 0.055		
0840	3RD FLOOR OPERATOR	10	1	219	284.839	< 0.013	< 0.047		
								< 0.025	
1070	ELECTRICIAN	10	1	273	330.679	< 0.013	< 0.040		
1150	ELECTRICIAN	10	1	186	225.298	< 0.013	< 0.059		
								< 0.024	
1230	OUTSIDE MACHINIST (FURNACE AREA)	10	1	197	230.798	< 0.013	< 0.058		
1310	OUTSIDE MACHINIST (FURNACE AREA)	10	1	236	276.490	< 0.013	< 0.048		
								< 0.026	
1570	PIPEFITTER (FURNACE AREA)	10	1	191	256.007	< 0.013	< 0.052		
1650	PIPEFITTER (FURNACE AREA)	10	1	240	321.684	< 0.013	< 0.041		
								< 0.023	
1730	ALLOY CHARGE POT OPERATOR	10	1	152	190.151	< 0.013	< 0.070		
1810	ALLOY CHARGE POT OPERATOR	10	1	244	305.243	< 0.013	< 0.044		
								< 0.027	
2040	OUTSIDE MACHINIST (FURNACE AREA)	10	1	199	203.505	0.018	0.091		
2120	OUTSIDE MACHINIST	10	1	236	241.343	< 0.013	< 0.055		

TABLE A-8 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT

TETRA ETHYL LEAD

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
(FURNACE AREA)								
2200	OUTSIDE MACHINIST (1ST FLOOR ALLOY)	10	1	202	262.729	0.013	0.051	< 0.057
2380	OUTSIDE MACHINIST (1ST FLOOR ALLOY)	10	1	233	303.048	< 0.013	< 0.044	< 0.035
2880	FURNACE SWINGMAN	10	1	222	288.741	< 0.013	< 0.046	< 0.027
3010	FURNACE SWINGMAN	10	1	161	209.402	< 0.013	< 0.064	< 0.092
3270	2ND FLOOR OPERATOR	10	1	197	256.225	0.031	0.121	
3350	2ND FLOOR OPERATOR	10	1	221	287.441	0.019	0.066	
4160	BLENDER OPERATOR	10	1	174	207.308	0.017	0.080	
4080	BLENDER OPERATOR	10	1	266	316.918	< 0.013	< 0.042	< 0.044
4320	BLENDER TRAINEE	10	1	250	327.641	0.017	0.053	
4240	BLENDER TRAINEE	10	1	192	251.629	< 0.013	< 0.053	< 0.042
4400	ELECTRICIAN	10	1	439	553.545	< 0.013	< 0.024	< 0.012
0420	TEL OFFICE	10	1	370	517.971	< 0.013	< 0.026	< 0.013
2460	CHANGE ROOM (CONTAMINATED SIDE)	10	1	363	400.050	< 0.013	< 0.033	< 0.017
2540	CHANGE ROOM ^M (CLEAN SIDE)	10	1	360	439.635	< 0.013	< 0.030	< 0.015
3430	IH OFFICE	10	1	394	457.685	< 0.013	< 0.029	< 0.015
3510	BREAK AREA	10	1	357	492.683	< 0.013	< 0.027	< 0.013

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TABLE A-9

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT	LEAD									
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (UG)	CONCENTRATION (UG/CU.M.)	TWA CONCENTRATION (UG/CU.M.)		
4773	CHIEF OPERATOR	08	1	315	440.975	< 3.000	< 6.803	< 3.402		
4853	3RD FLOOR OPERATOR	08	1	345	352.810	< 3.000	< 8.503	< 4.252		
2313	4TH FLOOR OPERATOR	10	1	415	560.366	< 5.000	< 8.923	< 4.461		
5243	2ND FLOOR OPERATOR	08	1	159	200.487	< 3.000	< 14.964	< 7.482		
5323	PIPEFITTER (FURNACE AREA)	08	1	376	485.306	12.000	24.727	24.727		
5583	CARPENTER (SLUDGE PIT)	08	1	314	439.575	52.000	118.296	118.296		
5663	BLENDER OPERATOR	08	1	301	364.595	3.000	8.228	8.228		
6133	ALLOY CHARGE POT OPERATOR	08	1	293	381.087	< 3.000	< 7.872	< 3.936		
6213	FURNACE BREAKER	08	1	322	377.244	14.000	37.111	37.111		
6473	ALLOY HOPPER BOOTH OPERATOR	08	1	297	401.033	< 3.000	< 7.481	< 3.740		
6553	FURNACE RELIEF OPERATOR	08	1	363	439.695	11.000	25.017	25.017		
6633	A FURNACE OPERATOR	08	1	365	456.613	14.000	30.661	30.661		
6713	B-1 FURNACE OPERATOR	08	1	363	457.715	15.000	32.771	32.771		
1763	A FURNACE OPERATOR	10	1	388	466.124	12.000	25.744	25.744		
7023	2ND FLOOR OPERATOR	08	1	333	386.825	< 3.000	< 7.755			

