OPERATING MANUAL
D-700 PVC REACTORS
ABERDEEN, MISSISSIPPI

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I. INTRODUCTION

A. Operator Responsibilities

The purpose of this plant is to safely and economically convert vinyl chloride monomer (VCM) into a useable form of poly vinyl chloride (PVC). This is accomplished by a batch process in which VCM, water, initiator and colloid solution are charged into the reactor and under carefully controlled conditions, PVC with the desired physical properties is produced. This chemical reaction, which changes VCM to PVC, is called polymerization.

The operator helps fulfill the plant's purpose by making sure that quality production is obtained from his equipment without endangering his fellow workers or his equipment. The operator is able to attain his goals in safety, job performance and efficient operation through a training period and on the job experience.

The operator fulfills his responsibilities by:

1. Understanding how his equipment functions.
2. Understanding what role each piece of equipment plays in the process.
3. Keeping a close and regular check on equipment.
4. Knowing how to spot malfunctions and correct them.
5. Keeping his area of responsibility safe and clean.
6. Keeping complete and accurate records.

I. INTRODUCTION (CONTINUED)

A. Operator Responsibilities (Continued)

The operating Manual will cover the normal responsibilities and duties of the Lead Operator and the Reactor "A" Operator. Each phase in the production method will be covered. In addition to normal operating methods, it will also discuss operations under abnormal and emergency conditions. The operator must be prepared to meet these situations with temporary measures until the abnormal condition is corrected or the emergency crisis ceases to exist.

Safety takes second place to no plant activity. The safety of the plant personnel and equipment is to be carefully considered before any job is started. The Conoco safety slogan, "our work is never so urgent or important that we cannot take time to do it safely", is an idea that can help make the work area safer for everyone when it is put into practice.

Good housekeeping is also an important responsibility of the operators. It requires careful attention for safety reasons and to maintain good working conditions. Cleaning up after job completion is the responsibility of the person doing the job. A job should not be considered complete until all materials are picked up and properly stored.

I. INTRODUCTION (CONTINUED)

B. Process Information

Several types of resins are produced. Resin type is determined by a set of physical properties such as particle size and viscosity. Each type of resin produced requires that a certain set of operating conditions be closely followed so that the desired resin properties are obtained. Minor changes in formulas or operating conditions can cause major differences in the physical properties of the resin. Some factors in determining resin properties are reaction temperature, which helps determine viscosity, colloid, which influences particle size, and the amount of recovered VCM charged, which also effects particle size.

The phases of reactor operation and a brief description of each follows:

1. Evacuation

This step removes all air possible by steam eductors. Too much air left in a reactor will alter particle size. Evacuation should require about five minutes.

2. Charge

Water, Colloid and VCM are charged to the reactor simultaneously through a timed sequence system. The temperature of the reactor contents at the end of charging is determined by the charge water temperature. The reactor will be below run temperature at the end of the charge and jacket steam will be used to raise the temperature to the desired level. Charge should take about nine minutes.

I. INTRODUCTION (CONTINUED)

B. Process Information (Continued)

3. Initiator

The initiator is manually loaded into the initiator injection pot and charged into the reactor after reactor charge is complete.

4. Polymerization

This is the time from the initiator addition until most of the VCM has been converted to resin. The reaction generates heat continuously as liquid VCM becomes PVC resin. Heat that is generated is removed by cooling water on the reactor jacket and condenser. Reaction times varies, but generally requires five to six hours.

5. Recovery and Steam Stripping

Recovery and steam stripping removes most of the un-reacted VCM from the reactor via a compressor-vacuum pump system. Steam is added to the bottom of the reactor and rises through the PVC and water slurry to help remove unreacted VCM. Recovery and steam stripping takes about 40 minutes.

6. Dumping

The PVC resin, after reaction is complete, is in a slurry form. The slurry is dumped to a strainer and dump tank and is pumped to blend tanks in the Dryer Room for drying. Dump requires about 25 minutes.

II. GENERAL PROCESS DESCRIPTION

A. Evacuation

Before charging, the inerts present in the polymerization reactor are removed by evacuation. The interlock selector switch is placed on "evacuation" position. The main condenser valve is opened and the evacuation valve is opened, which automatically starts the reactor steam ejector. Any condensate in the steam to the ejector is removed by a cyclone separator. The emergency cooling water supply valve to the reactor is then opened. When the reactor pressure reaches 28.5 inches of mercury vacuum, as indicated by the pressure indicator in the control room and at the reactor, evacuation is complete. This portion of the cycle requires about five minutes.

B. Charge

1. Precharge Preparations

After evacuation, the reactor is ready to be charged. In preparation for charge, adequate quantities of VCM, hot water, colloid solution, and initiator are made ready for the charge sequence.

Prior to charge, fresh VCM is transferred from the VCM storage sphere to the fresh VCM storage tank. This transfer of VCM begins automatically when the VCM liquid level falls below a certain level. When the high liquid level is regained, the transfer process shuts down automatically. Two 200 gpm VCM transfer pumps are used to transfer the VCM from the VCM storage sphere.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

B. Charge (Continued)

1. Precharge Preparations (Continued)

Process water is automatically supplied to the hot water tank when the water level drops below a certain point. The water is filtered by the process water filter, and is heated in the hot water preheater, enroute to the hot water tank. The hot water tank temperature is maintained by the external steam coils on the hot water tank. The colloid solution, previously made-up, remains in the makeup tank until there is less than one reactor charge remaining in the colloid storage tank. The colloid is then pumped from the makeup tank through the colloid transfer filter to the colloid storage tank. While this transfer takes place, the colloid circulation pump is used to mix the new colloid with the colloid remaining in the storage tank. When the solution is transferred the pumps are shut down and a sample is taken to the laboratory for analysis.

After each reactor charge, colloid is transferred at 50 gpm from the storage tank to the colloid charge tank by the colloid circulation pump. When the storage tank contains less than one charge, the full charge tank will contain sufficient colloid to charge seven reactors. The colloid charge tank can be emptied to less than one charge while the new colloid solution is being transferred and analyzed.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

B. Charge (Continued)

1. Precharge Preparations (Continued)

Immediately before the reactor is to be charged, the initiator injection system is made ready for charge in the following manner. First, the initiator injection pot is drained to the sewer. Enough water is manually added from the board so that the pot will be full after the initiator has been added. The initiator is then manually added to the initiator injection pot. The pot is then blocked in and pressurized with high pressure service water to at least 180 psig. The initiator injection system is now ready for the next reactor charge.

2. Reactor Charge

After evacuation is completed, the interlock selector switch is moved to the "charge" position. If the following precharge conditions are met, the charge sequence is ready to begin:

a. Levels in the fresh VCM storage tank, the hot water tank, and the colloid charge tank are adequate for a complete reactor charge.

b. There is sufficient pressure in the initiator injection pot and in the high pressure service water header.

c. The charge meters are reset to the charge quantities.

Steam is usually applied to the reactor jacket at the start of charge by manually opening the steam valve from the Control Room.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

B. Charge (Continued)

2. Reactor Charge (Continued)

This aids in heating the reaction mass to the desired temperature during and immediately following charge. The automatic charge sequence begins with the hot water charge. The hot water is pumped from the hot water tank, to the reactor by the hot water charge pump. After a predetermined quantity of hot water has been charged, the colloid charge pumps and the second hot water charge pump start. The next step in the charge sequence begins with the fresh and recovered VCM charges. The fresh VCM is pumped to the reactor from the fresh VCM storage tank, by one of the two VCM charge pumps. The recovered VCM is pumped from one of two recovered VCM storage tanks by the recovered VCM charge pump into the suction of the VCM charge pump. The recovered VCM is filtered in the recovered VCM filter and the total VCM charge is filtered enroute to the reactor by the VCM charge filter.

Shortly after the beginning of the VCM charge, one of the hot water charge pumps shuts down until the VCM charge is completed and then restarts. This insures that there will be an adequate amount of water charge remaining to flush out the charge line. Both hot water charge pumps continue to run until charge is completed.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

B. Charge (Continued)

2. Reactor Charge (Continued)

When the VCM, water and colloid charge is complete, the initiator is charged by opening the initiator charge valve from the Control Room. Loading the initiator and preparation of the initiator charge pot was discussed in the precharge preparations section.

C. Polymerization

After charge is completed, the reactor interlock selector switch is placed in the "polymerization" position, and the reactor temperature controller is placed on automatic. When the reaction mass reaches the desired temperature the steam is turned off. The reaction mass temperature is automatically controlled by varying the amount of cooling water that is passed through the top-mounted knockback condenser and the reactor jacket.

The reaction mass is continually mixed and kept in suspension by the bottom-mounted single speed agitator. The agitator mechanical seals are lubricated and cooled by seal oil from a seal oil pressure unit.

During polymerization, mechanical seal purge water is injected into the reactor through the reactor cleaning nozzle and inboard of the agitator mechanical seal. The water is added to keep the reactor

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

C. Polymerization (Continued)

cleaning nozzle and agitator mechanical seals clean. The purge water flow for each service is indicated with a rotameter and manually adjusted.

The inerts present in the reactor during polymerization accumulate in the reactor condenser head space. These inerts are vented to the recovery system to prevent inert blanketing.

Approximately one and one-half hour after the beginning of each polymerization cycle, a sample of resin is taken. The sample is checked for unusual resin conglomerates which indicate a potentially bad batch. If these resin conglomerates occur, several more samples are taken. Depending on the severity of the problem, the batch may be killed early or the resin may be isolated after recovery.

Before the sample is taken, the blowdown tank is recovered if it is not already under vacuum. To take a resin sample, the one-hour resin sampler is attached to the appropriate reactor sampling line and the valve opened until the sampling pressure gauge reads 60 psig. The sampling system lines are cleared of VCM vapors and resin by evacuating to the blowdown tank and flushing with water. The sampling system lines are then vented to the atmosphere and the sampler disconnected. The resin is removed from the sampler by removing the screen insert.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

C. Polymerization (Continued)

When the desired degree of polymerization is reached and the reactor pressure has dropped to the desired pressure, the reaction is stopped by manually adding a mixture of AMS, BHT and OMS (the short stop solution) to the reactor. High pressure service water is used to pressure the short stop solution from the AMS short stop charge pot into the reactor through the same piping as the agitator mechanical seal purge water. The AMS short stop charge pot is then blocked in and refilled with the short stop solution. This system is also used to "kill" runaway reactions.

A nitric oxide (NO) short stop addition system is provided to inject NO into the reactors in the event of power failure, major VCM releases, fires, or other emergencies. The system is activated either locally or from the control room. NO is supplied from the emergency NO short stop bottles and is injected into the reactor through the same piping as the agitator mechanical seal purge water.

D. Recovery and Steam Stripping

1. Recovery

When reaction is completed, the interlock selector switch is moved to the "recovery and steam stripping" position. The following sequence then occurs. The recovery compressor seal water systems, the water recirculation systems for the recovery knockout drums, and two of the three recovery compressors are

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

D. Recovery and Steam Stripping (Continued)

1. Recovery (Continued)

manually started from the board. Cooling water to the recovered VCM condenser and the water recirculation cooler starts automatically with the compressors, and the hydroquinone injection system starts with the compressor seal water systems.

The vapor from the reactor flows through a pressure control valve to two resin knockout drums in series which remove carryover resin. The pressure control valve prevents excessive carryover of resin from the reactor by limiting the pressure to the recovery system to about 35 psig. Each of the knockout drums have an internal water spray system and a recirculation pump. Both knockout drums have an on-off level control system which, on high liquid level, diverts the discharge of the water recirculation pumps to the blowdown tank. A water recirculation cooler, (the function of which is explained in the steam stripping portion of the recovery system process description), is provided and can be used in the water recirculation loop of either scrubbing stage.

The VCM vapors from the knockout drums are compressed by the recovery compressors.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

D. Recovery and Steam Stripping (Continued)

1. Recovery (Continued)

The recovery compressors are constant volume liquid ring compressors with a water seal. The discharge streams from the compressors flow to two parallel seal water recirculation systems which operate as follows. Seal water is separated from the VCM vapors in the seal water separators, filtered by the seal water filters, cooled by the seal water coolers, and pumped back to the compressors by the seal water pumps. The flow of seal water to each compressor is controlled at 50 gpm. The seal water temperature is controlled just above the VCM condensation temperature (95-105°F). Automatic draining of the seal water separators to the blowdown tank is provided to maintain the correct water level.

The VCM vapors from the seal water system are condensed in two recovered VCM condensers. The condensed VCM is collected in the recovered VCM collect tank which is on automatic on-off level control. VCM is transferred to the recovered VCM storage tanks by the recovered VCM transfer pump when there is high liquid level in the VCM collect tank.

Inerts are bled from the collect tank to the V-11 area blowdown tank.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

D. Recovery and Steam Stripping (Continued)

1. Recovery (Continued)

When the reactor pressure drops to 7 psig, the two recovery vacuum pumps automatically start. The VCM flow from the recovery knockout drums and the seal water flow are both diverted to the vacuum pumps which discharge into the suction of the compressors.

2. Steam Stripping

In order to reduce residual VCM in the slurry, the slurry in the reactor is heated and stripped with steam. At the start of a normal recovery, steam addition to the reactor is manually started from the control room and the slurry mass is heated. When the temperature of the reactor has risen to the desired temperature, the steam stripping operation is completed.

As recovery proceeds, less and less VCM is recovered from the reactor. To supply sufficient VCM vapor to the recovery vacuum pumps and compressors, a VCM backpressure system is used. This is done to prevent cavitation and overheating of the vacuum pumps and compressors. Before entering the recovery knockout drums, the steam and VCM from the reactor are combined with a bleed stream of VCM from the recovered VCM storage tanks. The amount of VCM bled into the recovery system is adjusted by the backpressure control valve such that a set supply pressure to the vacuum pumps is maintained.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

D. Recovery and Steam Stripping (Continued)

2. Steam Stripping (Continued)

The majority of the steam is condensed in the first knockout drum described in the normal recovery process description. The first stage of the scrubbing system consists of a recovery knockout drum with an internal water spray system, a water recirculation pump and the water recirculation cooler. The water cooler reduces the water temperature sufficiently to allow the internal spray system in the knockout drum to cool the VCM and condense much of the steam in the vapor stream. After leaving the first stage of the water scrubbing system, the VCM vapor flows to the second stage of the scrubbing system and then to the rest of the recovery system in the same manner as during normal recovery.

3. Hydroquinone Injection

The VCM removed from the reactor during recovery still contains a small amount of initiator. As a result, the VCM will continue to polymerize, resulting in plugged recovery lines, charge lines, and recovered VCM storage tanks. Polymerization is significantly reduced by the addition of an inhibitor such as hydroquinone to the VCM stream as it is being recovered.

A 4.6 percent solution of hydroquinone in water is prepared in the hydroquinone storage tank.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

D. Recovery and Steam Stripping (Continued)

3. Hydroquinone Injection (Continued)

The hydroquinone solution is pumped by the hydroquinone injection pump into the suction of the recovery seal water pumps. The injection pump starts and stops automatically with the seal water pumps. The metering pump has a variable stroke which can be adjusted manually to maintain the preset hydroquinone injection rate.

4. Recovery of Blowdown Tank

The blowdown tank is to collect the various steam and water streams containing VCM from the four-reactor module. The recovery system is used to recover VCM vapor. The tank can be recovered during the steam stripping portion of a reactor recovery or during a period between reactor recoveries. When the pressure of the tank drops below the desired pressure, recovery of the tank is stopped.

E. Reactor Dump and Rinse

After the reactor is recovered and steam stripped, the reactor interlock selector switch is moved to the "dump" position. The appropriate dump valves are opened from the control room and the slurry flows by gravity to the dump system. The slurry passes through an enclosed vibrating slurry strainer where the PVC culls are collected until dump is completed. The slurry then flows to the slurry dump tank. The slurry transfer pumps transfer the slurry to the blend tanks. The dump tank level is automatically controlled.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

E. Reactor Dump and Rinse (Continued)

Near the end of dump, the reactor condenser is flushed with water by turning on the condenser rinse system from the board. Hot water is pumped from the hot water tank by the hot water charge pumps through the cleaning nozzle in the reactor condenser. The rinse water mixes with any remaining slurry and is pumped with the slurry to the blend tanks flushing out the slurry transfer lines.

The slurry strainer and the slurry dump tank are equipped with a water wash system to remove resin from the equipment between production of different types of resin.

F. Chem Wash and Rinse

If it has been determined that the reactor needs cleaning, the reactor interlock selector switch is moved to the "clean and rinse" position after the dump and rinse is completed.

The chem wash solution is a caustic solution. The cleaning solution pump or spare pumps the solution at 500 gpm from the cleaning solution tank through the cleaning solution heater to the reactor condenser spray nozzle. Steam to the cleaning solution heater is automatically adjusted such that the exit temperature of the chem wash solution is 190°F. When the level in the reactor is above the agitator blades (approximately 5,000 gallons) as determined by the level change in the cleaning solution tank, no more solution

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

F. Chem Wash and Rinse (Continued)

is added to the system. Recirculation is then started with chem wash solution being pumped from the reactor at approximately 250 gpm and back to the reactor through the reactor cleaning nozzle. Large PVC particles picked up in the reactor cleaning process are removed from the cleaning solution in the cleaning solution strainer before entering the suction of the cleaning solution pump. When chem wash has ended, the solution is pumped back to the cleaning solution tank at 500 gpm by the cleaning solution pump. The process requires ten minutes to fill the reactor through the condenser, five minutes to wash the reactor, and ten minutes to empty the reactor, for a total of twenty-five mintues.

After the chem wash is completed, the reactor is rinsed with hot water from the hot water tank. The hot water is pumped by the hot water charge pumps to the reactor. The water first enters through the condenser cleaning nozzle and then the reactor cleaning nozzle. The chem wash and rinse system is manually controlled from the control room.

G. Water Swirl

If the resin formula calls for a water swirl, the reactor interlock selector switch is placed in the "swirl" position after the chem wash rinse is completed. Cold or hot water enters the suction of the hot water charge pumps, and is pumped through the reactor

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

G. Water Swirl (Continued)

charge line into the reactor. When the water charge reaches a preset amount, the water charge system is automatically shut down. The reactor agitator is then used to swirl the water for approximately 25 minutes. The lead operator then drains the water to the sewer. This completes one reaction cycle; the reactor is now ready for evacuation.

H. Blowdown Collection System

Various waste water streams from the process must be collected in an enclosed system for treatment. Water streams containing PVC and VCM from the recovery system, the VCM storage tanks, line and vessel purges, and miscellaneous flush and seal waters are intermittently sent to the blowdown tank.

When the liquid in the blowdown tank reaches a level 22 inches from the top of the tank, a high level alarm sounds in the control room. At the discretion of the operator, the water in the blowdown tank is steam stripped at 175°F and 16 inches Hg vacuum, using the reactor recovery system.

The vapors from the blowdown tank are recovered in the manner previously described in the recovery section of the process description. Due to the operating pressures of streams collected in the tank, the pressure in the blowdown tank should be minimized.

II. GENERAL PROCESS DESCRIPTION (CONTINUED)

H. Blowdown Collection System (Continued)

When the recovery and stripping of the blowdown tank is completed, the lead operator activates the blowdown tank pump. The water is strained of PVC particles and is sent to the sewer. During draining, steam is used to maintain enough pressure in the tank to allow operation of the blowdown tank pump. When the liquid level drops to 12 inches from the bottom of the tank, the draining process is automatically stopped.

III. Operating Procedures

III. OPERATING PROCEDURES

A. Reactor Evacuation

Evacuation of the reactor is required prior to charging in order to remove as much of the air as possible. Air is introduced into the reactor during previous phases of the reactor batch cycle since dump, rinse, and chem wash require that the reactor be vented to the atmosphere. Air in the reactor during reaction causes poor temperature control during polymerization and may alter the particle size of the resin.

Evacuation is accomplished using a two-stage steam jet ejector system. Evacuation is controlled by the lead operator from the board. The "A" operator must confirm that all process equipment is operating correctly during evacuation.

Procedure

1. If the reactor has been opened, follow procedure given in the "Reactor Cleaning and Entry" section on how to close the reactor manhead.
2. The lead operator puts the interlock mode selector on "evacuation."
3. The lead operator checks to see that all valves are closed.
4. The lead operator then opens the condenser recovery valve and the evacuation reactor valve, which automatically starts the reactor evacuation steam jet used to evacuate the reactor. He then opens the emergency cooling water valve, which supplies cooling water to the reactor condenser.

III. OPERATING PROCEDURES (CONTINUED)

A. Reactor Evacuation (Continued)

Note: In the following steps, 5-10, the operators prepare the initiator for charge while evacuation is in progress.

5. The "A" operator will go to the initiator freezer and bring the specified amount of initiator to the initiator injection pot. Extreme caution must be exercised by the "A" operator to be sure that no VCM is allowed to get back into the initiator injection pot. When a small amount of VCM is mixed with a large amount of initiator, an extremely fast reaction takes place giving off heat and pressure. To guard against this situation, the operator must know that he has an adequate water supply and pressure. The reactor initiator injection valve must never be opened unless the bomb is fully pressurized with the inlet water valve open.

Note: The following precautions must be taken when handling initiator.

a. Full face shield and plastic gloves must be worn while handling initiator.

b. If any initiator is spilled on skin or clothing, immediately flush with water.

c. Should any initiator remain in the containers, return it to storage.

d. Take all empty containers to trash and split side of all containers.

III. OPERATING PROCEDURES (CONTINUED)

A. Reactor Evacuation (Continued)

6. The "A" operator must check the injection bomb to be sure that it is empty. Close the drain valve. Open the initiator addition valve.
7. The lead operator will manually open the HPSW inlet valve, CV-879, until the initiator water totalizer, FQI-703, shows that 55 counts of water are in the initiator injection pot.
8. The "A" operator will now add the initiator to the injection pot.
9. The "A" operator will now close the initiator addition valve and inform the lead operator that the initiator loading is complete and the bomb is ready to be pressurized.
10. The lead operator will now open CV-879, which supplies high pressure service water to the initiator injection pot. This should activate the high pressure light for the injection pot on the panel.
11. When a 25-inch Hg vacuum is reached in the reactor, an indicator on the board will light.
12. The lead operator will stop evacuation when a vacuum of 28.5 inches Hg is attained. The reactor pressure is double checked by the "A" operator at the reactor with a mercury manometer. The lead operator stops evacuation by closing the condenser

III. OPERATING PROCEDURES (CONTINUED)

A. Reactor Evacuation (Continued)

12. recovery valve and the evacuation reactor valve. This automatically shuts off the evacuation steam jets. He then closes the emergency cooling water valves.

13. Evacuation is now complete.

III. OPERATING PROCEDURES (CONTINUED)

B. Reactor Precharge

The reactor precharge procedure includes a series of precharge checks and precautions that must be carried out by the lead and "A" operators. If the necessary precharge conditions are not met, the modicon (a small computer which controls the automatic charge sequence) will not allow the automatic charge sequence to begin.

It is the responsibility of the lead operator to see that all precharge checks and precautions are carried out. He should also read the log book at the start of the shift, covering the period since he was last on the job. This will alert him to any changes in formula, mechanical, or operational procedures that may not have been passed on verbally.

1. Lead Operator Duties

a. Check level in fresh VCM receiver to see that it is adequate for charge. This is a level of at least 247 inches on the sight glass.

b. Drain water in the recovered VCM receiver to the blowdown tank. Valves from the recovered receiver are manually opened from the board until pressure rise in the blowdown tank indicates all the water is out and VCM is being transferred. Valves are then manually shut from the board.

c. Fill out the reactor charge sheet.

d. Check the hot water tank level and temperature.

III. OPERATING PROCEDURES (CONTINUED)

B. Reactor Precharge (Continued)

1. Lead Operator Duties (Continued)

e. Check to see that all valves on the reactor are closed.

f. Have the "A" operator make a precharge check and reading of the following:

(1) Dura-Seal* oil level and pressure.

(2) Mechanical seal purge water pressure and rate to the reactor agitator seal.

(3) Colloid charge tank level and temperature.

g. Record the readings on the charge sheet as they are transmitted by the "A" operator.

2. "A" Operator Duties

a. Check Dura-Seal* level and pressure. There are two Dura-Seal* units. One supplies seal oil pressure to all four reactor agitator mechanical seals and the other is a spare and starts automatically when the operating unit has low seal oil level or discharge pressure. If both units fail, an emergency supply of seal oil is provided by the emergency seal oil drum that is nitrogen pressurized. Valves must be opened manually at the unit if the emergency seal oil system is used.

*Registered Trademark

III. OPERATING PROCEDURES (CONTINUED)

B. Reactor Precharge (Continued)

2. "A" Operator Duties (Continued)

NOTE: When the primary and spare Dura-Seal* oil units are down and the emergency system is in operation, reactors are not to be charged until at least one of the Dura-Seal* oil units is operating. The emergency system is designed to be a backup system that should be used short term only.

When one of the Dura-Seal* oil units is not in operating condition, inform the lead operator so that repairs can be made.

The seal oil level should be checked in both units. The discharge pressure should be checked and be in the range of 205-250 psig. If the pressure falls below 205 psig, the spare unit will automatically start up and the primary unit shut down. The spare unit will also automatically start up and the primary unit shut down when a low seal oil level is detected in the primary unit. Report the seal oil pressure to the lead operator.

*Registered Trademark

III. OPERATING PROCEDURES (CONTINUED)

B. Reactor Precharge (Continued)

2. "A" Operator Duties (Continued)

b. Check the mechanical seal purge water pressure and rate of flow to the agitator mechanical seal. Pressure should be 180-220 psig. Adjust the water flow rate to that given in the formula.

Report the seal water pressure and flow rate to the lead operator.

c. Check the colloid charge tank level to be certain enough is in the tank to complete a charge. Notify the lead operator of the level present. A level of at least 26 inches should be shown on the sight glass before charge is started.

d. Inform the lead operator when checks are completed and the reactor is ready for charge.

III. OPERATING PROCEDURES (CONTINUED)

C. Reactor Charge

This section includes vacuum break and reactor charge. The reactor charge is one of the most critical operations in terms of product quality. Care must be taken to assure that all the raw materials are added in the proper order and in the proper amount.

Procedure

1. When evacuation and precharge checks are complete, the lead operator can move the interlock mode selector to "charge."
2. The lead operator should take the following steps and see that the following conditions are met before charge:
   a. VCM transfer should be in auto.
   b. Recovered VCM charge should be in auto with either the primary or spare pump selected for charge.
   c. Fresh VCM charge should be in auto with either the primary or spare pump selected for charge.
   d. Hot water charge should be in auto.
   e. Initiator charge should be in auto with high pressure light on.
   f. Colloid charge should be in auto with either the primary or spare pump selected for charge.
   g. Select recipe to be charged by dialing recipe number on the recipe selector on the board.
   h. Push meter reset button, which resets all charge meters.

III. OPERATING PROCEDURES (CONTINUED)

C. Reactor Charge (Continued)

Procedure (Continued)

1. The charge light will now come on if all the following conditions are met:

   (1) The fresh VCM storage tank, hot water tank, and colloid charge tank all have a level adequate for one complete charge.

   (2) One reactor is in charge mode.

   (3) The high pressure service water header is at least 150 psig.

   (4) The reactor being charged has at least 25 inches Hg vacuum.

   (5) The initiator injection pot is at least 180 psig.

3. When a charge light is obtained on the panel, the lead operator will inform the "A" operator to stand by for breaking vacuum. The lead operator will break vacuum by:

   a. Manually opening the reactor VCM charge valve from the board.

   b. Manually opening the reactor charge valve from the board.

   c. Turbine meters will start counting as VCM flows into the reactor.

   d. As soon as a positive pressure is indicated in the reactor, close the VCM charge valve.

III. OPERATING PROCEDURES (CONTINUED)

C. Reactor Charge (Continued)

Procedure (Continued)

4. The "A" operator will then watch the pressure gauge at the top of the reactor. When the pressure rises above zero, start checking the following:
   a. Inspect manhead visually and by moving hands around Lenape* lid feeling for escaping vapor.
   b. Check safety disc gauges for pressure. Any pressure indicates a leaking or ruptured disc.
   c. Turn flush water (injection water) on sprayhead. The purpose is to keep heads free of resin. Set rate according to recipe.
   d. If all checks okay, notify lead operator. If not, notify lead to hold on charge until problem can be corrected.
5. The lead operator can now push the charge button. In rapid sequence, the following occurs:
   a. Reactor water charge valve opens.
   b. "A" hot water pump starts, valves open, and water starts into the reactor.
   c. The valves from the fresh VCM receiver, 45-745, to the VCM charge pump and discharge valve open.
   d. At set point No. 1 on water meters:

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III. OPERATING PROCEDURES (CONTINUED)

C. Reactor Charge (Continued)

Procedure (Continued)

(1) "B" hot water pump starts and discharge valve opens.

(2) The colloid charge pump discharge valve will open and pump will start. The preset amount of colloid will be pumped into the reactor. When the colloid meter set point is reached, the colloid charge pump will cut off and the discharge valve and reactor colloid charge valve will close.

NOTE: The lead operator will turn on reactor jacket steam during colloid and water charge to assist reactor heatup.

e. At set point No. 2 on water meter, the reactor VCM charge valve opens and the VCM and recovered VCM charge pumps start.

f. At set point No. 3 on the water meter, "B" hot water pump stops and discharge valve closes. This allows time for all VCM to be charged to the reactor before the water charge is completed.

NOTE: A partially plugged filter pack can cause slow VCM flow, and it may be necessary to cut off "A" hot water pump also. If this should happen, be sure to have a minimum of 50 counts left on water charge meter. This is enough to clean lines and manifold of VCM. When the VCM is within ten counts of being complete, put "A" and "B" hot water pumps back on automatic and complete the charge.

III. OPERATING PROCEDURES (CONTINUED)

C. Reactor Charge (Continued)

Procedure (Continued)

NOTE: When a filter is known to be fouled, isolate and switch to the spare unit. If you continue to try to force VCM through fouled filters, the high pressure will cause the filter elements to collapse and greatly increase the time taken to change them out.

g. When VCM meters reach the set point (two meters running in tandem, first to reach the set point cuts pump off and closes valve), the VCM pump, outlet valve, inlet and discharge valve to VCM charge pump, and reactor VCM valve close. This action also starts "B" hot H_2O pump and opens discharge valve.

h. At set point No. 4 on the water meters, "A" and "B" hot water pumps stop and discharge valves close. Also, the reactor water charge valve and main dump valve close.

6. When the automatic charge sequence has been completed, it is safe to charge the initiator.

7. The lead operator charges the initiator by opening the initiator reactor charge valve.

8. When a preset amount of water has been charged through the initiator charge pot, the reactor initiator charge valve and the HPSW inlet valve are automatically closed.

9. The lead operator will now record the final reactor temperature. Adjust reactor temperature set point to setting called for in the formula and put temperature controller in "auto" position.

III. OPERATING PROCEDURES (CONTINUED)

D. Polymerization

Polymerization is the phase of the reactor cycle in which liquid VCM is converted into solid PVC. This portion of the reactor cycle is mainly accomplished by accurate instrumentation. The primary area of responsibility for the lead operator is coordination of the activities of the "A" operator. The "A" operator is required to sample the reactor and kill the reaction when polymerization has progressed to the point that product quality is satisfactory.

1. Lead Operator Duties

a. Change the interlock mode selector to "polymerization." Monitor the temperature and pressure closely until the reactor reaches the desired set point and lines out.

b. Cut off steam valve to jacket at two to four degrees below set point, depending on the rate of temperature rise.

c. After 1 1/2 hours at run temperature, have "A" operator obtain slurry sample with reactor sample bomb.

d. Examine the resin. At this stage of the reaction, the resin should be formed into individual, separate particles. Resin forms you would suspect as irregular are:

(1) Stringers--Several particles of resin stringing together.

(2) Conglomerates--Clusters of resin stuck together in little balls.

III. OPERATING PROCEDURES (CONTINUED)

D. Polymerization (Continued)

1. Lead Operator Duties (Continued)

If either of the above conditions are observed, have the "A" operator take samples every fifteen minutes until a definite trend can be established. If this irregularity clears up, continue the run; but if the condition worsens, notify the shift supervisor who will make the decision as to what corrective action should be taken.

e. It may become necessary to remove the inerts. Inerts in the condenser will cause the reactor pressure to rise as they blanket the condenser and do not allow VCM vapor to be condensed. Under these conditions, less heat can be removed even though the condenser water flow will be full open. Vent the inerts through the main condenser valve to the recovery system. Open the valve from the board. As soon as the "Valve Open" light comes on, push the "valve Close" button. One time should be enough; but if the reactor pressure does not stay at the set point, it may be necessary to vent twice.

f. Irregularities during polymerization:

(1) Slow Heatup--May be caused by weak or no initiator. Slow heatup can also be caused by no steam on reactor jacket or the cooling water valves may be open. Contact the shift supervisor if this condition persists.

III. OPERATING PROCEDURES (CONTINUED)

D. Polymerization (Continued)

1. Lead Operator Duties (Continued)

(2) Excessively Long Run--Caused by low initial initiator charge or a buildup of inhibitor or chem wash solution (caustic) in batch. If there is only slow reaction and the resin checks okay, the shift supervisor will give word on what to do.

If caustic is in the reactor, the batch will turn slightly yellow and coarsen. If this is found to be true, kill immediately with the amount of short stop solution specified in the formula.

(3) Simultaneous Temperature and Pressure Rise--Check cooling water temperature and valves. The reactor is producing more heat than the cooling water can remove. Also could be an overcharge of initiator. Notify shift supervisor for instructions.

(4) Simultaneous Temperature and Pressure Drop--The cooling water valves are probably wide open. This happens more often in freezing weather when relays freeze up. Throttle manual valves until malfunction is found and corrected.

(5) Agitator Kicks Out or Power Failure--Most power failures are of short duration (seconds to two minutes), and the reactor pressure does not have time to build to a dangerous level. If outage is prolonged, the pressure will build.

III. OPERATING PROCEDURES (CONTINUED)

D. Polymerization (Continued)

1. Lead Operator Duties (Continued)

If this situation occurs, follow the procedure in Section III.D.3, which outlines action to be taken during emergency shutdown (such as during a power failure).

2. "A" Operator Duties

a. When charge is complete, recheck water injection rates through the cleaning nozzle and seal flush.

b. On instruction from the lead operator, resin samples will be taken from the reactor. This normally occurs 1 1/2 hours after initiator injection. If the first sample shows formation of undesirable resin particles, additional samples may be called for every fifteen minutes until a decision is made about what should be done with the batch.

Before the sample is taken, the blowdown tank, 45-319, is recovered if it is not already under vacuum. To take a resin sample, the sampler is attached to the appropriate reactor sampling line and the reactor sampling ram valve opened until the sampling pressure gauge reads 60 psig. The reactor sampling system lines are cleared of VCM vapors and resin by evacuating to the blowdown tank and flushing with water. The sampling system lines are then vented to the atmosphere and sampler 45-770 disconnected. The resin is removed from the sampler by removing the screen insert.

III. OPERATING PROCEDURES (CONTINUED)

D. Polymerization (Continued)

2. "A" Operator Duties (Continued)

c. When the lead operator instructs the "A" operator to do so, the batch is killed by adding short stop solution to the reactor. High pressure service water is used to pressure the short stop solution from the AMS short stop charge pot into the reactor through the same piping as the agitator mechanical seal purge water inboard seal flush.

