

REACTOR OPENING LOSS CALCULATIONS

Date: 3-19-79

Reactor: D-742 BLEND No. 13734

SAMPLE No. 31

RESIN TYPE: 5425

DATA:

TOTAL REACTOR VOLUME = 2916 FT³
REACTOR TEMPERATURE = 113 °F + 460 = 573 °R
REACTOR PRESSURE = 29.89 in. Hg X 25.4 = 759 mm Hg
VCM CHARGE AMOUNT = 715 COUNTS X 10 = 7150 GAL.
VCM Density (T=51 °F) = 7.744 #/GAL
VCM TO PVC CONVERSION = 70 %
Measured Vapor Concentration = 31302 ppm
Avg. Measured Slurry Concentration = 631 # VCM / 111 # PVC
H₂O VAPOR Pressure @ Rx. Temp = 72 mm Hg

a) One mole of ideal gas occupies 359 cu. ft. at 32°F (492°R) and 760 mm Hg

b) The volume correction at the reactor's temperature and pressure is:

$$V_c = 359 \times \frac{760}{759} \times \frac{573}{492} = 418.7 \text{ cu. ft./# mole}$$

c) Total moles in reactor at time of sampling:

$$M = \frac{\text{Reactor Volume}}{V_c} = \frac{2916}{418.7} = 6.97 \text{ # moles}$$

d) Moles of dry gas in reactor at time of sampling:

$$M_{\text{DRY}} = M \times \frac{(R_{\text{X}} \text{ PRESS} - \text{H}_2\text{O VAPOR PRESS})}{\text{REACTOR PRESSURE}} = 6.97 \times \frac{(759 - 72)}{759} = 6.30 \text{ # moles}$$

e) VCM EMISSIONS:

$$\begin{aligned} \# &= M \times 10^{-6} \times \text{Vapor Concentration} \times \text{VCM Molecular Weight} \\ &= 6.97 \times 10^{-6} \times 31302 \times 62.499 = 13.63 \text{ # VCM} \end{aligned}$$

$$\begin{aligned} \#_{\text{DRY}} &= M_{\text{DRY}} \times 10^{-6} \times \text{VAPOR CONCENTRATION} \times \text{VCM MOLECULAR WEIGHT} \\ &= 6.30 \times 10^{-6} \times 31302 \times 62.499 = 12.32 \text{ # VCM} \end{aligned}$$

f) Lbs. of PVC produced in reactor:

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$$\begin{aligned} R &= \text{VCM Charge Amount} \times \text{VCM DENSITY} \times \text{VCM TO PVC CONVERSION} \\ &= 7150 \times 7.744 \times 0.70 = 38,759 \text{ # PVC} \end{aligned}$$

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REACTOR OPENING LOSS CALCULATIONS (CONT.)

g) VCM Emissions in Vapor per MM lbs. PVC

$$E = \frac{\# \times 10^6}{R} = \frac{13.63 \times 10^6}{38,759} = 352 \text{ \# VCM/MM \# PVC}$$

$$E_{\text{DRY}} = \frac{\#_{\text{DRY}} \times 10^6}{R} = \frac{12.32 \times 10^6}{38,759} = 318 \text{ \# VCM/MM \# PVC}$$

h) Total VCM Emissions from reactor in vapor and slurry

$$T = E + \text{Avg. Slurry Concentration} = 352 + 631 = 983 \frac{\text{\# VCM}}{\text{MM \# PVC}}$$

$$T_{\text{DRY}} = E_{\text{DRY}} + \text{Avg. Slurry Concentration} = 318 + 631 = 949 \frac{\text{\# VCM}}{\text{MM \# PVC}}$$