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TABLE A-9 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT	LEAD								
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (UG)	CONCENTRATION (UG/CU.M.)	TWA CONCENTRATION (UG/CU.M.)	
									< 3.878
2813	2ND FLOOR OPERATOR	10	1	417	604.468	7.000	11.580		11.580
7103	BLENDER OPERATOR	08	1	331	364.784	< 3.000	< 8.224	<	4.112
3043	2ND FLOOR OPERATOR	08	3	422	582.387	< 3.000	< 5.151	<	2.576
3123	4TH FLOOR OPERATOR	08	3	396	499.325	< 3.000	< 6.008	<	3.004
3203	BLENDER OPERATOR	08	3	388	466.124	< 3.000	< 6.436	<	3.218
3383	CHIEF OPERATOR	08	3	412	597.221	5.000	8.372		8.372
3463	3RD FLOOR OPERATOR	08	3	413	492.058	< 3.000	< 6.097	<	3.048
3543	2ND FLOOR OPERATOR (TRAINEE)	08	3	426	554.071	3.000	5.414		5.414
3623	2ND FLOOR OPERATOR	08	3	427	555.372	< 3.000	< 5.402	<	2.701
3703	MLA OPERATOR	08	3	375	487.739	6.000	12.302		12.302
3883	BLENDER FOREMAN	08	3	378	491.641	< 3.000	< 6.102	<	3.051
4013	ALLOY CHARGE POT OPERATOR	08	3	430	563.543	490.000	869.499		869.499
4273	B-2 FURNACE OPERATOR	08	3	204	257.228	51.000	198.268		198.268
4353	A FURNACE OPERATOR	08	3	449	526.033	13.000	24.713		24.713
4433	ALLOY HOPPER BOOTH OPERATOR	08	3	172	215.171	3.000	13.942		13.942

TABLE A-9 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT	LEAD							
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (UG)	CONCENTRATION (UG/CU.M.)	TWA CONCENTRATION (UG/CU.M.)
4513	FURNACE RELIEF OPERATOR	08	3	454	554.429	26.000	46.895	46.895
7432	CHIEF OPERATOR	09	2	417	505.104	46.000	91.070	91.070
7512	2ND FLOOR OPERATOR	09	2	423	545.970	< 3.000	< 5.495	< 2.747
7772	BLENDER FOREMAN	09	2	354	414.734	< 3.000	< 7.234	< 3.617
7852	3RD FLOOR OPERATOR	09	2	421	447.250	< 5.000	< 11.179	< 5.590
8082	BLENDER OPERATOR	09	2	402	447.022	< 5.000	< 11.185	< 5.593
8162	2ND FLOOR OPERATOR	09	2	424	509.373	< 5.000	< 9.816	< 4.908
8242	ALLOY CHARGE POT OPERATOR	09	2	428	599.167	100.000	166.899	166.899
8322	BLENDER OPERATOR	09	2	372	454.290	< 5.000	< 11.006	< 5.503
8402	4TH FLOOR OPERATOR	09	2	416	557.586	< 5.000	< 8.967	< 4.484
8582	ALLOY HOPPER BOOTH OPERATOR	09	2	434	491.224	9.000	18.322	18.322
8662	4TH FLOOR OPERATOR	09	2	418	460.664	< 5.000	< 10.854	< 5.427
8742	B-2 FURNACE OPERATOR	09	2	432	373.154	17.000	45.558	45.558
8822	A FURNACE OPERATOR	09	2	438	552.284	8.000	14.485	14.485
0033	B-1 FURNACE OPERATOR	09	2	445	379.965	< 5.000	< 13.159	< 6.580