3. Emergency Shutdown

Runaway Reaction

In the event of a runaway reaction the reactor will be killed with the addition of a minimum of 5 gallons AMS. A runaway reaction is defined as a 10°F increase or a 20 psig increase in 5305, 5385, 5425, or 5465 resins.

The following parameters are to be the maximum limits on a runaway reaction. The reaction should be immediately killed with NO if either one of the parameters is exceeded.

Resin	Maximum Temperature	Maximum Pressure
5385, 5425, 5465	142°F	145 psig
5305	155°F	155 psig

If the reaction is allowed to exceed these limits, it may not be controllable and result in a relief valve or rupture disc discharge to the atmosphere.

III. OPERATING PROCEDURES (CONTINUED)

D. Polymerization (Continued)

3. Emergency Shutdown (Continued)

Runaway Reaction (Continued)

CAUTION: NO is a highly poisonous orange-colored gas. A Scott Air Pack must be worn while killing a reactor with the NO short stop system.

Power Failure

During the event of a power failure the reactors must be killed with NO. The sequence of which reaction to be killed is as follows:

A. All 5305 reactors

B. Remaining reactors - the reactor in polymerization cycle the longest will be killed first.

In all cases of emergency kill the pressure rise in the reaction should continue to be monitored. If the pressure continues to rise, the following steps are to be taken:

A. Equalize the reactor with any other empty or killed reactor of the same type product.

B. If the pressure still continues to rise, vent through the main condenser valve to the recovery system and the recovered VCM receiver.

C. If this will not relieve the pressure buildup, then equalize the reactor with a reactor of different type resin.

D. The reactor pressure buildup may become sufficient to cause opening of the reactor relief valve system. It is possible that the reactor pressure will continue to increase despite the relief valve discharge. If this occurs, the manual vent should be opened as often as needed to prevent failure of the double disc relief assembly.

III. OPERATING PROCEDURES (CONTINUED)

E. Recovery and Steam Stripping

The reactor is ready for recovery when certain conditions are reached in the reaction process. The conditions under which recovery will start are:

Pressure Drop--There is not enought unreacted VCM left in the reactor to maintain run pressure. A pressure drop is accompanied by a drop in the cooling water flow to the reactor jacket and condenser.

Runaway--Reaction has increased to the point that it has outrun the capabilities of the cooling water to control. Temperature and pressure will both rise when this occurs. Follow instructions on each product formula as to the exact conditions at which the reaction is killed.

Temperature Rise--Pressure Drop--This is the ideal recovery situation and indicated proper initiator loading. The reaction will peak and slightly outrun the capabilities of the cooling water. This situation gives the best recovery conditions since there is less VCM to be recovered and more converted to resin.

Quick-Kill--A reactor is sometimes killed on specific products to meet certain customer specifications--lower dry time (higher plasticizer absorbtion). The reactor is killed with a specified amount of the short stop solution at a specified set of conditions. The short stop solution mixture stops the reaction chain.

III. OPERATING PROCEDURES (CONTINUED)

E. Recovery and Steam Stripping (Continued)

On a quick-kill batch, it is very important to guard against resin carryover to the recovery system. An injection of defoamer will help to control foaming. A fast recovery is also important and will affect the dry time.

1. "A" Operator Duties

When notified by the lead operator that the recovery conditions specified in the formula are met, the "A" operator will take the following steps:

a. Check the hydroquinone injection system to make sure that the proper valves are open and the hydroquinone level is adequate.

b. Check the blowdown tank level and pressure. Level and pressure must be low to allow the automatic drain on the water recirculation pump to operate.

c. Check the water levels in the seal water separators and knockout drums. These levels are controlled automatically but should be checked before startup. Knockout drum level should be at or below the mid-point of the inlet to the vessel. The seal water separator level should be at or below the mid-point of the inlet to the vessel.

d. Check the backflow pressure controller. It should be set at three inches Hg vacuum.

III. OPERATING PROCEDURES (CONTINUED)

E. Recovery and Steam Stripping (Continued)

1. "A" Operator Duties (Continued)

e. Check to see that the flush to the knockout drum and seal water separator level gauges are on and set at 1 gpm. These are FI-726, FI-727, FI-741, and FI-742.

f. Notify the lead operator that the recovery system is ready to startup.

g. Steam header pressure should be greater than 100 psig.

h. Reactor steam line should be checked and reactor steam valves should be checked to make sure they are opening correctly.

2. Lead Operator Duties

a. When the "A" operator has checked the recovery system, the lead operator can change reactor interlock mode to "recovery."

b. Start the water recirculation pumps, 72-889 and 72-890.

c. Start the seal water pumps, 72-891 and 72-892. This automatically starts hydroquinone injection pump 72-895.

d. Two recovery compressors, 72-903, 72-904, or 72-905, are placed in auto. The automatic recovery start switch is then pushed. This starts two compressors and opens the valves associated with compressor startup.

e. The vacuum pumps will automatically come on when the suction pressure of the compressor is 7 psig. The necessary valve changes are also automatically made.

III. OPERATING PROCEDURES (CONTINUED)

E. Recovery and Steam Stripping (Continued)

2. Lead Operator Duties (Continued)

f. When the reactor reaches the pressure specified in the product formula, the lead operator will move the reactor temperature set point to the specified stripping temperature and begin steam stripping.

g. Watch the temperature of the reactor condenser.

h. When stripping conditions specified in the formula are met, steam stripping is complete.

i. When steam stripping and recovery is complete, the recovery system is shut down as follows:

(1) Push stop buttons for the recovery compressors 72-903, 72-904, or 72-905. This also stops the vacuum pumps.

(2) Push stop buttons for seal water pumps 72-891 and 72-892. This also stops hydroquinone injection pump.

(3) Push stop buttoms for the water recirculation pumps, 72-889 and 72-890.

3. Recovery System Troubleshooting

a. High Compressor Outlet Temperature

Probable cause is poor or no water recirculation in the recovery knockout drum, 45-760. Check VCM backflow controller setting. Controller setting should be at 3 inches Hg.

III. OPERATING PROCEDURES (CONTINUED)

E. Recovery and Steam Stripping (Continued)

b. High Compressor Discharge Pressure

High pressure can be caused by:

(1) Plugged Condenser--Have lead operator report problem to the shift supervisor.

(2) Plug in the Line from the Condenser to the VCM Collect Tank--Line will have to be pulled and cleaned.

(3) High Level in the VCM Collect Tank

(a) Switch transfer pump to manual.

(b) Check level of the recovered VCM receiver--east or west.

(4) No Cooling Water to Condenser--Check inlet and outlet water valves.

(5) High Seal Water Temperature--This temperature should be 110° ± 10°. Check seal water pump for flow and pressure and check filter pack.

c. If the compressor is not compressing the VCM vapor and does not have a 50 to 70 psi discharge pressure:

(1) Check seal water flow.

(2) Check seal water separator water level and adjust as necessary.

(3) Check seal water temperature--below 80°F water will condenser the VCM vapor and cause displacement of the water seal around the compressor cone.

III. OPERATING PROCEDURES (CONTINUED)

E. Recovery and Steam Stripping (Continued)

3. Recovery System Troubleshooting (Continued)

d. Recirculation water pump 72-889 goes out (mechanical-electrical).

(1) Under normal operation, recirculation water pump 72-889 circulates water through the water recirculation cooler and into recovery knockout drum 45-760. Crossover piping is provided so that, if recirculation water pump 72-889 fails, recirculation water pump 72-890 will be valved to circulate through the recirculation water cooler and into recovery knockout drum 45-761.

Note: Normal operating temperatures for the recovery system during stripping are:

(a) Reactor Condenser - 215-225°F (Peak Temperature)

(b) 45-760 Knockout Drum Outlet - 122-128°F

(c) 45-761 Knockout Drum Outlet - 90-115°F

(d) Compressor Outlet - 130-140°F

The lead operator must monitor these temperatures on the multipoint recorder and have the "A" operator check out and correct deviations.

e. Reactor Foaming (carryover)--When foaming is detected, the "A" operator will:

III. OPERATING PROCEDURES (CONTINUED)

E. Recovery and Steam Stripping (Continued)

3. Recovery System Troubleshooting (Continued)

(1) Inject defoamer into the reactor to reduce slurry surface tension and lower the reactor slurry level. It may become necessary for the lead operator to shut down one compressor to slow the recovery. If excessive foaming occurs, shut down recovery and thoroughly flush the entire system with water until clear.

III. OPERATING PROCEDURES (CONTINUED)

F. Reactor Dump and Rinse

When the recovery of the reactor has been completed, the slurry is ready to be dumped to the slurry blend tank(s) that has been designated by the shift supervisor.

1. "A" Operator Duties

a. Check the selected blend tank or tanks to make sure it will hold the batch.

b. Set up the dump line to the selected blend tanks. Check to see that the blend tank sewer valve is closed and the agitator is on.

c. Check the slurry transfer pump valving to make sure the flow will be going to the correct line.

d. Place the coarse overflow collector into position. Inform the lead operator that the dump can begin.

e. Monitor the dump tank level until the flow to the pump and discharge from the reactor have leveled out to a steady rate.

f. Add calcium stearate to the dump tank as directed by the shift supervisor (except with 5425, 5465, and 5446 resins).

g. If instructed by the lead operator, open the reactor manhead to inspect the reactor internals. Follow opening procedure in "Reactor Cleaning and Entry" section.

III. OPERATING PROCEDURES (CONTINUED)

F. Reactor Dump and Rinse (Continued)

2. Lead Operator Duties

a. Check the sewer valve on the reactor to be sure it is closed.

b. Turn on the Sweco* strainer.

c. Check the Sweco* exhauster to be sure it is running. It should be running continuously.

d. Turn the interlock mode selector switch to the "dump" position.

e. After the "A" operator informs lead operator that dump can begin, place the slurry transfer pumps, 72-896 and/or 72-897, in the "run" position. This opens the slurry transfer pumps' seal water supply valves, CV-864 and/or CV-866, before the pumps start. The level in slurry dump tank 45-766 is automatically controlled.

f. Five minutes after the start of dump, open the reactor vent to the atmosphere.

g. When there is no slurry flow through FI-747, the reactor is rinsed according to formula instructions.

h. When dump and rinse are complete, place the slurry transfer pumps in the stop position. This shuts down the pumps, 72-896 and/or 72-897, and then closes the slurry transfer pump seal flush water valve, CV-864 and/or CV-866.

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III. OPERATING PROCEDURES (CONTINUED)

G. Chem Wash and Rinse

Chem wash and rinse is not done as a matter of routine on all reactors; however, if it has been determined that chem wash is needed, the shift supervisor will inform the lead operator to do so.

After the reactor has been rinsed during the dump cycle, it is ready to be chem washed. The chem wash cycle is necessary to remove polymer buildup from the reactor condenser, walls, baffles, and agitator. If polymer buildup is allowed to remain in the reactor, it continues to grow with each successive charge. Buildups will contribute to high gel, low quality resin, and will make reactor dumping very difficult it they get large enough to break off and plug dump valves and lines.

Operators must exercise caution during chem wash due to the caustic in the solution. If any solution should get on an opeator, flush immediately with water. Caustic feels slick to the touch and will start burning the skin just a few seconds after contact. If the solution should spray over the body, immediately get under a safety shower and remove your clothing. If any should get in the eyes, flush eyes for at least fifteen minutes but until all burning stops and report to your supervisor.

III. OPERATING PROCEDURES (CONTINUED)

G. Chem Wash and Rinse (Continued)

Procedure

1. The lead operator will check and make sure the reactor sewer valve is closed.
2. The lead operator will then place the interlock mode selector switch to "clean and rinse."
3. The lead operator then checks to see that the cleaning solution tank, 45-767, is at least 85 percent full.
4. The lead operator then opens the valves from the cleaning solution pumps, 72-989 or 72-899, to the reactor condenser cleaning nozzle. The atmospheric vent on the reactor should be open. All other reactor valves are closed.
5. The lead operator then opens the suction valves, CV-873, for the cleaning solution pumps, 72-898 or 72-899.
6. The lead operator will check to see that the cleaning solution heater temperature controller is set at 190°F.
7. The lead operator will then turn on one cleaning solution pump 72-898 or 72-899.
8. When 5,000 gallons have been flushed through the reactor condenser (this is a change of about 85 percent in the cleaning solution tank level), the lead operator will:
   a. Stop the cleaning solution pump.
   b. Close pump suction valve CV-873 from the cleaning solution tank.

III. OPERATING PROCEDURES (CONTINUED)

G. Chem Wash and Rinse (Continued)

Procedure (Continued)

c. Open chem wash return valve on reactor.

d. Open cleaning solution pump suction valve CV-874 from the reactor.

e. Close valves to the condenser cleaning nozzle.

f. Open valves to the reactor cleaning nozzle.

g. Restart the cleaning solution pump. The chem wash solution should now be circulating from the bottom of the reactor back to the reactor cleaning nozzle.

h. The reactor agitator remains on.

9. The lead operator will recirculate the chem wash solution through the reactor for five minutes and will then pump the chem wash solution back to the cleaning solution tank by:

a. Opening CV-872.

b. Closing CV-871. This sends the cleaning solution pump discharge to the cleaning solution tank.

10. The "A" operator should monitor the cleaning solution pump and notify the lead operator when it loses suction (check pressure gauge on pump discharge).

11. The lead operator will now shut off the cleaning solution pump.

III. OPERATING PROCEDURES (CONTINUED)

G. Chem Wash and Rinse (Continued)

Procedure (Continued)

12. The lead operator will then check the cleaning solution tank level indicator to see if all the chem wash solution has returned. If any solution is lost or accidentally dumped to the sewer, notify the utilities supervisor. The spilled solution must be neutralized to avoid upsetting the chemical balance in the lagoons.
13. The lead operator will now close the reactor cleaning valves and open the condenser cleaning valve and the reactor sewer valve.
14. The lead operator will cut on both hot water charge pumps and flush through the condenser to the sewer for ten minutes.
15. The lead operator will then close the condenser cleaning valve, open the reactor cleaning valve, and flush the reactor to the sewer for ten minutes.
16. The lead operator will now close the reactor sewer valve.
17. Because of water dilution and resin accumulation, chem wash solution must be disposed of and fresh caustic pumped to the cleaning solution tank once per week. Follow the procedure outlined under "Used Chem Wash Solution Disposal."

III. OPERATING PROCEDURES (CONTINUED)

H. Full and Partial Swirl

To assist in the production of quality resin, particularly low gel, it has been found that, by filling the reactor with water and agitating, the gel count is markedly lower.

Swirl is performed when specified in the formula.

1. Full Swirl

In this swirl, the reactor is almost completely filled with water.

Lead Operator Duties

a. Has "A" operator open manhead (refer to reactor manhead opening procedures).

b. Turn the interlock mode selector switch to the "swirl" position.

c. Opens the reactor main charge valve and water charge valve.

d. Starts both hot water charge pumps.

e. Adds 2,000 counts of water to reactor (20,000 gallons).

f. Cuts off pumps and closes valves.

g. Agitates for ten minutes.

h. Opens sewer valve and dumps.

2. Partial Swirl

This swirl procedure is the same as the full swirl except for the amount of water used. Charge 440 counts (4,400 gallons) and follow the same procedure as the full swirl.

III. OPERATING PROCEDURES (CONTINUED)

J. Hydroquinone Solution Makeup

Hydroquinone is injected into the recovery system to short stop the chain reaction and polymerization of vinyl chloride. If the hot VCM gases are allowed to flow through the recovery lines without any inhibitor, they continue the reaction that was started in the reactor and rapidly fill and plug the recovery lines. Plugged lines in the recovery system are very time consuming to pull and clean and cause considerable amounts of downtime.

Adequate and accurate injection of hydroquinone eliminates this problem. Hydroquinone (commercial name Tecquinol*) comes in a powder form and must be put into a solution with water for our use.

When the hydroquinone solution level is low, as determined by the low level alarm LA-733 in the control room and/or by the hydroquinone storage tank sight glass, a new batch is to be made on the next day shift. Each batch should last approximately one month.

1. Lead Operator Duties

As soon as it is determined that the hydroquinone storage tank is low, the day shift lead operator should schedule hydroquinone makeup between reactor recoveries.

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III. OPERATING PROCEDURES (CONTINUED)

I. Colloid Solution Makeup

The properties of polyvinyl chloride (PVC) are strongly dependent upon the type and quality of the colloid solution used. The colloid solution must be made very accurately and consistently every time it is prepared. The colloid solution is a 1 1/2 percent solution of Dow F-50 Methocel* powder in water.

There is a local instrument panel located near the colloid makeup tank on the second floor of the recovery building. These instruments are to aid the operator in making the colloid solution in a consistent manner.

1. Lead Operator Duties

As soon as the lead operator is notified by the "A" operator that the colloid storage tank level is below the straight wall, he will schedule the "A" operator to make up colloid solution as follows:

a. With the "A" operator at the colloid tanks, open the makeup tank outlet valve (CV-857) and start the colloid transfer pump to transfer the colloid solution to the storage tank.

b. To mix any remaining heel in the storage tank with the new colloid solution, open the storage tank inlet valve (CV-858)

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III. OPERATING PROCEDURES (CONTINUED)

I. Colloid Solution Makeup (Continued)

1. Lead Operator Duties (Continued)

and circulation pump inlet valve (CV-859) and start the colloid circulation pump. The charge tank inlet valve (CV-861) must be closed.

c. When the "A" operator indicates that the makeup tank is empty, close the makeup tank outlet valve (CV-857) and turn off the transfer pump.

d. With the circulation pump still running, notify the "A" operator to catch a colloid solution sample and take it to the laboratory for analysis.

e. Close the storage tank inlet valve (CV-858) and circulation pump inlet valve (CV-859) and turn off the circulation pump.

f. Schedule the "A" operator to makeup a new batch of colloid solution as soon as possible.

g. During the first part of the colloid makeup procedure when notified by the "A" operator, the lead operator will open the hot water charge valve (CV-706) and will start one hot water charge pump and the discharge valve associated with the charge pump to transfer hot water to the colloid makeup tank. The colloid makeup tank water meter will close the valves and shut down the hot water pump automatically when it reaches its set point.

III. OPERATING PROCEDURES (CONTINUED)

I. Colloid Solution Makeup (Continued)

2. "A" Operator Duties

The "A" operator aids in colloid solution transfer by notifying the lead operator when the colloid storage tank needs to be refilled. After transfer, the "A" operator notifies the lead operator that the makeup tank is empty and then catches a sample of the colloid solution in the storage tank and takes it to the laboratory.

When notified by the lead operator, the "A" operator makes up a new batch of colloid solution by the following procedure:

a. Bring eight bags of Dow F-50 Methocel* powder (50 pounds per bag) to the top of the colloid makeup tank.

b. Rinse the colloid makeup tank with water to the sewer until it is clean.

c. Reset the colloid makeup water meter to 538 gallons, open the colloid tank inlet valve (CV-856), and notify the lead operator to open the hot water charge valve (CV-706), start a hot water charge pump, and open the discharge valve associated with the pump selected. The water meter will stop the pump and close the actuated valves that were opened when the set point is reached. Check to see that the agitator blades are covered.

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III. OPERATING PROCEDURES (CONTINUED)

I. Colloid Solution Makeup (Continued)

2. "A" Operator Duties (Continued)

d. Start the colloid tank heater and the tank agitator. The temperature controller will close the steam valve when the water in the tank reaches 200°F.

e. When the heater is off, add the methocel powder very slowly with the agitator still on. Each bag should take about one minute to add. If the powder is added too quickly, it will form lumps and not dissolve properly. Carry the empty bags to a trash container.

f. Allow about thirty minutes to let the agitator thoroughly mix the powder into the hot water. Check the mixture for lumps and continue to mix if lumps are present.

g. When the mixture contains no lumps, reset the colloid makeup water meter to 2,623 gallons and open the colloid tank inlet valve (CV-856) and the colloid tank water valve (CV-828) to add cold water. The water meter will close the actuated valves that were opened when the set point is reached. Measure the outage on the colloid makeup tank to check the accuracy of the water meter. The straight wall portion of the tank contains 14.8 gallons per inch.

III. OPERATING PROCEDURES (CONTINUED)

I. Colloid Solution Makeup (Continued)

2. "A" Operator Duties (Continued)

h. Start the colloid tank cooler. The temperature controller will close the cooling jacket valve when the colloid solution reaches 85°F. Check the cooling water temperature. If it is 80°F or above, the solution will cool very slowly; so close the manual cooling water valves and open the process water valves to the jacket.

i. Check the temperature after four hours of cooling. If the temperature is 85°F and the temperature controller has closed the cooling jacket valve, turn off the agitator. If the tank is still cooling, leave the agitator on until the tank has reached 85°F. It is very important to cool the colloid solution completely each time to produce a good quality colloid solution.

III. OPERATING PROCEDURES (CONTINUED)

J. Hydroquinone Solution Makeup (Continued)

2. "A" Operator Duties

When notified by the lead operator to make up a new batch of hydroquinone solution, the "A" operator does the following:

a. Weight up twenty pounds of hydroquinone powder.

b. Turn off hydroquinone metering pump suction valve and, with the nitrogen turned on and the vent closed, drain the remaining heel to the sewer and rinse with water to the sewer.

c. Open the vent and add water until the tank is about half full.

d. Turn off the nitrogen temporarily and add the hydroquinone powder through the funnel.

e. Turn on the agitator and open the nitrogen line.

f. Fill with water to the full mark on the sight glass (fifty gallons).

g. Close the vent and mix until the powder is dissolved.

h. Make sure the valves are lined up to the hydroquinone metering pump.

3. Safety Precautions

Rubber gloves and full face shield must be worn while handling and transferring hydroquinone dust and liquid. Hydroquinone dust can irritate and seriously damage the eyes.

III. OPERATING PROCEDURES (CONTINUED)

J. Hydroquinone Solution Makeup (Continued)

3. Safety Precautions (Continued)

First Aid--In case of contact, immediately flush eyes with water for fifteen (15) minutes. Notify the plant nurse. Flush skin with water and wash clothing before reuse.

III. OPERATING PROCEDURES (CONTINUED)

K. Used Chem Wash Solution Disposal

A three-inch carbon steel line has been installed from the chem wash header to an existing three-inch carbon steel line connecting to tank 460 at the northwest corner of the plasticizer building, P-1. The purpose of this line is for transfer of spent chem wash solution for neutralization. Transfer of this solution will be done only on the day shift, Monday through Friday, due to the shortage of personnel in P-1 at night and during the weekends. Should it become necessary to transfer during the off-shifts, the shift supervisor will personally check the outage on tank 460 and set up the tank 460 valves.

Procedure

1. The shift supervisor must have given instructions to transfer the used chem wash solution and make up a fresh batch.
2. The lead operator will contact the P-1 operator and have him check the outage on tank 460.
3. If there is sufficient outage, the lead operator will instruct the P-1 operator to open the chain valve into 460. There must be at least a 15-foot outage on tank 460 before starting the transfer.

   NOTE: Do not open the valve to tank 460 if any of the reactors are chem washing.
4. The "A" operator will open the manual valve on the three-inch line to P-1.

III. OPERATING PROCEDURES (CONTINUED)

K. Used Chem Wash Solution Disposal (Continued)

Procedure (Continued)

5. The lead operator will close the chem wash inlet valve into the reactor and into the cleaning solution tank.
6. When the P-1 operator has the chain valve on tank 460 open, the lead operator will start the cleaning solution pump and pump all the solution in the cleaning solution tank to tank 460.
7. As soon as the tank is empty of solution, the "A" operator will open the three-inch process water valve to the cleaning solution tank to flush out the transfer line to tank 460 and then close the process water valve.
8. When the flush is complete, the lead operator will call the P-1 operator and instruct him to close the valve on tank 460.
9. The lead operator will then shut off the cleaning solution pump.
10. The "A" operator will close the valve to tank 460 and open the cleaning solution tank sewer valve.
11. The "A" operator can now flush out residual resin and solution from the cleaning solution tank to the sewer. Make up new batch.

NOTE: Notify the utility supervisor that about 100 gallons of caustic solution was dumped to the sewer.

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage

In the conversion of vinyl chloride monomer to polyvinyl chloride resin, an initiator is needed to start and help sustain the reaction process. The Aberdeen plant uses peroxide-type initiators. The physical properties of the type resin needed determines the type of initiator to be used. All of these products must be kept in cold storage because of rapid decomposition at room temperatures. The initiator is a skin and eye irritant and must be handled accordingly.

Safety precautions for all types of initiator are basically the same, with some differences in handling temperatures and explosive limits.

1. Safety Precautions in Handling Initiator

   a. Always wear impervious gloves.

   b. Wear full face shield when handling an open container.

   c. Avoid contact with skin or clothing (will bleach out clothes).

   d. Do not leave initiator unattended when not under refrigeration.

   e. If initiator is spilled, soak up with absorbent material, such as vermiculite, and spread thinly in an isolated area.

   f. Dispose of empty containers immediately. Leave cap off and split the side of this container.

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage (Continued)

1. Safety Precautions in Handling Initiator (Continued)

g. Bring only what is necessary to the production area. Do not allow the amount in the reactor area freezers to exceed one shift's consumption.

h. If a partial or full jug of initiator is found sitting out, it may be water, but always handle and dispose of just as if it were initiator.

i. If spilled on skin area, wash with large amounts of water.

j. If splashed in the eyes, flush with water for fifteen (15) minutes and notify your supervisor. Do not use oils or salves on the eyes.

k. Should any initiator catch on fire, use a dry chemical or foam fire extinguisher. Water will only spread the fire. However, if the fire is spreading and likely to ignite other initiator, get out of the area, since an explosion is very likely.

2. Physical Characteristics

The following physical characteristics are given for Lupersol 223-75 and Lup-11 because they are currently in use; however, a different initiator may be used in the future.

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage (Continued)

2. Physical Characteristics (Continued)

	223-75	Lup-11
Form	Liquid	Liquid
Freezing Point, °F	-110	-2
Top Safe Storage, °F	20	0-40
Decomposition Temp, °F	50	160
Container	One-Gallon Poly Jug	Five-Gallon Poly Jug
Label	Red*	Yellow**

*Red Label--Liquids with flash point below 80°F.
**Yellow Label--All liquids and solids with flash point above 80°F.

3. Initiator Storage Freezers

Two walk-in freezers and one chest-type freezer have been installed for initiator storage at temperatures ranging down to -30°F. Each freezer has two independent refrigeration compressors with one to be held in reserve. This is to insure continuous operation at temperature set points. High temperature in any freezer will activate the air horn and beacon flasher alarms. An automatic defrost system controlled by time clocks will provide frost-free operation.

a. Operating Conditions

(1) Temperature

The temperatures are adjustable. They can be set from -30°F to +30°F.

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage (Continued)

a. Operating Conditions (Continued)

(2) Alarms

Chest and walk-in freezers on high temperature setting will actuate the red beacon light and air horn. This is common to all initiator freezers in the plant. The present alarm's set point is 17°F (±2°).

(3) Compressors

Compressors are numbered 1 through 6.

(a) No. 1 and No. 2 compressors serve the east walk-in freezer.

(b) No. 3 and No. 4 compressors serve the west walk-in freezer.

(c) No. 5 and No. 6 compressors service the chest freezer on the west end.

(4) Compressor Shutdown Conditions (Automatic)

(a) Temperature of freezer at set point.

(b) Low oil level in the compressor.

(c) High or low compressor pressure.

(5) Circuit Breakers

(a) On the Compressor Panel--The compressor breakers in sequence No. 1 through No. 6.

(b) Fan Panel--The fans are numbered 2, 3, 5, and 6.

(c) The miscellaneous panel has lights, controls, alarms, fans, and clocks.

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage (Continued)

(6) Defrost Cycles--Adjustable

In the walk-in freezers, each compressor switches to hot gas bypass every six hours to provide a defrost cycle. This is controlled by a time clock.

(7) Freezer Capacity

(a) Walk-In Freezers - 550 gallons or 4,200 pounds.

(b) New Initiator freezer - 100 gallons or 770 pounds.

4. Design and Operational Functions

Each freezer is provided with two refrigeration units which are capable of maintaining the desired freezer temperature. Both units can be run simultaneously to allow a check on compressor operation.

The temperature element in each freezer is connected to a mercury switch which starts and stops the compressor. These are adjustable and can be set for different temperatures.

Each compressor has a timer which activates a solenoid valve in the hot gas line to send hot gas directly to the evaporator to allow for the defrost cycle. The fan normally runs with the compressor but is off during the defrost cycle. The east and west freezers defrost every six hours, and the chest freezer defrosts every eight hours. The water-cooled condensers on each compressor have water bypass to allow continuous flow

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage (Continued)

4. Design and Operational Functions (Continued)

and prevent freezeup during cold weather. The condensers also have inlet and outlet valves to allow for acid cleaning. Condenser cooling water is normally supplied by and returned to the cooling tower. During shutdowns and power outages, a bypass valve from the well/city water can be opened to supply water pressure. If the condensers are put on the well water, open the block valve in the manhole at the west end of the cooling tower to divert the water to the sewer.

5. Daily Operational Checks

a. Each compressor oil level by maintenance.

b. Temperature recorders by "A" operator.

c. Frost buildup on freezer coils by "A" operator.

NOTE: Manual defrost instructions are on the inside front of each time clock.

NOTE: Due to the explosive nature of this initiator, formal approval must be obtained from the operations superintendent and the mechanical superintendent before any changes are made to this operation.

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage (Continued)

6. Emergency Procedure for Initiator Freezers

If the power should go off, do not open the freezers but do the following:

a. Find out if the power failure is because of a malfunction in the plant.

(1) If trouble is inside the plant, survey the situation and estimate how long the outage will be. Freezers should hold temperature from 3-4 hours, depending on what is in them, the outside temperature, and how many times the door is opened.

(2) If trouble is determined to be outside the plant, call Berl Hill at 369-4731, 369-2159, or 369-2019.

(a) Keep in touch with the Light Department to determine how long the outage will be.

(b) If outage is expected to be over three (3) hours, call Jim Barton (369-4755) or Joann Pope (369-4949). They will arrange for purchase of dry ice.

b. If a compressor should fail and it is not an electrical problem, get in touch with maintenance as soon as possible.

(1) If help is not available from maintenance, get in touch with Dahlem Sales and Service at 369-2165 or residence 369-4435.

III. OPERATING PROCEDURES (CONTINUED)

L. Initiator Handling and Storage (Continued)

6. Emergency Procedure for Initiator Freezers (Continued)

(2) If the problem cannot be fixed, try to move all initiator to other freezers. If not possible, get dry ice.

NOTE: If compressors should go out on a freezer, make sure fans are turned off to that freezer. East freezer 1 and 2 fans, middle freezer 3 and 4 fans, and west freezer 5 and 6 fans.

c. Notify the following if an emergency should arise with the initiator freezers:

Jim Barton - 369-4755
Ed Kieschnick - 1-328-0350

7. Circle Chart Responsibility and Change Schedule

a. The "A" operator on each shift will check the charts to be sure they have ink and are rotating.

b. The "A" operator on the 11-7 shift will place new charts in the recorder and turn in the previous day's chart to the shift supervisor.

III. OPERATING PROCEDURES (CONTINUED)

M. Reactor Pressure Check

Prior to the startup of a reactor after an extended outage or following a maintenance outage such as replacing a main dump valve or rodding out the condenser tubes, the reactor must be hydrostatically pressure checked. This is to insure that no leakage occurs at the reactor, either inward or outward.

Procedure

1. The lead operator sets up the pressure check as follows:
   a. Place the reactor mode in "emergency" to gain use of both the charge water valve and the rinse valves.
   b. Open both hot water charge pump discharge valves CV-849 and CV-829.
   c. Open the reactor charge water valve.
   d. Open the main charge valve.
   e. Open the emergency vent valve.
2. The lead operator then turns on both hot water charge pumps and fills the reactor.
3. The "A" operator stands by to notify the lead operator when water comes out the atmospheric vent, showing that the reactor is full.
4. The lead operator then shuts down the hot water charge pumps and closes all valves. This must be done immediately to avoid overpressuring the reactor and blowing the rupture discs.

III. OPERATING PROCEDURES (CONTINUED)

M. Reactor Pressure Check (Continued)

Procedure (Continued)

5. The "A" operator then increases the reactor pressure by charging water into the reactor through the initiator injection system.
6. The lead operator monitors the reactor pressure from the control room and instructs the "A" operator to shut off water addition when the pressure reaches 130 psig.
7. The "A" operator then checks the reactor for leaks at the reactor bottom and top side. If a flange or gasket has been changed, check these very closely.
8. The lead operator then monitors the reactor pressure. If the reactor holds 130 psig for ten minutes, the pressure check is terminated. If the reactor loses pressure, instruct the "A" operator to bring the pressure back up to 130 psig with the high pressure service water and reinspect the reactor for leaks.

   NOTE: Do not charge a reactor that will not hold pressure.
9. When the pressure check is completed, the lead operator dumps the water in the reactor to the sewer. The reactor is now ready to start evacuation procedure.

III. OPERATING PROCEDURES (CONTINUED)

N. Reactor Cleaning and Entry

1. Reactor Manhead Opening Procedures

One of the most critical parts of the operator's job is the opening of the reactor Lenape* manhead. Following is a list of procedures that must be followed by the "A" operator or anyone else when opening a reactor manhead.

Procedure

a. Check the pressure gauge and/or bleed valve for pressure or vacuum.

b. Put on continuous flow fresh air mask.

c. Unlatch Lenape* lock on Lenape* manhead roll-bar and drop down.

NOTE: If the reactor has pressure when the roll-bar arm is lifted, the pressure will start escaping. If this should happen, immediately push lift-bar down and notify the lead operator.

d. Slowly raise manhead four to six inches and hold in that position.

e. Call lead operator and have him cut on the reactor evacuation ejector to pull air inward through the manhead.

f. Finish raising the manhead.

g. Remove continuous flow fresh air mask and process with task.

h. Change "O" ring on manhead.

*Registered Trademark

III. OPERATING PROCEDURES (CONTINUED)

N. Reactor Cleaning and Entry (Continued)

1. Reactor Manhead Opening Procedures (Continued)

i. Look at the bottom of rupture discs to determine if they are plugged with resin.

j. If the bottom manhead is to be opened, inspect the bottom of the reactor through the open manhead. The reactor should contain no liquids.

k. Go to the bottom of the reactor and make sure that the safety chain and jacking bolts are in proper position on the bottom manhead.

l. Remove bolts in manhead.

m. Carefully open manhead with jacking bolts.

2. Reactor Cleaning and Entry

This section will cover precautions taken prior to entry and during entry and cleaning of the reactor. The following is a check list stating conditions which must be met by anyone entering the reactor.

Procedure

a. The reactor must be empty and flushed with water.

b. The O_2 content must be greater than 20 percent.

c. The VCM content must be less than 10 ppm.

d. The top and bottom manways must be open.

e. The nitric oxide (NO) piping must be disconnected.

III. OPERATING PROCEDURES (CONTINUED)

N. Reactor Cleaning and Entry (Continued)

2. Reactor Cleaning and Entry (Continued)

f. The following lines must be blanked:

(1) Main eight-inch dump line.

(2) Four-inch steam stripping line.

(3) Six-inch condenser lines.

(4) Four-inch chem wash and rinse line to condenser.*

(5) Four-inch chem wash and rinse line to reactor.*

(6) One-inch initiator injection line.

(7) One-inch inerts vent.

(8) Three-inch colloid charge line.

(9) One-inch sample line.

g. Lock out and tag agitator breaker.

h. Test agitator switch.

i. Special precautions and safety equipment that may be needed are:

(1) Impervious suit.

