

1988 CAPITAL BUDGET

Lake Charles VCM Plant

H-101 Control Revisions

\$100,000 Capital

Project Description

200,000 LB
Reverse, a 4 ft/sec
line
This economic project provides recirculation of the cooling water used in H-101, the Direct Chlorination Reactor Cooler, to increase the shellside cooling water velocity and provide temperature control on R-101, the Direct Chlorination Reactor. The project includes installation of a cooling water recirculation line, a recirculation pump, and a temperature control valve.

Problem Description

SPACE
In August, 1986, H-101 developed a tube leak, resulting in an environmental incident and making replacement necessary. The exchanger historically has failed approximately every 30 months. Failure is caused by erosion on the process (tube) side and shell side corrosion caused by pitting. The process side corrosion is allowed to occur intentionally, as the tubes are sacrificed to provide iron for ferric chloride, which catalyzes the chlorination reaction. Sacrificial ferrules were installed in the tops of the exchanger tubes during the May 1987 turnaround. These will protect the tubes from process side corrosion while still providing ferric chloride.

Cooling water is currently supplied to the shellside of H-101 without temperature control by the main cooling water supply header. The cooling water lines supply approximately 6700 gpm to the shell side flow velocity of 2.7 ft/sec. A minimum velocity of 3 ft/sec. is recommended to minimize shellside pitting, which leads to premature tube failure. A shellside cooling water velocity of 4 ft/sec. can be obtained and is preferable *requiring* a cooling water flowrate of 9000 gpm. This project will supply 9000 gpm cooling water to H-101 by recirculating *with* a portion of the cooling water return back to the supply, thus reducing shellside pitting and extending the life of the exchanger to four or more years. *from the exchanger to the return supply header*

The project will also provide temperature control for R-101, the Direct Chlorinator Reactor. In the past, the cooling water flow to H-101 has sometimes been "pinched back" during

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8-21-87

even more
coldest
~~the~~
the winter months to maintain the reactor temperature at 55°C. However, the resulting cooling water velocities in H-101 are very low, making it susceptible to pitting. In recent years, the cooling water valve has been left wide open, resulting in reactor temperatures of 45-50°C. At these lower temperatures increased concentrations of 1,1,2-trichloroethane, an unwanted by-product, are formed in the reactor. This project will control operation at the desired temperature of 55°C while maintaining an adequate flowrate of cooling water to H-101 to minimize corrosion due to pitting.

Project Alternatives

The following alternatives were considered:

- This would*
- ✓ 1) Modify the tube pitch and the number of baffles in H-101 to give a more even velocity profile, thereby eliminating "dead zones" which are highly susceptible to pitting, ~~and~~ raise overall cooling water velocity. This alternative was rejected because it would require installation of a new exchanger and it would not provide the benefits of temperature control.
 - would* 2) Install a closed cooling water system which would allow ~~other water treatment systems such as chromate treatment to be used and allow leaks to be contained in the closed system.~~ This option was rejected due to the high associated cost.

STILL NEED ECONOMICS

- 3) Run a 4th cooling water pump

Talks about money / Dec. 1981

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VISTA

Vista Chemical Company
GENERAL ENGINEERING
HOUSTON, TEXAS

Estimate Summary

W. O. No. _____

Sheet No. _____ Of _____

Project Title 0-101 Temperature Control
Location 1311 Estimator WLB Class of Estimate Major
Department _____ Nelson Refinery Index _____
Checked By _____ Approved By _____ % Quoted _____

Capacity _____

Original Date _____

Rev. No. _____ Date 3-3-87

DESCRIPTION	LABOR		MATERIAL	SUBCONTRACT	TOTAL	%
	MH	\$				
EQUIPMENT						
Pressure Vessels						
Towers & Internals						
Exchangers						
Pumps & Compressors		8000	12000			
Furnaces						
TOTAL EQUIPMENT		8000	12000		20000	
OTHER MATERIALS						
Piping		15000	30000		45000	
Instruments		2000	5500		7500	
Electrical		2500	2500		5000	
Structural						
Concrete & Site		1500	500		2000	
Insulation						
Painting				2500	2500	
Fireproofing						
Buildings						
TOTAL OTHER MAT.		21000	38500	2500	62000	
TOTAL DIRECT COST		29000	50500	2500	82000	
FIELD COST						
HOME OFFICE COST						
BOND, ARI, SALES TAX					3000	
ESCALATION 3%					1500	
CONTINGENCY 10%					10500	
TOTAL					170000	

Control Valve	\$4,000
Temperature Controller	\$4,500
Pump	\$8,500
Motor	\$3,500

Globe Valve 18"Ø	\$11,000
Gate Valve 10"Ø 2on	4,000
Gate Valve 8"Ø 2on	2,600
Check Valve 8"Ø 2on	4,000
Globe Valve 6"Ø	1,200
Other Valves	1,000

\$23,800

Pipe	2,000
Flanges	\$1,500
wok	1,200
fittng	2,000
	6,500

Electrical	\$2,500
Electrical labor	\$2,600

Instrument	1,000
Instrument labor	2,000

Painting	500
labor	2,000