

LEAD THROUGH THE DECADES

AS THE WORLD
MOVES ON, LEAD

LEAD PRODUCTS DIVISION

August 1941

LEAD

"Lead lined acid storage tanks are a familiar sight in the chemical plant equipment of the past. In the last 19 years of trial and error, the lead and ferric sulfate tanks are being replaced by aluminum sulfate tanks.

Six 12-inch diameter lead tanks at the Baltimore plant are being replaced by 24-inch lead storage tanks. The lead tanks are being replaced by tanks obtained by heat of reaction. Lead is being given out in the service in the five dilution tanks at the Baltimore plant. The tanks at Baltimore are holding up well with a bimetallic coating lining.

Complete depreciation was assumed for the boiling tanks to be five years, yet in one to two years' time maintenance cost had become excessive. There is no objection to the use of lead by the waterworks engineer except for mechanical fatigue resulting from temperature changes causing bulging and sagging.

a. INTRODUCTORY HISTORY

Alum has been a useful chemical since ancient times. The Egyptians used it in certain medical preparations and the Romans used it to fireproof their siege machines. Alums are used in water treatment and in dyeing but are being replaced by aluminum sulfate, which has a greater alumina equivalent per unit weight. The word alum or filter alum is often used to denote aluminum sulfate which may be used in water treatment, in the textile industry, as mordant for dyes, and pharmaceutically in dilute solution as a mild astringent and antiseptic for the skin. Small amounts are used in sizing of paper and in making some baking powders, but most important is water clarifying which consumes 65% of all aluminum sulfate produced.

Large scale water treatment may take one of several forms depending on the condition of the water supply. Pure chlorine may be added to destroy any bacteria present when the natural water is clear. Filtration through slow sand filters and subsequent treatment with chlorine is often practiced where there is suspended matter present. Treatment with aluminum sulfate (or ferrous and ferric sulfate), filtration, and subsequent treatment with chlorine is often required. As most of our natural waters are basic the addition of aluminum sulfate causes the formation of aluminum hydroxide as a colloidal dispersion throughout the water. This coagulates slowly and, as it settles, carries down any suspended matter present, including bacteria and many absorbed coloring materials.



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b. PROCESS DESCRIPTION

In the Baltimore process, the liquor is distilled in a still which is tilted to 15° from the vertical. The still is heated by steam which is introduced into a coil around the still. The liquor is distilled at a pressure of 10 in. Hg. and the distillate is collected in a receiver. The residue is then distilled at a pressure of 10 in. Hg. and the distillate is collected in a receiver. (Aluminum chloride, calcium chloride, magnesium chloride, sodium chloride, and aluminum chloride are used in the process.)

Agitation may be brought about by stirring or by air blast. The still is heated by steam which is introduced into a coil around the still. The liquor is distilled at a pressure of 10 in. Hg. and the distillate is collected in a receiver. The residue is then distilled at a pressure of 10 in. Hg. and the distillate is collected in a receiver. The process is to have one or two reaction tanks which are heated by steam and the reaction is carried out at a temperature of 100° to 120° C. and the reaction is carried out for 2 to 4 hours. The reaction is carried out in a tank which is lined with lead and the reaction is carried out in a tank which is lined with lead.

In Baltimore the reaction is run at more than once a day while at the Dalecarlia plant in Washington, D.C., they often run two batches per day and claim a slightly higher temperature. The batch is cooled for three hours at one degree per minute.

For uses other than water treatment the concentrated liquor may be poured into flat pans to be cooled and completely solidified. The solid cake is then broken and ground to size for shipment.

c. EQUIPMENT DESCRIPTION

In the Baltimore filtration plant on Hillian Road there are six steel tanks (see first drawing), 15 ft. in diameter and 17 ft. in overall depth. The circular tanks have a hemispherical bottom with a 7-1/2 ft. radius which is not generally regarded as easy to fabricate or line. A shallow "V" bottom is far easier to construct, less difficult to repair, and allows a better lead installation. Three of these tanks are used for dilution and are lined with a bituminous enamel which is a product of the Waukesha-Dove-Harnett Corporation, Westfield, New Jersey. The other three tanks are lined with 20-lb. lead with vertical straps every 16 in. These straps merge toward the center, terminating at the outer edge of a circular lead plate 3 ft. in diameter.