(2) Continuous flow fresh air mask.

(3) Rubber gloves.

(4) Scaffolding for work above bottom level.

(5) Two-way radio communication plus manway watch.

(6) Safety harness and rope.

*When preparing to blank or remove blank in chem wash line, lock out cleaning solution pump, open chem wash line to reactor, and bleed line at discharge of pump before breaking chem wash flange.

III. OPERATING PROCEDURES (CONTINUED)

N. Reactor Cleaning and Entry (Continued)

2. Reactor Cleaning and Entry (Continued)

j. While cleaning the buildups from the baffles and blade, take extreme care not to scratch the reactor walls. These walls have been polished to eliminate giving the resin being formed during reaction a place to create a buildup. NEVER SCRAPE THE WALLS.

k. Around the shaft at the bottom of each reactor is a carbon throttle bushing. The purpose of the throttle bushing is to protect the reactor seal from resin. The seal water flush will not be effective if the throttle bushing or holder is damaged. If there is any buildup in this area, it is the Maintenance Department's responsibility to remove it. Operators are NOT to clean the throttle bushing. Damage to the throttle bushing may cause seal failure.

l. If hammer and chisel are required to clean the reactor, be careful of chisel placement to avoid it kicking back out of the buildup and causing personal injury.

m. While in the reactor, check the safety discs for buildups, nozzles for plugs, and the bottom of the condenser for plugging.

n. When internal job is completed, remove scaffolding from the reactor and store neatly. Remove any loose buildup on the reactor bottom and close the bottom manhead.

o. Clean up any debris, rags, etc. The job is never complete until the area is clean.

III. OPERATING PROCEDURES (CONTINUED)

O. Housekeeping Guidelines

Good housekeeping is a major portion of any task to be undertaken, and no task can be called complete until the work area has been cleaned. Return all tools and materials used to their proper place and do not leave lying around to create a safety hazard.

The housekeeping of the reactor area is the responsibility of all people working there. This includes supervisors, operators, maintenance, and contractors.

Individual areas of housekeeping responsibilities are:

1. Control Room and Reactor Area--To be kept clean by each shift.
2. Food Preparation Area--To be kept clean by each shift.
3. Control Room Refrigerator--To be cleaned and washed by the 7-3 shift each Monday.
4. Storage Shed Area--To be cleaned and straightened by the 7-3 shift each Tuesday.
5. Initiator Storage Area--To be kept orderly by each shift and cleaned thoroughly by the 7-3 shift each Wednesday.

All reactor personnel are responsible for the entire reactor area; but certain areas are set up for shift responsibility as to special housekeeping, painting, and general upkeep. These are:

1. 7-3 Shift
   a. Reactor condenser level.
   b. Reactor manhead level.
   c. Reactor bottom level.

III. OPERATING PROCEDURES (CONTINUED)

O. Housekeeping Guidelines (Continued)

2. 3-11 Shift

a. Reactor table top level.

b. VCM receiver area.

c. Initiator freezer area.

3. 11-7 Shift

a. First floor recovery building.

b. Second floor recovery building.

IV. Equipment Index

IV. EQUIPMENT INDEX

A. Reactors

1. Polymerization Reactors 45-741, 45-742, 45-743, and 45-744

a. Purpose

Vessel used to react VCM to PVC in a water suspension.

b. Description

Vertical-mounted, bottom-agitated vessel, 12-foot diameter by 22-foot straight wall height (28 feet overall height), jacketed, and with top-mounted condenser. The reactor is stainless steel, and the cooling water and steam jacket is carbon steel. Approximate capacity is 19,000 gallons.

c. Normal Operating Conditions

The reactor produces various resin types, operating in a pressure range of 28.5 inches Hg vacuum to 150 psig and a temperature range of 80-225°F.

d. Design Conditions

	Shell	Jacket
Temperature, °F	250	200
Pressure, psig	200 (and full vacuum)	30

B. Heat Exchangers

1. Reactor Condensers 55-328, 55-329, 55-330, and 55-331

a. Purpose

To remove the heat of reaction from the polymerization reactor by condensing VCM vapor.

IV. EQUIPMENT INDEX (CONTINUED)

B. Heat Exchangers (Continued)

b. Description

Each of the reactor condensers are vertical, mounted on top of the polymerization reactors. Cooling water (shell side) is used to condenser VCM (tube side). Each condenser has 2,100 square foot surface area provided by 999 tubes which are eight feet long by one-inch diameter. Materials of construction are stainless steel or stainless steel clad for all surfaces in contact with VCM.

c. Normal Operating Conditions

Condensers operate in a temperature range of 80-225°F and pressure range of 28.5 inches Hg vacuum to 150 psig during the reactor cycle.

d. Design Conditions

	Shell	Tubes
Temperature, °F	200	250
Pressure, psig	120	200 (and full vacuum)

2. Hot Water Preheater 55-332

a. Purpose

To heat process water to 145°F before it enters the hot water tank, 45-748.

IV. EQUIPMENT INDEX (CONTINUED)

B. Heat Exchangers (Continued)

b. Description

Horizontal shell and tube type exchanger with steam on the shell side and water on the tube side. Surface area of 331 square feet is provided by 64 tubes 20 feet long by one-inch diameter. The tubes are stainless steel, and the shell is carbon steel.

c. Normal Operating Conditions

Steam temperature and pressure on the shell side will vary. Water on the tube side will be around 50 psig and will enter near 60°F and exit at 145°F.

d. Desgin Conditions

	Shell	Tube
Temperature, °F	400	400
Pressure, psig	175	200

3. Hot Water Tank Heater 55-333

a. Purpose

To maintain water temperature in hot water tank 45-748.

b. Description

External plate coil type heat exchanger that will be clamped outside the hot water tank; stainless steel construction.

IV. EQUIPMENT INDEX (CONTINUED)

B. Heat Exchangers (Continued)

c. Normal Operating Conditions

Steam in the coil should be around 341°F and 105 psig.

Water in the hot water tank should be near 145°F.

d. Design Conditions

400°F and 175 psig

4. Water Recirculation Cooler 55-334

a. Purpose

To cool the recirculation water in recovery knockout drum 45-760.

b. Description

Horizontal mounted, shell and tube type heat exchanger. Cooling water is on the shell side and recirculating water is on the tube side. Surface area of 1,441 square feet is provided by 466 tubes, 16 feet long by 3/4-inch diameter. The tubes are stainless steel and the shell is carbon steel.

c. Normal Operating Conditions

d. Design Conditions

	Shell	Tube
Temperature, °F	450	400
Pressure, psig	150	150

IV. EQUIPMENT INDEX (CONTINUED)

B. Heat Exchangers (Continued)

5. Seal Water Coolers 55-335 and 55-336

a. Purpose

To cool the circulating vacuum pump and compressor seal water.

b. Description

Horizontal-mounted shell and tube type heat exchanger. Cooling water is on the shell side and recirculating seal water is on the tube side. Surface area of 339 square feet is provided by 182 tubes 10 feet long by 3/4-inch diameter. The tubes are stainless steel and the shell is carbon steel.

c. Normal Operating Conditions

d. Design Conditions

	Shell	Tube
Temperature, °F	200	380
Pressure, psig	150	150

6. Recovered VCM Condensers 55-337 and 55-338

a. Purpose

To condense VCM vapor during recovery as it is removed from the polymerization reactors.

IV. EQUIPMENT INDEX (CONTINUED)

B. Heat Exchangers (Continued)

b. Description

Horizontal-mounted shell and tube type heat exchangers. Cooling water is on the shell side, and VCM is on the tube side. Surface area of 1,030 square feet is provided by 450 tubes 12 feet long by 3/4-inch diameter. The tubes are stainless steel, and the shell is carbon steel.

c. Normal Operating Conditions

d. Design Conditions

	Shell	Tube
Temperature, °F	400	400
Pressure, psig	150	150

7. Cleaning Solution Heater 55-339

a. Purpose

To heat and maintain chem wash solution temperature during chem wash of the reactors.

b. Description

Horizontal-mounted shell and tube type heat exchanger. Steam is on the shell side, and chem wash solution (caustic) is on the tube side. Surface area of 214 square feet is provided by 79 tubes 14 feet long by 3/4-inch diameter. The tubes are stainless steel, and the shell is carbon steel.

IV. EQUIPMENT INDEX (CONTINUED)

B. Heat Exchangers (Continued)

c. Normal Operating Conditions

Steam temperature and pressure on the shell side will vary. Cleaning solution on the tube side is estimated to enter at 175°F and leave at 190°F with a pressure of 125 psig.

d. Design Conditions

	Shell	Tube
Temperatue, °F	175	200
Pressure, psig	400	400

C. Tanks and Vessels

1. Instrument Air Capacity Tank 45-301

a. Purpose

To provide adequate instrument air during periods of high demand and temporarily supply air during instrument air failure.

b. Description

Vertical-mounted, five-foot nine-inch straight wall height, four-foot diameter, carbon steel construction.

c. Normal Operating Conditions

100 psig and 80°F

d. Design Conditions

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

2. Recovered VCM Storage Tanks 45-317 and 89-520

a. Purpose

Storage of recovered VCM and charge tank for recovered VCM.

b. Description

Vertical-mounted, 18-foot straight wall height, 22-foot overall height, eight-foot diameter with an approximate capacity of 7,200 gallons, carbon steel construction

c. Normal Operating Conditions

Ambient temperature and 20-70 psig.

3. Blowdown Tank 45-319

a. Purpose

To provide for collection and recovery of various VCM containing vapor vents and waste waters.

b. Description

Horizontal-mounted, 26-foot straight wall length, six-foot diameter, approximate capacity 5,500 gallons, carbon steel construction.

c. Normal Operating Conditions

Ambient temperature to 150°F and pressure from 10 inches Hg vacuum to 10 psig.

d. Design Conditions

350°F and full vacuum to 80 psig.

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

4. Fresh VCM Storage Tank 45-745

a. Purpose

VCM storage tank which holds fresh VCM used in reactor charge.

b. Description

Vertical-mounted, 22-foot straight wall height, 26-foot overall height, eight-foot diameter with an approximate capacity of 8,700 gallons, carbon steel construction.

c. Normal Operating Conditions

Ambient temperature and 20-70 psig.

d. Design Conditions

150°F and full vacuum to 150 psig.

5. Hot Water Tank 45-748

a. Purpose

To supply a large volume of hot water for reactor charge and rinse.

b. Description

Vertical, cone roof, 42-foot straight wall height, 12-foot diameter with an approximate capacity of 35,000 gallons, aluminum construction.

c. Normal Operating Conditions

Atmospheric pressure and 145°F.

d. Design Conditions

212°F and 1.5 inches of water.

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

6. Initiator Injection Pot 45-750

a. Purpose

To inject initiator into the reactor during charge.

b. Description

Vertical-mounted, two-foot straight wall height with one-foot diameter, approximate capacity 12 gallons, stainless steel construction.

c. Normal Operating Conditions

Temperature near 70°F and 180-260 psig.

d. Design Conditions

150°F and 300 psig

7. Colloid Makeup Tank 45-751

a. Purpose

To provide for consistent colloid solution makeup.

b. Description

Top agitated, vertical-mounted, flat top, 11 1/2-foot straight wall height, seven-foot diameter, approximate capacity 3,300 gallons, bottom jacket for heating, side jacket for cooling, stainless steel construction.

c. Normal Operating Conditions

Atmospheric pressure and 70-200°F.

d. Design Conditions

400°F and 0 psig

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

8. Colloid Storage Tank 45-752

a. Purpose

To provide colloid solution storage.

b. Description

Vertical-mounted, flat top, cone bottom, 12-foot straight wall height, seven-foot diameter, approximate capacity 3,400 gallons, stainless steel construction.

c. Normal Operating Conditions

Atmospheric pressure and 70-85°F.

d. Design Conditions

150°F and 0 psig

9. Colloid Charge Tank 45-753

a. Purpose

To provide a sufficient quantity of quality colloid solution for charge.

b. Description

Vertical-mounted, flat top, cone bottom, 14-foot straight wall height, 5 1/2-foot diameter, capacity approximately 2,400 gallons, stainless steel construction.

c. Normal Operating Conditions

Atmospheric pressure and 70-85°F.

d. Design Conditions

150°F and 0 psig

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

10. Seal Oil Storage Drum 45-754

a. Purpose

To provide seal oil storage.

b. Description

Horizontal-mounted, five-foot straight wall length by three-foot diameter, carbon steel construction, approximate capacity 270 gallons.

c. Normal Operating Conditions

Atmospheric pressure, ambient temperature.

d. Design Conditions

150°F and 0 psig

11. AMS Short Stop Charge Pots 45-755, 45-756, 45-757, and 45-758

a. Purpose

To provide a means for injecting short stop solution into any or all of the reactors to stop the reaction.

b. Description

Vertical-mounted, two-foot straight wall height, six-inch diameter, capacity approximately three gallons, stainless steel construction.

c. Normal Operating Conditions

Approximately 70°F and 180-260 psig.

d. Design Conditions

150°F and 300 psig

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

12. Mechanical Seal Purge Water Surge Drum 45-759

a. Purpose

To provide seal purge water in the event of electrical power failure.

b. Description

Vertical-mounted, seven-foot straight wall height, 3 1/2-foot diameter, capacity approximately 500 gallons, stainless steel construction.

c. Normal Operating Conditions

Approximately 70°F and 200 psig.

d. Design Conditions

150°F and 300 psig

13. Recovery Knockout Drums 45-760 and 45-761

a. Purpose

To prevent liquid and solids carryover to the recovery vacuum pumps and compressors during reactor recovery.

b. Description

Vertical-mounted; bottom section has five-foot straight wall height; five-foot diameter; top section has ten-foot straight wall height; three-foot diameter; top section has water spray to help remove carryover; carbon steel construction.

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

c. Normal Operating Conditions

100-200°F and 0-35 psig

d. Design Conditions

300°F and full vacuum to 150 psig

14. Seal Water Separators 45-762 and 45-763

a. Purpose

To separate the circulating vacuum pump and compressor seal water from the recovered VCM vapor.

b. Description

Vertical-mounted, seven-foot straight wall height, four-foot diameter, approximate capacity 650 gallons, carbon steel construction.

c. Normal Operating Conditions

100-150°F and 40-80 psig

d. Design Conditions

300°F and full vacuum to 150 psig

15. Recovered VCM Collect Tank 45-764

a. Purpose

To collect recovered VCM and provide liquid head for VCM transfer pump to allow pumping of recovered VCM to recovered VCM storage tank.

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

b. Description

Horizontal-mounted, ten-foot straight wall length, three-foot diameter, approximate capacity 520 gallons, carbon steel construction.

c. Normal Operating Conditions

70-100°F and 35-75 psig

d. Design Conditions

160°F and full vacuum to 150 psig

16. Hydroquinone Storage Tank 45-765

a. Purpose

Provide for hydroquinone storage and makeup.

b. Description

Top-agitated, vertical-mounted, 2'6" straight wall height, two-foot diameter, approximate capacity 60 gallons, carbon steel construction.

c. Normal Operating Conditions

Temperature near ambient; pressure about 1 psig.

d. Design Conditions

150°F and 16 psig

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

17. Slurry Dump Tank 45-766

a. Purpose

To provide sufficient head for the slurry transfer pumps to operate correctly.

b. Description

Vertical-mounted, flat top, cone bottom, three-foot straight wall height, five-foot diameter, approximate capacity 440 gallons, stainless steel construction.

c. Normal Operating Conditions

One-inch water vacuum and 150-200°F.

d. Design Conditions

250°F and two-inch water pressure.

18. Cleaning Solution Tank 45-767

a. Purpose

To provide an adequate amount of chem wash solution during reactor chem wash.

b. Description

Vertical-mounted, flat top, cone bottom, ten-foot straight wall height, ten-foot diameter, approximate capacity 5,800 gallons, carbon steel construction.

c. Normal Operating Conditions

Atmospheric pressure and 60-190°F

d. Design Conditions

250°F and ± five-inch water pressure.

IV. EQUIPMENT INDEX (CONTINUED)

C. Tanks and Vessels (Continued)

19. Reactor Evacuation Ejector Cyclone Separator 45-768

a. Purpose

To remove any condensate present in the motive steam to the reactor evacuation steam ejector.

b. Description

High efficiency horizontal separator, Anderson type L5-4-175, 10 3/4-inch outside diameter, 26 inches long, carbon steel construction with stainless steel internal baffles.

c. Normal Operating Conditions

Steam in is 125 psig and 353°F.

d. Design Conditions

400°F and 175 psig

20. Reactor Sampling Bomb 45-770

a. Purpose

To safely obtain a resin sample from the reactor.

b. Description

3/4-inch stainless steel pipe, three inches long. One end is capped, and the other is fitted with a coupling. A basket strainer fits inside the sampler for easy resin removal.

c. Normal Operating Conditions

Slight vacuum to 60 psig and 70-140°F.

IV. EQUIPMENT INDEX (CONTINUED)

D. Filters

1. Process Water Charge Filter 64-716

a. Purpose

To remove dirt and scale from the charge water.

b. Description

Filterite Model 88MS04-316-4FD-C300, cartridge type, stainless steel.

c. Normal Operating Conditions

40 psig and 70°F

d. Design Conditions

300 psig and 200°F. Particle retention size is ten microns.

2. VCM Charge Filters 64-718 and 64-742

a. Purpose

To remove any PVC particles from the VCM charge to the reactor.

b. Description

Filterite model 906415-001, cartridge type, stainless steel filter with polypropylene filtering element.

c. Normal Operating Conditions

150-200 psig and ambient temperature.

d. Design Conditions

150°F, 300 psig, 1,000 gpm, particle retention size is ten microns.

IV. EQUIPMENT INDEX (CONTINUED)

D. Filters (Continued)

3. Recovered VCM Filter 64-719

a. Purpose

To remove PVC particles from the recovered VCM charge to the reactor.

b. Description

Filterite Model 909596, cartridge type, stainless steel filter with polypropylene filtering element.

c. Normal Operating Conditions

40-130 psig and ambient temperature.

d. Design Conditions

150°F, 190 psig, 250 gpm, particle retention size ten microns.

4. Process Water Filter 64-720

a. Purpose

To remove dirt and scale from process water to the hot water tank.

b. Description

Dollinger Model LL-122-280, cartridge type, carbon steel filter with polypropylene filtering element.

c. Normal Operating Conditions

40 psig and 70°F

d. Design Conditions

100°F, 100 psig, 200 gpm, particle retention size ten microns.

IV. EQUIPMENT INDEX (CONTINUED)

D. Filters (Continued)

5. Colloid Makeup Water Filter 64-721

a. Purpose

To remove dirt and scale from water used in colloid makeup.

b. Description

Dollinger Model LL-222-180, Series 150, cartridge type, stainless steel filter, cotton filtering element.

c. Normal Operating Conditions

40 psig and 70°F

d. Design Conditions

250°F, 250 psig, 125 gpm, particle retention size ten microns.

6. Colloid Transfer Filters 64-722 and 64-723

a. Purpose

To remove any undissolved F-50 methocel (the powder that is dissolved in water to make the colloid solution) from the colloid solution.

b. Description

Dollinger Model LL-222-66, cartridge type, stainless steel filter with polypropylene filtering element.

c. Normal Operating Conditions

35 psig and 85°F

d. Design Conditions

100°F, 75 psig, 50 gpm, particle retention size 90 microns.

IV. EQUIPMENT INDEX (CONTINUED)

D. Filters (Continued)

7. Service Water Filter 64-724

a. Purpose

To remove dirt and scale from service water.

b. Description

Dollinger Model LL-222-280, cartridge type, stainless steel filter with cotton filtering element.

c. Normal Operating Conditions

40 psig and 70°F

d. Design Conditions

100°F, 100 psig, 190 gpm, particle retention size ten microns.

8. Seal Oil Supply Filters 64-725 and 64-726

a. Purpose

Removes dirt and scale from seal oil.

b. Description

Dollinger Model LL-222-39, Series 150, cartridge type, stainless steel filter with cotton filtering element.

c. Normal Operating Conditions

245 psig and 100°F

d. Design Conditions

150°F, 275 psig, 4 gpm, particle retention size one micron.

IV. EQUIPMENT INDEX (CONTINUED)

D. Filters (Continued)

9. Seal Oil Return Filters 64-727 and 64-728

a. Purpose

Removes dirt and scale from seal oil.

b. Description

Dollinger Model LL-222-39, Series 150, cartridge type, stainless steel filter with cotton filtering elements.

c. Normal Operating Conditions

220 psig and 100°F

d. Design Conditions

150°F, 275 psig, 4 gpm, particle retention size one micron.

10. Seal Water Filters 64-731 and 64-732

a. Purpose

To remove PVC resin from the circulating seal water for the recovery vacuum pumps and compressors.

b. Description

Dollinger Model LL-122-140, cartridge type, carbon steel filter with polypropylene filtering element.

c. Normal Operating Conditions

90-130 psig and 100-150°F

d. Design Conditions

300°F, 150 psig, 160 gpm, particle retention size 100 microns.

IV. EQUIPMENT INDEX (CONTINUED)

D. Filters (Continued)

11. Slurry Strainer 64-733

a. Purpose

To remove large resin particles from the slurry.

b. Description

Sweco Model LS605 1210, vibrating screen, stainless steel filter and filtering element.

c. Normal Operating Conditions

One-inch water vacuum and 150-200°F

d. Design Conditions

250°F, two-inch water pressure, 1,000 gpm, particle retention on four-mesh screen.

12. Cleaning Solution Strainer 64-734

a. Purpose

To remove PVC particles from the cleaning solution.

b. Description

Ten-inch Elco line strainer, carbon steel construction.

c. Normal Operating Conditions

2 psig and 180°F

d. Design Conditions

200°F, 20 psig, 500 gpm, particle retention on four-mesh screen.

IV. EQUIPMENT INDEX (CONTINUED)

D. Filters (Continued)

13. Breathing Air Filters 64-735, 64-736, 64-737, 64-738, 64-739, 64-740

a. Purpose

To remove dirt and scale from the breathing air.

b. Description

Dollinger Model GP-246-15, cartridge type, stainless steel filter, Nylon 147 filtering element.

c. Normal Operating Conditions

70-90 psig and 60-70°F

d. Design Conditions

100°F, 125 psig, 6,000 standard cubic feet per hour (SCFH), particle retention size five microns.

14. Blowdown Tank Drain Strainer 64-741

a. Purpose

To remove PVC particles in water dumped to the sewer from the blowdown tank.

b. Description

Andale type 105 simplex strainer, basket strainer, cast iron with stainless steel filtering element.

c. Normal Operating Conditions

8-9 psig and 100-150°F

d. Design Conditions

200°F, 125 psig, 200 gpm, particle retention size 3/8 inch.

IV. EQUIPMENT INDEX (CONTINUED)

E. Pumps

1. VCM Charge Pumps 72-875 and 72-876

a. Purpose

To supply reactors with VCM during charge.

b. Description

Centrifugal type, Goulds Model 3736, 3X6-13DV, Group L, 150-HP, 3,560 RPM. The casing is carbon steel and the impeller is cast iron.

c. Normal Operating Conditions

Rated for 800 gpm at 450 feet of differential head.

2. Recovered VCM Charge Pumps 72-877 and 72-878

a. Purpose

To supply recovered VCM to the suction of the VCM charge pumps during charge.

b. Description

Centrifugal type, Goulds Model 3196 MT, 2X3-13, 10-HP, 1,750 rpm. The casing is stainless steel and the impeller is cast iron.

c. Normal Operating Conditions

Rated for 250 gpm at 82 feet of differential head.

IV. EQUIPMENT INDEX (CONTINUED)

E. Pumps (Continued)

3. Hot Water Charge Pumps 72-879 and 72-880

a. Purpose

To supply the reactor with hot water during charge.

b. Description

Centrifugal type, Goulds Model 3196 LTC, 2X3-13, 100-HP, 3,550 rpm. The casing is stainless steel and the impeller is cast iron.

c. Normal Operating Conditions

Rated for 450 gpm at 410 feet of differential head.

4. Colloid Batch Transfer Pump 72-881 and Colloid Circulation Pump 72-882

a. Purpose

The batch transfer pump is used primarily to transfer colloid from the colloid makeup tank to the colloid storage tank. The colloid circulation pump is used primarily to circulate colloid in the storage tank and to transfer colloid from the storage tank to the colloid charge tank. These pumps are piped so they can be used to spare each other.

b. Description

Centrifugal type, Goulds Model 3196 MT, 1X2-10, 3-HP, 1,750 rpm. The casing and impeller are stainless steel.

c. Normal Operating Conditions

Rated for 50 gpm at 69 feet differential head.

IV. EQUIPMENT INDEX (CONTINUED)

E. Pumps (Continued)

5. Colloid Charge Pumps 72-883 and 72-884

a. Purpose

Used to charge colloid to the reactor.

b. Description

Centrifugal type, Goulds Model 3736, 1X2-11B, 50-HP, 3,550 rpm. The casing and impeller are stainless steel.

c. Normal Operating Conditions

Rated for 100 gpm at 470 feet differential head.

6. High Pressure Service Water Pumps 72-885 and 72-886

a. Purpose

To provide high pressure water for a variety of uses.

b. Description

Centrifugal type, Goulds Model 3196 LTC, 2X3-13, 60-HP, 3,550 rpm. The casing and impeller are stainless steel.

c. Normal Operating Conditions

Rated for 150 gpm at 415 feet of differential head.

7. Mechanical Seal Purge Water Pumps 72-887 and 72-888

a. Purpose

To supply high pressure water to the reactor agitator seals and the reactor cleaning nozzle flush.

b. Description

Centrifugal type, Goulds 3196 MT, 1X2-10, 30-HP, 3,500 rpm. The casing and the impeller are stainless steel.

IV. EQUIPMENT INDEX (CONTINUED)

E. Pumps (Continued)

c. Normal Operating Conditions

Rated for 40 gpm at 415 feet of differential head.

8. Water Recirculation Pumps 72-889 and 72-890

a. Purpose

To circulate water in the recovery knockout drums.

b. Description

Centrifugal type, Goulds Model 3196 MT, 2X3-10, 7 1/2 HP, 1,750 rpm. The casing is stainless steel and the impeller is cast iron.

c. Normal Operating Conditions

Rated for 200 gpm at 68 feet differential head.

9. Seal Water Pumps 72-891 and 72-892

a. Purpose

To circulate the seal water used by the recovery vacuum pumps and compressors.

b. Description

Centrifugal type, Goulds Model 3196 MT, 2X3-10, 10-HP, 1,750 rpm. The casing is stainless steel and the impeller is cast iron.

c. Normal Operating Conditions

Rated for 160 gpm at 94 feet of differential head.

IV. EQUIPMENT INDEX (CONTINUED)

E. Pumps (Continued)

10. Recovered VCM Transfer Pumps 72-893 and 72-894

a. Purpose

To transfer recovered VCM from the recovered VCM collect tank to a recovered VCM storage tank.

b. Description

Centrifugal type, Goulds Model 3196 MT, 1X2-10, 3-HP, 1,750 rpm. The casing is stainless steel and the impeller is cast iron.

c. Normal Operating Conditions

Rated for 50 gpm at 75 feet of differential head.

11. Hydroquinone Injection Pump 72-895

a. Purpose

To supply hydroquinone solution for injection into recovery system seal water during reactor recovery.

b. Description

Reciprocating type, Milton-Roy Model DB-1-30R, 1/4 HP, 1,750 rpm, carbon steel construction.

c. Normal Operating Conditions

0.081 gph at approximately 282 feet of differential head.

12. Slurry Transfer Pumps 72-896 and 72-897

a. Purpose

To transfer slurry from the reactor to the slurry blend tanks.

IV. EQUIPMENT INDEX (CONTINUED)

E. Pumps (Continued)

b. Description

Centrifugal type, Goulds Model 3196 MT, 4X6-13, 40-HP, 1,770 rpm. The casing and impeller are stainless steel.

c. Normal Operating Conditions

Rated for 600 gpm at 126 feet of differential head.

13. Cleaning Solution Pumps 72-898 and 72-899

a. Purpose

To supply chem wash solution to the reactors during chem wash.

b. Description

Centrifugal type, Durco Model Mark II, Group II, 4X3-10/80, 75-HP, 3,550 rpm, stainless steel casing and impeller.

c. Normal Operating Conditions

Rated for 500 gpm at 165 feet of differential head.

14. Blowdown Tank Pump 72-900

a. Purpose

To pump water which has been stripped of VCM from the blowdown tank to the sewer.

b. Description

Centrifugal type, Durco Model Mark II, Group II, 4X3-10/84, 7 1/2 HP, 1,750 rpm. The casing is stainless steel and the impeller is cast iron.

c. Normal Operating Conditions

Rated for 200 gpm at 63 feet of differential head.

IV. EQUIPMENT INDEX (CONTINUED)

F. Compressors and Fans

1. Recovery Vacuum Pumps 72-901 and 72-902

a. Purpose

To recover unreacted VCM from the polymerization reactors.

b. Description

Bingham Model 4G-M, 75-HP, 1,200 rpm. Constant volume liquid ring with a water seal. The liquid ring is driven by a multivaned impeller in a circular pumpcase. Construction is cast iron casing and ductile iron impeller.

c. Normal Operating Conditions

24 inches Hg vacuum to 7 psig inlet, 0-10 psig dishcarge, and 100-150°F.

2. Recovery Compressors 72-903, 72-904, and 72-905

a. Purpose

To recover unreacted VCM from the polymerization reactors.

b. Description

Nash Model 1256, 150-HP, constant volume liquid ring with water seal. The liquid ring is driven by a multivaned impeller in a circular pumpcase. Construction is cast iron casing and stainless steel impeller.

c. Normal Operating Conditions

0-35 psig inlet, 40-80 psig outlet, and 100-150°F.

IV. EQUIPMENT INDEX (CONTINUED)

F. Compressors and Fans (Continued)

3. Slurry Strainer Exhauster 49-368

a. Purpose

To keep personnel exposure to VCM vapors to a minimum.

b. Description

Centrifugal fan, Buffalo Forge Model 365 DL, 3-HP, 1,800 rpm, stainless steel construction.

c. Normal Operating Conditions

Near atmospheric pressure and 150-200°F.

G. Agitators

1. Reactor Agitators 51-101, 51-102, 51-103, and 51-104

a. Purpose

To keep the colloid, VCM, and water in the reactor well mixed.

b. Description

Bottom entering, single speed, four blades at 45° angle, 200-HP, 125 rpm, stainless steel construction.

c. Normal Operating Conditions

15,000 gallons of liquid or slurry in vertical vessel, 22-foot straight wall by 12-foot diameter, at about 120°F and 130 psig.

IV. EQUIPMENT INDEX (CONTINUED)

G. Agitators (Continued)

2. Colloid Makeup Tank Agitator 51-105

a. Purpose

To provide agitation needed to dissolve F-50 methocel in water.

b. Description

Top entering, single speed, "Lightnin" Model 73-Q-5, 5-HP, 1,750 rpm. Wetted parts are stainless steel.

c. Normal Operating Conditions

3,000 gallons of colloid solution; tank is vertical; seven-foot diameter by 11'6" tall; temperature ranges from 70-250°F and atmospheric pressure.

3. Hydroquinone Storage Tank Agitator 51-106

a. Purpose

To provide agitation needed to dissolve hydroquinone powder in water.

b. Description

Top entering, single speed, "Lightnin" Model N33-33, 1/3-HP, 1,750 rpm.

c. Normal Operating Conditions

Approximately fifty gallons hydroquinone solution in vertical tank 2'6" high by two-foot diameter, 1 psig, and 70°F.

IV. EQUIPMENT INDEX (CONTINUED)

H. Package Units

1. Seal Oil Pressure Units 95-299 and 95-300

a. Purpose

To supply seal oil to the reactor agitator seals at the required temperature and pressure.

b. Description

Dura circulator Model SWAR-40-25.

c. Normal Operating Conditions

245-250 psig, 100-150°F. The seal oil is Di(2-Ethylhexy) phthalate (DOP) which has a viscosity of 35 cp.

V. Instrument Index

V. INSTRUMENT INDEX

A. Flow Controllers

Item No.	Service	Type	Set Point
FIRC-710 FIRC-711 FIRC-712 FIRC-713	Reactor Cooling Water Flow Controllers	Meter run with orifice plate, board-mounted indicators and recorders.	Cascade control; the temperature controller of each reactor sets the set point.

NOTE: FIRC-710 controls the cooling water to reactor 45-741.
FIRC-711 controls the cooling water to reactor 45-742.
FIRC-712 controls the cooling water to reactor 45-443.
FIRC-713 controls the cooling water to reactor 45-744.

FIC-738 FIC-739 FIC-740	Recovery Vacuum Pump and Compressor Seal Water Flow Controllers	Brooks Model 3611 Rotameter with transmitter and a local Foxboro flow controller	50 gpm

NOTE: FIC-738 controls the seal water to vacuum pump 72-901 and compressor 72-903.
FIC-739 controls the seal water to vacuum pump 72-902 and compressor 72-904.
FIC-740 controls the seal water to compressor 72-905.

FCi-749 FCi-750 FCi-751 FCi-752	Reactor Agitator Mechanical Seal Oil Supply Flow Regulators	Kates Model MFA1-1 Flow Regulator	1.0 gpm

NOTE: FCi-749 controls the seal oil flow to reactor 45-741 double mechanical seal.
FCi-750 controls the seal oil flow to reactor 45-742 double mechanical seal.
FCi-751 controls the seal oil flow to reactor 45-743 double mechanical seal.
FCi-752 controls the seal oil flow to reactor 45-744 double mechanical seal.

V. INSTRUMENT INDEX (CONTINUED)

B. Flow Totalizers

Item No.	Service	Type	Set Point
FQIC-701A FQIC-701B	VCM Charge Totalizers	Foxboro Turbine Meter, Board-Mounted Readout	Determined by specific batch recipe.
FQIC-702	Recovered VCM Charge Totalizer	Fischer/Porter Vortex Shedding Meter, Board Mounted Readout	Determined by specific batch recipe.
FQIC-703	Initiator Injection Pot Service Water Flow Totalizer	Foxboro Turbine Meter, Board-Mounted Readout	Determined by specific batch recipe.
FQIC-704	Hot Water Charge Totalizer	Foxboro Turbine Meter, Board-Mounted Readout	Determined by specific batch recipe.
FQIC-705	Colloid Charge Totalizer	Brooks Oval Meter, Board-Mounted Readout	Determined by specific batch recipe.
FQIC-706	Colloid Makeup Water Flow Totalizer	Brooks Oval Meter, Local Colloid Board Readout	Hot Water, 538 Gallons Cold Water, 2,623 Gallons
FQI-708	Reactor Steam Stripping Flow Totalizer	Orifice Plate with D/P Cell, Board-Mounted Readout	None; totalizes only.
FQI-757	Hot Water Charge Totalizer	Orifice Plate with D/P Cell, Board-Mounted Readout	None; totalizes only.
FQI-811	Steam to Reactor Module Flow Totalizer	Orifice Plate with D/P Cell, Board-Mounted Readout	None; totalizes only.

V. INSTRUMENT INDEX (CONTINUED)

C. Level Controllers

Item No.	Service	Type	Set Point
LC-720 LC-722	Seal Water Separator Level Controllers	Displacer, Fisher Model 2500T	16 Inches from Bottom of Displacer Float

NOTE: LC-720 controls the water level in seal water separator 45-762.
LC-722 controls the water level in seal water separator 45-763.