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TABLE A-9 (cont)
SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT. LEAD								
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (UG)	CONCENTRATION (UG/CU.M.)	TWA CONCENTRATION (UG/CU.M.)
0113	PIPEFITTER (FURNACE AREA)	10	1	434	547.240	5.000	9.137	9.137
0373	MACHINIST	10	1	437	546.684	7.000	12.804	12.804
0533	B-1 FURNACE OPERATOR	10	1	399	503.108	7.000	13.914	13.914
0613	3RD FLOOR OPERATOR	10	1	406	528.058	< 5.000	< 9.469	< 4.734
0873	ELECTRICIAN	16	1	459	555.977	12.000	21.584	21.584
1003	OUTSIDE MACHINIST (FURNACE AREA)	10	1	433	507.288	< 5.000	< 9.856	< 4.928
1343	ALLOY CHARGE POT OPERATOR	10	1	396	495.394	28.000	56.521	56.521
1263	OUTSIDE MACHINIST (FURNACE AREA)	10	1	435	444.848	11.000	24.728	24.728
1423	OUTSIDE MACHINIST (1ST FLOOR ALLOY)	10	1	435	565.777	7.000	12.372	12.372
1843	FURNACE SWINGMAN	10	1	383	498.144	10.000	20.075	20.075
2073	2ND FLOOR OPERATOR	10	1	418	543.666	7.000	12.876	12.876
2573	BLENDER OPERATOR	10	1	440	524.226	6.000	11.445	11.445
2653	BLENDER TRAINEE	10	1	442	579.270	< 5.000	< 8.632	< 4.316
2733	ELECTRICIAN	10	1	439	553.545	< 5.000	< 9.033	< 4.516
0453	TEL OFFICE	10	1	370	517.971	< 5.000	< 9.653	

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TABLE A-9 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT	LEAD								
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (UG)	CONCENTRATION (UG/CU.M.)	TWA CONCENTRATION (UG/CU.M.)	
1503	CHANGE ROOM (CONTAMINATED SIDE)	10	1	363	400.050	< 5.000	< 12.498	< 4.827	
1683	CHANGE ROOM (CLEAN SIDE)	10	1	360	439.635	< 5.000	< 11.373	< 6.249	
2153	IH OFFICE	10	1	394	457.685	< 5.000	< 10.925	< 5.687	
5163	4TH FLOOR OPERATOR	08	1	354	474.484	< 3.000	< 6.323	< 3.161	

EC 3051

TABLE A-10

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT ETHYLENE DIBROMIDE

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
8071	BLENDER OPERATOR	08	1	297	60.373	< 0.010	< 0.166	< 0.083
8151	BLENDER OPERATOR	08	1	333	32.055	< 0.010	< 0.312	< 0.156
7421	BLENDER OPERATOR	08	3	387	77.021	< 0.010	< 0.130	< 0.065
7681	MLA OPERATOR	08	3	374	80.518	< 0.010	< 0.124	< 0.062
7603	BLENDER OPERATOR	09	2	396	68.368	< 0.010	< 0.146	< 0.073
7523	BLENDER OPERATOR	09	2	370	73.364	< 0.010	< 0.136	< 0.068
7341	BLENDER OPERATOR	10	1	440	115.601	< 0.010	< 0.087	< 0.043
7001	BLENDER TRAINEE	10	1	441	92.341	< 0.010	< 0.108	< 0.054
8571	EDB	08	1	337	40.533	< 0.010	< 0.247	< 0.123
8311	EDC	08	1	333	90.766	< 0.010	< 0.110	< 0.055
7501	2ND FLOOR BLENDING	08	3	395	81.153	< 0.010	< 0.123	< 0.062
7761	3RD FLOOR BLENDING	08	3	400	71.866	< 0.010	< 0.139	< 0.070
7841	1ST FLOOR BLENDING	08	3	386	68.973	< 0.010	< 0.145	< 0.072
7283	2ND FLOOR BLENDING	09	2	406	89.608	< 0.010	< 0.112	< 0.056
7443	3RD FLOOR BLENDING	09	2	409	91.837	< 0.010	< 0.109	< 0.054
7363	1ST FLOOR BLENDING	09	2	397	93.469	< 0.010	< 0.107	< 0.053
7181	2ND FLOOR BLENDING	10	1	432	77.017	< 0.010	< 0.130	

