[I] Fluid Meters, Their Selection and Installation (*American Society of Mechanical Engineers*, 1933).

[J] The Orifice Meter for Measurement of Flow of Gases and Liquids, by Allen D. MacLean (Pittsburgh Equitable Meter Co., 1938).

[K] Flow Measurement (*American Society of Mechanical Engineers*, 1940).

[L] Pitot Tube Practice, by Edward S. Cole (*A.S.M.E. Transactions 57*; 1935, 281–294; Discussion, idem. *58*, 1936, 146–156).

[M] Pitot Tubes in Large Pipes, by Edward S. Cole and E. Shaw Cole (*A.S.M.E. Transactions, 61*, 1939, 465–473; Discussion, idem. *61*, 1939, 473–475).

[N] Investigation of Errors of Pitot Tubes, by C. W. Hubbard (*A.S.M.E. Transactions, 61*, 477–497; Discussion, idem. *61*, 1939, 497–506).

[O] Piping Arrangements for Acceptable Flowmeter Accuracy, by R. E. Sprenkle (*A.S.M.E. Transactions, 67*, 345–357, 1945; Discussion, idem. *67*, 357–360, 1945).

CHAPTER 5

FUNDAMENTALS OF HEAT TRANSFER

Conduction, Convection, Radiation, Combined Convection and Radiation, Heat-Flow Resistance, Practical Heat Transfer Problems, Unit Conductances for Convection Flow Systems, Radiation Factors or Emissivities, Solutions for Steady-State Conduction Problems

HEAT is that form of energy that is transferred by virtue of an existing temperature difference. The temperature difference is the potential which causes the transfer, the latter in turn being resisted by the thermal properties of the material combined in a single term known as the resistance. Energy exchange associated with evaporation, condensation, etc. is treated elsewhere such as in the section on *cooling tower design* in Chapter 37. The objectives of this chapter are to:

1. Describe the mechanisms and present the rate equations for the different modes of heat transfer.
2. Illustrate the application of the basic concepts to steady-state problems (temperature independent of time or a cyclic variable thereof) by means of several typical solutions of heat transfer systems.

Further applications to specific systems will be found throughout THE GUIDE.

CONDUCTION, CONVECTION AND RADIATION

Thermal conduction is the term applied to the mechanism of heat transfer whereby the molecules of higher kinetic energy transmit part of their energy to adjacent molecules of lower kinetic energy by direct molecular action. Since the temperature is proportional to the average kinetic energy of the molecules, thermal transfer will occur in the direction of decreasing temperature. The motion of the molecules is random; there is no net material flow associated with the conduction mechanism. In the case of flowing fluids, thermal conduction is significant in the region very close to a solid boundary or wall, for in this region the flow is laminar, parallel with the wall surface, and there are practically no cross currents in the direction of the heat transfer across the solid fluid boundary. In solid bodies the significant mechanism of heat transfer is always thermal conduction.

Contrasted to the thermal conduction mechanism, *thermal convection* involves energy transfer by eddy mixing and diffusion[1] in addition to conduction. This is shown schematically in Fig. 1 which exhibits transfer from a pipe wall at surface temperature t_s to a colder fluid at a bulk temperature t_f. (Bulk temperature is that which would be attained if the fluid stream were drawn off at a certain section and mixed. It is therefore slightly higher than the lowest temperature in the stream). In the *laminar* sublayer, immediately adjacent to the wall, the heat transfer occurs by thermal conduction; in the *transition* region, which is called the buffer layer, eddy mixing as well as conduction effects are significant; in the *eddy* or *turbulent* region the major fraction of the transfer occurs by eddy mixing.

In most commercial equipment the main body of the fluid is in turbulent flow, and the laminar film exists at the solid walls only, as shown in