LIC-725	Slurry Dump Tank 45-766 Level Controller	Displacer, Fisher Model 2500T	To be determined in field.

D. Pressure Controllers

Item No.	Service	Type	Set Point
PCi-704	Recovered VCM Storage Tanks 89-520 and 45-317 Inert Vent Backpressure Regulator	Self-Contained Pressure Regulator	60 psig
PCi-706	Steam Stripping Header Steam Supply Backpressure Regulator	Self-Contained Pressure Regulator	100 psig
PIC-725	Recovery Knockout Drum 45-760 Inlet Pressure Controller	Diaphragm with Foxboro Controller	35 psig
PIC-726	VCM Bleed Stream to Recovery System Pressure Controller	Vacuum D/P Transmitter with a Local Foxboro Controller	3" Hg Vacuum
PCi-729	Hydroquinone Storage Tank 45-765 Nitrogen Pressure Regulator	Self-Contained Pressure Regulator	1 psig
PCi-731	Mechanical Seal Purge Water Surge Drum 45-759 Nitrogen Supply Pressure Regulator	Self-Contained Pressure Regulator	180 psig

V. INSTRUMENT INDEX (CONTINUED)

D. Pressure Controllers (Continued)

Item No.	Service	Type	Set Point
PCi-739	Seal Oil Pressure Unit 95-299 Nitrogen Supply Pressure Regulator	Self-Contained Pressure Regulator	200 psig
PCi-741	Seal Oil Pressure Unit 95-300 Nitrogen Supply Pressure Regulator	Self-Contained Pressure Regulator	200 psig
PCi-743 PCi-744 PCi-745 PCi-746 PCi-747 PCi-752	Breathing Air Station Supply Pressure Regulator	Self-Contained Pressure Regulator	20 psig

NOTE: PCi-743 regulates breathing air to the reactor area, ground level.
PCi-744 regulates breathing air to the reactor area, second level.
PCi-745 regulates breathing air to the recovery building, first floor.
PCi-746 regulates breathing air to the recovery building, second floor.
PCi-747 regulates breathing air to the charge area.
PCi-752 regulates breathing air to the reactor area, third level.

PCi-754 PCi-755 PCi-756 PCi-757	NO Short Stop Supply Pressure Regulator	Self-Contained Pressure Regulator	200 psig

NOTE: PCi-754 regulates NO supply pressure to reactor 45-741.
PCi-755 regulates NO supply pressure to reactor 45-742.
PCi-756 regulates NO supply pressure to reactor 45-743.
PCi-757 regulates NO supply pressure to reactor 45-744.

PIC-759	Blowdown Tank 45-319 Pressure Controller	Vacuum D/P Transmitter with Local Foxboro Controller	To be Determined in Field

V. INSTRUMENT INDEX (CONTINUED)

E. Temperature Controllers

Item No.	Service	Type	Set Point
TIC-701	Hot Water Tank 45-748 Temperature Controller	Resistance Bulb with Board-Mounted Foxboro Controller	140°F
TIC-702	Hot Water Preheater 55-332 Discharge Temperature Controller	Filled System with Local Foxboro Controller	145°F
TRC-703	Charge Water Temperature Controller	Resistance Bulb with Board-Mounted Foxboro Controller	Determined by Specific Batch Recipe
TIRC-706 TIRC-707 TIRC-708 TIRC-709	Reactor Polymerization Temperature Controllers	Resistance Bulb with Foxboro Controller	Determined by Specific Batch Recipe

NOTE: TIRC-706 controls reactor 45-741 polymerization temperature.
TIRC-707 controls reactor 45-742 polymerization temperature.
TIRC-708 controls reactor 45-743 polymerization temperature.
TIRC-709 controls reactor 45-744 polymerization temperature.

TIRC-710 TIRC-711 TIRC-712 TIRC-713	Reactor Steam Stripping Temperature Controller	Resistance Bulb with Board-Mounted Foxboro Controller	225°F

NOTE: TIRC-710 controls reactor 45-741 steam stripping temperature.
TIRC-711 controls reactor 45-742 steam stripping temperature.
TIRC-712 controls reactor 45-743 steam stripping temperature.
TIRC-713 controls reactor 45-744 steam stripping temperature.

TIC-716 TIC-717	Seal Water Temperature Controller	Filled System with Local Foxboro Controller	To be Determined in Field

NOTE: TIC-716 controls seal water cooler 55-335 outlet temperature.
TIC-717 controls seal water cooler 55-336 outlet temperature.

V. INSTRUMENT INDEX (CONTINUED)

E. Temperature Controllers (Continued)

Item No.	Service	Type	Set Point
TIC-718	Cleaning Solution Heater 55-339 Outlet Temperature Controller	Filled System with Local Foxboro Controller	190°F
TIC-730	Blowdown Tank 45-319 Temperature Controller	Filled System with Local Foxboro Controller	175°F

VI. Alarms, Switches, and Safety Equipment

VI. ALARMS AND SAFETY EQUIPMENT

A. Continuous Flow Fresh Air System

In order to provide personnel protection, a continuous flow fresh air system has been installed. This system consists of personnel fresh air masks and a constant flow breathing air supply. The supply lines are piped to all affected areas of the plant. The individual hookup stations consist of quick connect/disconnect-type fittings.

The individual lines to the designated areas are designed to allow a minimum flow of 6 SCFM to each mask at approximately 10-15 psig. An air pressure regulator, shutoff valve, and an air filter are provided at the piping header to each individual area.

The air supply system utilizes two Nash compressors supplying 100 SCFM each at a maximum pressure of 80 psig. Each compressor will supply about fifteen masks with air at one time. The compressors normally are both in operation at the same time, except in cases of mechanical failure.

The system is equipped with both visable and audible low pressure alarms which are activated at 50 psig. The revolving beacon light is mounted on a pole to give wider visibility, and the horn is mounted at the compressor. An on-off switch is provided at each compressor.

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

A. Continuous Flow Fresh Air System (Continued)

The following job operations will REQUIRE the wearing of a continuous flow fresh air mask supplied through the fresh air lines or a Scott Air Pak:

1. Venting or changing filters in any VCM vessel.

   NOTE: No vessel or line should be vented unless there is no alternative, such as using pipe or hose to transfer VCM into the recovery system or blowdown tank.

2. Entering any vessel that normally contains VCM, such as reactors, blowdown tanks, knockout drums, receivers, etc (except for scaffolding construction).
3. Opening large reactor manhead (wear mask until the manway is partially open and the evacuation jet is moving air through the manway).
4. Opening any line that may possibly contain VCM vapors.
5. At ANY location where the VCM concentration is above the current allowable limit. Anytime VCM is detected by sight or smell, the concentration is well above the limits and precaution is mandatory.

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches

1. Amperage Alarms

Item No.	Service	Type	Set Point
AAHL-701 AAHL-702 AAHL-703 AAHL-704	Low or High Amperage to the Reactor Agitator Motor	Board-Mounted Alarm	To be determined in the field.

NOTE: AAHL-701 indicates abnormal amperage to reactor 45-741 agitator motor.
AAHL-702 indicates abnormal amperage to reactor 45-742 agitator motor.
AAHL-703 indicates abnormal amperage to reactor 45-743 agitator motor.
AAHL-704 indicates abnormal maperage to reactor 45-744 agitator motor.

2. Flow Alarms and Switches

Item No.	Service	Type	Set Point
FSL-701A and B	Low VCM Flow during Charge	Switch that Activates Alarm (FAL-701) on Board	400 gpm
FAL-701	Low VCM Flow during Charge	Board-Mounted Alarm	400 gpm
FAL-714 FAL-715 FAL-716 FAL-717	Low Seal Water Flow to the Reactor Agitators	Board-Mounted Alarm	2 gpm

NOTE: FAL-714 indicates low flow to reactor 45-741.
FAL-715 indicates low flow to reactor 45-742.
FAL-716 indicates low flow to reactor 45-743.
FAL-717 indicates low flow to reactor 45-744.

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches (Continued)

3. Level Alarms and Switches

Item No.	Service	Type	Set Point
LAH-701	High VCM Level in Fresh VCM Storage Tank 45-745	Board-Mounted Alarm	252 Inches above Bottom Tangent
LSH-701A	High VCM Level in Fresh VCM Storage Tank 45-745	Switch Activates LAH-701	252 Inches above Bottom Tangent
LSH-701B	High VCM Level in Fresh VCM Storage Tank 45-745	Switch that Serves as Charge Permissive	252 Inches above Bottom Tangent
LSH-701C	Level Control of Fresh VCM Receiver 45-745	Switch which Stops VCM Transfer	225 Inches Above Discharge Nozzle
LSL-701D	Level Control of Fresh VCM Receiver 45-745	Switch which Starts Transfer	219 Inches Above Discharge Nozzle
LAH-710	High Level in Colloid Makeup Tank 45-751	Alarm on Colloid Local Board	8 Inches from Top of Tank
LSH-711B	High Water Level in Hot Water Tank 45-748	Switch that Serves as Charge Permissive	129 Inches above Discharge Nozzle
LSH-711C	Hot Water Tank 45-758 Level Control	Switch which Stops Water Transfer on High Level	360 Inches above Bottom Tangent
LSL-711D	Hot Water Tank 45-748 Level Control	Switch which Starts Water Transfer	350 Inches above Discharge Nozzle
LAH-713	High Level in Colloid Storage Tank 45-752	Board-Mounted Alarm	6 Inches from Top of Tank

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches (Continued)

3. Level Alarms and Switches (Continued)

Item No.	Service	Type	Set Point
LAH-714	High Level in Colloid Charge Tank 45-753	Board-Mounted Alarm	8 Inches from Top of Tank
LSL-715	Low Level in Colloid Charge Tank 45-753	Switch Serves as Charge Permissive	24 Inches above Bottom Tangent
LSH-716	Level Control of Recovery Knockout Drum 45-760	Switch Opens Valve to Blowdown Tank on High Level	28 Inches above Bottom Tangent
LSL-717	Level Control of Recovery Knockout Drum 45-760	Switch Closes Valve to Blowdown Tank on Low Level	18 Inches above Bottom Tangent
LSH-718	Level Control of Recovery Knockout Drum 45-761	Switch Opens Valve to Blowdown Tank on High Level	28 Inches above Bottom Tangent
LSH-719	Level Control of Recovery Knockout Drum 45-761	Switch Closes Valve to Blow down Tank on Low Level	18 Inches Above Bottom Tangent
LAH-720	High Level in Seal Water Separator 45-762	Local Alarm	44 Inches above Bottom Tangent
LAL-720	Low Level in Seal Water Separator 45-762	Local Alarm	16 Inches above Bottom Tangent
LAH-722	High Level in Seal Water Separator 45-763	Local Alarm	44 Inches above Bottom Tangent
LAL-722	Low Level in Seal Water Separator 45-763	Local Alarm	16 Inches above Bottom Tangent

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches (Continued)

3. Level Alarms and Switches (Continued)

Item No.	Service	Type	Set Point
LAH-725	High Level in Slurry Dump Tank 45-766	Board-Mounted Alarm	6 Inches from Top of Tank
LAH-727	High Level in Cleaning Solution Tank 45-767	Board-Mounted Alarm	6 Inches from Top of Tank
LAL-729	Low Level in Cleaning Solution Tank 45-767	Board-Mounted Alarm	6 Inches from Bottom of Tank
LSL-730	Low Level in Seal Oil Reservoir 95-299	Switch Activates LAL-730, Starts Spare Seal Oil Unit 95-300, and Turns Off 95-299	To be Defined by Vendor
LAL-730	Low Level in Seal Oil Reservoir 95-299	Board-Mounted Alarm	To be Defined by
LSL-731	Low Level in Seal Oil Reservoir 95-300	Switch Activates LAL-731, Starts Spare Seal Oil Unit 95-299, and Turns Off 95-300	To be Defined by Vendor
LAL-731	Low Level in Seal Oil Reservoir 95-300	Board-Mounted Alarm	To be Defined by Vendor
LAL-733	Low Level in Hydroquinone Storage Tank 45-765	Board-Mounted Alarm	6 Inches above Bottom Tangent
LAH-734	High Level in Cleaning Solution Tank 45-767	Switch Shuts Down Cleaning Solution Pumps 72-898 and 72-899 and Caustic Transfer Pumps	6 Inches from Top of Tank
LAL-739	Low Level in Colloid Makeup Tank 45-751	Board-Mounted Alarm	One Inch above Bottom Tangent

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches (Continued)

3. Level Alarms and Switches (Continued)

Item No.	Service	Type	Set Point
LAH-740	High Level in Blowdown Tank 45-319	Board-Mounted Alarm	22 Inches from Top of Tank
LSL-741	Low Level in Blowdown Tank 45-319	Switch will Shut Off Blowdown Tank Pump 72-900 and Close Valves CV-880 and CV-891	12 Inches from Bottom of Tank

4. Pressure Alarms and Switches

Item No.	Service	Type	Set Point
PSH-703	High Pressure in Initiator Injection Pot 45-750	Switch turns on high pressure light on the board and is a precharge condition.	180 psig
PSL-707	Low Pressure in Steam Stripping Header	Switch closes control valve that supplies steam to the reactor during steam stripping.	100 psig
PSL-712 PSL-713 PSL-714 PSL-715	Low Pressure in Reactor during Recovery	Switch prevents opening of reactor dump valve unless pressure during recovery has been at least as low as set point.	8 psig

NOTE: PSL-712 senses pressure in reactor 45-741.
PSL-713 senses pressure in reactor 45-742.
PSL-714 senses pressure in reactor 45-743.
PSL-715 senses pressure in reactor 45-744.

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches (Continued)

4. Pressure Alarms and Switches (Continued)

Item No.	Service	Type	Set Point
PSL-716 PSL-717 PSL-718 PSL-719	Low Pressure in Reactors during Evacuation	Switch keeps charge from starting by preventing main reactor charge valve from opening unless pressure is at least as low as set point.	25" Hg Vacuum

NOTE: PSL-716 senses pressure in reactor 45-741.
PSL-717 senses pressure in reactor 45-742.
PSL-718 senses pressure in reactor 45-743.
PSL-719 senses pressure in reactor 45-744.

PAH-720 PAH-721 PAH-722 PAH-723	High Pressure in Reactors	Board-Mounted Alarm	140 psig

NOTE: PAH-720 indicates high pressure in reactor 45-741.
PAH-721 indicates high pressure in reactor 45-742.
PAH-722 indicates high pressure in reactor 45-743.
PAH-723 indicates high pressure in reactor 45-744.

PSL-727	Low Recovery Compressor Suction Pressure	Switch will start recovery vacuum pumps 72-901 and 72-902 and activate proper valving sequence during recovery.	7 psig
PDS-728	High Differential Pressure Between Recovery Vacuum Pump Suction and Recovery Compressor Discharge	Switch shuts off recovery compressors 72-903, 72-904, and 72-905 and vacuum pumps 72-901 and 72-902.	80 psig
PSL-732	Low Pressure on High Pressure Service Water System	Switch prevents automatic charge sequence from beginning and activates PAL-732.	150 psig

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches (Continued)

4. Pressure Alarms and Switches (Continued)

Item No.	Service	Type	Set Point
PAL-732	Low Pressure on High Pressure Service Water System	Board-Mounted Alarm	150 psig
PSL-737	Low Pressure on Mechanical Seal Purge Water System (MSPW)	Switch activates PAL-737 and turns on spare (MSPW) pump 72-887 or 72-888.	180 psig
PAL-737	Low Pressure on Mechanical Seal Purge Water System	Board-Mounted Alarm	180 psig
PSL-738	Low Pressure from Seal Oil Unit 95-299	Switch activates spare seal oil unit 95-300, turns off 95-299, activates the necessary valves, and activates PAL-738.	205 psig
PAL-738	Low Pressure from Seal Oil Unit 95-299	Board-Mounted Alarm	205 psig
PSL-740	Low Pressure from Seal Oil Unit 95-300	Switch activates spare seal oil unit 95-299, turns off 95-300, activates the necessary valves, and activates PAL-740.	205 psig
PAL-740	Low Pressure from Seal Oil Unit 95-300	Board-Mounted Alarm	205 psig
PAH-750	High Pressure on Initiator Injection Pot 45-750	Board-Mounted Alarm	225 psig

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

B. Alarms and Switches (Continued)

4. Pressure Alarms and Switches (Continued)

Item No.	Service	Type	Set Point
PAH-751	High Seal Oil System Pressure	Board-Mounted Alarm	255 psig
PAL-753	Low Pressure on NO Short Stop Bottles	Board-Mounted Alarm	350 psig
PSL-758	Low Pressure on High Pressure Service Water System (HPSW)	Switch turns on spare HPSW pump 72-885 or 72-886.	180 psig
PAH-760	High Pressure in Blowdown Tank 45-319	Board-Mounted Alarm	10 psig
PSL-762	Low Steam Pressure to Blowdown Tank 45-319	Switch closes TCV-730 and PCV-759 and re-sets on rising steam pressure of 50 psig.	40 psig
PAL-763	Low Instrument Air Pressure	Board-Mounted Alarm	85 psig
TAH-706 TAH-707 TAH-708 TAH-709	High Temperature in the Reactors	Board-Mounted Alarm	160°F

NOTE: TAH-706 indicates high temperature in reactor 45-741.
TAH-707 indicates high temperature in reactor 45-742.
TAH-708 indicates high temperature in reactor 45-743.
TAH-709 indicates high temperature in reactor 45-744.

TAH-715	High Discharge Temperature on the Recovery Compressors	Board-Mounted Alarm	150°F
TAH-719	High Seal Oil Temperature	Board-Mounted Alarm	125°F
TAH-720	High Temperature in Initiator Injection Pot 45-750	Board-Mounted Alarm	75°F

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

C. Firewater System

The firewater system consists of a deluge system, combustible hydrocarbon analyzer, and fire monitors with hose connections.

1. Fire Monitors

The fire monitors are normally supplied from the city water system. A tie-in with the firewater system allows the fire monitors to operate off either water system. There are six fire monitors located around the perimeter of the recovery building and reactor area.

2. Hydrocarbon Analyzer

A continuous combustible hydrocarbon analyzer is used to detect major VCM leaks. When the VCM level at any sample point reaches the set point, the deluge system is activated automatically.

3. Deluge System

The deluge system is normally supplied from the firewater system. It can be operated on process water. The deluge system is a sprinkler system which will cover the reactors, dump system, fresh and recovered VCM storage tanks, and both floors of the recovery building with a water spray. The deluge system is designed to lower VCM concentrations in the reactor and recovery building area in the event of a VCM leak and as a sprinkler system to help put out fires. The deluge system can be activated manually, by the combustible hydrocarbon analyzer, or by thermal sensors.

VI. ALARMS AND SAFETY EQUIPMENT (CONTINUED)

C. Firewater System (Continued)

3. Deluge System (Continued)

The revised firewater system contains three new post indicator valves (PIV) and one PIV was relocated. These are valves which have indicators on them to show whether the valve is open or closed. These valves are used to direct water to either the D-700 reactor area or the V-11 area.

The valves are located at:

1. The southwest corner of the new cooling water tower.
2. East wall of the V-11 building.
3. Two are located at the northwest corner of the intersection of the entrance road and second street.

D. Fixed Point VCM Monitor

A fixed point VCM monitor is used to detect VCM and record the VCM concentration at various locations in the reactor and recovery building.

VII. Equipment Opening Procedures

VII. EQUIPMENT ENTRY PROCEDURE

EPA standards for VCM emissions and OSHA regulations on personnel exposure to VCM require that certain operating procedures be followed when there is the possibility of VCM emission to the atmosphere or personnel exposure to VCM. For this reason and to ensure safe working conditions at all times, the "Engineering and Work Practice Control Program for the Reduction of Employee Exposure to Vinyl Chloride" manual should be consulted whenever equipment in the reactor area is opened for any reason. This manual contains a list of detailed procedures as well as safety precautions for equipment opening.

VIII. Appendix

APPENDIX A

EQUIPMENT LIST

	Service
Reactors	
45-741	Polymerization Reactor
45-742	Polymerization Reactor
45-743	Polymerization Reactor
45-744	Polymerization Reactor
Heat Exchangers	
55-328	Reactor 45-741 Condenser
55-329	Reactor 45-742 Condenser
55-330	Reactor 45-743 Condenser
55-331	Reactor 45-744 Condenser
55-332	Hot Water Preheater
55-333	Hot Water Tank Heater
55-334	Water Recirculation Cooler
55-335	West Seal Water Cooler
55-336	East Seal Water Cooler
55-337	West Recovered VCM Condenser
55-338	East Recovered VCM Condenser
55-339	Cleaning Solution Heater
Eductors and Ejectors	
EE-701	Reactor 45-741 Jacket Eductor
EE-702	Reactor 45-742 Jacket Eductor
EE-703	Reactor 45-743 Jacket Eductor
EE-704	Reactor 45-744 Jacket Eductor
EE-705	Reactor Evacuation Ejector
Tanks and Vessels	
45-301	Instrument Air Capacity Tank
45-317	East Recovered VCM Storage Tank
89-520	West Recovered VCM Storage Tank
45-319	Blowdown Tank
45-745	Fresh VCM Storage Tank
45-748	Hot Water Tank
45-750	Initiator Injection Pot
45-751	Colloid Makeup Tank
45-752	Colloid Storage Tank
45-753	Colloid Charge Tank
45-754	Seal Oil Storage Drum
45-755	AMS Short Stop Charge Pot for Reactor 45-741
45-756	AMS Short Stop Charge Pot for Reactor 45-742
45-757	AMS Short Stop Charge Pot for Reactor 45-743
45-758	AMS Short Stop Charge Pot for Reactor 45-744

APPENDIX A

EQUIPMENT LIST - CONTINUED

	Service
Tanks and Vessels (Continued)	
45-759	Mechanical Seal Purge Water Surge Drum
45-760	South Recovery Knockout Drum
45-761	North Recovery Knockout Drum
45-762	South Seal Water Separator
45-763	North Seal Water Separator
45-764	Recovered VCM Collect Tank
45-765	Hydroquinone Storage Tank
45-766	Slurry Dump Tank
45-767	Cleaning Solution Tank
45-768	Reactor Evacuation Ejector Cyclone Separator
45-770	Reactor Sampling Bomb
Filters	
64-716	Process Water Charge Filter
64-718	North VCM Charge Filter
64-719	Recovered VCM Filter
64-720	Process Water Filter
64-721	Colloid Makeup Water Filter
64-722	North Colloid Transfer Filter
64-723	South Colloid Transfer Filter
64-724	Service Water Filter
64-725	Seal Oil Supply Filter for Seal Oil Pressure Unit 95-299
64-726	Seal Oil Supply Filter for Seal Oil Pressure Unit 95-300
64-727	Seal Oil Return Filter for Seal Oil Pressure Unit 95-299
64-728	Seal Oil Return Filter for Seal Oil Pressure Unit 95-300
64-731	South Seal Water Filter
64-732	North Seal Water Filter
64-733	Slurry Strainer
64-734	Cleaning Solution Strainer
64-735	Breathing Air Filter (Reactors, First Level)
64-736	Breathing Air Filter (Reactors, Second Level)
64-737	Breathing Air Filter (Recovery Building First Floor)
64-738	Breathing Air Filter (Recovery Building, Second Floor)
64-739	Breathing Air Filter (Charge Area)
64-740	Breathing Air Filter (Reactors, Third Level)
64-741	Blowdown Tank Drain Strainer
64-742	South VCM Charge Filter

APPENDIX A

EQUIPMENT LIST - CONTINUED

Pumps	Motor	Service
72-875	70-875	VCM Charge Pump
72-876	70-876	VCM Charge Pump
72-877	70-877	Recovered VCM Charge Pump
72-878	70-878	Recovered VCM Charge Pump
72-879	70-879	Hot Water Charge Pump
72-880	70-880	Hot Water Charge Pump
72-881	70-881	Colloid Batch Transfer Pump
72-882	70-882	Colloid Circulation Pump
72-883	70-883	Colloid Charge Pump
72-884	70-884	Colloid Charge Pump
72-885	70-885	High Pressure Service Water Pump
72-886	70-886	High Pressure Service Water Pump
72-887	70-887	Mechanical Seal Purge Water Pump
72-888	70-888	Mechanical Seal Purge Water Pump
72-889	70-889	Water Recirculation Pump
72-890	70-890	Water Recirculation Pump
72-891	70-891	Seal Water Pump
72-892	70-892	Seal Water Pump
72-893	70-893	Recovered VCM Transfer Pump
72-884	70-894	Recovered VCM Transfer Pump
72-895	70-895	Hydroquinone Injection Pump
72-896	70-896	Slurry Transfer Pump
72-897	70-897	Slurry Transfer Pump
72-898	70-898	Cleaning Solution Pump
72-899	70-899	Cleaning Solution Pump
72-900	70-900	Blowdown Tank Pump

Compressors and Fans	Motor	
72-901	70-901	Recovery Vacuum Pump
72-902	70-902	Recovery Vacuum Pump
72-903	70-903	Recovery Compressor
72-904	70-904	Recovery Compressor
72-905	70-905	Recovery Compressor
49-368	70-864	Slurry Strainer Exhauster

Agitators	Motor	
51-101	70-814	Reactor 45-741 Agitator
51-102	70-815	Reactor 45-742 Agitator
51-103	70-816	Reactor 45-743 Agitator
51-104	70-817	Reactor 45-744 Agitator
51-105	70-818	Colloid Makeup Tank Agitator
51-106	70-819	Hydroquinone Storage Tank Agitator

APPENDIX A

EQUIPMENT LIST - CONTINUED

Package Units	Service
95-299	Seal Oil Pressure Unit
95-300	Seal Oil Pressure Unit
PA-703	Deluge System
PA-704	Deluge System Combustible Hydrocarbon Analyzer
PA-705	Fire Monitor
PA-706	Fire Monitor
PA-707	Fire Monitor
PA-708	Fire Monitor
PA-709	Fire Monitor
PA-710	Fire Monitor
PA-711	Deleted
PA-712	Fixed Point VCM Monitor
PA-713	Emergency NO Short Stop Bottles
PA-714	Emergency NO Short Stop Bottles
PA-715	Emergency NO Short Stop Bottles
PA-716	Emergency NO Short Stop Bottles
PA-717	Programmable Logic Controller

APPENDIX B

INSTRUMENT LIST

Item No.	Service
Amperage Instruments	
AI-701	Reactor Agitator 51-101 Motor Amperage Indicator
AAHL-701	Reactor Agitator 51-101 Motor High or Low Amperage Alarm
AI-702	Reactor Agitator 51-102 Motor Amperage Indicator
AAHL-702	Reactor Agitator 51-102 Motor High or Low Amperage Alarm
AI-703	Reactor Agitator 51-103 Motor Amperage Indicator
AAHL-703	Reactor Agitator 51-103 Motor High or Low Amperage Alarm
AI-704	Reactor Agitator 51-104 Motor Amperage Indicator
AAHL-704	Reactor Agitator 51-104 Motor High or Low Amperage Alarm
AI-705	Recovery Vacuum Pump 72-901 Motor Amperage
AI-706	Recovery Vacuum Pump 72-902 Motor Amperage
AI-707	Recovery Compressor 72-903 Motor Amperage
AI-708	Recovery Compressor 72-904 Motor Amperage
AI-709	Recovery Compressor 72-905 Motor Amperage
Control Valves	
CV-701	Fresh VCM Storage Tank 45-745 Outlet Valve
CV-702	Deleted
CV-703	Recovered VCM Valve to VCM Charge Pumps 72-875 and 72-876
CV-704	VCM Charge Pump 72-875 Discharge Valve
CV-705	VCM Charge Pump 72-876 Discharge Valve
CV-706	Hot Water Tank 45-748 Outlet Valve
CV-707	Colloid Charge Pump 72-885 Discharge Valve
CV-708	Deleted
CV-709	Hot Water Valve to Colloid Makeup Tank 45-751
CV-710	Reactor 45-741 Main Charge Valve
CV-711	Reactor 45-741 Colloid Charge Valve
CV-712	Reactor 45-741 Steam Stripping Valve
CV-713	Reactor Condenser 55-328 Cleaning and Rinse Valve
CV-714	Reactor 45-741 Vent Valve
CV-715	Reactor 45-741 Inert Vent Valve
CV-716	Reactor 45-741 Recovery and Evacuation Valve
CV-717	Reactor 45-741 Cleaning and Rinse Valve
CV-718	Deleted
CV-719	Deleted
CV-720	Reactor 45-742 Main Charge Valve
CV-721	Reactor 45-742 Colloid Charge Valve
CV-722	Reactor 45-742 Steam Stripping Valve
CV-723	Reactor Condenser 55-329 Cleaning and Rinse Valve
CV-724	Reactor 45-742 Vent Valve
CV-725	Reactor 45-742 Inert Vent Valve
CV-726	Reactor 45-742 Recovery and Evacuation Valve
CV-727	Reactor 45-742 Cleaning and Rinse Valve
CV-728	Deleted

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Control Valves (Continued)	
CV-729	Deleted
CV-730	Reactor 45-743 Main Charge Valve
CV-731	Reactor 45-743 Colloid Charge Valve
CV-732	Reactor 45-743 Steam Stripping Valve
CV-733	Reactor Condenser 55-330 Cleaning and Rinse Valve
CV-734	Reactor 45-743 Vent Valve
CV-735	Reactor 45-743 Inert Vent Valve
CV-736	Reactor 45-743 Recovery and Evacuation Valve
CV-737	Reactor 45-743 Cleaning and Rinse Valve
CV-738	Deleted
CV-739	Deleted
CV-740	Reactor 45-744 Main Charge Valve
CV-741	Reactor 45-744 Colloid Charge Valve
CV-742	Reactor 45-744 Steam Stripping Valve
CV-743	Reactor Condenser 55-331 Cleaning and Rinse Valve
CV-744	Reactor 45-744 Vent Valve
CV-745	Reactor 45-744 Inert Vent Valve
CV-746	Reactor 45-744 Recovery and Evacuation Valve
CV-747	Reactor 45-744 Cleaning and Rinse Valve
CV-748	Deleted
CV-749	Deleted
CV-750	Reactor 45-741 Hot Water Rinse Supply Valve
CV-751	Reactor Condenser 45-741 Chem Wash Solution Supply Valve
CV-752	Reactor 45-741 Recovery Valve
CV-753	Reactor 45-741 Initiator Charge Valve
CV-754	Reactor 45-741 VCM Charge Valve
CV-755	Reactor 45-741 Water Charge Valve
CV-756	Deleted
CV-757	Reactor 45-741 Initiator Charge Line Sewer Valve
CV-758	Reactor 45-741 Slurry Dump Valve
CV-759	Reactor 45-741 Sewer Drain Valve
CV-760	Reactor 45-741 Chem Wash Solution Return Valve
CV-761	Deleted
CV-762	Reactor 45-741 Evacuation Valve
CV-763	Reactor 45-741 Initiator Charge Valve
CV-764	Reactor 45-742 Hot Water Rinse Supply Valve
CV-765	Reactor 45-742 Evacuation Valve
CV-766	Reactor 45-742 Chem Wash Solution Supply Valve
CV-767	Reactor 45-742 Recovery Valve
CV-768	Reactor 45-742 Initiator Charge Valve
CV-769	Reactor 45-742 VCM Charge Valve
CV-770	Reactor 45-742 Water Charge Valve
CV-771	Deleted
CV-772	Reactor 45-742 Slurry Dump Valve

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Control Valves (Continued)	
CV-773	Reactor 45-742 Chem Wash Solution Return Valve
CV-774	Reactor 45-742 Sewer Drain Vlave
CV-775	Deleted
CV-776	Reactor 45-742 Initiator Charge Valve
CV-777	Reactor 45-742 Initiator Charge Line Sewer Valve
CV-778	Reactor 45-743 Hot Water Rinse Supply Valve
CV-779	Reactor 45-743 Evacuation Valve
CV-780	Reactor 45-743 Chem Wash Solution Supply Valve
CV-781	Reactor 45-743 Recovery Valve
CV-782	Reactor 45-743 Initiator Charge Valve
CV-783	Reactor 45-743 VCM Charge Valve
CV-784	Reactor 45-743 Water Charge Valve
CV-785	Deleted
CV-786	Reactor 45-743 Slurry Dump Valve
CV-787	Reactor 45-743 Chem Wash Solution Return Valve
CV-788	Reactor 45-743 Sewer Drain Valve
CV-789	Deleted
CV-790	Reactor 45-743 Initiator Charge Valve
CV-791	Reactor 45-743 Initiator Charge Line Sewer Valve
CV-792	Reactor 45-744 Hot Water Rinse Supply Valve
CV-793	Reactor 45-744 Evacuation Valve
CV-794	Reactor 45-744 Chem Wash Solution Supply Valve
CV-795	Reactor 45-744 Initiator Charge Valve
CV-796	Reactor 45-744 VCM Charge Valve
CV-797	Reactor 45-744 Water Charge Valve
CV-798	Deleted
CV-799	Reactor 45-744 Slurry Dump Valve
CV-800	Reactor 45-744 Chem Wash Solution Return Valve
CV-801	Reactor 45-744 Sewer Drain Vlave
CV-802	Deleted
CV-803	Reactor 45-744 Initiator Charge Valve
CV-804	Reactor 45-744 Initiator Charge Line Sewer Valve
CV-805	Reactor 45-744 Recovery Valve
CV-806	Colloid Charge Pump 72-884 Discharge Valve
CV-807	Deleted
CV-808	Cold Water Addition Valve for Swirl
CV-809	Cold Water Addition Valve for Charge
CV-810	Recovery Vacuum Pump 72-901 Suction Valve
CV-811	Recovery Vacuum Pump 72-901 Discharge Valve
CV-812	Recovery Vacuum Pump 72-901 Seal Water Supply Valve
CV-813	Recovery Vacuum Pump 72-901 Mechanical Seal Water Supply Valve
CV-814	Reactor Jacket Eductor EE-701 Steam Valve

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Control Valves (Continued)	
CV-815	Reactor Jacket Eductor EE-702 Steam Valve
CV-816	Reactor Jacket Eductor EE-703 Steam Valve
CV-817	Reactor Jacket Eductor EE-704 Steam Valve
CV-818	Fresh VCM Storage Tank 45-745 Inlet Valve
CV-819	Hot Water Preheater 55-332 Water Inlet Valve
CV-820	Recovery Vacuum Pump 72-902 Suction Valve
CV-821	Recovery Vacuum Pump 72-902 Discharge Valve
CV-822	Recovery Vacuum Pump 72-902 Seal Water Supply Valve
CV-823	Recovery Vacuum Pump 72-902 Mechanical Seal Water Supply Valve
CV-824	Deleted
CV-825	Deleted
CV-826	Deleted
CV-827	Deleted
CV-828	Colloid Makeup Tank 45-751 Process Water Valve
CV-829	Hot Water Charge Pump 72-880 Discharge Valve
CV-830	Recovery Compressor 72-903 Suction Valve
CV-831	Recovery Compressor 72-903 Discharge Valve
CV-832	Recovery Compressor 72-903 Seal Water Supply Valve
CV-833	Recovery Compressor 72-903 Mechanical Seal Water Supply Valve
CV-834	Deleted
CV-835	Water Recirculation Cooler 55-334 Cooling Water Return Valve
CV-836	Recovery Knockout Drum 45-760 Water Recirculation Inlet Valve
CV-837	Recovery Knockout Drum 45-760 Water Blowdown Valve
CV-838	Recovery Knockout Drum 45-761 Water Recirculation Inlet Valve
CV-839	Recovery Knockout Drum 45-761 Water Blowdown Valve
CV-840	Recovery Compressor 72-904 Suction Valve
CV-841	Recovery Compressor 72-904 Discharge Valve
CV-842	Recovery Compressor 72-904 Seal Water Supply Valve
CV-843	Recovery Compressor 72-904 Mechanical Seal Water Supply Valve
CV-844	Recovered VCM Condensers 55-337 and 55-338 Cooling Water Return Valve
CV-845	Deleted
CV-846	Deleted
CV-847	Reactor Evacuation Ejector EE-706 First Stage Steam Valve
CV-848	Reactor Evacuation Ejector EE-706 Second Stage Steam Valve
CV-849	Hot Water Charge Pump 72-879 Discharge Valve
CV-850	Recovery Compressor 72-905 Suction Valve
CV-851	Recovery Compressor 72-905 Discharge Valve