EC 3052

TABLE (A-2) (cont)

**SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX**

H	REAGENT	ETHYLENE DIBROMIDE
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SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
6871	3RD FLOOR BLENDING	10	1	430	88.972	< 0.010	< 0.112	< 0.065
7261	1ST FLOOR BLENDING	10	1	441	102.099	< 0.010	< 0.098	< 0.056

TABLE A-11

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT	ETHYLENE DICHLORIDE										
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA	CONCENTRATION (MG/CU.M.)		
8071	BLENDER OPERATOR	08	1	297	60.373	< 0.010	< 0.166	<	0.083		
8151	BLENDER OPERATOR	08	1	333	32.055	< 0.010	< 0.312	<	0.156		
7421	BLENDER OPERATOR	08	3	387	77.021	< 0.010	< 0.130	<	0.065		
7681	MLA OPERATOR	08	3	374	80.518	< 0.010	< 0.124	<	0.062		
7603	BLENDER OPERATOR	09	2	396	68.368	< 0.010	< 0.146	<	0.073		
7523	BLENDER OPERATOR	09	2	370	73.364	< 0.010	< 0.136	<	0.068		
7341	BLENDER OPERATOR	10	1	440	115.601	< 0.010	< 0.087	<	0.043		
7001	BLENDER TRAINEE	10	1	441	92.341	< 0.010	< 0.108	<	0.054		
8571	EDB	08	1	337	40.533	< 0.010	< 0.247	<	0.123		
8311	EDC	08	1	333	90.766	< 0.010	< 0.110	<	0.055		
7501	2ND FLOOR BLENDING	08	3	395	81.153	< 0.010	< 0.123	<	0.062		
7761	3RD FLOOR BLENDING	08	3	400	71.866	< 0.010	< 0.139	<	0.070		
7841	1ST FLOOR BLENDING	08	3	386	68.973	< 0.010	< 0.145	<	0.072		
7283	2ND FLOOR BLENDING	09	2	406	89.608	< 0.010	< 0.112	<	0.056		
7443	3RD FLOOR BLENDING	09	2	409	91.837	< 0.010	< 0.109	<	0.054		
7363	1ST FLOOR BLENDING	09	2	397	93.469	< 0.010	< 0.107	<	0.053		
7181	2ND FLOOR BLENDING	10	1	432	77.017	< 0.010	< 0.130	<			

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TABLE A-1 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT ETHYLENE DICHLORIDE

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
6871	3RD FLOOR BLENDING	10	1	430	88.972	< 0.010	< 0.112	< 0.065
7261	1ST FLOOR BLENDING	10	1	441	102.099	< 0.010	< 0.098	< 0.056
								< 0.049