At the Dalecarlia filtration plant in Washington, D.C., there are six 10,000 gal. tanks, 12 ft. in diameter, all lined with lead until recently when lead was torn out of the boiling tank and replaced by an acid resistant brick. In the brick lined tank Pyroflex No. 100 cement was used and an asphalt lining was applied to the steel. For better bonding the asphalt was warmed before the placing of each batch. Three coats of primer were applied before the final coat of pitch. The hemispherical bottom of the tank was double lined with two courses of four inch brick and the side walls were of one course, six inches thick. For unobstructed lead pipe has been replaced with ceramic tubing. Vertical straps, 15 in. apart had been installed in all six tanks. The lead linings were not wrapped over or secured at the top except by the upper end of the vertical straps.

c. EXPERIMENTAL INVESTIGATION (CONTINUED)

The 60° 30' tanks are 1 ft. apart in three long cylindrical steel tanks in the basement. Safety lead joints are fastened around the tanks and 3 in. diameter holes are cut in the lead lining from the tanks to the lead lined concrete floor. Safety lead joints are also cut at the top of the pipe line from the tanks to the floor.

d. LEAD LINING OF THE TANKS

The history of the lead lining of the tanks in the basement and the tanks are closely parallel. In 1927, the tanks were lined with lead and over efforts were made during the summer of 1927 to improve the tanks. Their first plan was to use 10 lb. lead. The first installation in the tanks was with 10 lb. lead and the tanks were 6 ft. apart. The tops were wrapped over in the ground and the eight lead sections were carried to the bottom of the tank where they were cut in orange peel pattern. The bottom consisted of a circular disc of lead, 3 ft. in diameter, with a heavy lead casting over the outlet to serve as a valve seat.

In 1932, 12 lb. lead was installed with horizontal straps as shown in the second drawing. These straps were no more effective than the previous arrangement as they buckled and sagged with repeated heating cycles. The bottom construction retained the arrangement of eight straps converging toward the central disc.

The first drawing shows the last attempt that was made in 1933 to make lead linings give reasonable service in alum boiling tanks. Vertical straps were installed 36 in. apart with 20 lb. lead lining left unfastened at the top.

e. PERFORMANCE OF LEAD

The leakage has occurred only around the lower edges of the vertical straps in the two reaction tanks. These two tanks were said to require as much maintenance as all the rest. The lead lining expands with heating and does not contract, leaving a buckled area of disturbed or "cracked" metal which is probably more readily corroded. The buckling movement of the lead would also tend to weaken the weld metal at the edge of the straps. The expanded metal shows up in the cylindrical portion of the tank as wrinkles and bulges between the straps; however, there is no leakage in this area. Leaks occur only in the bottom area and are always along a seam of welded metal. There is no question of failure through abrasive or chemical action on the lead itself.

The first installation in 1927 of 10-lb. lead using only eight vertical straps failed, but was continued in use with excessive maintenance for five years. The Washington tanks were 12 ft. in diameter and the straps for joining the eight sheets of lead were well over 6-1/2 ft. apart.

The combination of 12-lb. lead with horizontal straps installed in 1932 failed in a year's time. Excessive sagging occurred in the sheet lead just above the horizontal straps and many of the bulges became too large to dress back into place. These had to be cut out and a new seam turned in. There were even horizontal cracks in the lead.

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c. PERFORMANCE OF LEAD (CONTINUED)

The 1936 installations have served to date only under variable strains and with constant repair. Vertical stress is low, stress due to acid factory as the lead formed the upper third of the tank, and the effect of the temperature change of approximately 150° F. in the process. The lead was tried during this period and was said to be very satisfactory.

CONCLUSIONS

Conclusions pertaining only to the Washington and Baltimore water works have been reached as follows:

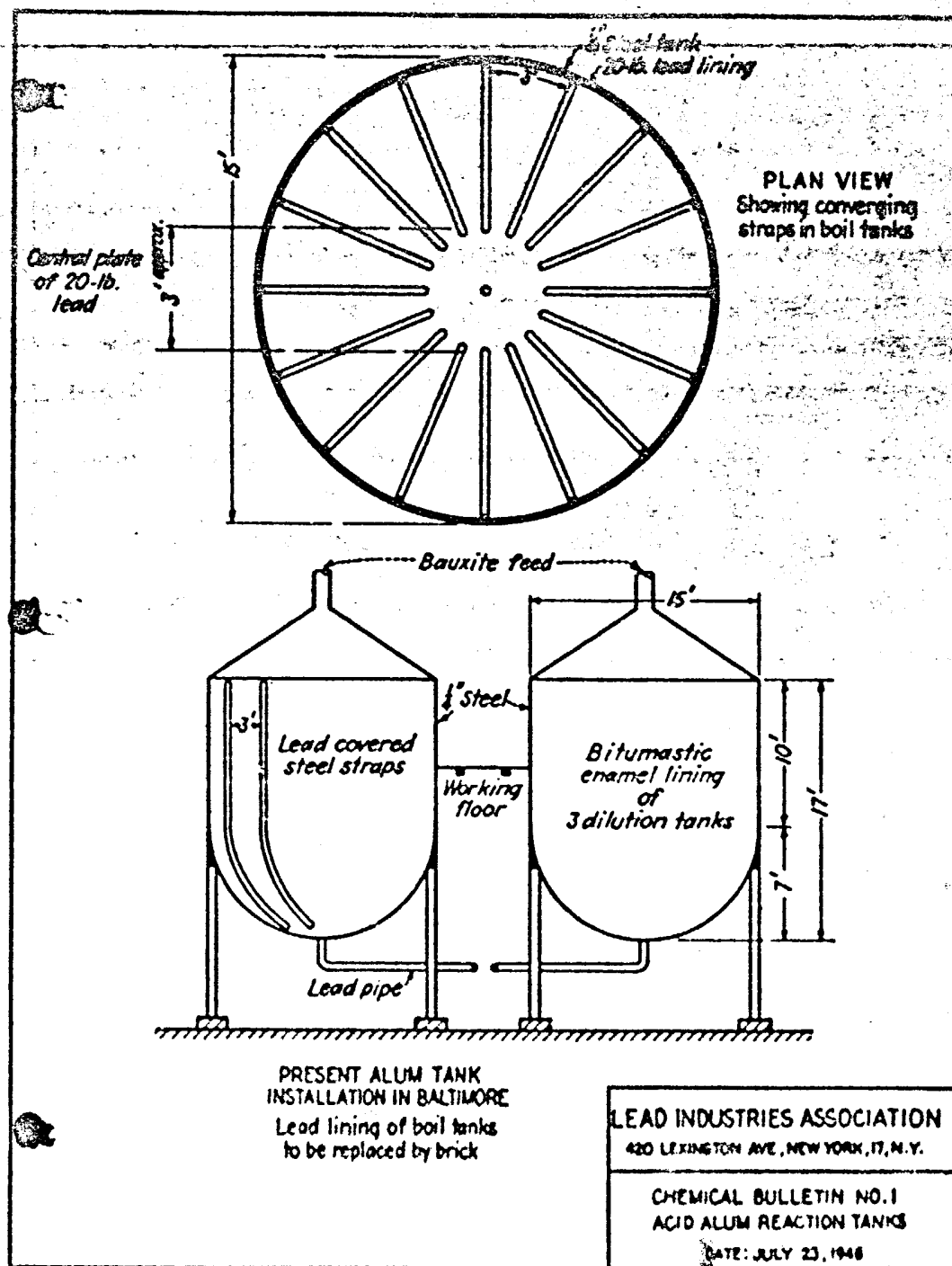
1. Lead linings with certain combinations of straps have failed in the acid alum reaction tank.
2. Lead has been replaced by brick in the reaction tanks.
3. Bitumastic linings are giving good service in three dilution tanks in the Baltimore plant while lead linings are serving the same function in a satisfactory manner in the Washington plant.
4. The brick lining recently installed in the Washington reaction tank has an excellent appearance, but it is too early to judge the worth of its service.