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Control Valves (Continued)	
CV-852	Recovery Compressor 72-905 Seal Water Supply Valve
CV-853	Recovery Compressor 72-905 Mechanical Seal Water Supply Valve
CV-854	Recovery Vacuum Pumps 72-901 and 72-902 Bypass Valve
CV-855	Recovery Compressors 72-903, 72-904, and 72-905 Bypass Valve
CV-856	Colloid Makeup Tank 45-751 Water Inlet Valve
CV-857	Colloid Makeup Tank 45-751 Colloid Outlet Valve
CV-858	Colloid Recirculation Valve to Colloid Storage Tank 45-752
CV-859	Colloid Circulation Pump 72-882 Inlet Valve
CV-860	Deleted
CV-861	Colloid Charge Tank 45-753 Inlet Valve
CV-862	Deleted
CV-863	Dump System Water Rinse Valve
CV-864	Slurry Transfer Pump 72-896 Mechanical Seal Water Valve
CV-865	Deleted
CV-866	Slurry Transfer Pump 72-897 Mechanical Seal Water Valve
CV-867	Deleted
CV-868	Deleted
CV-869	Deleted
CV-870	Deleted
CV-871	Cleaning Solution Heater 55-339 Inlet Valve
CV-872	Cleaning Solution Storage Tank 45-767 Top Inlet Valve
CV-873	Cleaning Solution Pumps 72-898 and 72-899 Suction Valve
CV-874	Reactor Cleaning Solution Return Valve to Cleaning Solution Tank 45-767
CV-875	Seal Oil Pressure Unit 95-300 Seal Oil Return Valve
CV-876	Seal Oil Pressure Unit 95-299 Seal Oil Return Valve
CV-877	Seal Oil Pressure Unit 95-300 Seal Oil Supply Valve
CV-878	Seal Oil Pressure Unit 95-299 Seal Oil Supply Valve
CV-879	Initiator Injection Pot 45-750 Service Water Inlet Valve
CV-880	Blowdown Tank Pump 72-900 Discharge Valve
CV-881	45-741 Emergency NO Short Stop Three-Way Valve
CV-882	45-742 Emergency NO Short Stop Three-Way Valve
CV-883	45-743 Emergency NO Short Stop Three-Way Valve
CV-884	45-744 Emergency NO Short Stop Three-Way Valve
CV-885	45-741 Emergency NO Short Stop Valve
CV-886	45-742 Emergency NO Short Stop Valve
CV-887	45-743 Emergency NO Short Stop Valve
CV-888	45-744 Emergency NO Short Stop Valve
CV-889	Recovery Seal Water and VCM Diverter Valve
CV-890	Recovery Seal Water and VCM Diverter Valve

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Control Valves (Continued)	
CV-891	Steam Valve for Blowdown Tank 45-319 Pressure Regulation
CV-892	Water Drain Valve from Recovered VCM Storage Tank 89-520 to the Blowdown Tank 45-319
CV-893	Water Drain Valve from Recovered VCM Storage Tank 45-317 to the Blowdown Tank 45-319
CV-894	VCM Recovery Valve for Blowdown Tank 45-319
CV-895	VCM Recovery Valve for VCM Storage Tank 45-745, 89-520, and 45-317
CV-896	Instrument Air Supply Valve to Reactors 45-741, 45-742, 45-743, and 45-744
CV-897	Hot Water Rinse Header Valve to Reactors 45-741, 45-742, 45-743, and 45-744
Flow Instruments	
FQIC-701A and B	VCM Charge Totalizers
FSL-701A and B	VCM Charge Low Flow Switches
FAL-701	VCM Charge Low Flow Alarm
FQIC-702	Recovered VCM Charge Totalizer
FQIC-703	Initiator Injection Pot 45-750 Service Water Flow Totalizer
FQIC-704	Hot Water Charge Totalizer
FQIC-705	Colloid Charge Totalizer
FQIC-706	Colloid Makeup Tank 45-751 Makeup Water Flow Totalizer
FI-707	Deleted
FR-708	Reactor Steam Stripping Flow Recorder
FQI-708	Reactors Steam Stripping Flow Totalizer
FCi-709	Deleted
FIRC-710	Reactor 45-741 Cooling Water Flow Controller
FIRC-711	Reactor 45-742 Cooling Water Flow Controller
FIRC-712	Reactor 45-743 Cooling Water Flow Controller
FIRC-713	Reactor 45-744 Cooling Water Flow Controller
FI-714	Reactor Agitator 51-101 Inboard Seal Water Flush Rotameter
FAL-714	Reactor Agitator 51-101 Seal Water Low Flow Alarm
FI-715	Reactor Agitator 51-102 Inboard Seal Water Flush Rotameter
FAL-715	Reactor Agitator 51-102 Seal Water Low Flow Alarm
FI-716	Reactor Agitator 51-103 Inboard Seal Water Flush Rotameter
FAL-716	Reactor Agitator 51-103 Seal Water Low Flow Alarm
FI-717	Reactor Agitator 51-104 Inboard Seal Water Flush Rotameter
FAL-717	Reactor Agitator 51-104 Seal Water Low Flow Alarm
FI-718	Reactor 45-741 Spray Nozzle Flush Rotameter

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Flow Instruments (Continued)	
FI-719	Reactor 45-742 Spray Nozzle Flush Rotameter
FI-720	Reactor 45-743 Spray Nozzle Flush Rotameter
FI-721	Reactor 45-744 Spray Nozzle Flush Rotameter
FI-722	Deleted
FI-723	Deleted
FI-724	Deleted
FI-725	Deleted
FI-726	Recovery Knockout Drum Level Controller LC-716 Water Flush Rotameter
FI-727	Recovery Knockout Drum Level Controller LC-718 Water Flush Rotameter
FI-728	Recovery Vacuum Pump 72-901 Double Mechanical Seal Water Rotameter
FI-729	Recovery Vacuum Pump 72-901 Inboard Flush Water Rotameter
FI-730	Recovery Vacuum Pump 72-902 Double Mechanical Seal Water Rotameter
FI-731	Recovery Vacuum Pump 72-902 Inboard Flush Water Rotameter
FI-732	Rocovery Comprassor 72-903 Double Mechanical Seal Water Rotameter
FI-733	Deleted
FI-734	Recovery Compressor 72-904 Double Mechanical Seal Water Rotameter
FI-735	Deleted
FI-736	Recovery Compressor 72-905 Double Mechanical Seal Water Rotameter
FI-737	Deleted
FIC-738	Recovery Vacuum Pump 72-901 and Recovery Compressor 72-903 Seal Water Flow Controller
FIC-739	Recovery Vacuum Pump 72-902 and Recovery Compressor 72-904 Seal Water Flow Controller
FIC-740	Recovery Compressor 72-905 Seal Water Flow Controller
FI-741	Seal Water Separator Level Controller LC-720 Flush Water Rotameter
FI-742	Seal Water Separator Level Controller LC-722 Flush Water Rotameter
FIC-743	Deleted
FI-744	Recovered VCM to Recovery Knockout Drum 45-760 Bullseye
FI-745	Deleted
FI-746	Deleted
FI-747	Slurry Dump to Slurry Strainer FD-717 Bullseye
FI-748	Deleted
FCi-749	Reactor Agitator 51-101 Mechanical Seal Oil Supply Flow Regulator

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Flow Instruments (Continued)	
FCi-750	Reactor Agitator 51-102 Mechanical Seal Oil Supply Flow Regulator
FCi-751	Reactor Agitator 51-103 Mechanical Seal Oil Supply Flow Regulator
FCi-752	Reactor Agitator 51-104 Mechanical Seal Oil Supply Flow Regulator
FI-753	Reactor Agitator 51-101 Mechanical Seal Oil Supply Rotameter
FI-754	Reactor Agitator 51-102 Mechanical Seal Oil Supply Rotameter
FI-755	Reactor Agitator 51-103 Mechanical Seal Oil Supply Rotameter
FI-756	Reactor Agitator 51-104 Mechanical Seal Oil Supply Rotameter
FQI-757	Hot Water Charge Totalizer
RO-758	Colloid Makeup Water Supply Restriction Orifice
OF-759	Reactor 45-741 Cooling Water System Orifice Flanges
OF-760	Reactor 45-742 Cooling Water System Orifice Flanges
OF-761	Reactor 45-743 Cooling Water System Orifice Flanges
OF-762	Reactor 45-744 Cooling Water System Orifice Flanges
FI-763	Slurry Transfer Pump 72-896 Inboard Seal Flush Water Rotameter
FI-764	Slurry Transfer Pump 72-897 Inboard Seal Flush Water Rotameter
FI-765	Deleted
FI-766	Deleted
FI-767	VCM Charge Pump 72-875 Double Mechanical Seal Water Rotameter
FI-768	VCM Charge Pump 72-876 Double Mechanical Seal Water Rotameter
FI-769	Recovered VCM Charge Pump 72-877 Double Mechanical Seal Rotameter
FI-770	Recovered VCM Charge Pump 72-878 Double Mechanical Seal Rotameter
RO-771	VCM Charge Pump 72-875 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-772	VCM Charge Pump 72-876 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-773	Recovered VCM Charge Pump 72-877 Mechanical Seal Water Back Pressure Restriction Orifice
RO-774	Recovered VCM Charge Pump 72-878 Mechanical Seal Water Back Pressure Restriction Orifice

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Flow Instruments (Continued)	
FI-775	Water Recirculation Pump 72-889 Inboard Seal Flush Water Rotameter
FI-776	Deleted
FI-777	Water Recirculation Pump 72-890 Inboard Seal Flush Water Rotameter
FI-778	Seal Water Pump 72-891 Inboard Seal Flush Water Rotameter
FI-779	Seal Water Pump 72-892 Inboard Seal Flush Water Rotameter
RO-780	Recovery Vacuum Pump 72-901 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-781	Recovery Vacuum Pump 72-902 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-782	Recovery Compressor 72-903 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-783	Recovery Compressor 72-904 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-784	Recovery Compressor 72-905 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-785	Recovered VCM Transfer Pump 72-893 Mechanical Seal Water Back Pressure Restriction Orifice
RO-786	Recovered VCM Transfer Pump 72-894 Mechanical Seal Water Back Pressure Restriction Orifice
FI-787	Recovered VCM Transfer Pump 72-893 Mechanical Seal Water Rotameter
FI-788	Recovered VCM Transfer Pump 72-894 Mechanical Seal Water Rotameter
FI-789	Recovery Vacuum Pump 72-901 Inboard Flush Water Rotameter
FI-790	Recovery Vacuum Pump 72-901 Double Mechanical Seal Water Rotameter
FI-791	Recovery Vacuum Pump 72-902 Inboard Flush Water Rotameter
FI-792	Recovery Vacuum Pump 72-902 Double Mechanical Seal Water Rotameter
FI-793	Deleted
FI-794	Recovery Compressor 72-903 Double Mechanical Seal Water Rotameter
FI-795	Deleted
FI-796	Recovery Compressor 72-904 Double Mechanical Seal Water Rotameter
FI-797	Deleted
FI-798	Recovery Compressor 72-905 Double Mechanical Seal Water Rotameter

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Flow Instruments (Continued)	
RO-799	Recovery Vacuum Pump 72-901 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-800	Recovery Vacuum Pump 72-902 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-801	Recovery Compressor 72-903 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-802	Recovery Compressor 72-904 Double Mechanical Seal Water Back Pressure Restriction Orifice
RO-803	Recovery Compressor 72-905 Double Mechanical Seal Water Back Pressure Restriction Orifice
FI-804	AMS Short Stop Charge Pot 45-755 Water Flush Rotameter
FI-805	AMS Short Stop Charge Pot 45-756 Water Flush Rotameter
FI-806	AMS Short Stop Charge Pot 45-757 Water Flush Rotameter
FI-807	AMS Short Stop Charge Pot 45-758 Water Flush Rotameter
FI-808	Blowdown Tank 45-319 Level Cage Water Flush Rotameter
FI-809	Recovered VCM Sampling System Bullseye
FI-810	Recovered VCM Sampling System Bullseye
FQI-811	Steam to Reactor Module Flow Totalizer
RO-812	Deleted
RO-813	Deleted
FI-814	Blowdown Tank Pump 72-900 Double Mechanical Seal Water Rotameter
FI-815	Blowdown Tank Pump 72-900 Inboard Seal Water Flush Rotameter
RO-816	Blowdown Tank Pump 72-900 Double Mechanical Seal Water Back Pressure Restriction Orifice
Level Gauges	
LG-701A, B, C, and D	Fresh VCM Storage Tank 45-745 Level Gauge
LG-702A, B, C and D	Recovered VCM Storage Tank 89-520 Level Gauge
LG-703A, B, C and D	Recovered VCM Storage Tank 45-317 Level Gauge
LG-704A, B, C and D	Hot Water Tank 45-748 Level Gauge
LG-705	Deleted
LG-706A, B, and C	Colloid Storage Tank 45-752 Level Gauge
LG-707A, B and C	Colloid Charge Tank 45-753 Level Gauge
LG-708	Recovery Knockout Drum 45-760 Level Gauge
LG-709	Recovery Knockout Drum 45-761 Level Gauge
LG-710	Hydroquinone Storage Tank 45-765 Level Gauge

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Level Gauges (Continued)	
LG-711	Seal Water Separator 45-762 Level Gauge
LG-712	Seal Water Separator 45-763 Level Gauge
LG-713	Recovered VCM Collect Tank 45-764 Level Gauge
LG-714	Seal Oil Storage Drum 45-754 Level Gauge
LG-715	Deleted
LG-716	Blowdown Tank 45-319 Level Gauge
LG-717	Mechanical Seal Purge Water Surge Drum 45-759 Level Gauge
Level Instruments	
LI-701	Fresh VCM Storage Tank 45-745 Level Indicator
LAH-701	Fresh VCM Storage Tank 45-745 High Level Alarm
LS-701A, B, C and D	Fresh VCM Storage Tank 45-745 Level Switches
LA-702	Deleted
LA-703	Deleted
LI-704	Recovered VCM Storage Tank 89-520 Level Indicator
LA-705	Deleted
LA-706	Deleted
LI-707	Recovered VCM Storage Tank 45-317 Level Indicator
LA-708	Deleted
LA-709	Deleted
LAH-710	Colloid Makeup Tank 45-751 High Level Alarm
LI-711	Hot Water Tank 45-748 Level Indicator
LS-711A	Deleted
LA-711B, C, and D	Hot Water Tank 45-748 Level Switches
LA-712	Deleted
LAH-713	Colloid Storage Tank 45-752 High Level Alarm
LAH-714	Colloid Charge Tank 45-753 High Level Alarm
LSL-715	Colloid Charge Tank 45-753 Low Level Switch
LSH-716	Recovery Knockout Drum 45-760 High Level Switch
LSL-717	Recovery Knockout Drum 45-760 Low Level Switch
LSH-718	Recovery Knockout Drum 45-761 High Level Switch
LSL-719	Recovery Knockout Drum 45-761 Low Level Switch
LC-720	Seal Water Separator 45-762 Level Controller
LAH-720	Seal Water Separator 45-762 High Level Alarm
LAL-720	Seal Water Separator 45-762 Low Level Alarm
LA-721	Deleted
LC-722	Seal Water Separator 45-763 Level Controller
LAH-722	Seal Water Separator 45-763 High Level Alarm
LAL-722	Seal Water Separator 45-763 Low Level Alarm
LA-723	Deleted
LC-724	Recovered VCM Collect Tank 45-764 Level Controller
LIC-725	Slurry Dump Tank 45-766 Level Controller
LAH-725	Slurry Dump Tank 45-766 High Level Alarm

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Level Instruments (Continued)	
LIC-726	Deleted
LA-726	Deleted
LAH-727	Cleaning Solution Tank 45-767 High Level Alarm
LI-728	Cleaning Solution Tank 45-767 Level Indicator
LAL-729	Cleaning Solution Tank 45-767 Low Level Alarm
LSL-730	Seal Oil Pressure Unit 95-299 Reservoir Low Level Switch
LAL-730	Seal Oil Pressure Unit 95-299 Reservoir Low Level Alarm
LSL-731	Seal Oil Pressure Unit 95-300 Reservoir Low Level Switch
LAL-731	Seal Oil Pressure Unit 95-300 Reservoir Low Level Alarm
LC-732	Deleted
LAL-733	Hydroquinone Storage Tank 45-765 Low Level Alarm
LSH-734	Cleaning Solution Tank 45-767 High Level Switch
LA-735	Deleted
LA-736	Deleted
LA-737	Deleted
LA-738	Deleted
LAL-739	Colloid Makeup Tank 45-751 Low Level Alarm
LAH-740	Blowdown Tank 45-319 High Level Alarm
LSL-741	Blowdown Tank 45-319 Low Level Switch
Pressure Gauges	
PG-701	VCM Charge Pump 72-875 Discharge Pressure Gauge
PG-702	VCM Charge Pump 72-876 Discharge Pressure Gauge
PG-703	Recovered VCM Charge Pump 72-877 Discharge Pressure Gauge
PG-704	Recovered VCM Charge Pump 72-878 Discharge Pressure Gauge
PG-705	Fresh VCM Storage Tank 45-745 Pressure Gauge
PG-706	Recovered VCM Storage Tank 89-520 Pressure Gauge
PG-707	Recovered VCM Storage Tank 45-317 Pressure Gauge
PG-708	Deleted
PG-709	Deleted
PG-710	Deleted
PG-711	Deleted
PG-712	Process Water Filter 64-720 Inlet Pressure Gauge
PG-713	Process Water Filter 64-720 Outlet Pressure Gauge
PG-714	Hot Water Charge Pump 72-879 Discharge Pressure Gauge
PA-715	Hot Water Charge Pump 72-880 Discharge Pressure Gauge
PG-716	Deleted
PG-717	Deleted
PG-718	Deleted

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Pressure Gauges (Continued)	
PG-719	Colloid Makeup Water Filter 64-721 Inlet Pressure Gauge
PG-720	Colloid Makeup Water Filter 64-721 Outlet Pressure Gauge
PG-721	Colloid Batch Transfer Pump 72-881 Discharge Pressure Gauge
PG-722	Colloid Transfer Filter 64-722 Outlet Pressure Gauge
PG-723	Colloid Circulation Pump 72-882 Discharge Pressure Gauge
PG-724	Colloid Transfer Filter 64-723 Outlet Pressure Gauge
PG-725	Colloid Charge Pump 72-883 Discharge Pressure Gauge
PG-726	Colloid Charge Pump 72-884 Discharge Pressure Gauge
PG-727	Steam Stripping Header Pressure Gauge
PG-728	Reactor 45-741 Steam Stripping Line Pressure Gauge
PG-729	Deleted
PG-730	Reactor Condenser 55-328 Pressure Gauge
PG-731	Reactor Agitator 51-101 Seal Oil Return Pressure Gauge
PG-732	Reactor 45-742 Steam Stripping Line Pressure Gauge
PG-733	Reactor Condenser 55-329 Pressure Gauge
PG-734	Deleted
PG-735	Reactor Agitator 51-102 Seal Oil Return Pressure Gauge
PG-736	Reactor 45-743 Steam Stripping Line Pressure Gauge
PG-737	Reactor Condenser 55-330 Pressure Gauge
PG-738	Deleted
PG-739	Reactor Agitator 51-103 Seal Oil Return Pressure Gauge
PG-740	Reactor 45-744 Steam Stripping Line Pressure Gauge
PG-741	Reactor Condenser 55-331 Pressure Gauge
PG-742	Deleted
PG-743	Reactor Agitator 51-104 Seal Oil Return Pressure Gauge
PG-744	Recovery Knockout Drum 45-760 Pressure Gauge
PG-745	Water Recirculation Pump 72-889 Discharge Pressure Gauge
PG-746	Deleted
PG-747	Recovered VCM Bleed Back Line Pressure Gauge
PG-748	Recovery Knockout Drum 45-761 Pressure Gauge
PG-749	Water Recirculation Pump 72-890 Discharge Pressure Gauge
PG-750	Deleted
PG-751	Recovery Vacuum Pump 72-901 Inlet Pressure Gauge
PG-752	Recovery Compressors 72-904 or 72-905 Suction Pressure Gauge
PG-753	Recovery Compressors 72-903, 72-904, and 72-905 Discharge Pressure Gauge
PG-754	Seal Water Separator 45-762 Pressure Gauge
PG-755	Seal Water Separator 45-763 Pressure Gauge
PG-756	Seal Water Pump 72-891 Discharge Pressure Gauge
PG-757	Seal Water Filter 64-731 Outlet Pressure Gauge
PG-758	Seal Water Pump 72-892 Discharge Pressure Gauge
PG-759	Seal Water Filter 64-732 Outlet Pressure Gauge

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Pressure Gauges (Continued)	
PG-760	Recovered VCM Collect Tank 45-764 Pressure Gauge
PG-761	Recovered VCM Transfer Pumps 72-893 and 72-894 Discharge Pressure Gauge
PG-762	Recovery Knockout Drum 45-760 VCM Inlet Line Pressure Gauge
PG-763	Hydroquinone Storage Tank 45-765 Pressure Gauge
PG-764	Hydroquinone Injection Pump 72-895 Discharge Pressure Gauge
PG-765	Slurry Transfer Pump 72-896 Discharge Pressure Gauge
PG-766	Deleted
PG-767	Slurry Transfer Pump 72-897 Discharge Pressure Gauge
PG-768	Deleted
PG-769	Caustic Solution Pump 72-898 Discharge Pressure Gauge
PG-770	Caustic Solution Pump 72-899 Discharge Pressure Gauge
PG-771	Cleaning Solution Heater 55-339 Outlet Pressure Gauge
PG-772	Service Water Filter 64-724 Inlet Pressure Gauge
PG-773	Service Water Filter 64-724 Outlet Pressure Gauge
PG-774	Service Water Pumps 72-885 and 72-886 Discharge Pressure Gauge
PG-775	Mechanical Seal Purge Water Pumps 72-887 and 72-888 Discharge Pressure Gauge
PG-776	AMS Short Stop Charge Pot 45-755 Outlet Pressure Gauge
PG-777	AMS Short Stop Charge Pot 45-756 Outlet Pressure Gauge
PG-778	AMS Short Stop Charge Pot 45-757 Outlet Pressure Gauge
PG-779	AMS Short Stop Charge Pot 45-758 Outlet Pressure Gauge
PG-780	Deleted
PG-781	Blowdown Tank Pump 72-900 Discharge Pressure Gauge
PG-782	Blowdown Tank 45-319 Pressure Gauge
PG-783	Seal Oil Return Header Pressure Gauge
PG-784	Seal Oil Pressure Unit 95-299 Pressure Gauge
PG-785	Seal Oil Pressure Unit 95-300 Pressure Gauge
PG-786	Seal Oil Supply Header Pressure Gauge
PG-787	Deleted
PG-788	Deleted
PG-789	Deleted
PG-790	Deleted
PG-791	Reactor Ejector Cyclone Separator 45-768 Outlet Pressure Gauge
PG-792	Breathing Air Header Pressure Gauge
PG-793	Recovery Vacuum Pump 72-902 Suction Pressure Gauge
PG-794	Deleted
PG-795	Initiator Injection Pot 45-750 Pressure Gauge
PG-796	Seal Oil Return Filter 64-727 Outlet Pressure Gauge
PG-797	Seal Oil Return Filter 64-728 Outlet Pressure Gauge

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Pressure Gauges (Continued)	
PG-798	Emergency NO Short Stop Bottle PA-713 Pressure Gauge
PG-799	Emergency NO Short Stop Bottle PA-714 Pressure Gauge
PG-800	Emergency NO Short Stop Bottle PA-715 Pressure Gauge
PG-801	Emergency NO Short Stop Bottle PA-716 Pressure Gauge
PG-802	VCM Charge Filter 64-718 and 64-742 Discharge Pressure Gauge
PG-803	Recovered VCM Charge Filter 64-719 Discharge Pressure Gauge
PG-804	Reactor 45-741 Resin Sampling System Pressure Gauge
PG-805	Reactor 45-742 Resin Sampling System Pressure Gauge
PG-806	Reactor 45-743 Resin Sampling System Pressure Gauge
PG-807	Reactor 45-744 Resin Sampling System Pressure Gauge
PG-808	Instrument Air Capacity Tank 45-301 Pressure Gauge
PG-809	Mechanical Seal Purge Water Surge Drum 45-759 Pressure Gauge
PG-810	High Pressure Service Water Header Pressure Gauge (Downstream of PCi-817)
PG-811	Mechanical Seal Purge Water Header Pressure Gauge (Downstream of PCi-818)
Pressure Instruments	
PA-701	Deleted
PCi-702	Deleted
PSH-703	Initiator Injection Pot 45-750 High Pressure Switch
PCi-704	Recovered VCM Storage Tanks 89-520 and 45-317 Inert Vent Back Pressure Regulator
PI-705	Reactor Evacuation Header Pressure Indicator
PCi-706	Steam Stripping Header Steam Supply Back Pressure Regulator
PSL-707	Steam Stripping Header Low Pressure Switch
PCi-708	Deleted
PCi-709	Deleted
PCi-710	Deleted
PCi-711	Deleted
PSL-712	Reactor 45-741 Pressure Switch (Prevents dump before recovery)
PSL-713	Reactor 45-742 Pressure Switch (Prevents dump before recovery)
PSL-714	Reactor 45-743 Pressure Switch (Prevents dump before recovery)
PSL-715	Reactor 45-744 Pressure Switch (Prevents dump before recovery)
PSL-716	Reactor 45-741 Pressure Switch (Prevents charge before evacuation)
PSL-717	Reactor 45-742 Pressure Switch (Prevents charge before evacuation)

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Pressure Instruments (Continued)	
PSL-718	Reactor 45-743 Pressure Switch (Prevents charge before evacuation)
PSL-719	Reactor 45-744 Pressure Switch (Prevents charge before evacuation)
PR-720	Reactor 45-741 Pressure Recorder
PAH-720	Reactor 45-741 High Pressure Alarm
PR-721	Reactor 45-742 Pressure Recorder
PAH-721	Reactor 45-742 High Pressure Alarm
PR-722	Reactor 45-743 Pressure Recorder
PAH-722	Reactor 45-743 High Pressure Alarm
PR-723	Reactor 45-744 Pressure Recorder
PAH-723	Reactor 45-744 High Pressure Alarm
PI-724	Reactor Recovery Pressure Indicator
PIC-725	Recovery Knockout Drum 45-760 Inlet Pressure Controller
PIC-726	VCM Bleed Stream to Recovery System Pressure Controller
PSL-727	Recovery Compressors 72-903, 72-904, and 72-905 Suction Low Pressure Switch
PDS-728	Recovery Vacuum Pumps 72-901 and 72-902 Suction and Recovery Compressors 72-903, 72-904, and 72-905 Discharge Differential Pressure Switch
PCi-729	Hydroquinone Storage Tank 45-765 Nitrogen Pressure Regulator
PCi-730	Deleted
PCi-731	Mechanical Seal Purge Water Surge Drum 45-759 Nitrogen Supply Pressure Regulator
PSL-732	High Pressure Service Water System Low Pressure Switch
PAL-732	High Pressure Service Water System Low Pressure Alarm
PCi-733	Deleted
PCi-734	Deleted
PCi-735	Deleted
PSL-737A and B	Mechanical Seal Water System Low Pressure Switches
PAL-737	Mechanical Seal Water System Low Pressure Alarm
PSL-738	Seal Oil Pressure Unit 95-299 Discharge Low Pressure Switch
PAL-738	Seal Oil Pressure Unit 95-299 Discharge Low Pressure Alarm
PCi-739	Seal Oil Pressure Unit 95-299 Nitrogen Supply Pressure Regulator
PSL-740	Seal Oil Pressure Unit 95-300 Discharge Low Pressure Switch
PAL-740	Seal Oil Pressure Unit 95-300 Discharge Low Pressure Alarm
PCi-741	Seal Oil Pressure Unit 95-300 Nitrogen Supply Pressure Regulator
PA-742	Deleted

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Pressure Instruments (Continued)	
PCi-743	Breathing Air Station Supply Pressure Regulator (Reactors, Ground Level)
PCi-744	Breathing Air Station Supply Pressure Regulator (Reactors, Second Level)
PCi-745	Breathing Air Station Supply Pressure Regulator (Recovery Building, First Floor)
PCi-746	Breathing Air Station Supply Pressure Regulator (Recovery Building, Second Floor)
PCi-747	Breathing Air Station Supply Pressure Regulator (Charge Area)
PCi-748	Deleted
PCi-749	Deleted
PAH-750	Initiator Injection Pot 45-750 High Pressure Alarm
PAH-751	Seal Oil Supply High Pressure Alarm
PCi-752	Breathing Air Station Supply (Reactors, Third Level)
PAL-753	Emergency NO Short Stop Bottles Low Pressure Alarm
PCi-754	PA-713 NO Supply Pressure Regulator to Reactor 45-741
PCi-755	PA-714 NO Supply Pressure Regulator to Reactor 45-742
PCi-756	PA-715 NO Supply Pressure Regulator to Reactor 45-743
PCi-757	PA-716 NO Supply Pressure Regulator to Reactor 45-744
PSL-758	High Pressure Service Water Low Pressure Switch
PIC-759	Blowdown Tank 45-319 Pressure Controller
PAH-760	Blowdown Tank 45-319 High Pressure Alarm
PI-760	Blowdown Tank 45-319 Pressure Indicator
PS-761	Deleted
PSL-762	Blowdown Tank 45-319 Stripping Steam Low Pressure Switch
PAL-763	Reactor Area Instrument Air Low Pressure Alarm
Rupture Discs	
RD-701	Reactor 45-741 Rupture Disc
RD-702	Reactor 45-742 Rupture Disc
RD-703	Reactor 45-743 Rupture Disc
RD-704	Reactor 45-744 Rupture Disc
RD-705	Reactor Condenser 55-328 Rupture Disc
RD-706	Reactor Condenser 55-329 Rupture Disc
RD-707	Reactor Condenser 55-330 Rupture Disc
RD-708	Reactor Condenser 55-331 Rupture Disc
RD-709	Reactor 45-741 First of Double Rupture Discs
RD-710	Reactor 45-742 First of Double Rupture Discs
RD-711	Reactor 45-743 First of Double Rupture Discs
RD-712	Reactor 45-744 First of Double Rupture Discs
RD-713	Reactor 45-741 Second of Double Rupture Discs
RD-714	Reactor 45-742 Second of Double Rupture Discs

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Rupture Discs (Continued)	
RD-715	Reactor 45-743 Second of Double Rupture Discs
RD-716	Reactor 45-744 Second of Double Rupture Discs
RD-717	Fresh VCM Storage Tank 45-745 Rupture Disc
RD-718	Recovered VCM Storage Tank 89-520 Rupture Disc
RD-719	Recovered VCM Storage Tank 45-317 Rupture Disc
RD-720	Deleted
RD-721	Deleted
RD-722	Deleted
RD-723	Deleted
RD-724	Deleted
RD-725	Deleted
RD-726	Recovery Knockout Drum 45-760 Rupture Disc
RD-727	Recovery Knockout Drum 45-761 Rupture Disc
RD-728	Initiator Injection Pot 45-750 Rupture Disc
RD-729	Deleted
RD-730	Deleted
RD-731	Recovery Vacuum Pump 72-901 Inlet Rupture Disc
RD-732	Recovery Vacuum Pump 72-902 Inlet Rupture Disc
RD-733	Deleted
RD-734	Deleted
RD-735	Seal Water Separator 45-762 Rupture Disc
RD-736	Seal Water Separator 45-763 Rupture Disc
RD-737	Deleted
RD-738	Deleted
RD-739	Recovered VCM Condenser 55-337 VCM Outlet Rupture Disc
RD-740	Recovered VCM Condenser 55-338 VCM Outlet Rupture Disc
RD-741	Recovered VCM Collect Tank 45-764 Rupture Disc
RD-742	Deleted
RD-743	Deleted
RD-744	Blowdown Tank 45-319 Rupture Disc
RD-745 to RD-759	Deleted
RD-760	Recovered VCM Collect Tank 45-764 Inlet Line Rupture Disc
RD-761	Deleted
RD-762	Deleted
RD-763	Deleted
RD-764	Deleted
RD-765	Slurry Dump Line Rupture Disc
RD-766	Cleaning Solution Strainer 64-734 Inlet Piping Rupture Disc
RD-767	Deleted
Safety-Relief Valves	
SV-701	Reactor 45-741 Relief Valve
SV-702	Reactor 45-742 Relief Valve
SV-703	Reactor 45-743 Relief Valve

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Safety-Relief Valves (Continued)	
SV-704	Reactor 45-744 Relief Valve
SV-705	Reactor Condenser 55-328 Relief Valve
SV-706	Reactor Condenser 55-329 Relief Valve
SV-707	Reactor Condenser 55-330 Relief Valve
SV-708	Reactor Condenser 55-331 Relief Valve
SV-709	Reactor 45-741 Jacket Relief Valve
SV-710	Reactor 45-742 Jacket Relief Valve
SV-711	Reactor 45-743 Jacket Relief Valve
SV-712	Reactor 45-744 Jacket Relief Valve
SV-713	Hot Water Preheater 55-332 Relief Valve
SV-714	Deleted
SV-715	Deleted
SV-716	Deleted
SV-717	Fresh VCM Storage Tank 45-745 Relief Valve
SV-718	Recovered VCM Storage Tank 89-520 Relief Valve
SV-719	Recovered VCM Storage Tank 45-317 Relief Valve
SV-720	VCM Charge Pumps 72-875 and 72-876 Suction Piping Relief Valve
SV-721	Recovered VCM Charge Pumps 72-877 and 72-878 Suction Piping Relief Valve
SV-722	Recovered VCM Charge Filter 64-719 Relief Valve
SV-723	Recovered VCM Charge Pumps 72-877 and 72-878 Discharge Piping Relief Valve
SV-724	VCM Charge Filter 64-718 Relief Valve
SV-725	VCM Charge Line Relief Valve (Down Stream of VCM Charge Totalizers FQIC-701A and B)
SV-726	Recovery Knockout Drum 45-760 Relief Valve
SV-727	Recovery Knockout Drum 45-761 Relief Valve
SV-728	Deleted
SV-729	Water Recirculation Cooler 55-334 Relief Valve
SV-730	Deleted
SV-731	Recovery Vacuum Pump 72-901 Inlet Relief Valve
SV-732	Recovery Vacuum Pump 72-902 Inlet Relief Valve
SV-733	Hydroquinone Storage Tank 45-765 Relief Valve
SV-734	Hydroquinone Injection Pump 72-895 Discharge Relief Valve
SV-735	Seal Water Separator 45-762 Relief Valve
SV-736	Seal Water Separator 45-763 Relief Valve
SV-737	Seal Water Filter 64-731 Relief Valve
SV-738	Seal Water Filter 64-732 Relief Valve
SV-739	Recovered VCM Condenser 55-337 VCM Outlet Relief Valve
SV-740	Recovered VCM Condenser 55-338 VCM Outlet Relief Valve
SV-741	Recovered VCM Collect Tank 45-764 Relief Valve
SV-742	Cleaning Solution Heater (Tubes) 55-339 Relief Valve
SV-743	Mechanical Seal Purge Water Surge Drum 45-759 Relief Valve