EC 3055

TABLE A-12
SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

REAGENT		ETHYL CHLORIDE		PASADENA, TX						
SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)		CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)	
6462	4TH FLOOR OPERATOR	08	1	128	26.141	<	0.010	<	0.383	
6542	4TH FLOOR OPERATOR	08	1	128	26.141	<	0.010	<	0.383	
6622	4TH FLOOR OPERATOR	08	1	213	43.626	<	0.010	<	0.229	
6702	4TH FLOOR OPERATOR	08	1	213	43.626	<	0.010	<	0.229	
									< 0.143	
0362	4TH FLOOR OPERATOR	10	1	415	62.412		0.020		0.320	
0442	4TH FLOOR OPERATOR	10	1	415	62.412	<	0.010	<	0.160	
									0.200	
6042	B-8	08	1	201	42.330	<	0.010	<	0.236	
6122	B-8	08	1	201	42.330	<	0.010	<	0.236	
6202	B-8	08	1	153	28.896	<	0.010	<	0.346	
6382	B-8	08	1	153	28.896	<	0.010	<	0.346	
									< 0.142	
6882	B-9	08	1	200	34.693	<	0.010	<	0.288	
7012	B-9	08	1	200	34.693	<	0.010	<	0.288	
7272	B-9	08	1	151	25.520	<	0.010	<	0.392	
7352	B-9	08	1	151	25.520	<	0.010	<	0.392	
									< 0.166	
5572	B-4	08	1	200	30.543	<	0.010	<	0.327	
5652	B-4	08	1	200	30.543	<	0.010	<	0.327	
5732	B-4	08	1	156	24.936	<	0.010	<	0.401	
5812	B-4	08	1	156	24.936	<	0.010	<	0.401	
									< 0.180	
5072	B-13	08	1	200	41.722	<	0.010	<	0.240	
5152	B-13	08	1	200	41.722	<	0.010	<	0.240	
5232	B-13	08	1	147	30.706	<	0.010	<	0.326	
5312	B-13	08	1	147	30.706	<	0.010	<	0.326	
									< 0.138	
2722	B-9	08	3	243	56.137		0.050		0.891	
3032	B-9	08	3	161	36.067		0.030		0.832	
2802	B-9	08	3	243	56.137	<	0.010	<	0.178	
3112	B-9	08	3	161	36.407	<	0.010	<	0.275	
									< 0.488	
3372	B-6	08	3	240	47.769		0.020		0.419	
3532	B-6	08	3	162	31.363		0.020		0.638	
3452	B-6	08	3	240	47.769	<	0.010	<	0.209	
3612	B-6	08	3	162	31.363	<	0.010	<	0.319	
									< 0.317	
3872	B-2	08	3	236	28.779	<	0.010	<	0.347	
4002	B-2	08	3	236	28.779	<	0.010	<	0.347	
4182	B-2	08	3	163	4.357	<	0.010	<	2.295	

TABLE A-12 (cont)

SUMMARY OF SAMPLES TAKEN ON
APRIL 8-10, 1980
ETHYL CORPORATION
PASADENA, TX

H REAGENT

ETHYL CHLORIDE

SAMPLE NUMBER	JOB TITLE/LOCATION	DATE	SHIFT	SAMPLE TIME (MINUTES)	SAMPLE VOLUME (LITERS)	ANALYTICAL RESULTS (MG)	CONCENTRATION (MG/CU.M.)	TWA CONCENTRATION (MG/CU.M.)
4262	B-2	08	3	163	4.357	< 0.010	< 2.295	< 0.572
4342	B-5	08	3	238	61.422	0.020	0.326	
4502	B-5	08	3	162	42.964	0.020	0.466	
4422	B-5	08	3	238	61.422	< 0.010	< 0.163	
4682	B-5	08	3	162	42.964	< 0.010	< 0.233	< 0.239
0522	B-8	09	2	225	59.856	0.020	0.334	
0782	B-8	09	2	190	48.707	0.010	0.205	
0602	B-8	09	2	225	59.856	< 0.010	< 0.167	< 0.208
1172	B-12	09	2	225	45.828	0.020	0.436	
1332	B-12	09	2	188	37.874	0.010	0.264	
1252	B-12	09	2	225	45.828	< 0.010	< 0.218	
1412	B-12	09	2	188	37.874	< 0.010	< 0.264	< 0.239
2062	B-4	09	2	223	44.656	0.020	0.448	
1832	B-4	09	2	223	44.656	< 0.010	< 0.224	< 0.280
2142	B-3	09	2	223	37.675	0.010	0.265	
2562	B-3	09	2	194	35.114	0.010	0.285	
2222	B-3	09	2	223	37.675	< 0.010	< 0.265	
2642	B-3	09	2	194	35.114	< 0.010	< 0.285	< 0.206
8431	B-7	10	1	418	88.287	0.030	0.340	
8731	B-7	10	1	418	88.922	0.030	0.337	
8651	B-7	10	1	418	88.287	< 0.010	< 0.113	
8731	B-7	10	1	418	88.922	< 0.010	< 0.112	< 0.198
8811	B-15	10	1	417	84.903	0.040	0.471	
0022	B-15	10	1	417	84.903	< 0.010	< 0.118	< 0.265
0102	B-1	10	1	418	58.519	0.030	0.513	
0282	B-1	10	1	418	58.519	< 0.010	< 0.171	< 0.299