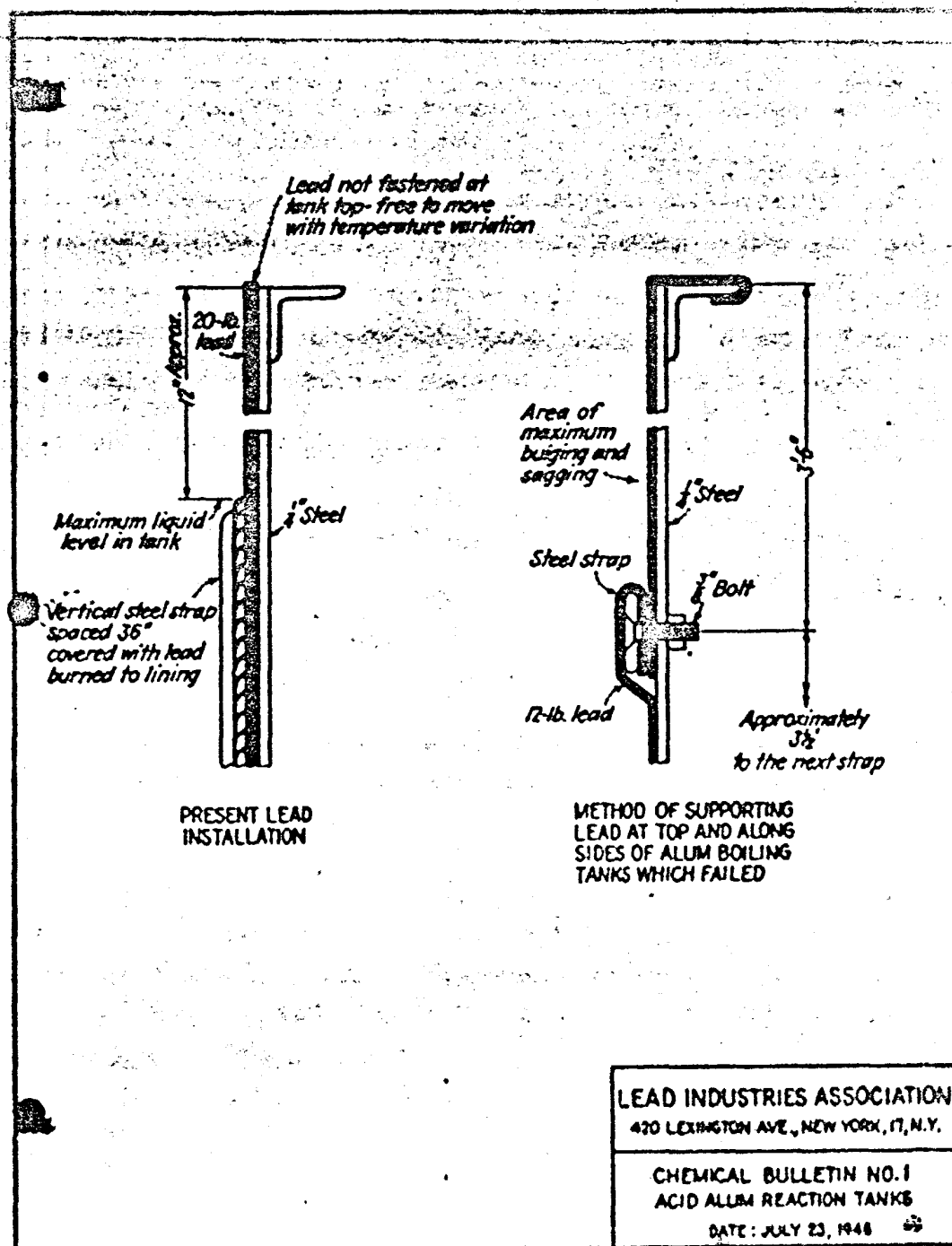
Lead has a black eye at these two plants and probably others for failing to do the job. Actually it has not been given a proper test. If straps had been tried at a distance of 2 1/2 in., undoubtedly the increased length of service of the lead lining would more than offset the cost of additional straps.

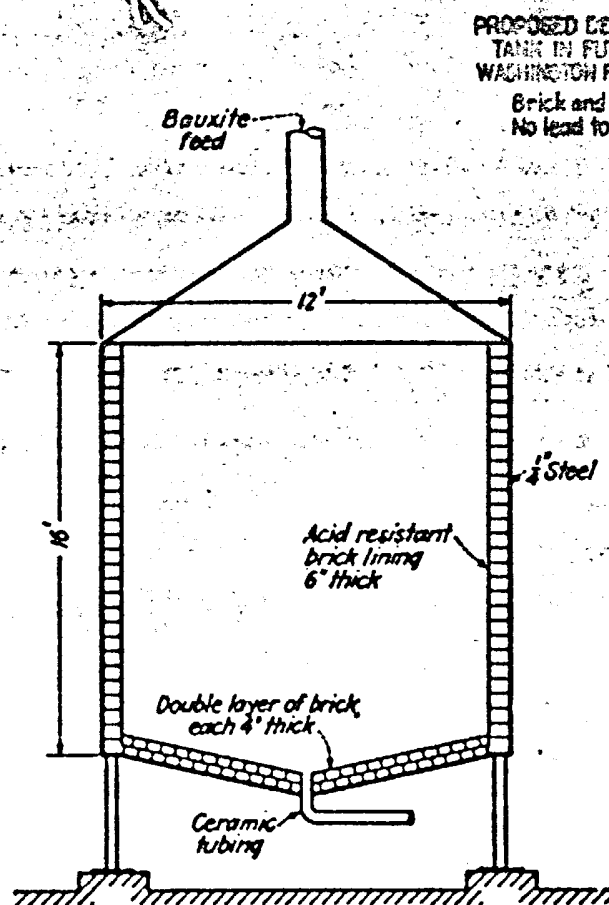
It is planned in Washington to build a new filtration plant about 1950. Designs for the alum tanks incorporate a shallow "V" bottom and show a brick lining with no section of lead (see third drawing).

Future bulletins hope to point out the advisability of using lead and brick combinations. Advantages would include:

1. Eliminate the need of using straps for support as the brick lining would prevent the lead from bulging outward.
2. Depending upon local conditions, it might be possible to use a lighter lead inner lining.
3. Abrasive protection would be furnished for lead.
4. Thermal effect of brick as insulation would allow lead to be used at higher temperatures.







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CHEMICAL BULLETIN NO. 1
ACID ALUM REACTION TANKS
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