APPENDIX B

INSTRUMENT LIST - CONTINUED

Item No.	Service
Safety-Relief Valves (Continued)	
SV-744	Blowdown Tank 45-319 Relief Valve
SV-745	Breathing Air Station Supply Piping Relief Valve (Reactors, Ground Level)
SV-746	Breathing Air Station Supply Piping Relief Valve (Reactors, Ground Level)
SV-747	Breathing Air Station Supply Piping Relief Valve (Recovery Building First Floor)
SV-748	Breathing Air Station Supply Piping Relief Valve (Recovery Building Second Floor)
SV-749	Breathing Air Station Supply Piping Relief Valve (Charge Area)
SV-750	AMS Short Stop Charge Pot 45-755 Relief Valve
SV-751	AMS Short Stop Charge Pot 45-756 Relief Valve
SV-752	AMS Short Stop Charge Pot 45-757 Relief Valve
SV-753	AMS Short Stop Charge Pot 45-758 Relief Valve
SV-754	Reactor 45-741 Steam Stripping Line Relief Valve
SV-755	Reactor 45-742 Steam Stripping Line Relief Valve
SV-756	Reactor 45-743 Steam Stripping Line Relief Valve
SV-757	Reactor 45-744 Steam Stripping Line Relief Valve
SV-758	Deleted
SV-759	Deleted
SV-760	Recovered VCM Collect Tank 45-764 Inlet Line Relief Valve
SV-761	Recovered VCM Transfer Pumps 72-893 and 72-894 Discharge Relief Valve
SV-762	Recovered VCM Storage Tanks 89-520 and 45-317 Inlet Line Relief Valve
SV-763	VCM Charge Pumps 72-875 and 72-876 Discharge Relief Valve
SV-764	Breathing Air Station Supply Piping Relief Valve (Reactors, Third Level)
SV-765	Cleaning Solution Filter 64-734 Relief Valve
SV-766	Deleted
SV-767	VCM Charge Filter 64-742 Relief Valve
SV-768	Instrument Air Capacity Tank 45-301 Relief Valve
Temperature Gauges	
TG-701	Hot Water Preheater 55-332 Outlet Temperature Gauge
TG-702	Recovered VCM Storage Tank 89-520 Temperature Gauge
TG-703	Recovered VCM Storage Tank 45-317 Temperature Gauge
TG-704	Colloid Makeup Tank 45-751 Temperature Gauge
TG-705	Colloid Storage Tank 45-752 Temperature Gauge
TG-706	Colloid Charge Tank 45-753 Temperature Gauge
TG-707	Reactor Jacket 45-741 Cooling Water Return Temperature Gauge
TG-708	Reactor Condenser 55-328 Cooling Water Return Temperature Gauge

APPENDIX B

INSTURMENT LIST - CONTINUED

Item No.	Service
Temperature Gauges (Continued)	
TG-709	Reactor Jacket 45-742 Cooling Water Return Temperature Gauge
TG-710	Reactor Condenser 55-329 Cooling Water Return Temperature Gauge
TG-711	Reactor Jacket 45-743 Cooling Water Return Temperature Gauge
TG-712	Reactor Condenser 55-330 Cooling Water Return Temperature Gauge
TG-713	Reactor Jacket 45-744 Cooling Water Return Temperature Gauge
TG-714	Reactor Condenser 55-331 Cooling Water Return Temperature Gauge
TG-715	Water Recirculation Cooler 55-334 Outlet Temperature Gauge
TG-716	Deleted
TG-717	Water Recirculation Cooler 55-334 Cooling Water Return Temperature Gauge
TG-718	Water Recirculation Cooler 55-334 Inlet Temperature Gauge
TG-719	Seal Water Cooler 55-335 Cooling Water Return Temperature Gauge
TG-720	Seal Water Separator 45-762 Seal Water Outlet Temperature Gauge
TG-721	Deleted
TG-722	Seal Water Cooler 55-336 Cooling Water Return Temperature Gauge
TG-723	Seal Water Separator 45-763 Seal Water Outlet Temperature Gauge
TG-724	Recovered VCM Condenser 55-337 Cooling Water Return Temperature Gauge
TG-725	Recovered VCM Condenser 55-337 VCM Outlet Temperature Gauge
TG-726	Deleted
TG-727	Recovered VCM Condenser 55-338 Cooling Water Return Temperature Gauge
TG-728	Recovered VCM Condenser 55-338 VCM Outlet Temperature Gauge
TG-729	Deleted
TG-730	Cleaning Solution Tank 45-767 Temperature Gauge
TG-731	Seal Oil Return Temperature Gauge
TG-732	Seal Oil Pressure Unit 95-299 Cooling Water Return Temperature Gauge
TG-733	Seal Oil Pressure Unit 95-300 Cooling Water Return Temperature Gauge

APPENDIX B

INSTRUMENT LIST - CONTINUED

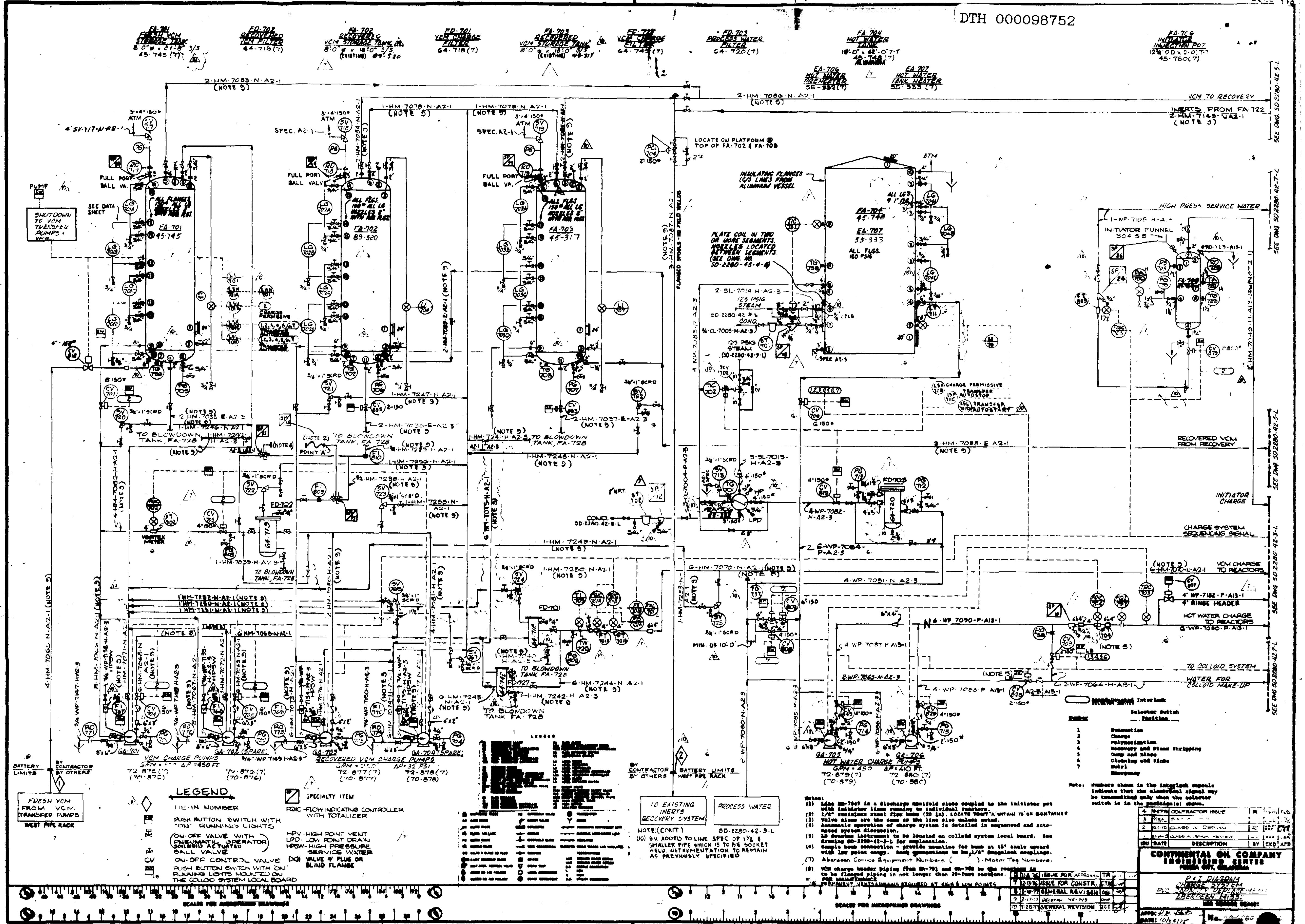
Item No.	Service
Temperature Gauges (Continued)	
TG-734	Seal Oil Supply Temperature Gauge
TG-735	Colloid Makeup Tank Jacket 45-751 Cooling Water Return Temperature Gauge
TG-736	Fresh VCM Storage Tank 45-745 Temperature Gauge
TG-737	Process Water Temperature Gauge
TG-738	Hot Water Tank 45-748 Temperature Gauge
TG-739	Initiator Charge Pot 45-750 Temperature Gauge
TG-740	Blowdown Tank 45-319 Temperature Gauge
Temperature Instruments	
TIC-701	Hot Water Tank 45-748 Temperature Controller
TIC-702	Hot Water Preheater 55-332 Discharge Temperature Controller
TRC-703	Charge Water Temperature Controller
TR-704	Colloid Makeup Tank 45-751 Temperature Recorder
TSH-704	Colloid Makeup Tank 45-751 High Temperature Switch
TSL-704	Colloid Makeup Tank 45-751 Low Temperature Switch
TI-705	VCM Charge Temperature Indicator
TIRC-706	Reactor 45-741 Polymerization Temperature Controller
TAH-706	Reactor 45-741 High Temperature Alarm
TIRC-707	Reactor 45-742 Polymerization Temperature Controller
TAH-707	Reactor 45-742 High Temperature Alarm
TIRC-708	Reactor 45-743 Polymerization Temperature Controller
TAH-708	Reactor 45-743 High Temperature Alarm
TIRC-709	Reactor 45-744 Polymerization Temperature Controller
TAH-709	Reactor 45-744 High Temperature Alarm
TIRC-710	Reactor 45-741 Steam Stripping Temperature Controller
TIRC-711	Reactor 45-742 Steam Stripping Temperature Controller
TIRC-712	Reactor 45-743 Steam Stripping Temperature Controller
TIRC-713	Reactor 45-744 Steam Stripping Temperature Controller
TR-714	Reactor Multipoint Temperature Recorder (For all Four Reactors)
TAH-715	Recovery Compressors 72-903, 72-904, and 72-905 Discharge High Temperature Alarm
TIC-716	Seal Water Cooler 55-335 Outlet Temperature Controller
TIC-717	Seal Water Cooler 55-336 Outlet Temperature Controller
TIC-718	Cleaning Solution Heater 55-339 Outlet Temperature Controller
TAH-719	Seal Oil Pressure Units 95-299 or 95-300 Discharge High Temperature Alarm
TAH-720	Initiator Injection Pot 45-750 High Temperature Alarm
TW-721	Cleaning Solution Heater 55-339 Steam Inlet Thermowell
TW-722	Cleaning Solution Heater 55-339 Solution Inlet Thermowell

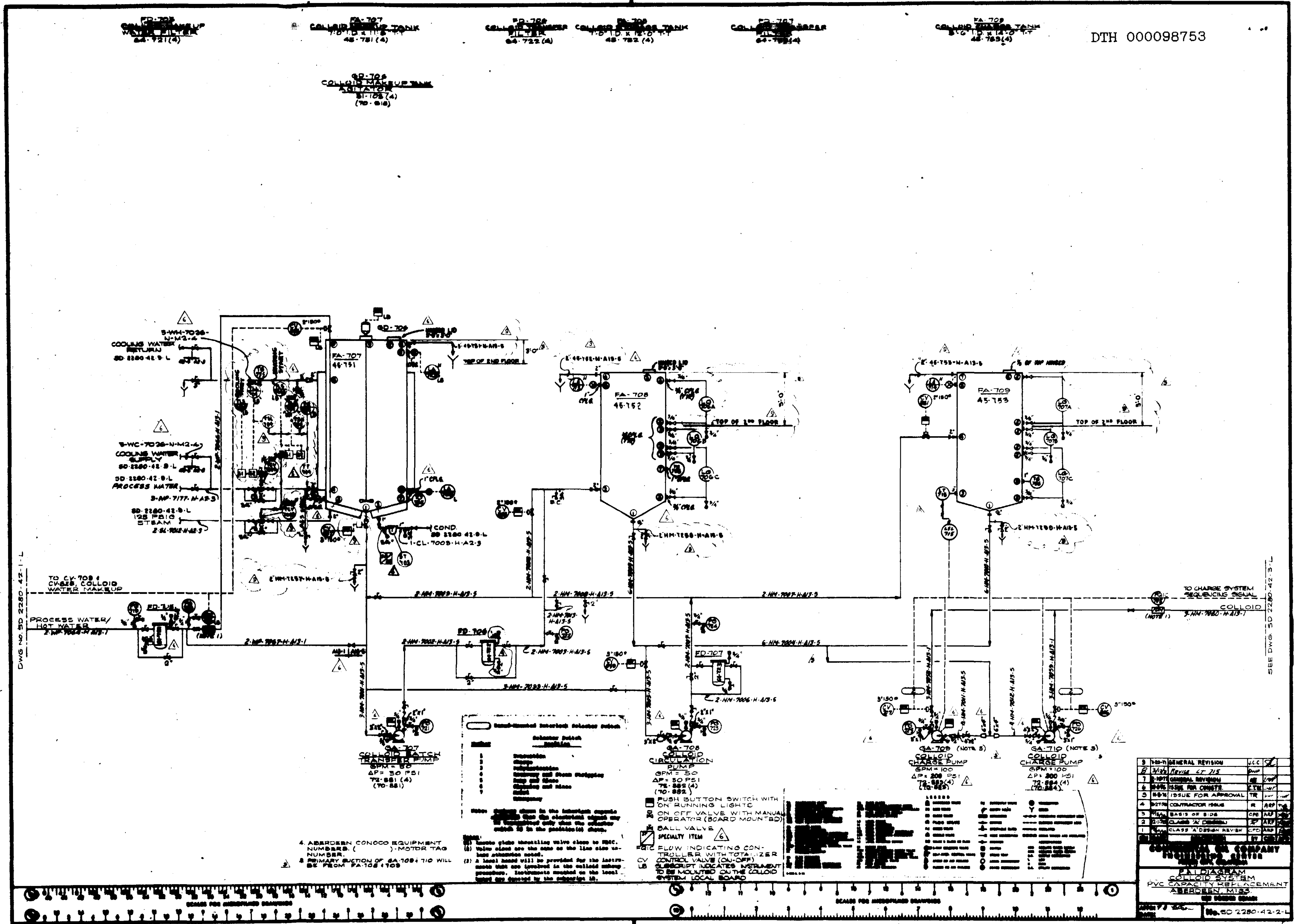
APPENDIX B

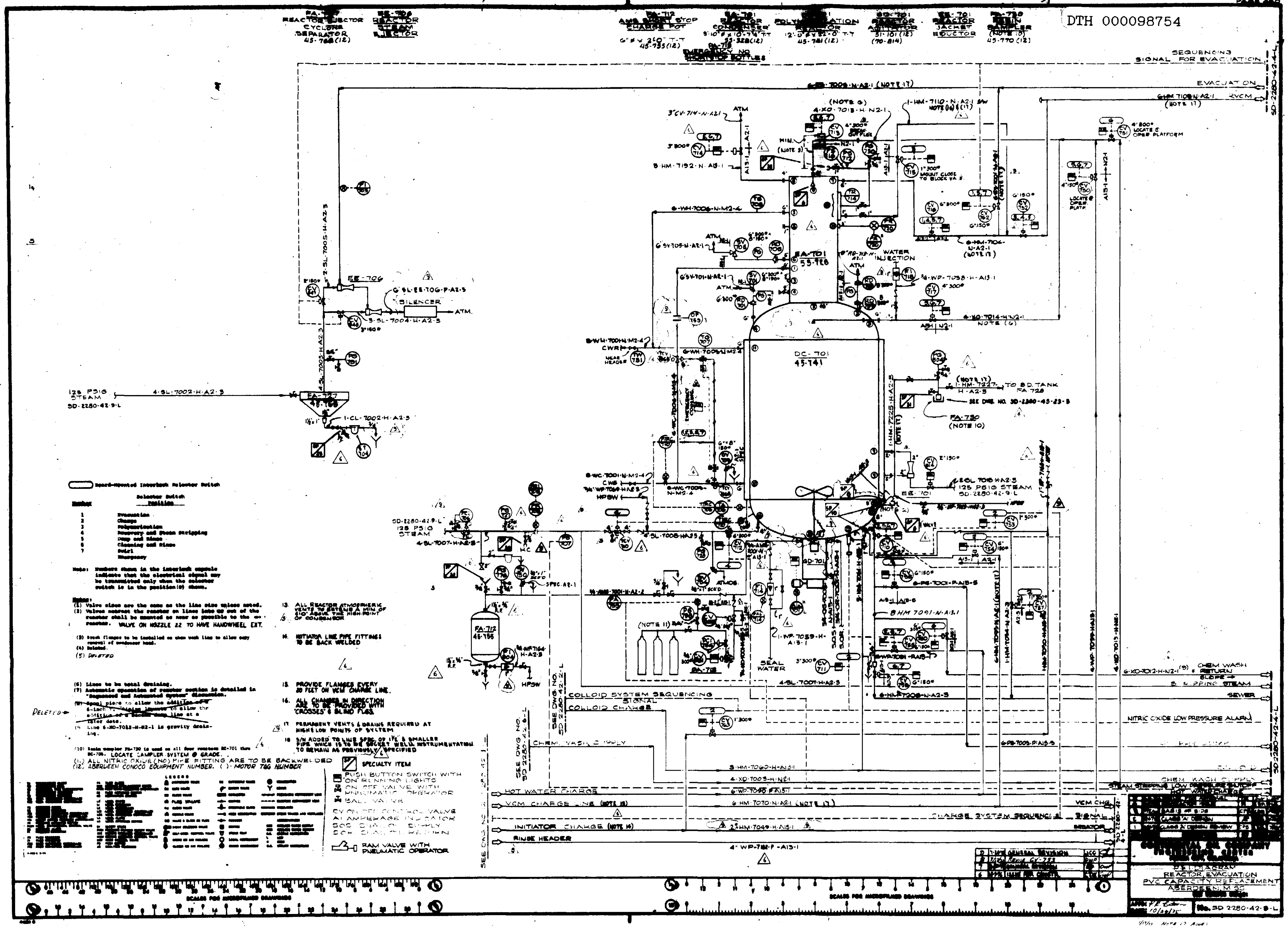
INSTRUMENT LIST - CONTINUED

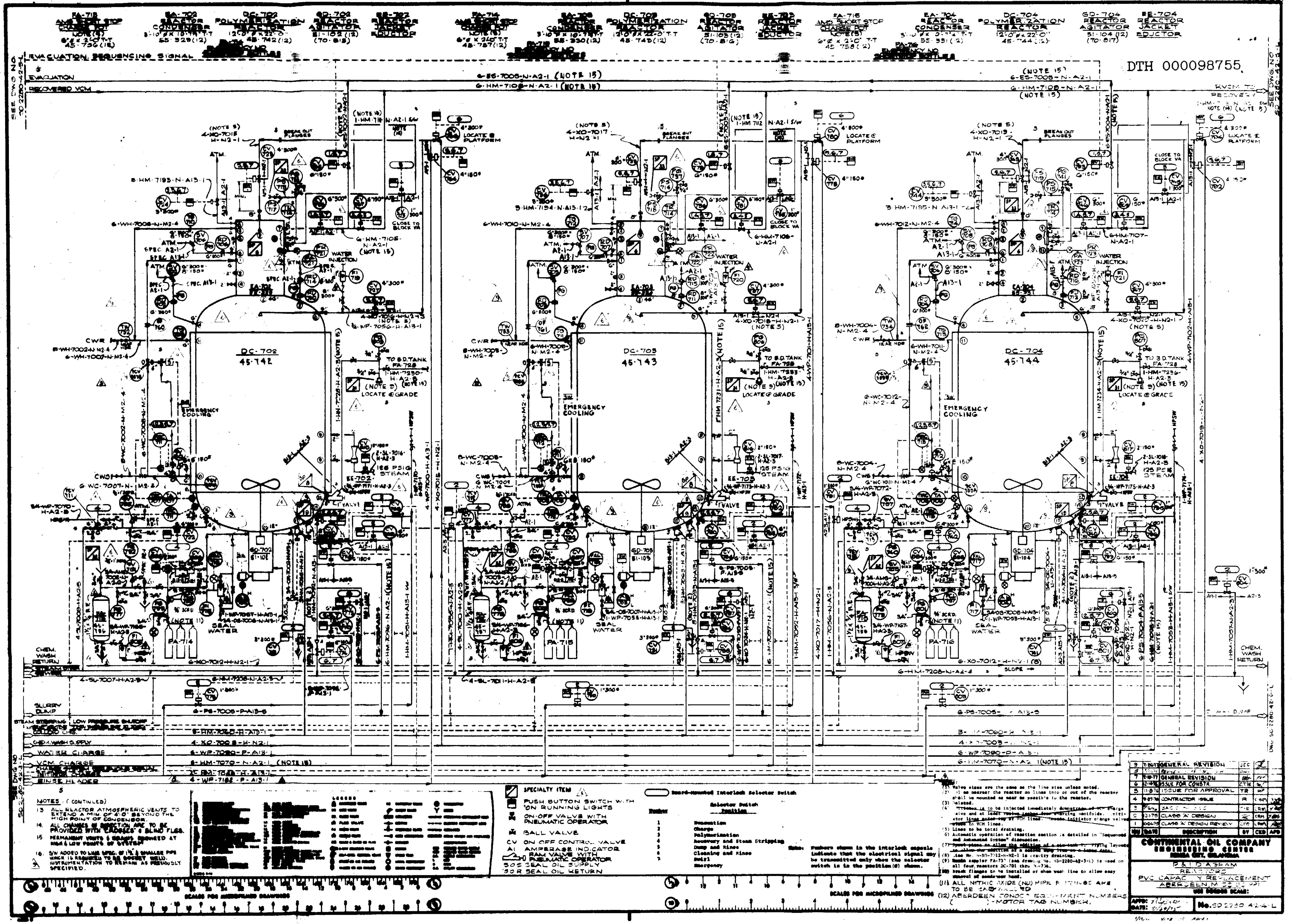
Item No.	Service
Temperature Instruments (Continued)	
TW-723	Deleted
TW-724	Cleaning Solution Heater 55-339 Solution Outlet Thermowell
TW-725	VCM Charge Filters 64-718 and 64-742 Outlet Piping Thermowell
TR-726	Recovery System Multipoint Temperature Recorder
TW-727	Water Recirculation Cooler 55-334 Cooling Water Supply Thermowell
TW-728	Seal Water Cooler 55-335 Cooling Water Supply Thermowell
TW-729	Recovered VCM Condenser 55-337 Cooling Water Supply Thermowell
TIC-730	Blowdown Tank 45-319 Temperature Controller
TW-731	Reactor 45-741 Cooling Water Return Thermowell
TW-732	Reactor 45-742 Cooling Water Return Thermowell
TW-733	Reactor 45-743 Cooling Water Return Thermowell
TW-734	Reactor 45-744 Cooling Water Return Thermowell

DTH 000098752

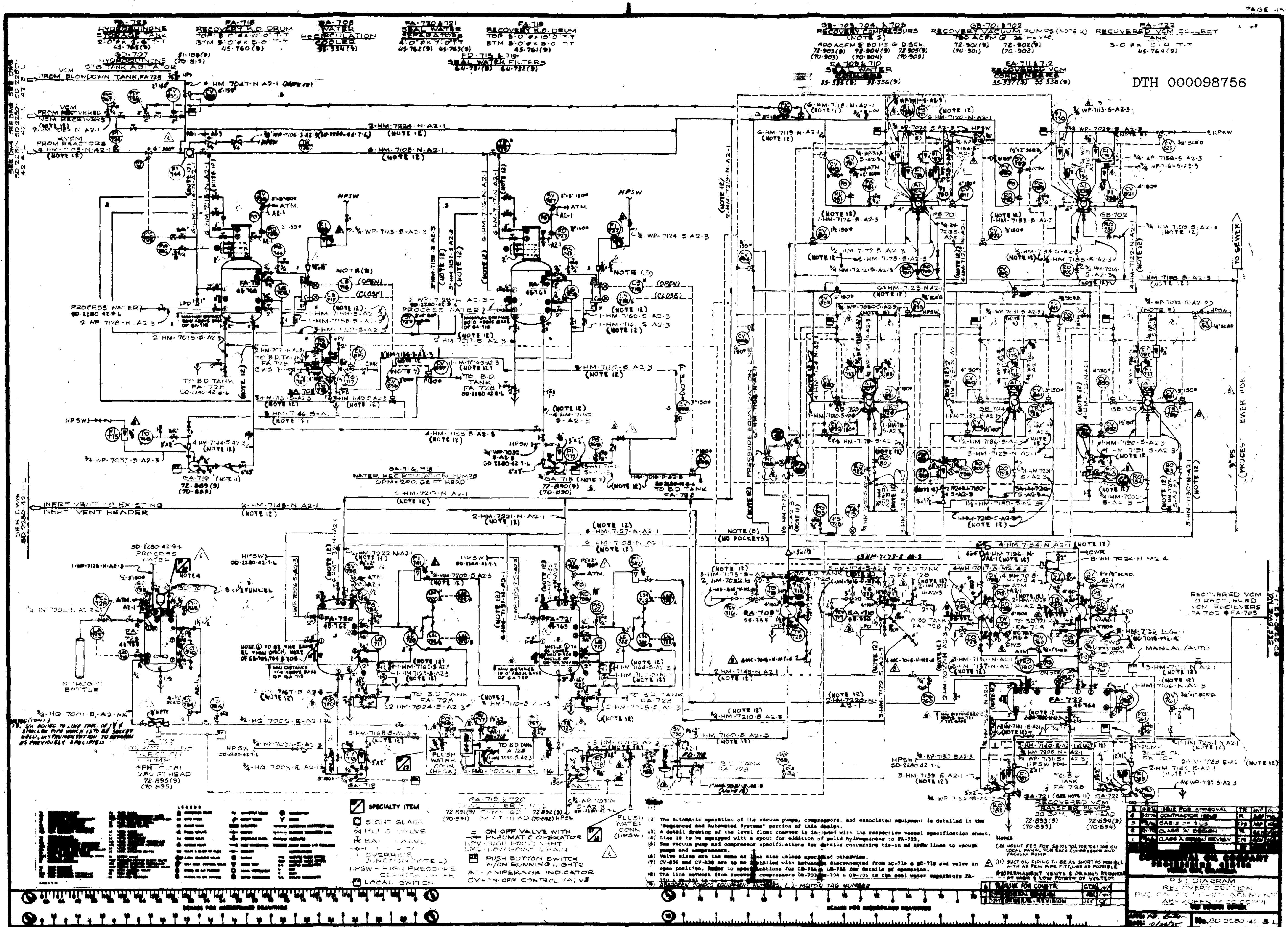



DTH 000098753
FA-707
45-751 (4)
FD-706
64-722 (4)
FA-708
45-752 (4)
FA-709
45-753 (4)
SD-706
COLLOID MAKEUP TANK
AGITATOR
51-105 (4)
(70-818)
FA-707
45-751
FA-708
45-752
FA-709
45-753
TOP OF 2ND FLOOR
COOLING WATER
RETURN
SD 2280-42-9-L
COOLING WATER
SUPPLY
SD 2280-42-9-L
PROCESS WATER
125 PSIG
STEAM
COND.
SD 2280-42-9-L
1-CL-7005-H-A2-3
TO CV-703 &
CV-828, COLLOID
WATER MAKEUP
PROCESS WATER/
HOT WATER
DWG NO. SD 2280-42-1-L
SEE DWG. SD 2280-42-3-L
TO CHARGE SYSTEM
SEQUENCING SIGNAL
COLLOID
FD-706
FD-707
GA-707
COLLOID BATCH
TRANSFER PUMP
GPM = 50
ΔP = 30 PSI
72-881 (4)
(70-881)
GA-708
COLLOID
CIRCULATION
PUMP
GPM = 50
ΔP = 30 PSI
72-882 (4)
(70-882)
GA-709 (NOTE 5)
COLLOID
CHARGE PUMP
GPM = 100
ΔP = 200 PSI
72-883 (4)
(70-883)
GA-710 (NOTE 5)
COLLOID
CHARGE PUMP
GPM = 100
ΔP = 200 PSI
72-884 (4)
(70-884)
PUSH BUTTON SWITCH WITH
ON RUNNING LIGHT
ON OFF VALVE WITH MANUAL
OPERATOR (BOARD MOUNTED)
BALL VALVE
SPECIALTY ITEM
FLOW INDICATING CON-
TROLLER WITH TOTALIZER
CONTROL VALVE (ON-OFF)
SUBSCRIPT INDICATES INSTRUMENT
TO BE MOUNTED ON THE COLLOID
SYSTEM LOCAL BOARD
4. ABERDEEN CONOCO EQUIPMENT
NUMBERS. ( ) - MOTOR TAG
NUMBER.
5. PRIMARY SUCTION OF GA-709 & 710 WILL
BE FROM FA-708 & 709
9 GENERAL REVISION
8 REVISE
7 GENERAL REVISION
6 ISSUE FOR CONSTR.
5 ISSUE FOR APPROVAL
4 CONTRACTOR ISSUE
3 BASIS OF BIDS
2 CLASS "A" DESIGN
1 CLASS "A" DESIGN REVIEW
CONTINENTAL OIL COMPANY
P & I DIAGRAM
COLLOID SYSTEM
PVC CAPACITY REPLACEMENT
ABERDEEN, MISS.
No. SD 2280-42-2-L
SCALES FOR MICROFILMED DRAWINGS

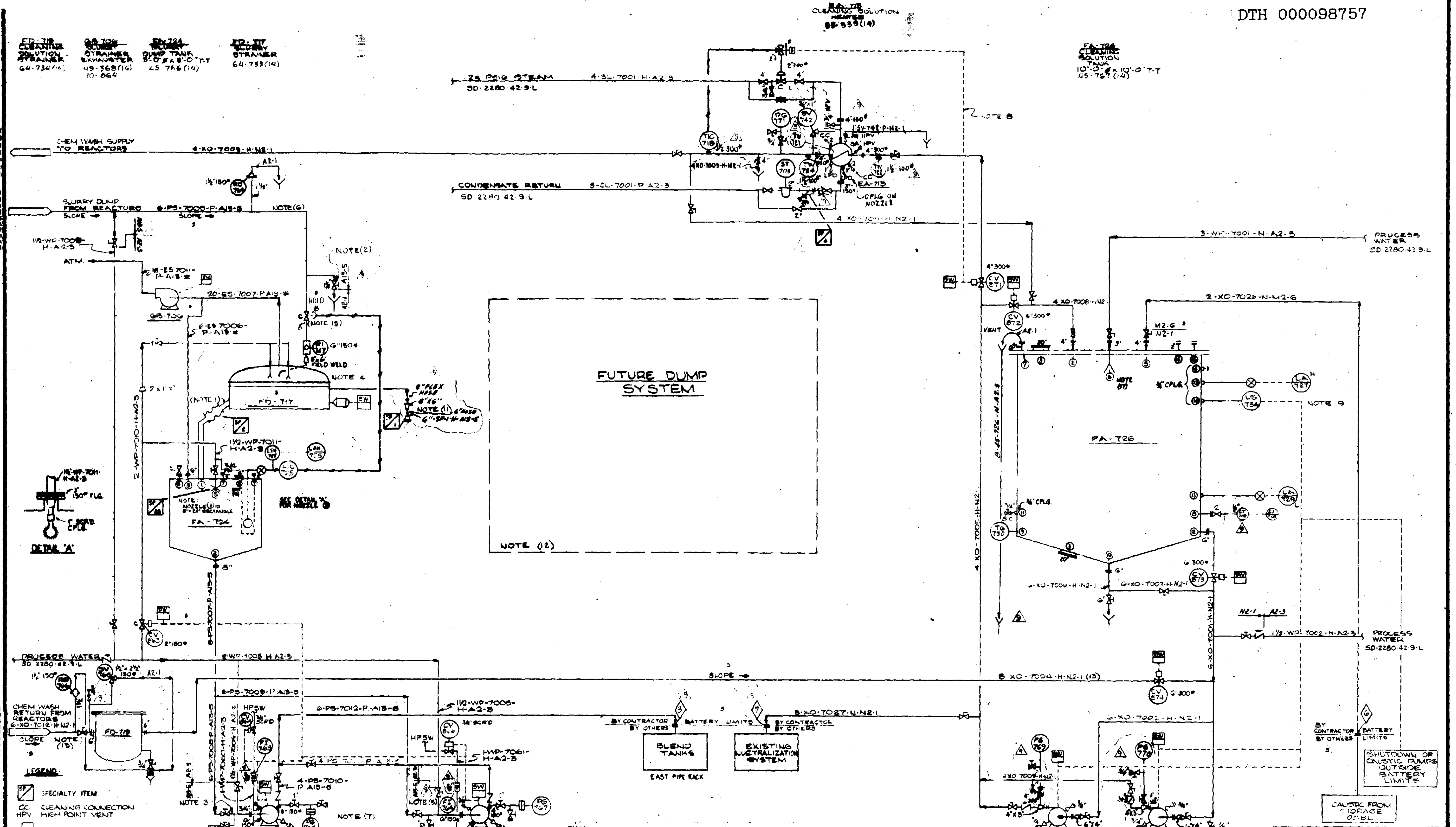



PAGE 45
DTH 000098755
FA-713 AMB. SHORT STOP CHARGE POT
EA-702 REACTOR CONDENSER
DC-702 POLYMERIZATION REACTOR
GD-702 REACTOR AGITATOR
EE-702 REACTOR JACKET EDUCTOR
FA-714 AMB. SHORT STOP CHARGE POT
EA-703 REACTOR CONDENSER
DC-703 POLYMERIZATION REACTOR
GD-703 REACTOR AGITATOR
EE-703 REACTOR JACKET EDUCTOR
FA-716 AMB. SHORT STOP CHARGE POT
EA-704 REACTOR CONDENSER
DC-704 POLYMERIZATION REACTOR
GD-704 REACTOR AGITATOR
EE-704 REACTOR JACKET EDUCTOR
EVACUATION SEQUENCING SIGNAL
EVACUATION
RECOVERED VCM
DC-702 45-742
DC-703 45-743
DC-704 45-744
EMERGENCY COOLING
WATER INJECTION
LOCATE @ PLATFORM
LOCATE @ GRADE
TO B.D. TANK
125 PSIG STEAM
SEAL WATER
CHEM. WASH RETURN
SLURRY DUMP
WATER CHARGE
VCM CHARGE
RINSE HEADER
NOTES: (CONTINUED)
13 ALL REACTOR ATMOSPHERIC VENTS TO EXTEND A MIN. OF 4'-0" BEYOND THE HIGH POINT OF CONDENSOR.
SPECIALTY ITEM
PUSH BUTTON SWITCH WITH "ON RUNNING LIGHTS"
ON-OFF VALVE WITH PNEUMATIC OPERATOR
BALL VALVE
CV ON OFF CONTROL VALVE
AI AMPERAGE INDICATOR
RAM VALVE WITH PNEUMATIC OPERATOR
SOS SEAL OIL SUPPLY
SOR SEAL OIL RETURN
SCALES FOR MICROFILMED DRAWINGS
CONTINENTAL OIL COMPANY
ENGINEERING CENTER
P & I DIAGRAM
REACTORS
PVC CAPACITY REPLACEMENT
No. SD 2280-42-4-L

DTH 000098756



DTH 000098757


FD-719 CLEANING SOLUTION STRAINER 64-734(14)
GB-726 SLURRY STRAINER EXHAUSTER 49-368(14) 70-864
FA-724 SLURRY DUMP TANK 8'-0" x 8'-0" T-T 45-766(14)
FD-717 SLURRY STRAINER 64-733(14)
FA-715 CLEANING SOLUTION HEATER 85-559(14)
FA-726 CLEANING SOLUTION TANK 10'-0" x 10'-0" T-T 45-767(14)
25 PSIG STEAM
SD-2280-42-9-L
CHEM WASH SUPPLY TO REACTORS
CONDENSATE RETURN
SLURRY DUMP FROM REACTORS
CHEM WASH RETURN FROM REACTORS
PROCESS WATER
FUTURE DUMP SYSTEM
NOTE (12)
FA-726
FA-724
FD-717
FD-718
DETAIL "A"
SEE DETAIL "A" FOR NOZZLE
BY CONTRACTOR BY OTHERS
BATTERY LIMITS
BLEND TANKS
EXISTING NEUTRALIZATION SYSTEM
EAST PIPE RACK
SHUTDOWN OF CAUSTIC PUMPS OUTSIDE BATTERY LIMITS
CAUSTIC FROM STORAGE OSBL
GA-724 SLURRY TRANSFER PUMP 600 GPM ΔP=126 FT. 72-896(14) (70-896)
GA-725 SLURRY TRANSFER PUMP 600 GPM ΔP=126 FT. 72-897(14) (70-897)
GA-728 & 729 CLEANING SOLUTION PUMPS 500 GPM ΔP= 86 PSI 72-898(14) (70-898) 72-899(14) (70-899)
LEGEND
SPECIALTY ITEM
CC HPV CLEANING CONNECTION HIGH POINT VENT
SIGHT GLASS
BALL CONTROL VALVE
BALL VALVE
PUSH BUTTON SWITCH WITH "ON" RUNNING LIGHTS
ON-OFF VALVE WITH PNEUMATIC ACTUATOR
LPD LOW POINT DRAIN
TIE IN NUMBER
DUCT WORK
DAMPER
SEE DWG NO SD-2280-42-9-L

NOTES:

(1) To be 9" x 24" flexible vulanized reinforced rubber connector. Final design of connector to be made after equipment positions are finalized. Connector to have metal shield.
(2) Drain to be located as near to ball control valve as possible.
(3) Water flush inlet to be adjacent to pump and drain to be adjacent to ball valve.
(4) Elevation of slurry strainer shall be minimized.
(5) All slurry lines shall be routed to minimize distance and bends. All bends are to be constructed such that pressure drop is minimized.
(6) Slurry dump line is to have a continuous downward slope from the reactor.
(7) Pumps to be close coupled to dump tank.
(8) TIC-718 control valve cannot open unless CV-871 is open. This will allow steam flow to the exchanger only when caustic is flowing through the exchanger.
(9) LS-734 will shut down GA-728 and 729 and caustic pumps at battery limits in the event of high level.
(10) Valve sizes are the same as the line size unless otherwise noted.
(11) Culls outlet to be field adapted with male KAM-LOCK coupling with dust cover-ALUM.
(12) Equipment and piping layouts to include space for the addition of a second dump system.
(13) Line 6-XO-7004-H N2-1 and 6-XO-7012-H N2-1 are gravity draining.
(14) ABERDEEN CONOCO EQUIPMENT NUMBERS. ( ) - MOTOR TAG NUMBERS
(15) LIC-725 CONTROL VALVE IS TO BE FULL PORT BALL VALVE
(16) FOR FA-724 DETAILS SEE DWG. NO. SD-2280-43-20B
(17) FOR FA-726 DETAILS SEE DWG. NO. SD-2280-43-21C

9	7-28-77	GENERAL REVISION	JCC		
8	3/11/77	Rev. [illegible]	DWP		
7	2-10-77	GENERAL REVISION			
6	12-8-76	ISSUE FOR CONSTR.	C.T.W.		
5	11-8-76	ISSUE FOR APPROVAL	TR	DWP	
4	[illegible]	CONTRACTOR ISSUE	R	AGP	PGR
3	[illegible]	BASIS OF BIDS	CPB	AGP	
2	[illegible]	CLASS "A" DESIGN			
1	[illegible]	CLASS "A" DESIGN REVIEW			

CONTINENTAL OIL COMPANY
ENGINEERING CENTER
PONCA CITY, OKLAHOMA

P&I DIAGRAM
CHEMICAL WASH AND DUMP
PVC CAPACITY REPLACEMENT
ABERDEEN, MISS.

APPR: H.B. [illegible]
DATE: 10/24/75

No. SD2280-42-6-L

SCALES FOR MICROFILMED DRAWINGS

FD-709 SERVICE WATER FILTER 64-724(7)

FA-717 MECHANICAL SEAL PUMP 316 SS 5 X 10 T-T 45-759(7)

FD-712 SEAL OIL FILTER 64-728(7)

FD-711 SEAL OIL FILTER 64-727(7)

FA-703 SEAL OIL PUMP 95-500(7)

FA-716 SERVICE WATER PUMP 316 SS 6 X 8 X 10 T-T 45-754(7)

FD-710 SEAL OIL FILTER 64-726(7)

FD-708 SEAL OIL FILTER 64-725(7)

FA-710 45-754

PA-702(1)(3) 56-500

PA-701(1)(3) 56-555

FA-715 SERVICE WATER PUMP 316 SS 6 X 8 X 10 T-T 45-753(7)

FA-714 MECHANICAL SEAL WATER PUMP 316 SS 6 X 8 X 10 T-T 45-752(7)

FD-708

NITROGEN BOTTLE

EMERGENCY SEAL OIL DRUM

SEAL OIL RESERVOIR

SEAL OIL PUMP

PROCESS WATER 4-WP-7014-N-A2-3 SD-2280-42-8-L

TO CATALYST INJECTION POT FA-706 1-WP-7105-H-A1B-1

Notes:
(1) All controls and piping not numbered are part of the package unit.
(2) Locate near PA-701 and PA-702.
(3) While one pressure unit is on stream, the other pressure unit serves as an automatic in-line spare which will automatically start up on low seal oil supply pressure or low seal oil reservoir level.
(4) Locate valve at reservoir.
(5) Header system to be dismantled after final equipment layout is determined.
(6) Valve sizes are the same size as the line unless otherwise noted.
(7) ABERDEEN CONOCO EQUIPMENT NUMBERS

MOTOR TAG NO:

SPECIALTY ITEM
ON-OFF VALVE WITH MANUAL OPERATOR (BOARD-MOUNTED)
BALL VALVE
RTV SELF OPERATED RETAINING VALVE.

8	7-27-77	GENERAL REVISION	JCC		
7	2-18-77	GENERAL REVISION			
6	12-13-76	ISSUE FOR CONSTR.	CTK		
5	11-8-76	ISSUE FOR APPROVAL	TR		
4	9-27-76	CONTRACTOR ISSUE	PA	AAD	
3	7/24/76	BASIS OF BIDS	CHB	AAD	
2	2-1-75	CLASS 'A' DESIGN	RP		
1	12-6-74	CLASS 'A' DESIGN REVIEW	RP	AAD	
NO.	DATE	REVISION	BY	CHK'D	APP'D

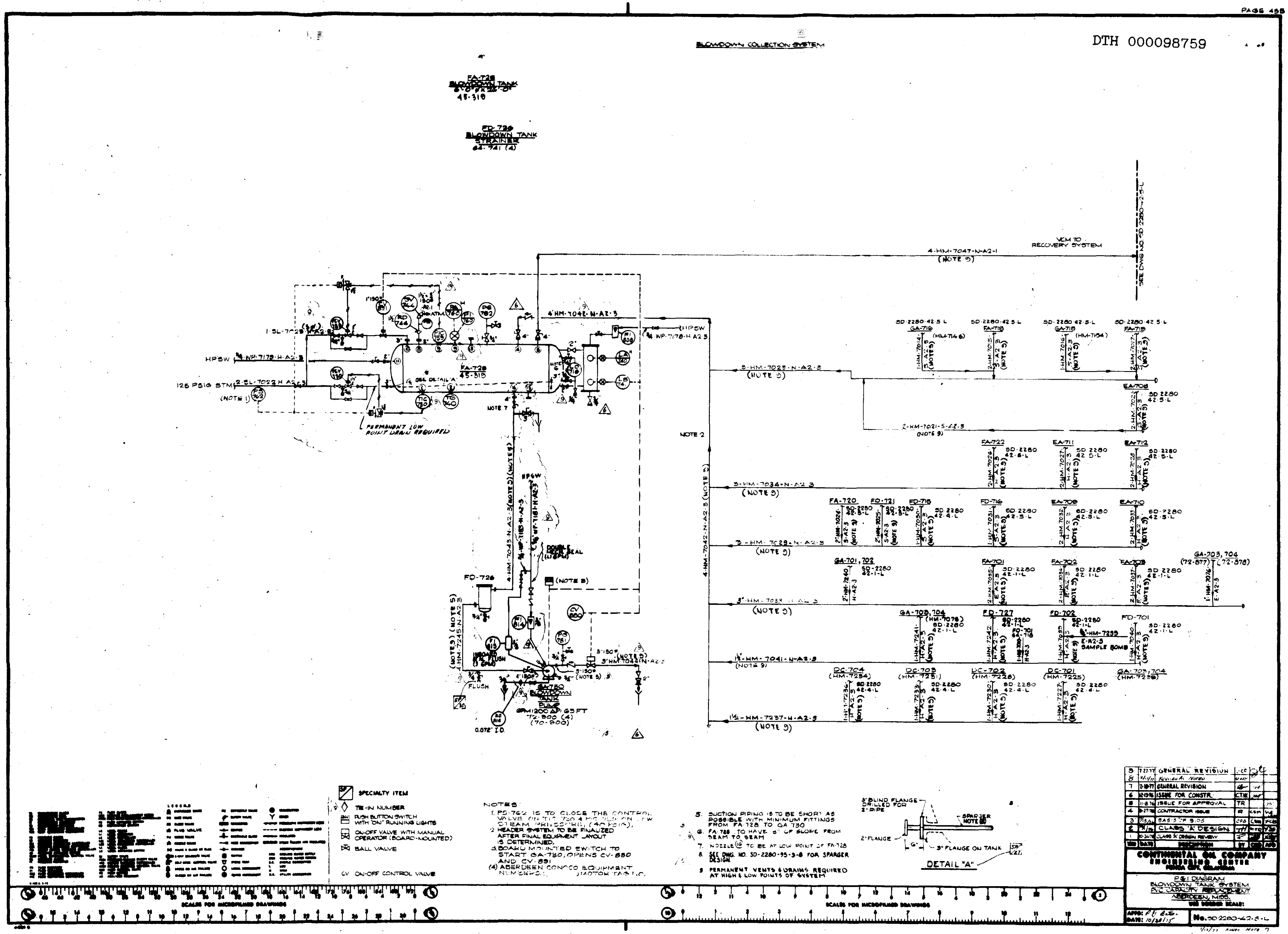
CONTINENTAL OIL COMPANY
ENGINEERING SERVICES
HOUSTON, TEXAS

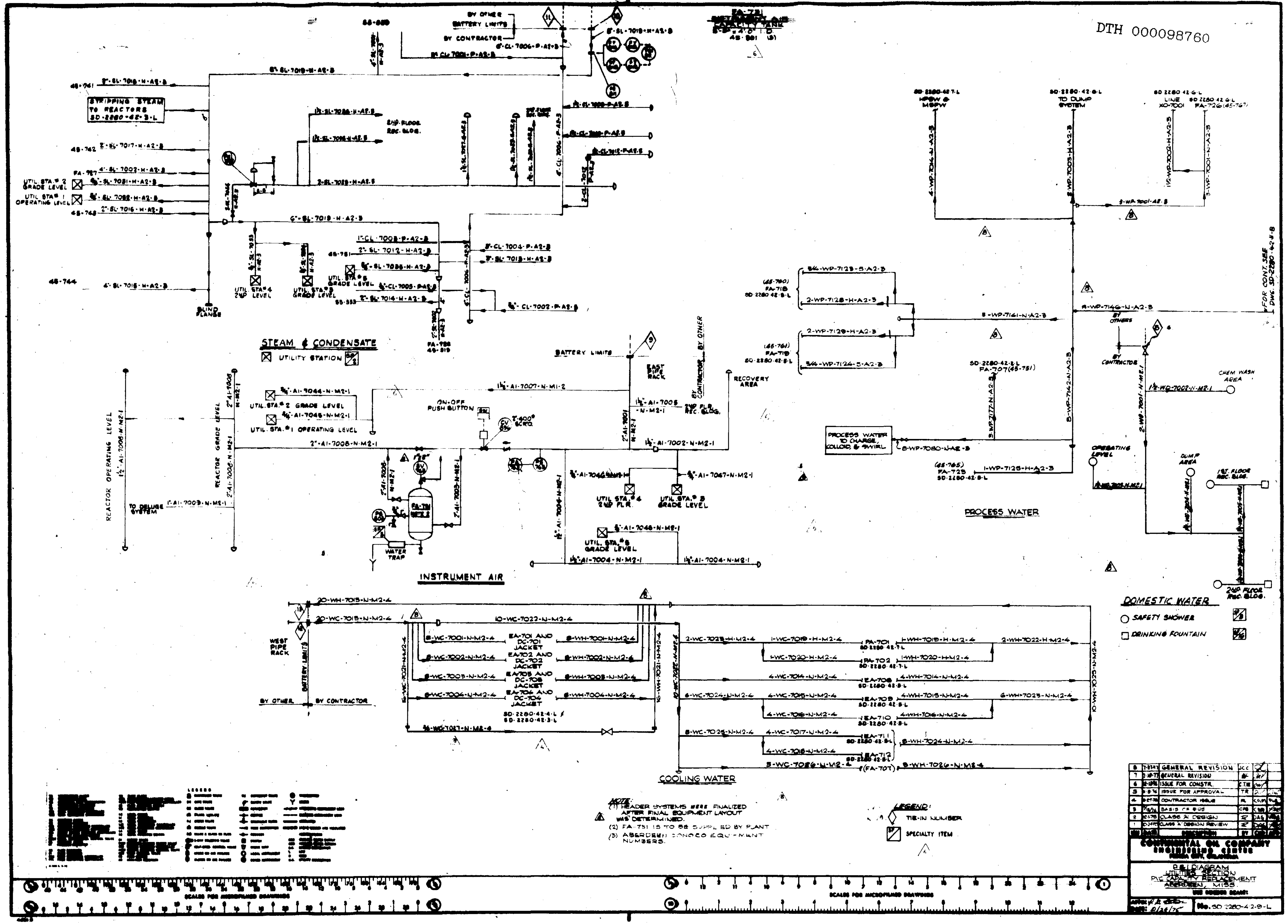
P & I DIAGRAM
SERVICE WATER, MECHANICAL SEAL WATER, AND SEAL OIL SYSTEMS
PVC CAPACITY REPLACEMENT
ABERDEEN, MISSISSIPPI

APPR: D. B. Bass
DATE: 10/26/76

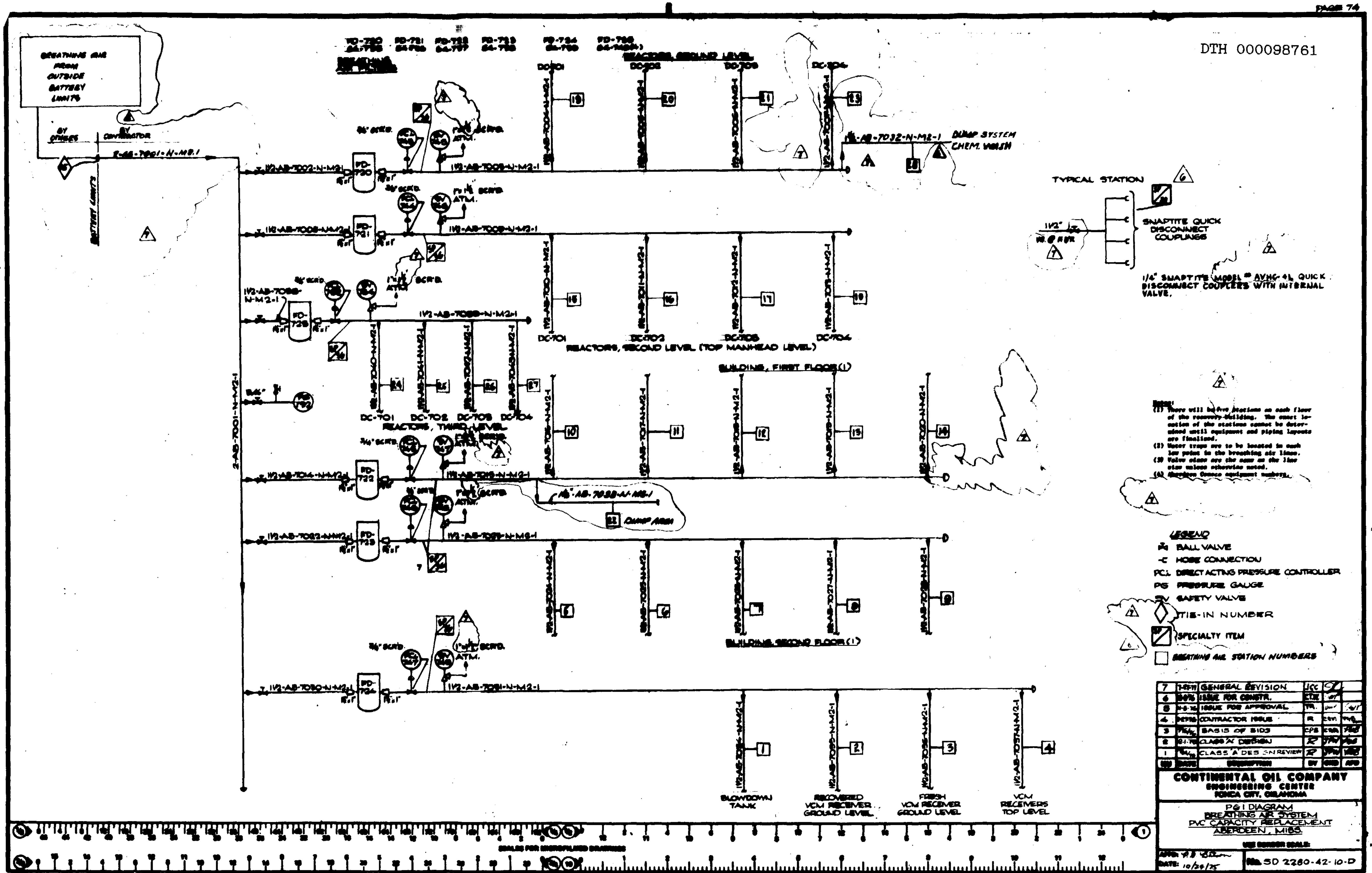
No. SD 2280-42-7-L

SCALES FOR MICROFILMED DRAWINGS


DTH 000098759
BLOWDOWN COLLECTION SYSTEM
FA-728
BLOWDOWN TANK
45-310
FD-726
BLOWDOWN TANK
STRAINER
64-741 (4)
VCM TO
RECOVERY SYSTEM
4-HM-7047-N-A2-1
(NOTE 9)
4-HM-7042-N-A2-3
HPSW
HPSW
125 PSIG STM
(NOTE 1)
PERMANENT LOW POINT DRAIN REQUIRED
NOTE 2
NOTE 7
FD-726
GA-730
BLOWDOWN TANK PUMP
DOUBLE SEAL
FLUSH
0.072" I.D.
5-HM-7025-N-A2-3
(NOTE 9)
3-HM-7034-N-A2-3
(NOTE 9)
3-HM-7029-N-A2-3
(NOTE 9)
3"-HM-7039
(NOTE 9)
1½-HM-7041-N-A2-3
(NOTE 9)
1½-HM-7237-N-A2-3
(NOTE 9)
2-HM-7021-S-A2-3
(NOTE 9)
FA-716
FA-718
GA-718
FA-719
EA-708
FA-722
EA-711
EA-712
FA-720
FD-721
FD-716
FD-716
EA-709
EA-710
GA-701, 702
FA-701
FA-702
EA-703
GA-703, 704
GA-703, 704
FD-727
FD-702
FD-701
SAMPLE BOMB
DC-704
DC-703
DC-702
DC-701
GA-703, 704
SPECIALTY ITEM
TIE-IN NUMBER
PUSH BUTTON SWITCH WITH "ON" RUNNING LIGHTS
ON-OFF VALVE WITH MANUAL OPERATOR (BOARD-MOUNTED)
BALL VALVE
CV ON-OFF CONTROL VALVE
NOTES:
1. PS-762 IS TO CLOSE THE CONTROL VALVE ON TIC-730 & PIC-731 ON LOW STEAM PRESSURE (40 PSIG).
2. HEADER SYSTEM TO BE FINALIZED AFTER FINAL EQUIPMENT LAYOUT IS DETERMINED.
3. BOARD MOUNTED SWITCH TO START GA-730, OPENS CV-880 AND CV-891
(4) ABERDEEN CONOCO EQUIPMENT NUMBER / MOTOR TAG NO.
5. SUCTION PIPING IS TO BE SHORT AS POSSIBLE WITH MINIMUM FITTINGS FROM FA 728 TO GA 730
6. FA-728 TO HAVE 6" OF SLOPE FROM SEAM TO SEAM
7. NOZZLE TO BE AT LOW POINT OF FA-728
8. SEE DWG. NO. SD-2280-95-3-8 FOR SPARGER DESIGN
9. PERMANENT VENTS & DRAINS REQUIRED AT HIGH & LOW POINTS OF SYSTEM
3" BLIND FLANGE DRILLED FOR 2" PIPE
SPARGER NOTE 8
2" FLANGE
3" FLANGE ON TANK
DETAIL "A"
GENERAL REVISION
GENERAL REVISION
ISSUE FOR CONSTR.
ISSUE FOR APPROVAL
CONTRACTOR ISSUE
CLASS "A" DESIGN
CLASS "A" DESIGN REVIEW
CONTINENTAL OIL COMPANY
ENGINEERING CENTER
P&I DIAGRAM
BLOWDOWN TANK SYSTEM
PVC CAPACITY REPLACEMENT
ABERDEEN, MISS.
SCALES FOR MICROFILMED DRAWINGS
No. SD-2280-42-3-L

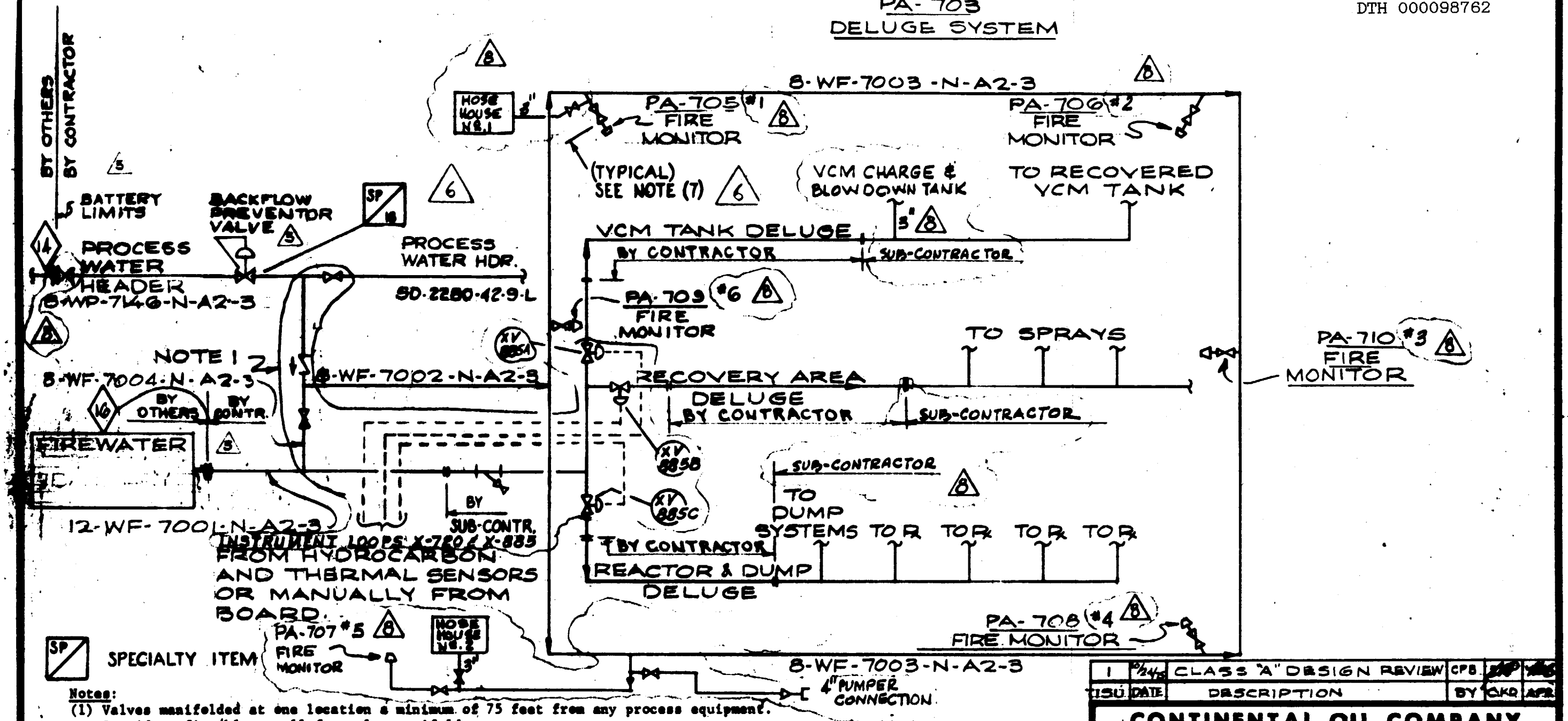

DTH 000098760
STEAM & CONDENSATE
UTILITY STATION
STRIPPING STEAM TO REACTORS SD-2280-42-3-L
INSTRUMENT AIR
ON-OFF PUSH BUTTON
WATER TRAP
REACTOR OPERATING LEVEL
REACTOR GRADE LEVEL
TO DELUGE SYSTEM
BATTERY LIMITS
EAST PIPE RACK
RECOVERY AREA
PROCESS WATER
PROCESS WATER TO CHARGE, COLLOID & SWIRL
CHEM WASH AREA
DUMP AREA
OPERATING LEVEL
1ST FLOOR REC. BLDG.
2ND FLOOR REC. BLDG.
FOR CONT. SEE DWG. SD-2280-42-11-B
DOMESTIC WATER
SAFETY SHOWER
DRINKING FOUNTAIN
COOLING WATER
WEST PIPE RACK
BY OTHER
BY CONTRACTOR
NOTE:
(1) HEADER SYSTEMS WERE FINALIZED AFTER FINAL EQUIPMENT LAYOUT WAS DETERMINED.
(2) FA-751 IS TO BE SUPPLIED BY PLANT
(3) ABERDEEN CODED EQUIPMENT NUMBERS.
LEGEND:
TIE-IN NUMBER
SPECIALTY ITEM
SCALES FOR MICROFILMED DRAWINGS
8 GENERAL REVISION
7 GENERAL REVISION
6 ISSUE FOR CONSTR.
5 ISSUE FOR APPROVAL
4 CONTRACTOR ISSUE
3 BASIS FOR BIDS
2 CLASS A DESIGN
1 CLASS A DESIGN REVIEW
CONTINENTAL OIL COMPANY
ENGINEERING CENTER
P&I DIAGRAM
UTILITIES SECTION
PVC QUALITY IMPROVEMENT
ABERDEEN, MISS.
No. SD-2280-42-8-L

DTH 000098761



DTH 000098762

PA-703
DELUGE SYSTEM



Notes:

(1) Valves manifolded at one location a minimum of 75 feet from any process equipment. Provide a fire/blast wall for valve manifold.

(2) Automatic spray system vendor to design battery limits--headers, lines, spray manifolds, and instrumentation.

(3) Hose house, 300 feet of soft hose, 150 feet of hard hose, and quick-acting reel at the two monitors on a line north and south through FA-724.

(4) Provide fire/blast walls for fire monitors.

(5) Deluge header and valves shown for illustrative purposes only.

(6) CONTRACTOR SHALL PROVIDE BACKFLOW PREVENTER AT TIE-IN OF PROCESS WATER TO FIREWATER LOOP

(7) MONITORS TO BE PROVIDED BY FIRE-WATER SUB-CONTRACTOR.

ISU	DATE	DESCRIPTION	BY	CKD	APD
8	8/15/77	GENERAL REVISIONS	WTR		
7	3/14/77	ISSUE FOR APPROVAL	DWP		
6	12/5/76	ISSUE FOR CONSTR.	C.T.W.		
5	11/6/76	ISSUE FOR APPROVAL	TR	DWP	
4	10/26/76	Added backflow prevent.	RLF	RLF	
3	7/15/76	BASIS OF BIDS	CPB	CRM	
2	4/1/76	CLASS 'A' DESIGN			
1	3/24/76	CLASS "A" DESIGN REVIEW	CPB		

CONTINENTAL OIL COMPANY
ENGINEERING CENTER
PONCA CITY, OKLAHOMA

P & I DIAGRAM
FIRE WATER SYSTEM
PVC CAPACITY REPLACEMENT
ABERDEEN, MISS.

SCALE:

APPD: R.D. Burton
DATE: 10/24/75

No. SD 2280-42-11-B

4-281 S

P. O. Box 1267
PONCA CITY, OKLAHOMA 74601

CHARGE SECTION

VCM TRANSFER

AUTO-MAN XS-821	OFFSITES PUMPS 72-4XX	OFFSITE VALVE CV-818
AUTO	START	OPEN
ON / OFF	STOP	CLOSE

RECOVERED VCM CHARGE

AUTO-MAN XS-877	PRIMARY PUMP 72-877	PUMP SELECTOR X-877	SPARE PUMP 72-878	RECOVERED VCM CV-703
AUTO	START	PRIMARY OFF	START	OPEN
ON / OFF	MOTOR RUN	SPARE OFF	MOTOR RUN	CLOSE
	STOP		STOP	

FRESH VCM CHARGE

AUTO-MAN XS-875	PRIMARY CHARGE PUMP 72-875	PUMP SELECTOR X-875	SPARE CHARGE PUMP 72-876
AUTO	START	PRIMARY OFF	START
ON / OFF	MOTOR RUN	SPARE OFF	MOTOR RUN
	STOP		STOP

RECEIVER OUTLET CV-701	PRIMARY CHG. PUMP DISCH. CV-704	SPARE CHARGE PUMP DISCH. CV-705
OPEN	OPEN	OPEN
CLOSE	CLOSE	CLOSE

HOT WATER CHARGE

AUTO-MAN XS-879	CHARGE PUMP A 72-879	CHARGE PUMP B 72-880
AUTO	START	START
ON / OFF	MOTOR RUN	MOTOR RUN
	STOP	STOP

HOT WATER CHARGE CV-706	PRIMARY PUMP DISCH. CV-849	SPARE PUMP DISCH. CV-829
OPEN	OPEN	OPEN
CLOSE	CLOSE	CLOSE

WATER CHARGE

COLD WATER CV-809	HOT WATER TK. MAKEUP CV-818
OPEN	OPEN
CLOSE	CLOSE

COLD WATER SWIRL CV-808
OPEN
CLOSE

INITIATOR CHARGE

AUTO-MAN XS-801	HPSW INLET CV-879	INIT. POT PRESSURE PI-H-703
AUTO	OPEN	
ON / OFF	CLOSE	

REACTOR 45-741 CV-753	REACTOR 45-742 CV-776	REACTOR 45-743 CV-790	REACTOR 45-744 CV-803
OPEN	OPEN	OPEN	OPEN
CLOSE	CLOSE	CLOSE	CLOSE

COLLOID CHARGE

AUTO-MAN XS-883	PRIMARY CHARGE PUMP 72-883	PUMP SELECTOR X-883	SPARE CHARGE PUMP 72-884
AUTO	START	PRIMARY OFF	START
ON / OFF	MOTOR-RUN	SPARE OFF	MOTOR-RUN
	STOP		STOP

PRIMARY PUMP DISCH. CV-847	SPARE PUMP DISCH. CV-848
OPEN	OPEN
CLOSE	CLOSE

LAMP TEST XS-839

PUSH TO TEST

AUTOMATIC CHARGE XS-760

READY / START

COLLOID TRANSFER AND CIRCULATION

MAKEUP TK. INLET CV-857	TRANSFER PUMP 72-881	CHARGE TK. INLET CV-861
OPEN	START	OPEN
CLOSE	MOTOR RUN	CLOSE
	STOP	

CIRC. PUMP INLET CV-859	CIRCULATION PUMP 72-882	STORAGE TK. INLET CV-868
OPEN	START	OPEN
CLOSE	MOTOR RUN	CLOSE
	STOP	

4½" | 2½" | 2½" | 2½" | 2½" | 5" | 2½" | 2½" | 2½" | 2½" | 2½" | 4"

3'-0"

DTH 000098763

MARK	COORD.	REVISIONS	BY	DATE	APP.
A		FOR CONSTRUCTION	BW	6-1-77	RWD
B					
C					
D					

OUR JOB NO. 7471

DRAWN C.T.W. DATE 4-1-77
TRACED DATE
CHECKED B.R.W DATE 4-6-77
APPROVED RWD DATE 6/16/77

OWNER
CONTINENTAL OIL COMPANY

TELLEPSEN PETRO-CHEM CONSTRUCTORS
A DIVISION OF
TELLEPSEN CONSTRUCTION CO.
CONTRACTORS AND ENGINEERS • HOUSTON, TEXAS

PROJECT PVC CAPACITY REPLACEMENT
MAIN CONTROL PANEL PUSHBUTTON
LAYOUT CHARGE SECTION
ABERDEEN MISSISSIPPI

CONSOLE INSTRUMENT
DRAWING NO. PT-220 57-5-D
REV. A
SCALE: ¾" = 1"

REACTOR SECTION 45-741

EVACUATION AND RECOVERY

OPEN
CLOSE

VENTS

OPEN
CLOSE

CLEANING

OPEN
CLOSE

REACTOR CHARGE

OPEN
CLOSE

CHEMICAL VIEW

OPEN
CLOSE

OPEN
CLOSE

OPEN
CLOSE

RINSE

OPEN
CLOSE

STEAM

OPEN
CLOSE

OPEN
CLOSE

EVACUATION
CHARGE
POLYMERIZATION
RECOVERY
DUMP
CLEAN AND RINSE
SWIRL
OFF

SLURRY

OPEN
CLOSE

AGITATOR

START
MOTOR RUN
STOP

EMERGENCY

OPEN
CLOSE

EMER.
ON
OFF

LAMP TEST
PUSH TO TEST

OPEN
CLOSE

3½" 2½" 2½" 5" 2½" 5" 2½" 3½"
3'-0"

DTH 000098764

MARK	CODE	REVISIONS	BY	DATE	APP.
A		FOR CONSTRUCTION		6-1-77	
B					
C					
D					

OUR JOB NO. 7471

DRAWN C.T.W. DATE 4-13-77
TRACED DATE
CHECKED DATE
APPROVED DATE 6/16/77

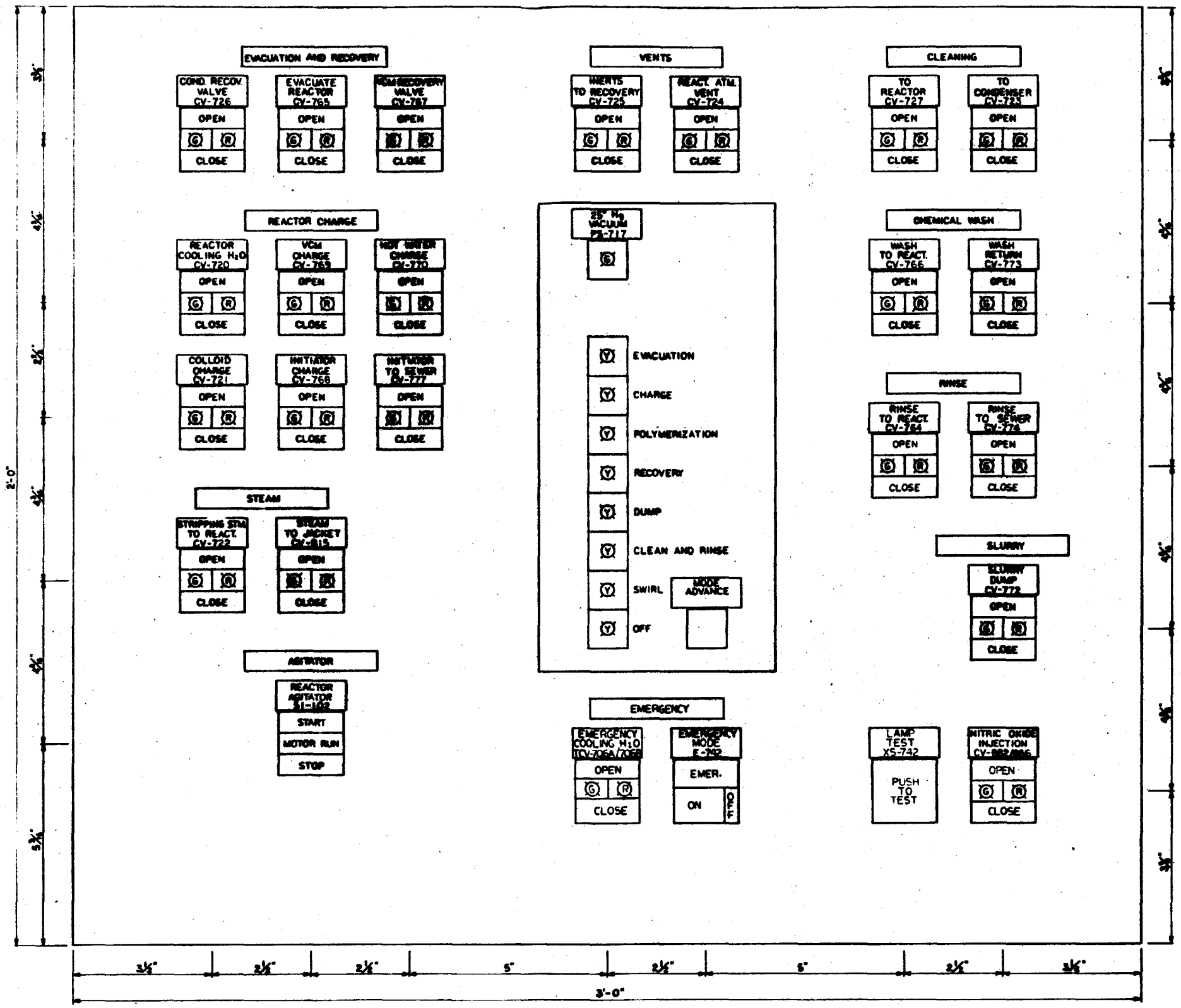
OWNER
CONTINENTAL OIL COMPANY

TELLEPSEN PETRO-CHEM CONSTRUCTORS
A DIVISION OF
TELLEPSEN CONSTRUCTION CO.
CONTRACTORS AND ENGINEERS • HOUSTON, TEXAS

PROJECT PVC CAPACITY REPLACEMENT
MAIN CONTROL PANEL PUSHBUTTON
LAYOUT REACTOR SECTION 45-741
ABERDEEN MISSISSIPPI

CONSOLE INSTRUMENT
DRAWING NO. PT-220 57-6-D
REV. A
SCALE ½" = 1'

REACTOR SECTION 45-742



DTH 000098765

MARK	COORD.	REVISIONS	BY	DATE	APP.
A		FOR CONSTRUCTION	EW	6-1-77	RWD
B					
C					
D					

OUR JOB NO. 7471

DRAWN C.T.W. DATE 4-13-77
TRACED DATE
CHECKED DATE
APPROVED RWD DATE 6/16/77

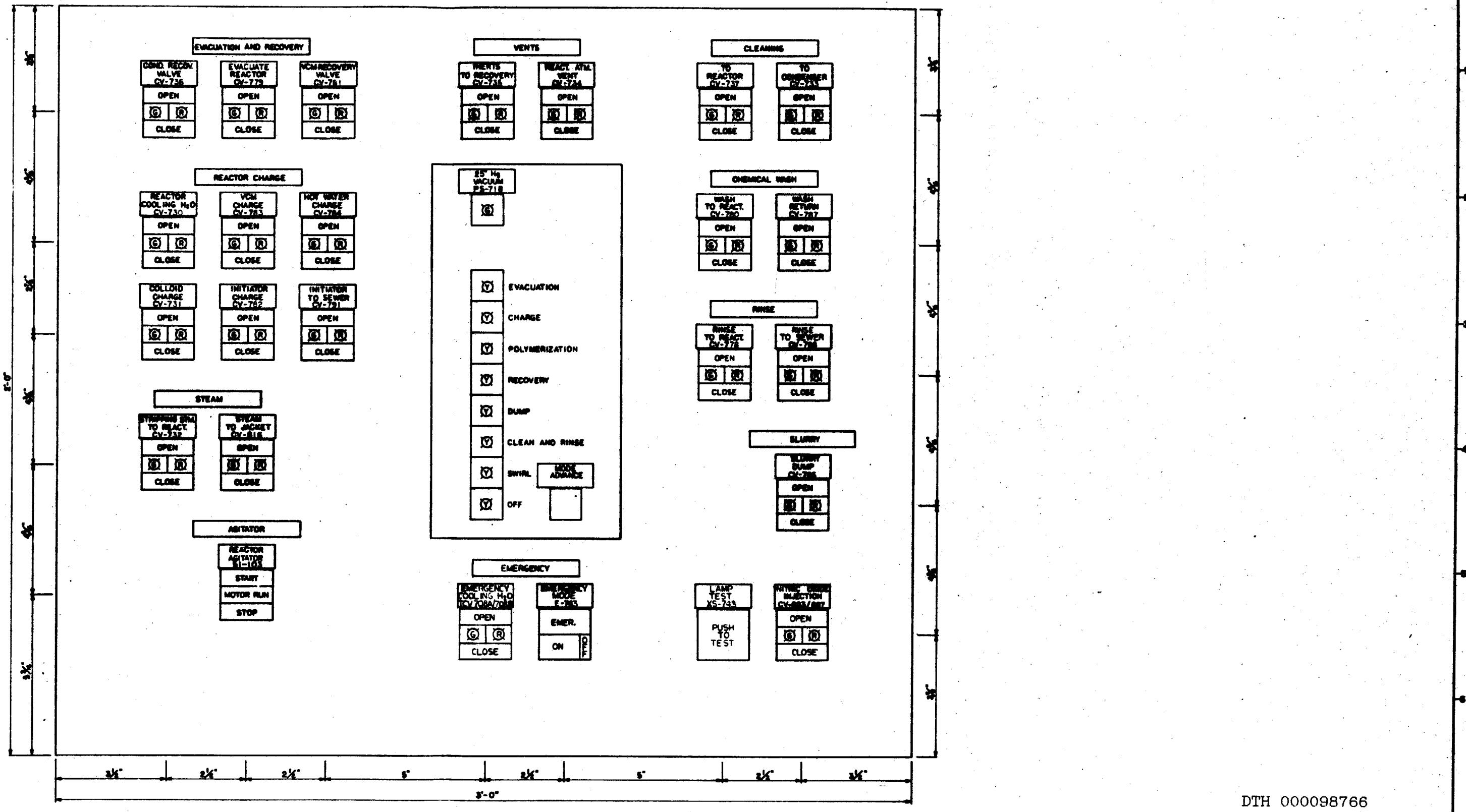
OWNER
CONTINENTAL OIL COMPANY

TELLEPSEN PETRO-CHEM CONSTRUCTORS
A DIVISION OF
TELLEPSEN CONSTRUCTION CO.
CONTRACTORS AND ENGINEERS • HOUSTON, TEXAS

PROJECT PVC CAPACITY REPLACEMENT
MAIN CONTROL PANEL PUSHBUTTON
LAYOUT REACTOR SECTION 45-742
ABERDEEN MISSISSIPPI

CONSOLE INSTRUMENT
DRAWING NO. PT-220 57-7-D
REV. A
SCALE 3/4" = 1'

REACTOR SECTION 45-743



DTH 000098766

MARK	CODES	REVISIONS	BY	DATE	APP.
A		FOR CONSTRUCTION	E.	6-1-77	RWD
B					
C					
D					

OUR JOB NO. 7471

DRAWN C.T.W. DATE 4-18-77
TRACED DATE
CHECKED DATE
APPROVED DATE

OWNER
CONTINENTAL OIL COMPANY

TELLEPSEN PETRO-CHEM CONSTRUCTORS
A DIVISION OF
TELLEPSEN CONSTRUCTION CO.
CONTRACTORS AND ENGINEERS • HOUSTON, TEXAS

PROJECT PVC CAPACITY REPLACEMENT
MAIN CONTROL PANEL PUSHBUTTON LAYOUT REACTOR SECTION 45-743
ABERDEEN MISSISSIPPI

CONSOLE INSTRUMENT
DRAWING NO. PT-220 57-8-0
REV A
SCALE 3/4" = 1'

REACTOR SECTION 45-744

EVACUATION AND RECOVERY

- COND. RECOV. VALVE CV-746 — OPEN / S R / CLOSE
- EVACUATE REACTOR CV-793 — OPEN / S R / CLOSE
- NCM RECOVERY VALVE CV-805 — OPEN / S R / CLOSE

REACTOR CHARGE

- REACTOR COOLING H_2O CV-740 — OPEN / S R / CLOSE
- VCM CHARGE CV-786 — OPEN / S R / CLOSE
- HOT WATER CHARGE CV-797 — OPEN / S R / CLOSE
- COLLOID CHARGE CV-741 — OPEN / S R / CLOSE
- INITIATOR CHARGE CV-795 — OPEN / S R / CLOSE
- INITIATOR TO SEWER CV-804 — OPEN / S R / CLOSE

STEAM

- STRIPPING STM. TO REACT. CV-742 — OPEN / S R / CLOSE
- STEAM TO JACKET CV-817 — OPEN / S R / CLOSE

AGITATOR

- AGITATOR REACTOR 51-104 — START / MOTOR RUN / STOP

VENTS

- INERTS TO RECOVERY CV-745 — OPEN / S R / CLOSE
- REACT. ATM. VENT CV-744 — OPEN / S R / CLOSE

- EST H_2 VACUUM PS-719 — R

- EVACUATION
- CHARGE
- POLYMERIZATION
- RECOVERY
- DUMP
- CLEAN AND RINSE
- SWIRL — MODE ADVANCE
- OFF

EMERGENCY

- EMERGENCY COOLING H_2O HCV/CSA/7088 — OPER. / S R / CLOSE
- EMERGENCY MODE E-744 — EMER. / ON / OFF

- LAMP TEST XS-744 — PUSH TO TEST

CLEANING

- TO REACTOR CV-747 — OPEN / S R / CLOSE
- TO CONDENSER CV-743 — OPEN / S R / CLOSE

CHEMICAL WASH

- WASH TO REACT. CV-794 — OPEN / S R / CLOSE
- WASH RETURN CV-800 — OPEN / S R / CLOSE

RINSE

- RINSE TO REACT. CV-792 — OPEN / S R / CLOSE
- RINSE TO SEWER CV-801 — OPEN / S R / CLOSE

SLURRY

- SLURRY DUMP CV-739 — OPEN / S R / CLOSE

- NITRIC OXIDE INJECTION CV-884/888 — OPEN / S R / CLOSE

3½" 2½" 2½" 5" 2½" 5" 2½" 3½" = 3'-0"

DTH 000098767

MARK	CODED	REVISIONS	BY	DATE	APP.
A		FOR CONSTRUCTION		6/1/77	RWS
B					
C					
D					

OUR JOB NO. 7471

DRAWN C.T.W. DATE 4-13-77
TRACED DATE
CHECKED DATE
APPROVED RWS DATE 6/14/77

OWNER
CONTINENTAL OIL COMPANY

TELLEPSEN PETRO-CHEM CONSTRUCTORS
A DIVISION OF
TELLEPSEN CONSTRUCTION CO.
CONTRACTORS AND ENGINEERS • HOUSTON, TEXAS

PROJECT PVC CAPACITY REPLACEMENT
MAIN CONTROL PANEL PUSHBUTTON LAYOUT REACTOR SECTION 45-744
ABERDEEN MISSISSIPPI

CONSOLE INSTRUMENT
DRAWING NO. PT-220 57-9-D
REV. A
SCALE 3/4" = 1'

RECOVERY SECTION

RECOVERY

- AUTOMATIC RECOVERY XS-906: READY / START
- VACUUM PUMPS RUNNING: 72-901 / 72-902
- COMPRESSOR 72-903: RUN OFF (G) (R) AUTO OFF
- COMPRESSOR 72-904: RUN OFF (G) (R) AUTO OFF
- COMPRESSOR 72-905: RUN OFF (G) (R) AUTO OFF
- RECIRC. PUMP 72-869: START / MOTOR RUN / STOP
- RECIRC. PUMP 72-870: START / MOTOR RUN / STOP
- SEAL WATER PUMP 72-891: START / MOTOR RUN / STOP
- SEAL WATER PUMP 72-892: START / MOTOR RUN / STOP

SLURRY

- SWECO 64-733: START / MOTOR RUN / STOP
- EXHAUSTER 70-864: START / MOTOR RUN / STOP
- SLURRY DUMP 72-896: START / MOTOR RUN / STOP
- SLURRY DUMP 72-897: START / MOTOR RUN / STOP
- SPRAY VALVE CV-863: OPEN (G) (R) CLOSE

CLEANING SOLUTION

- TK. OUTLET CV-873: OPEN (G) (R) CLOSE
- REACTOR CV-871: OPEN (G) (R) CLOSE
- TK. BYPASS CV-874: OPEN (G) (R) CLOSE
- CLNG. PUMP 72-868: MOTOR RUN ON OFF
- CLNG. PUMP 72-869: MOTOR RUN ON OFF
- TK. INLET CV-872: OPEN (G) (R) CLOSE
- RINSE WATER CV-867: OPEN (G) (R) CLOSE

- DELUGE FIREWATER XS-885: FIREWATER ON OFF

BLOWDOWN

- BLOWDOWN TK. PUMP 72-900: START / MOTOR RUN / STOP
- RECOVERY VALVE CV-836/CV-837: OPEN (G) (R) CLOSE
- EAST RCVR RVOM DRAIN CV-893: OPEN (G) (R) CLOSE
- WEST RCVR RVOM DRAIN CV-892: OPEN (G) (R) CLOSE

- LAMP TEST XS-887: PUSH TO TEST

UTILITIES

- SEAL OIL 95-299: START / MOTOR RUN / STOP
- SEAL OIL 95-300: START / MOTOR RUN / STOP
- INSTRUMENT AIR SHUTOFF CV-886: OPEN (G) (R) CLOSE

4" 2½" 2½" 5" 2½" 5" 2½" 2½" 5" 4½"

3'-0"

DTH 000098768

MARK	COORD.	REVISIONS	BY	DATE	APP.
A		FOR CONSTRUCTION	BW	6-1-77	Rwb
B					
C					
D					

OUR JOB NO. 7471

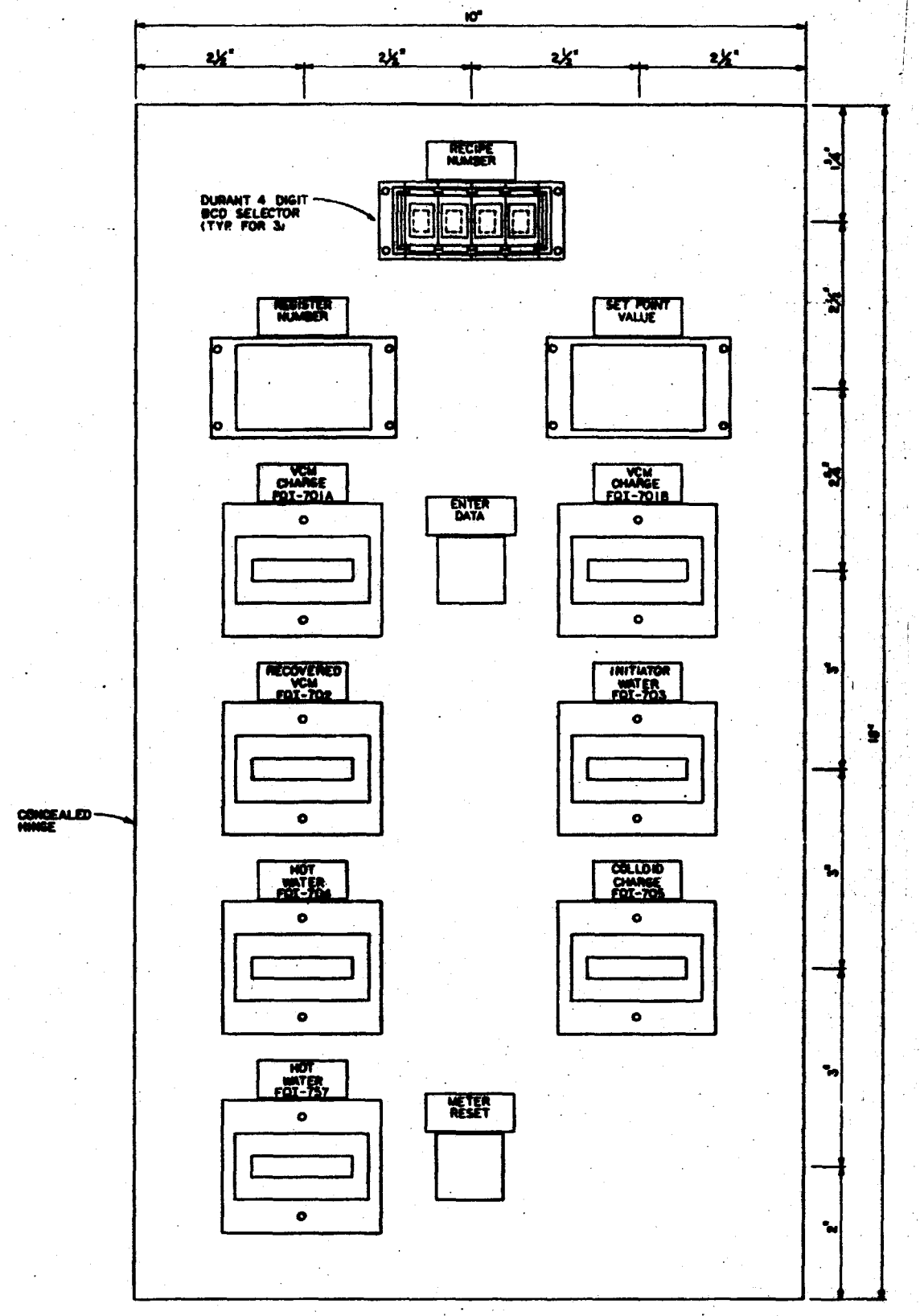
DRAWN C.T.W. DATE 4-6-77
TRACED DATE
CHECKED B.R.W. DATE 4-11-77
APPROVED Rwb DATE 6/14/77

OWNER
CONTINENTAL OIL COMPANY

TELLEPSEN PETRO-CHEM CONSTRUCTORS
A DIVISION OF
TELLEPSEN CONSTRUCTION CO.
CONTRACTORS AND ENGINEERS • HOUSTON, TEXAS

PROJECT PVC CAPACITY REPLACEMENT
MAIN CONTROL PANEL PUSHBUTTON LAYOUT RECOVERY SECTION
ABERDEEN MISSISSIPPI

DRAWING NO. PT-220 57-10-D
REV. A
SCALE 3/4" = 1'



NOTES

(1.) SEE DWG. NO. PT-220-57-2-D FOR PANEL LOCATION.

DTH 000098769

MARK	COORD.	REVISIONS	BY	DATE	APP.
A		FOR CONSTRUCTION	BW	4-1-77	
B					
C					
D					

OUR JOB NO. 7471

DRAWN C.T.W. DATE 4-25-77
TRACED DATE
CHECKED B.R.W DATE 4-26-77
APPROVED DATE 6/16/77

OWNER
CONTINENTAL OIL COMPANY

TELLEPSEN PETRO-CHEM CONSTRUCTORS
A DIVISION OF
TELLEPSEN CONSTRUCTION CO.
CONTRACTORS AND ENGINEERS • HOUSTON, TEXAS

PROJECT PVC CAPACITY REPLACEMENT
CHARGE SECTION TOTALIZER
PANEL LAYOUT
ABERDEEN, MISSISSIPPI

CONSOLE INSTRUMENT
DRAWING NO. PT-220 57-17-D
REV A
SCALE FULL

P. O. Box 1267
NCA CITY, OKLAHOMA 74601

FRESH VCM STORAGE TK 45-745

RECOVERED VCM STORAGE TANK (EXISTING)

RECOVERED VCM STORAGE TANK (EXISTING)

HOT WATER RE-HEATER 45-832

HOT WATER TANK 45-748

COLLOID STORAGE TANK 45-734

COLLOID STORAGE TANK 45-52

COLLOID WAKE-UP TANK 45-751

COLLOID BATCH TRANSFER PUMP

BLOWDOWN TANK

RECOVERY VCM CHARGE PUMPS

HOT WATER CHARGE PUMPS

COLLOID CHARGE PUMPS

FRESH VCM PUMPS

VCM CHARGE PUMPS

FILTER

PROCESS WATER

STEAM

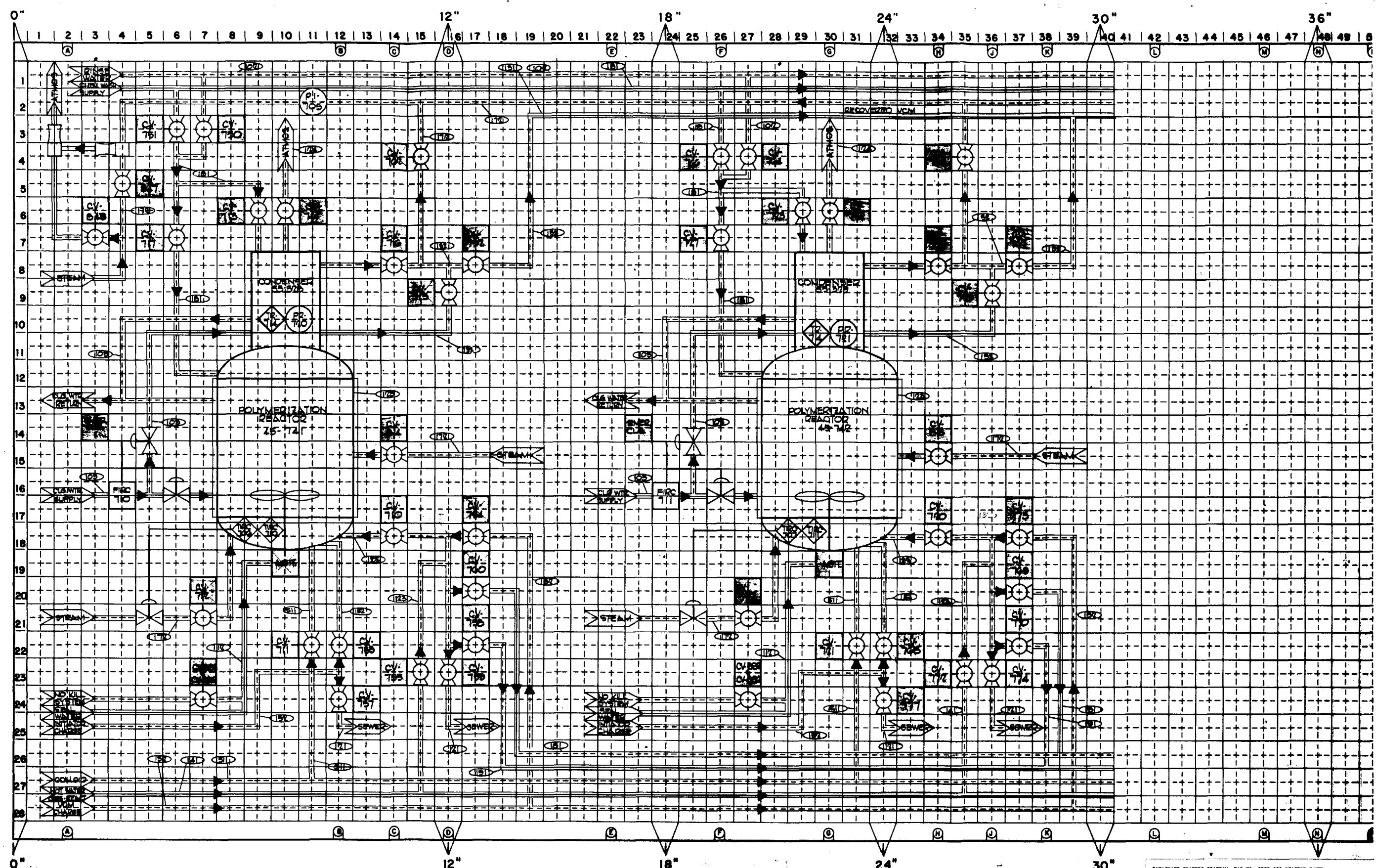
CONDENT

INITIATOR INJECTION 45-750

RINSE WATER

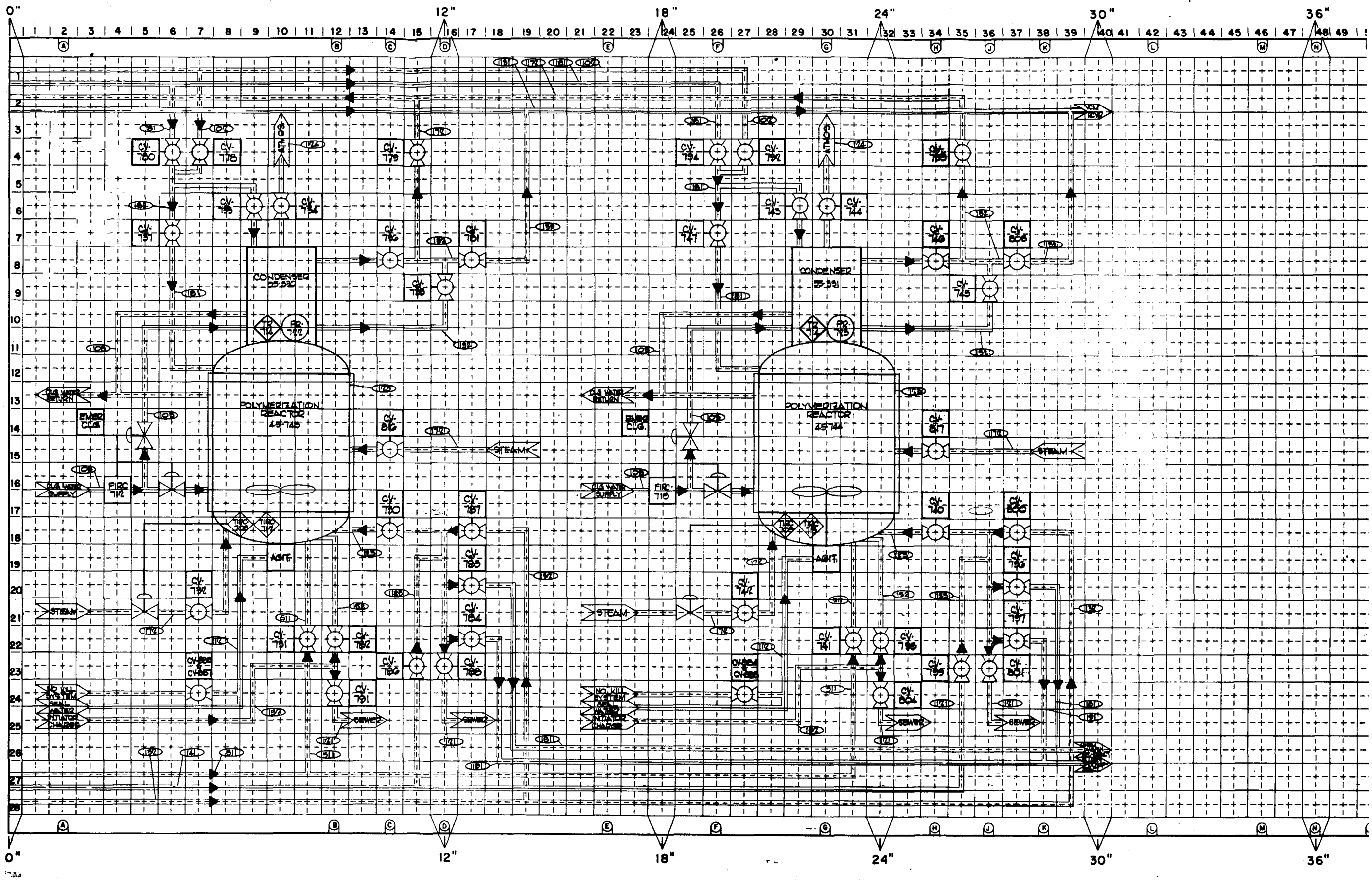
NOTE - (107) PANTONE COLOR CODE SEE CHART PROCESS

DTH 0000987?0



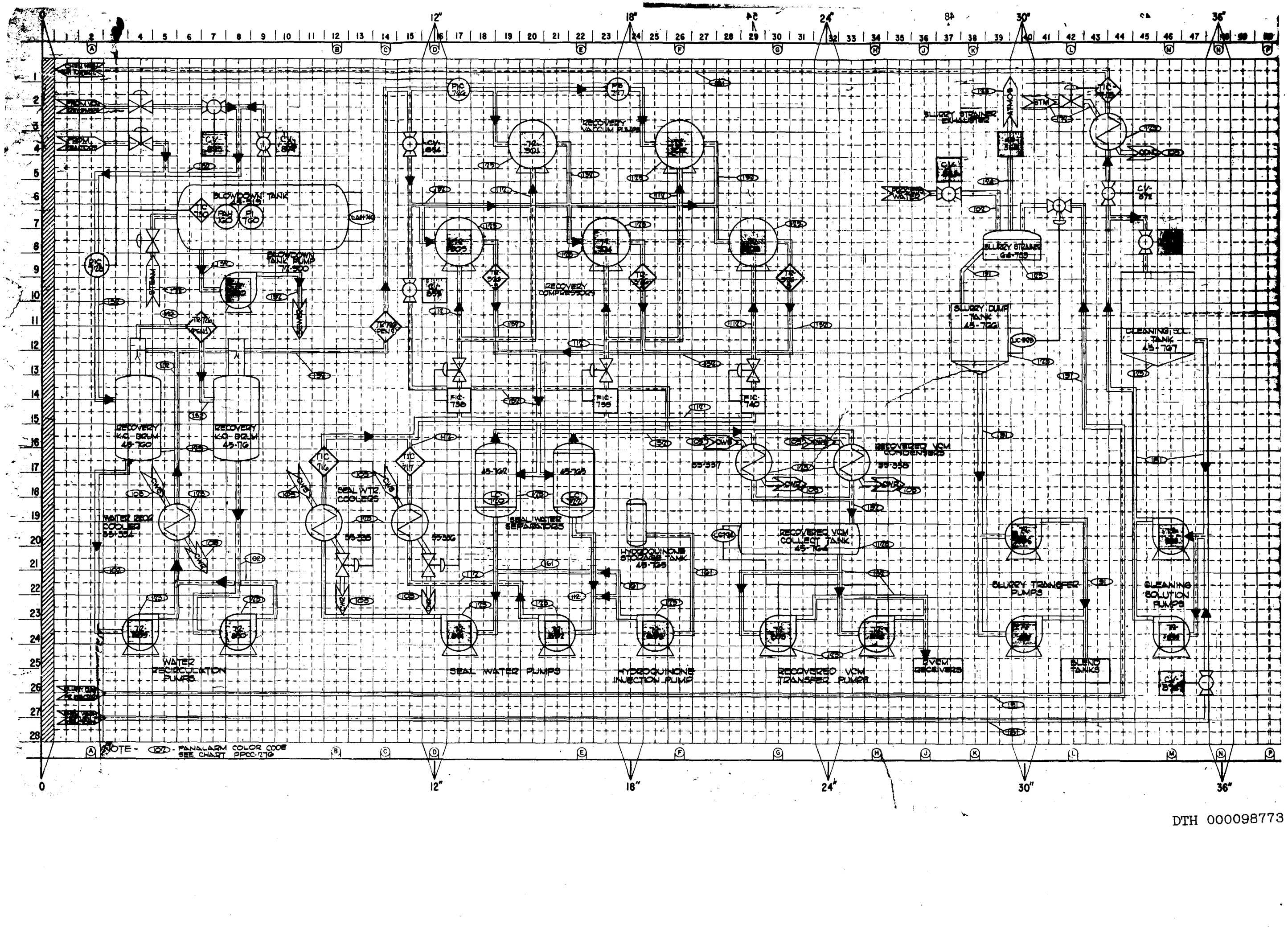
PARAGRAPH GRAPHIC DIAGRAM, TAG NO. 3705-230 REACTOR PANEL
PVC CAPACITY REPLACEMENT, ABERDEEN, MISSISSIPPI
ORIGINAL ISSUE 8/24/77; THIS ISSUE 9/30/77, FOR OPERATOR TRAINING ONLY

DTH 000098771



PANAGRAPH GRAPHIC DIAGRAM, TAG NO. 3705-330 REACTOR PANEL
PVC CAPACITY REPLACEMENT, ABERDEEN, MISSISSIPPI
ORIGINAL ISSUE 8/24/77; THIS ISSUE 9/30/77, FOR OPERATOR TRAINING ONLY

DTH 000098772



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